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U.S. DEPARTMENT OF COMMERCE  
National Oceanic and Atmospheric Administration  
National Marine Fisheries Service

## Engineering Economic Model for Fish Protein Concentration Processes

K.K. ALMENAS, L.C. DURILLA, R.C. ERNST,  
J.W. GENTRY, M.B. HALE, and J.M. MARCHELLO

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# Engineering Economic Model For Fish Protein Concentration Processes

By

K. K. Almenas,<sup>1</sup> L. C. Durilla,<sup>2</sup> R. C. Ernst,<sup>2</sup>  
J. W. Gentry,<sup>1</sup> M. B. Hale,<sup>2</sup> and J. M. Marchello<sup>1</sup>

## I. ABSTRACT

A process engineering economic model for fish protein concentration processes has been developed. The model predicts the construction and operating costs for fish meal plants and for plants producing fish protein concentrate (FPC) by: isopropyl alcohol extraction, biological, and press cake-isopropyl alcohol extraction.

Typical process flow sheets and a computer program were developed to be used in the design and cost computations. The model provides for each process to be studied both internally and externally in comparison with alternate processes. The program and model were prepared in such a way that changes and updating may be accomplished quite readily as new information becomes available. This report contains directions for users and descriptions of the processes. A listing of the computer program and example calculations for each process are presented in the Appendix to guide the user and to illustrate the nature of the model output.

While the model does develop construction, operating, and production aspects of the processes, it does not deal with the economics of selling the products and the resulting profit and return on investment. Problems of allocation of costs and marketing arrangements are not covered in this report, but must be considered in the final decisions relating to a complete evaluation of alternatives.

## II. INTRODUCTION

Fish protein concentrate (FPC) production holds substantial promise of helping to meet the growing food and dietary requirements for the world's human population. It appears that several of the processes now being developed will be successful in making FPC available on a competitive basis with other sources of protein (1, 2). To provide for the orderly and rapid development of these processes it is necessary to continually review the internal steps of each process and to compare processes on a common basis.

The objective of this study was to develop a process cost and design model which can predict construction and operating costs for a wide range of FPC process conditions. The model was to handle a number of the FPC processes, operated singly or in conjunction with associated operations such as fish meal manufacture. This approach of making predesign computer estimates (3, 4) is becoming a common tool of management in process industry research and development.

### A. Engineering Economic Model

The model consists primarily of a digital computer program which determines the size and cost of major items of equipment for each process and then estimates the costs. The model is constructed so that new information

<sup>1</sup> University of Maryland, Department of Chemical Engineering, College Park, MD 20740.

<sup>2</sup> National Marine Fisheries Service, College Park Fishery Products Technology Laboratory, College Park, MD 20740.

at the bench scale, pilot plant, and demonstration plant levels can be easily incorporated to keep the program current with the available knowledge about each process.

Typical process flow sheets were developed with suitable options for each of the processes. These were used along with the available information on the process to prepare the material and energy balance portions of the program. Changes in flow sheets, types of equipment, processing sequences, and operating conditions, may be made following the internal program changes procedures.

From the material and energy calculations, the major items of equipment are sized and their cost estimated through built-in design and cost information. The program then determines the operating and manufacturing costs subject to the input data and internal assumptions of the model.

Two important features of the program are the built-in consistency of estimates for different processes and the continuity of estimates during the several stages of development of a given process. The uniformity of estimates results primarily from the use of a common set of equipment cost subroutines and a common set of assumptions regarding such cost items as indirect costs, land, engineering, etc. Since input data include the cost of labor, plant size, and cost indices, the program is useful in many broad-based studies of FPC production in different parts of the world at the present and in the future.

The model provides for each FPC process to be studied both internally and externally in comparison with alternate processes. Internal costs identify areas needing further research and development. The ability to estimate costs for a number of processes for a wide range of input conditions provides the broad comparison type information needed to guide a variety of research and development projects. The engineering economic model contains five process plant programs: fish meal; biological; isopropyl alcohol extraction; press cake-biological; and press cake-isopropyl alcohol extraction. Process descriptions and flow sheets are presented in the next chapter.

Fish meal processing is a common operation and there are many such plants throughout the world. Fish meal is used for animal feed while

the other processes make products for human consumption. It was included to provide a basis for comparison and because frequently intermediate meal products are a starting point for the FPC processes. The other processes are viable candidates for commercial manufacture of FPC.

## B. Cost Estimation

In the development and use of the model it is important to have accurate cost information. Equipment and capital cost data were obtained from a number of recent publications. These figures were compared and reviewed for consistency and accuracy. In several instances costs were adjusted to meet the actual experience of individuals knowledgeable in the field of marine protein manufacturing. Finally all costs were adjusted to the base of early 1970.

The adjustment of cost data from the past several years to an early 1970 value was made using the Marshall and Stevens Equipment Cost Index which is published in the periodical *Chemical Engineering*. The M & S Equipment Cost Index is based on a value of 100 in the year of 1926. The early 1970 base value of 297.5 is used for equipment costs in this report.

Adjustment in costs from one year to another is accomplished by multiplying the known cost by the ratio of the index values at the two years involved to obtain the desired cost. The choice of the M & S Index over several other indices that are available was based on the fact that the components used in the M & S Index are more nearly those present in FPC plants, and the general observation that all the indices have been moving at about the same rate in recent years.

Use of these indices over more than a few years leads to considerable uncertainty and is not recommended. It is hoped that users of the model will continually update the data from the best sources available and not resort to changing the cost index alone. Equipment is continually being developed and many specific items do not follow the average trends.

There is a wide variation in costs at any given time. This is due in part to the inventory and backlog situation of the individual manufacturers and suppliers. The best cost information is a written quotation for a specific item

to be purchased during a given period. In a number of instances, particularly for the IPA-Extraction process (17), quotes on equipment were available and were used in adjusting the literature data. Essentially the same thing was done, through discussions with experienced persons, for the typical fish meal process.

The capital cost estimating procedure of Guthrie (6) was used in developing the process engineering economic model. A module technique is employed in which cost elements having similar characteristics and relationships are grouped together. This grouping is discussed in the program output section. Published equipment cost information was obtained from a number of sources (6, 7, 8, 9, 10, 12, 13, 14, and 15). The cost data were fit to appropriate equations and are contained in the cost subroutine. This portion of the computer program and procedures for changing the data are discussed later in the report.

Costs of chemicals and raw materials were taken from recent issues of the *Oil, Drug and Paint Reporter* and from actual purchasing experience. Some of these are program input items and can be changed whenever the program is used. The cost of fish is quite varied and depends greatly on local conditions. Fish meal manufacturers often make contractual arrangements with the boat owners whereby the final price paid is dependent upon the income ultimately received from selling the fish meal. This input item will require close attention of the program user. The tradition of the industry of speaking in terms of fish rather than weight can also be a point of confusion. For menhaden, one million fish is taken to be 755,000 pounds of fish.

### C. Process Economics

The model develops the construction, operating, and production aspects of each process subject to specific input and internal information. It does not deal with the economics of selling the products and the resulting profits and return on investment.

Each of the processes makes several products and consequently requires the managerial decisions of cost allocation to establish selling prices of products. Marketing, inventory management, product distribution, and sales con-

tracting are important factors in the final decision on commercial operation. The model is intended to provide processing information upon which preliminary deliberations and decisions of the venture risk type can be made.

It is most important in using the model to recognize its limitations. Of the processes in the model only fish meal processing is a commercial operation at present. Even in this case the model attempts only to give representative information for a somewhat typical kind of plant under average conditions in the United States. Several IPA extraction plants for FPC production are under construction. The model IPA process is based on a modified analysis of the National Marine Fisheries Service Experiment and Demonstration Plant at Aberdeen, Washington. In all other instances the processes are in the early pilot plant level of development.

The model is also generally limited to use for plants handling 50 or more tons per day of fish. Modern domestic fish meal plants handle 1,000 or more tons per day and it is expected that FPC plants will be in the range of 100 or more tons per day. There is significant interest in processing FPC on board ships and developing small village industry operations. Use of the model in the 10 to 50 tons per day range will require some modification or at least close attention and judgment about the details of the output.

The model is presently applicable to coastal plants. To place one of these processes on board a ship will require significant changes. Generally space is a limiting factor on board ship and the processes would need to be redesigned for compactness. Special modifications to the ship could be costly, while certain land operation requirements, such as pollution control, might be eliminated, resulting in savings.

Village industry operation, and operation in foreign countries in general, will require a number of changes. The model provides for modern, instrumented, continuously operating plants. Equipment costs are for the United States and, in general, the plants are custom-made large facilities. Smaller plants, in the 10 ton per day sizes, might be mass-produced and thereby benefit from unit cost reduction much like appliances. If the appliance approach is not used on-site fabrication of village level

plant would probably be of the batch type. Such plants would have additional difficulties with quality control. A training program for village plant operators might be necessary to overcome potential health and operating problems.

### III. DESCRIPTION OF PROCESS MODELS

#### A. Fish Meal Process

The diagram of the fish meal plant is given in Figure 1. On the drawing, the streams are labeled. The fish are processed for three products, fish meal, fish oil, and fish solubles (50% water). An option is provided as to whether fish solubles are produced as a product or added to the fish meal.

Fish are unloaded from the boat by fish pumps. A weighing conveyor carries the fish to a storage unit which has a three-day capacity. A bucket conveyor takes fish from storage and drops them into a cooker. Oil is removed from the cooked fish in a continuous screw press.

The press cake leaving the press contains 50% solids. This stream in tons/day is labeled AA(91,2). The press liquor contains the oil and water from the fish and 15% of the total fish protein. It is labeled AA(91,3). The cookers are available in 100 ton/day and 250 ton/day sizes. Similarly two different sizes of screw presses are available. The selection of cookers, presses, and screens is internally handled in the program.

The program then branches to two processing streams. The stream containing most of the oil and water is discussed below. The first input option considered is whether to add the fish solubles streams to the fish meal stream [IPTION(1) = 2], or to market them as separate products, [IPTION(1) = 1].

From the presses, stream AA(91,2) passes through a mixer where the recycled fish solubles may be combined with the main stream. The stream then goes to steam tube drying in which approximately one-half of the weight is evaporated. Antioxidant, corresponding to 0.01 #/# of oil retained in the fish meal, is then added. The meal passes through a

mixer to a storage unit where it is cured for 15 days. The meal is milled prior to bagging.

Stream AA(91,3) is centrifuged. The centrifuge is sized from the flow in gallons/hour. The oil is then polished with hot water (10% of the oil weight of water is used) in a second centrifuge. The dummy variable TONSA is used for this stream at this point in the program. The fish oil product is designated AA(90,5). All hold tanks in the stream have a one-hour holding time. The fish oil storage capacity is 15 days.

The water and soluble protein are conveyed into an acid mix tank where it is mixed with sulfuric acid. This stream TONSWW then passes into a triple effect evaporator. The streams TONA and TONC are in tons/hr rather than tons/day. TONA is the inlet stream to the triple effect evaporator. TONC is the stream from the third effect going to the concentrator. The resulting fish solubles stream is 50% protein. It may be marketed as a product AA(90,4) or returned to the mixer and processed as fish meal. The storage capacity for fish solubles is 15 days.

In summary, three products may be produced—fish oil, fish solubles, and fish meal. Also, by an appropriate choice of option the fish solubles may be recycled and processed with the fish meal.

#### B. Biological Process

In the biological processes the proteins of the fish are partially hydrolyzed with enzymes to permit separation of the oil, bone, and proteinaceous material. The distinguishing feature of the process is large heated and stirred vessels into which the ground fish is fed and in which the digestion takes place. The subroutine handling this process is labeled "Subroutine Biolog"; the flow streams and equipment blocks of this subroutine are identified in Figure 2. In addition to the standard four-card input discussed in Section IVD, "Biolog" requires 5 input items which are entered on a fifth card in E12 format.

##### 1. UNLOADING, STORAGE AND GRINDING

The handling of the fish up to the digester stage includes fish pumps, conveyors with wash

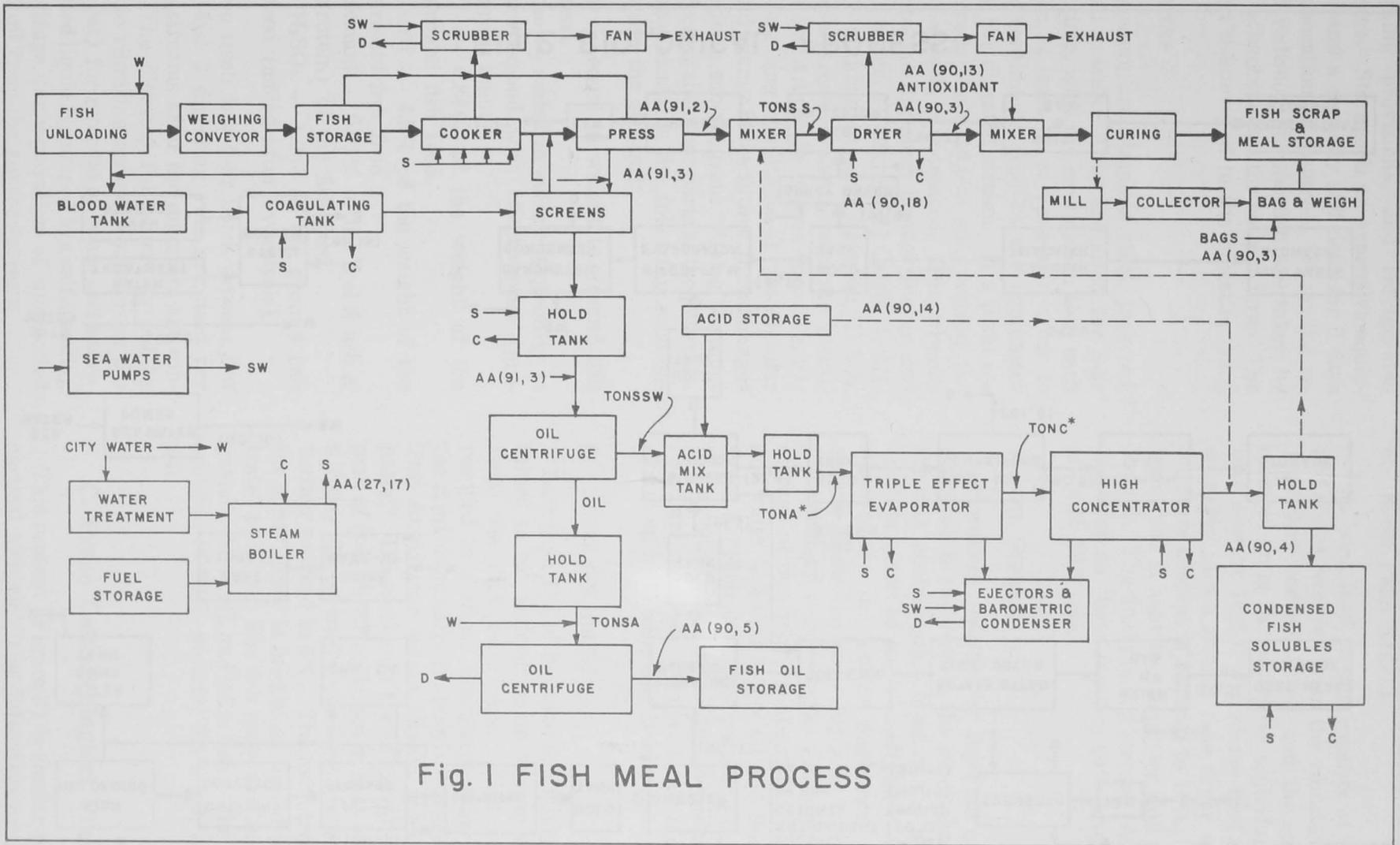
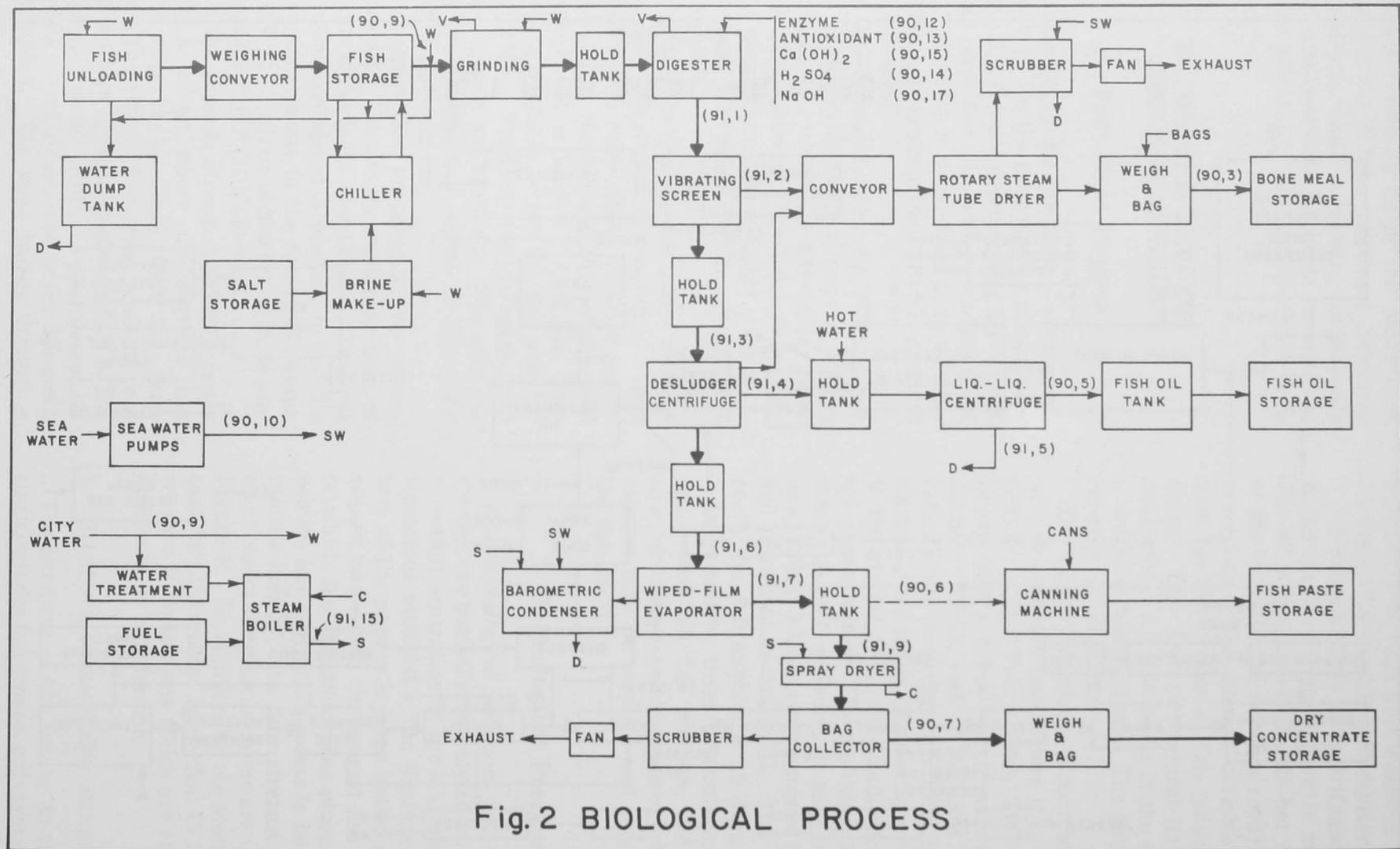


Fig. 1 FISH MEAL PROCESS



and weighing provisions, and refrigerated brine storage. Storage is an expensive equipment item and a capacity sufficient for 3 days of plant operation is assumed. From the refrigerated redwood bin the fish are taken by means of a bucket elevator to grinders. The ground fish is conveyed to the digesting vats.

## 2. DIGESTERS

The digesters are stainless steel, jacketed, and stirred vessels. They are sized for 5-hr residence time, with the assumption that each plant needs at least three vessels in order to provide a continuous feed to the equipment processing the digested stream. If a plant capacity exceeds three 10,000 gal. vessels, the number of vessels is increased. The streams feeding into the digesters besides the ground fish are 1) water, 2) enzyme, 3) CaOH, 4) 5N-NaOH, 5) antioxidant, and 6) conc. H<sub>2</sub>SO<sub>4</sub>. All of these streams have a separate identification in the AA (90,J) matrix (see Fig. 2); thus if processing conditions at the digester stage should change in the future, these changes can be made in sub-program "Biolog" without unduly affecting the other parts of the program. The program contains the following relationships between the streams:

- a water — equal in weight to ground fish feed.
- b enzyme — added in sufficient quantity to correspond with effectiveness (program input).
- c CaOH — 0.84% of the weight of the ground fish feed.
- d 5N-NaOH — 4.3% of the weight of the ground fish feed.
- e Antioxidant — 0.01% of the (oil & ash & protein) of the fish feed.
- f conc. H<sub>2</sub>SO<sub>4</sub> — 1.9% of the ground fish feed (added after hydrolysis).

Digestion itself is a 5-hr batch process, but since at least 3 digesting vats are used per plant, the streams after the digesters are continuous. The digested fish slurry is fed by gravity into vibrating screens (one screen per digesting vat) for removal of bones and scales. The screened liquid is pumped to a self-cleaning disk centrifuge for separation of undigested solids and oil from the aqueous stream.

## 3. BONE FEED STREAM

The bone feed stream consists of the bones and scales removed from the vibrating screens (moisture content 50%) and the sludge discharged from the desludger centrifuge (moisture content 76%). The bone feed stream is conveyed into a stream tube dryer where the moisture content is reduced to 10%. The dry bone feed is sent to a hammer mill and then bagged. The final product stream [AA (90,3)] identified as "bone feed" is 40% protein, 22% oil, and 28% ash.

## 4. OIL STREAM

Approximately 75% of the lipid content of fatty fish is removed in the oil discharge from the disk centrifuges. Most of the balance of lipids is adsorbed on the undigested solids and removed in the sludge discharge. The oil stream from the centrifuges is pumped into intermediary storage tanks (with a maximum storage of one hour). About 10% additional hot water is added to the oil and the mixture is fed to "Sharples" type polishing centrifuges in which the water including solvated solids and blood are removed. The product fish oil can be stored up to 15 days and is sold in bulk.

## 5. DISSOLVED SOLIDS

Less than 1% of the total fish lipids are contained in the aqueous main stream discharge from the disk centrifuge. This stream is pumped to a wiped film evaporator in which the stream moisture content is reduced to 50%. This evaporator output stream is called "fish paste." Depending on the input option, all or part of it is either packaged in cans or fed into a spray dryer where the moisture content is further reduced to 5%. The exit stream from the spray dryer is bagged as the "dry concentrate" product. The fish paste product is 41% protein, 0.3% oil, and 8.3% ash. The dry concentrate is 79% protein, 0.5% oil, and 16% ash.

## C. Press Cake-Biological Process

This process (Figure 3) is similar to the Biological process. The differences are that be-

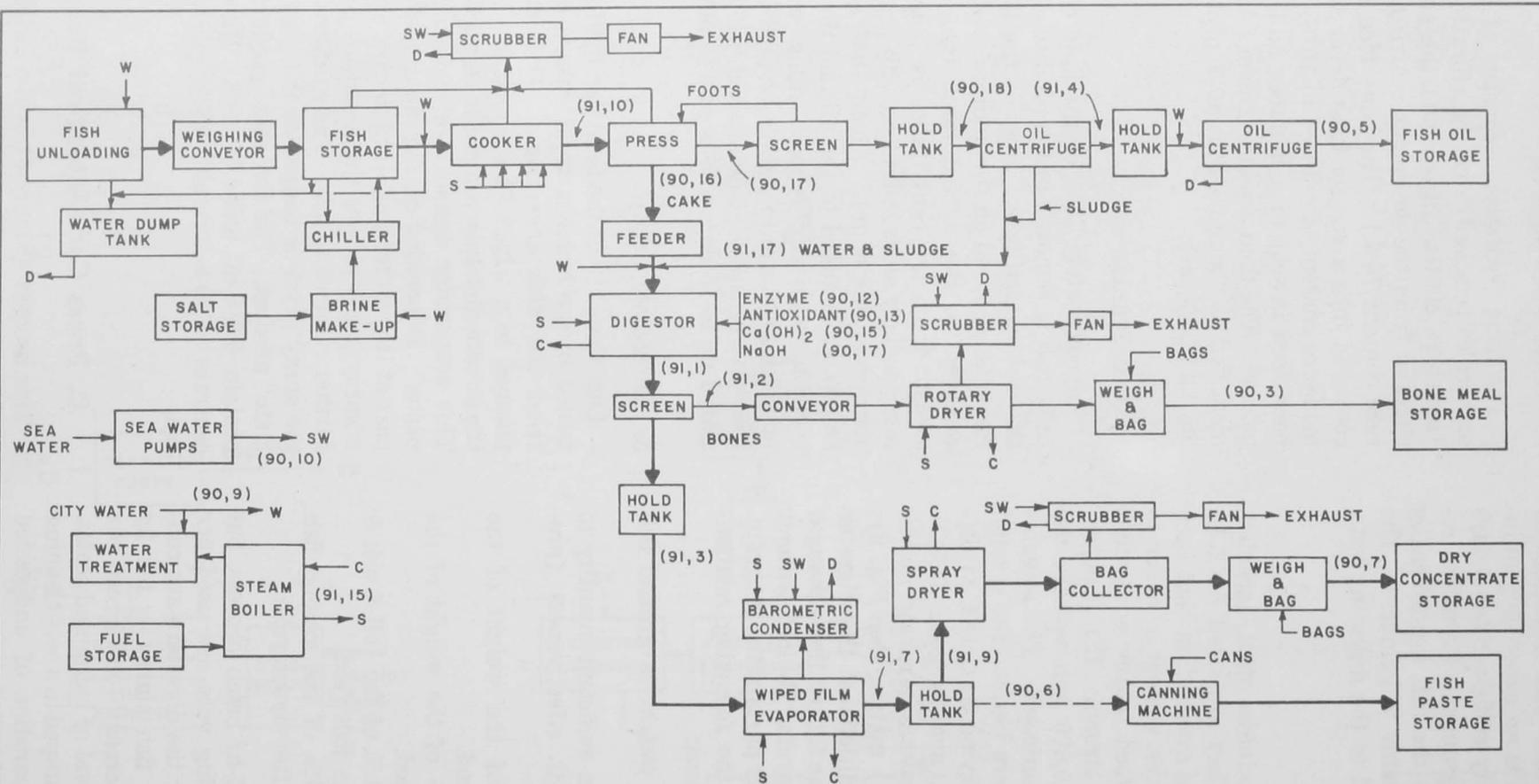


Fig. 3 PRESS CAKE-BIOLOGICAL PROCESS

fore being fed to the digestion vats the fish are cooked and pressed as in the Fish Meal Process. The separation of oil and stick water takes place before rather than after the digestion stage. Process description: a) Input (besides the standard input) is the same as for the Biological process, except that in this case the enzyme which is added to the digester is based on 100 lb. of cooked and pressed fish (referred to as press cake) rather than on raw ground fish; b) Unloading and storage processes include fish pumps, conveyors with wash and weighing provisions, and refrigerated brine storage for up to 3 days of plant operation. The stored fish is lifted by bucket elevators into steam cookers. The fish are cooked and pass into screw presses where the moisture content of the "press cake" is reduced to 60%.

The press liquor is screened and pumped from a hold tank to a centrifuge for oil separation and "foots" removed by screening are recycled to the press. The separated oil is polished with hot water in a second liquid-liquid centrifuge, as in the Biological process, and pumped to bulk storage.

The aqueous "stickwater" stream from the first centrifuge contains both soluble and insoluble solids. It is added to the press cake in the digesting vats along with additional water to form a press cake slurry for enzymatic hydrolysis. For hydrolysis with the alkaline enzyme the pH is adjusted with 5N NaOH at 2.2% of the weight of raw fish feed.

After a 4-hr hydrolysis the slurry is passed through a vibrating screen. Bones and scales with a 50% moisture content are conveyed from the screen to a stream tube dryer where the moisture content is reduced to 10%. The dry bone meal is sent to a hammer mill and then bagged.

The screened hydrolysate is concentrated to a fish paste containing 50% solids in a wiped film evaporator. Depending on the input option, all or part of it is either packaged in cans or fed into a spray dryer where the moisture content is further reduced to 5%.

The final products are bone meal (36% protein, 9.7% oil, 47.4% ash), fish paste (39% protein, 6% oil, 5% ash), dry concentrate (75% protein, 11% oil, 9% ash) and fish oil. Insoluble solids are not removed by centrifuga-

tion as in Biological process.

## D. IPA Extraction Process

The IPA process is shown in Figure 4. This is a solvent extraction process in which water and lipids are removed using isopropyl alcohol (17). Solvent recovery and recycle is an important part of the process. The first decision variable is whether wet deboning or no deboning is used. In wet deboning the bones are dried, ground in a hammer mill, packaged and sold as bone meal. This option is activated when IPTION(1) is equal to one. If no deboning is desired, no option is specified. In this case, the dried concentrate product will contain both protein concentrate and bone meal.

Unloading and storage processes include fish pumps, conveyors with wash and weighing provisions, and refrigerated brine storage for 3 days of plant operation. The ground fish is pumped to a slurry mix tank where solvent miscella M-2 is added. The solids go through four stages of extraction. They are separated from the miscella between stages by screens and presses.

For the material balance on the extraction vessels the miscella stream are designated STRMM(I) where I is the stage number. The constituent streams of oil, protein, ash, water, and isopropyl alcohol are designated STRM(I, J). Here, however, the index I designates the stream entering the Ith stage or leaving the I + 1 stage. The unit operation of this part of the process is a 4-stage liquid-slurry extraction process in which an azeotrope of isopropyl alcohol and water is used as the extractive solvent. The solvent to fish ratio is 2:1.

### 1. FISH PROTEIN CONCENTRATE STREAM

The slurry stream leaving the fourth stage of extraction contains the ash, most of the protein, and a small residual amount of oil. This stream enters a series of dryers (dryer, stripper dryer, and conditioner) in order to reduce the moisture of the stream to approximately 8% and to reduce the IPA residual to below 250 ppm. The amount of material leaving the conditioner is designated TASB. The fraction

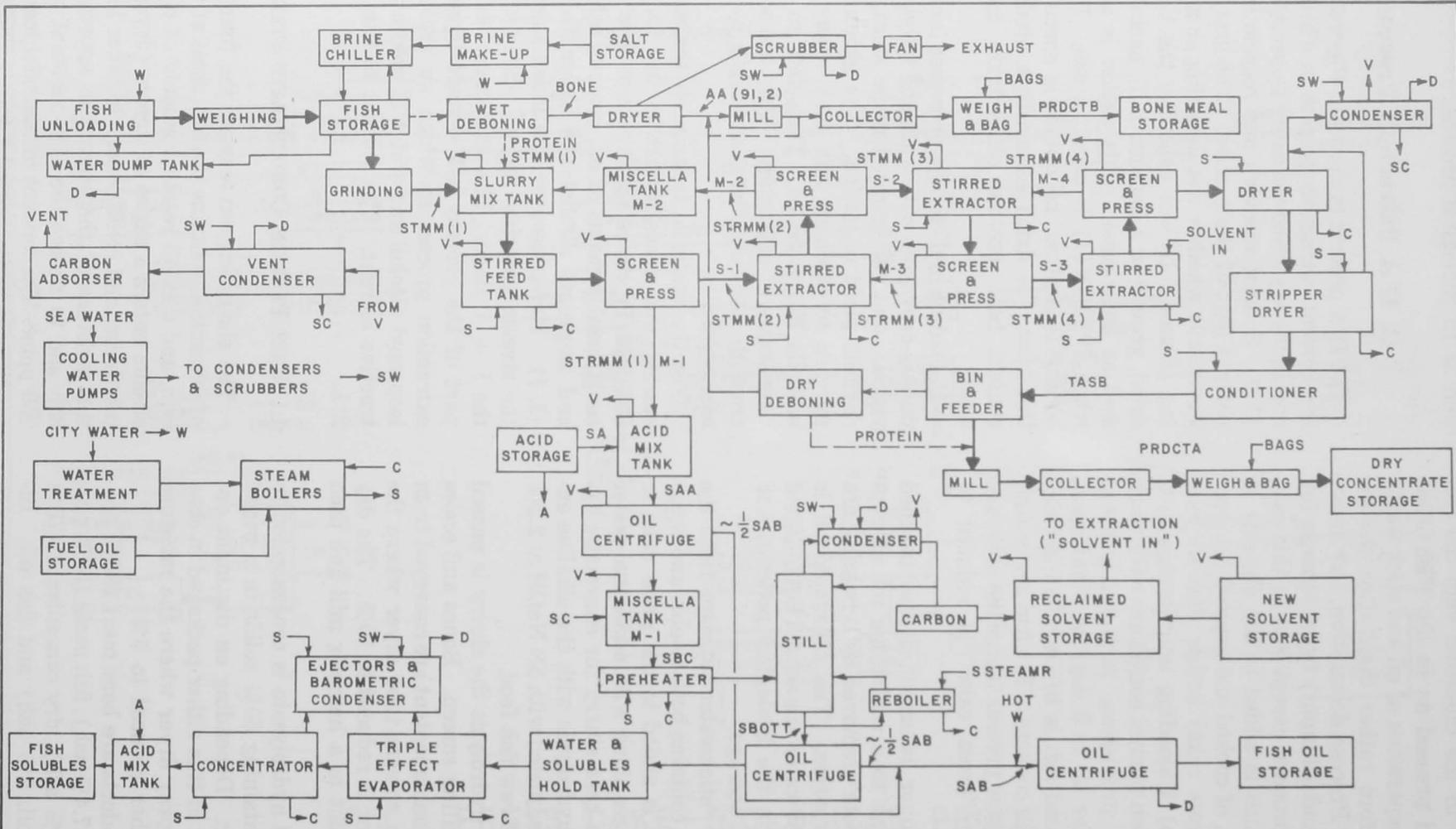


Fig. 4 ISOPROPYL ALCOHOL EXTRACTION PROCESS

## E. Press Cake--IPA Process

of protein retained in the fish protein concentrate is designated as ZA7 and the amount of bone meal in the FPC is ZA8. The original fractions chosen are 0.96 and 0.04 respectively. They can be changed readily without affecting the main body of the program. The finished concentrate and bone meal are then milled and packaged.

### 2. OIL STREAM

The stream containing the bulk of the oil is the miscella stream leaving the first stage. This stream is acidified (conc.  $H_2SO_4$  at 1.9% of fish feed) and enters an oil-water centrifuge. Approximately one-half of the oil is removed. This oil plus the oil from the still bottoms product, which was centrifuged, are combined into one stream. About 10% hot water is added to this stream before it enters a polishing centrifuge. This oil can be stored up to 15 days and is sold in bulk.

### 3. SOLVENT RECOVERY

The rest of the oil and solvent from the first oil-water centrifuge is heated prior to the distillation process. The solvent, which is mostly isopropyl alcohol, is distilled in a 25-tray column. SBOT(I) designates the constituent bottoms consisting of isopropyl alcohol, water, oil, and soluble protein. The product at the top of the column is designated STOP(I) and consists of isopropyl alcohol and water. The recovered solvent is then pumped to the storage tank where make-up isopropyl alcohol is added as needed.

### 4. FISH SOLUBLES

The non-oil portion of the centrifuged column's bottoms is fed to a triple effect evaporator. The product is further concentrated to 50% protein in a concentrator evaporator.

The products stream consists of fish protein concentrate AA(90,7), bone meal AA(90,3) (if wet deboning is specified), fish oil AA(90,5), and fish solubles AA(90,4).

The Press Cake-IPA process combines the proved technology of IPA extraction with a pre-processing of the raw fish in order to provide a more concentrated and more easily stored feed. A diagrammatic representation of the process is shown in Figure 5.

### 1. UNLOADING, STORAGE, AND PRESS CAKE PRODUCTION

The fish is unloaded by means of fish pumps, weighed and washed and stored in refrigerated brine. A storage capacity sufficient to provide 3 days of feed to the press cake production unit is provided. From the brine storage vat the fish is lifted by bucket elevators into steam cookers. The fish is cooked, crushed, and passes into a screw press which reduces its moisture content to 60%. The excess liquid passes through a vibrating screen filter into a hold tank. This liquid is processed separately in order to recover the oil and dissolved solids. The compressed bulk fish, called "press cake," is ground, transported by screw conveyors either into a closed redwood bin for intermediate storage in IPA or directly into the IPA extraction stages. The capacity of the intermediate storage is sufficient to provide a 50-day backlog for the IPA extraction portion of the plant.

### 2. IPA EXTRACTION

The press cake is turned into the final FPC product through multistage countercurrent IPA extraction. The program is set up in such a way that the number of extraction stages and their individual efficiencies can be changed readily. The standard number of stages is assumed to be four; however, any number up to eight can be specified in the input. If the desired number of stages is *other than four*, that number should be entered in column 40 of the first input card.

After each separation stage a detailed material balance on each component of the input-output streams is performed. The separation efficiencies for each component and each stage can be specified separately. They are stored in the library subprogram LIBRE and can be

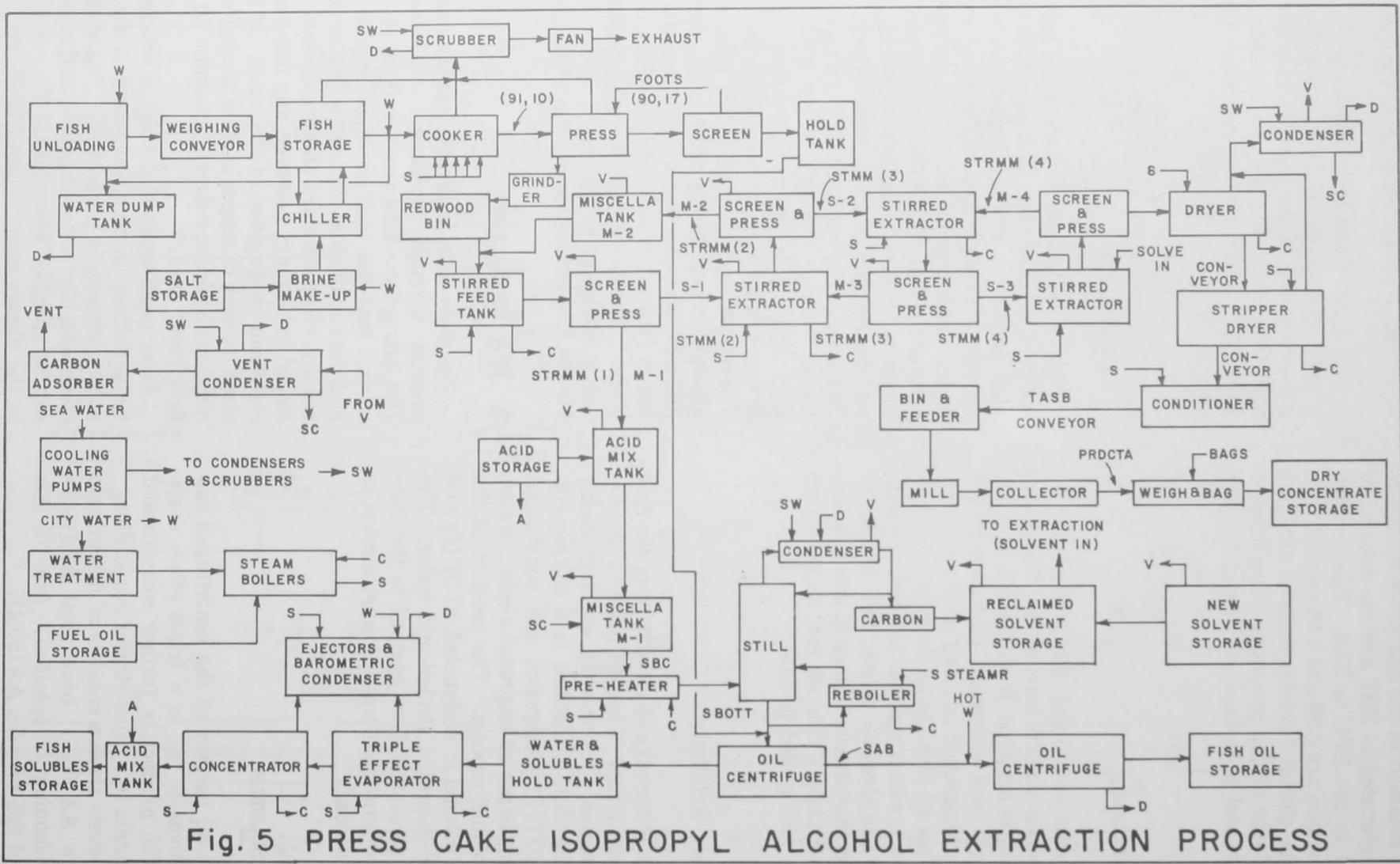
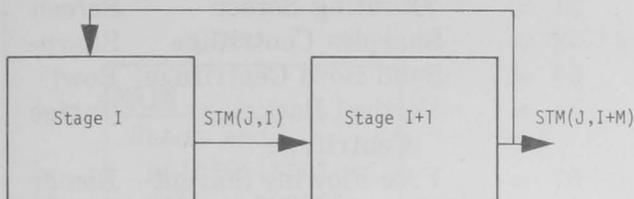


Fig. 5 PRESS CAKE ISOPROPYL ALCOHOL EXTRACTION PROCESS

changed readily without modifying the main program.

Consider two sequential stages I and I + 1:



The J index describes the five main components of the stream. The relationship is as follows:

- J = 1 — Oil
- J = 2 — Protein
- J = 3 — Ash
- J = 4 — Water
- J = 5 — IPA

The quantity for each component exiting from stage I + 1 is computed by the following relationship:

$$STM(J,I+1) = STM(J,I) * DATB(I,J)$$

Where: 1-DATB(I,J) is the extraction efficiency for component J in the I + 1 stage. These quantities are thus stored in the readily accessible LIBRE subprogram.

The above definition has to be modified for the case of the IPA content leaving the first extraction stage. The modification is:

$$STM(5,1) = STM(4,1) * DATB(1,5)$$

### 3. FISH PROTEIN CONCENTRATE STREAM

The slurry stream leaving the final extraction stage contains the ash, most of the protein, and a small residual amount of oil. The stream enters—in sequence—a dryer, a stripper dryer, and a conditioner in which its moisture content is reduced to about 8% and the IPA residual falls below 250 ppm. The solid stream leaving the conditioner is labeled TASB. It is milled, weighed, and packaged.

### 4. OIL STREAM

The stored liquid from the press cake production process and the still bottoms from the solvent recovery still are fed into a liquid-liquid centrifuge. Oil separation efficiency is assumed to be 94%. Bottoms containing the dissolved solids are fed into a storage tank in order to be processed through evaporators, the top oil containing fraction is pumped into a polishing "Sharples" type centrifuge. Here 10% volume fraction of hot water is added. The purpose of this centrifugation is to remove entrained blood and remaining solids. The polished oil is fed into final oil storage tanks. A storage capacity sufficient for 15 days production is designed.

### 5. FISH SOLUBLES

The stream containing dissolved solids from the liquid-liquid oil separation centrifuge is fed into a triple effect evaporator followed by a concentrator. The moisture content is reduced to about 50%, the product is acidified and stored as fish solubles.

### 6. SOLVENT RECOVERY

The solvent-containing stream is preheated and passed into a 25-tray distillation column. The bottoms of the column pass, as noted, into the liquid-liquid centrifuge of the oil separation stream, the solvent-containing tops go through a charcoal filter and, after addition of requisite amounts of makeup solvent, are recycled to the IPA separation stages.

## IV. COMPUTER USER INFORMATION

### A. Program Outline

The programs making up the FPC cost analysis code can be divided into three classes.

1 Programs handling input and output data and performing calculations which are common to all FPC production processes. This class includes the MAIN program and the subprograms MATER, CAPTOL, and OPERAT.

2 The programs describing each of the five separate processes. The main portion of the computations is performed by these programs. The material and energy balances are computed. On the basis of this information and on

built-in decisions regarding equipment sizes (see Section B) the required capacity for the major equipment items are calculated. The six programs in this class and the process which they analyze are:

<i>Program Name</i>	<i>Process</i>
FPCXXI	Fish meal plant
BIOLOG	Biological process
PRESCK	Press cake biological process
XXIPA	Isopropyl alcohol extraction
PRSIPA	Press cake-IPA extraction process

3 The service and information subprograms. These consist of a large number of largely similar subprograms which calculate the cost for individual equipment items and of the library subprogram LIBRE which contains all of the costing data. The costing subroutines are discussed in more detail in Section C. Usually they are named directly by the equipment name and given an equipment capacity return, its cost and the cost breakdown. In some cases similar types of equipment are handled by single subroutines. The list of the equipment subroutines is:

<i>Identification Number</i>	<i>Equipment</i>	<i>Sub-routine Name</i>
6 =	Conical Hopper	Hopper
7 =	Fish Storage	Silo
8 =	Scrubbers	Conden
11 =	Pulveriser	Pulver
17 =	Screw Conveyor	Screw
18 =	Hammer Mill	Hammer
19 =	Drum Dryer	Dryer
20 =	Pan Dryer	Deyerp
21 =	Rotary Vacuum Dryer	Dryerr
27 =	Boiler	Boiler
30 =	Spray Evaporator	Evpspr
31 =	Wiped Film Evaporator	Evpflm
32 =	Forced Circulation Evaporator	Evpfrc
33 =	Vertical Evaporator	Evphor
40 =	Shop Fabricated Tank	Storag
42 =	Pressure Vessel	Vessel

43 =	Distillation Column	Column
49 =	Jacketed Reacting Vessel	Reactr
50 =	Fish Grinder	Grinder
51 =	Vibrating Screen	Screen
52 =	Sharples Centrifuge	Sharp
53 =	Solid Bowl Centrifuge	Bowl
54 =	Vertical Basket Centrifuge	Cntfge
57 =	Free Flowing Solvent Blender	Blendr
65 =	Reciprocal Pumps	Pmprec
66 =	Centrifugal Pumps	Pmpcnt
67 =	Shell-Tube Heat Exchangers	Heatex
70 =	Belt Conveyor	Belt
71 =	Bucket Conveyor	Bucket
72 =	Scale	Scale
73 =	Agitator-Propeller	Agitor
74 =	Ball Mill	Balmil
75 =	Bagging Machine	Baggma
78 =	Rotary Drum Filter	Filter
80 =	Overhead Crane	Cranes
81 =	Drag Conveyor	Dragma
85 =	Mechanical Refrigeration	Refrig
99 =	Facilities	Fascil

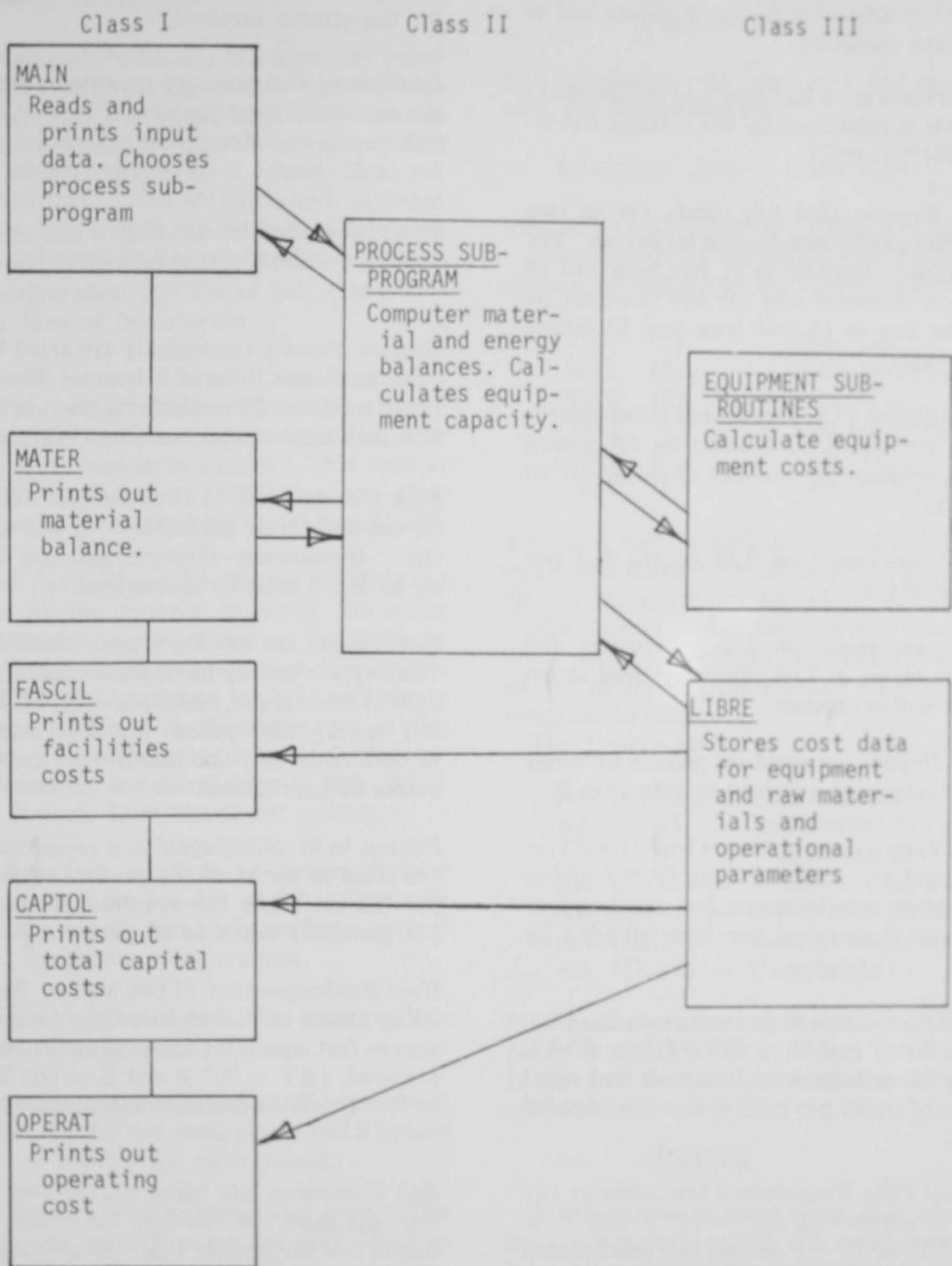
The library program LIBRE performs no other function besides storing the cost data for all equipment items and those process raw materials which are not given in the input data. These data are made available to all the subroutines by reading the contents of LIBRE into a large common block which is made up of two rectangular matrices and a linear matrix, namely AA (100,20), IA (100,5), and BB (100). The first index of the AA and IA matrix usually refers to the identification number of specific equipment items. The BB matrix contains raw material cost data. Thus LIBRE has to be called just once for each individual cost calculation. This is done from the MAIN program.

Most of the program changes which will be necessary as cost data change or become more accurately known can be done in LIBRE. This is discussed in more detail in Appendix A.

The interrelationship of programs during a typical calculation is shown diagrammatically in Figure 6.

Figure 6

Simplified Flow Diagram for the  
FPC Cost Analysis Program



## B. Equipment Sizing

This section follows the listing of equipment in subroutine LIBRE. Only those items of equipment about which design decisions had to be made are discussed.

*Pulp Presses* are 6 feet long and the diameter in inches is calculated by the relation  $8(\text{ton-days}/50)^{1/2}$  up to 24.

*Screw Presses* (for fish meal) are in two sizes with preference for the large one. For 250 ton-days the size is 21 feet long and 16 inches in diameter and for 100 ton-days, or less, the size is 15 feet long and 12 inches in diameter.

*Rotary Steam Tube Dryers* are sized according to amount of feed based on 2.5 square feet to process one ton-day of material fed per day.

*Cookers* are based on 0.25 square feet per ton-day of fish.

*Boilers* are based on 150 psig steam and sized in terms of 1.05 times required steam for the entire process.

*Spray Dryers* are sized on pounds of water to be evaporated as given in reference 7.

*Wiped Film Evaporators* are based on  $\Delta T = 50^\circ \text{F}$  and  $U = 500 \text{ BTU/hr ft}^2 \text{ }^\circ \text{F}$  giving the relation area in square feet equal pounds of water evaporated per hour divided by 25.

*Forced Circulation Evaporators* are based on  $\Delta T = 50^\circ \text{F}$  and  $U = 400 \text{ BTU/hr ft}^2 \text{ }^\circ \text{F}$  giving the relation area in square feet equal pounds of water per hour evaporated divided by 20.

*Vertical Tube Evaporators* are taken as (a) three in series with  $\Delta T = 50^\circ \text{F}$  and  $U = 400 \text{ BTU/hr ft}^2 \text{ }^\circ \text{F}$  giving the relationship area in square feet equal pounds of water evaporated divided by 20, or (b) the concentrator evaporator which has  $\Delta T = 50^\circ \text{F}$  and  $U = 500 \text{ BTU/hr ft}^2 \text{ }^\circ \text{F}$  giving the area in

square feet equal to the pounds of water evaporated divided by 25.

*Storage Tanks* are based on the holding time for the stream involved.

*Distillation Columns* are prorated from the Experiment-Demonstration Plant (EDP) still design and directly scaled. Stage number is 25, height is 54 feet and reflux ratio is two as they are in the EDP. The diameter of a still cannot be less than 4 feet and increases in 2-foot intervals of diameter (4, 6, 8, etc.).

*Reactor Vessels* (biological) are sized based on a residence time of 5 hours. The minimum number of vessels for a plant is three. The maximum vessel size is 10,000 gallons.

*Fish Grinders* are in two sizes for 150 and 75 ton-days with preference for the larger size. Horsepower requirements are based on 40 Hp/3 tons/hr throughout.

*Centrifuges* are of two types. Solid-liquid (disk-type slimers) having 2000 gallons per hour of throughput, and liquid-liquid (Sharples) having 1000 gallons per hour capacity. In both cases only one size is used and it requires 20 horsepower.

*Pumps*, both centrifugal and reciprocating, are sized in terms of the product of gallons per minute times the required pressure in psi, generally taken as 30 psi.

*Heat Exchangers* are of two kinds. Heaters using steam are sized according to area in square feet equals 0.1 times pounds of steam required, ( $\Delta T = 20^\circ \text{F}$  and  $U = 500 \text{ BTU/hr ft}^2 \text{ }^\circ \text{F}$  and the cooling water rise is  $20^\circ \text{F}$ ).

*Belt Conveyors* are taken as 100 feet long. For less than 150 ton-days the width is 36 inches and for greater than 150 ton-days the width is 48 inches.

*Bucket Conveyors* are based on a lifting height of 20 feet.

*Agitators* are for two purposes. For slurries the required horsepower is 0.01 times the tank volume in gallons. For waterlike liquids the horsepower is 0.005 times the tank volume in gallons.

*Bagging and Packaging Machines* are based on bags or cans per minute. 100-pound bags are used for fish meal, 25-pound bags for FPC and other dry products, and 5-gallon cans for paste products.

*Refrigeration* includes brine recycle pump and heat exchanger and is based on 0.5 tons of refrigeration per ton of fish stored and three days of fish storage.

*Brine make-up* — This is a unit called a Brinopac, which delivers 50 gal/hr of 100° brine. It is 24 inches in diameter. The price FOB with hopper is \$1,190. This unit is good for any plant up to 300 ton-days. For any larger plant, the unit would cost \$1,880.

*Boiler Feed Water Treatment* — This includes all the material to purify the boiler feed water, i.e., the water in the make-up tank is deaerated to get rid of dissolved O<sub>2</sub> and CO<sub>2</sub>. Ion exchange is used to eliminate Mg and Ca ions. A pH adjustment is also made. The initial unit for boiler feed water treatment for any size is about \$1,000. After that, it costs \$100/month for upkeep.

*Buildings* are sized at 14 square feet of ground floor per ton-day of fish. Generally buildings are 40 feet high and have several levels depending on operations.

*Real Estate* is based on 0.0050 acres per ton-day of plant capacity.

*Warehouse* space is taken as 15 square feet per ton-day for fish meal plants and 3 square feet per ton-day for other plants.

*Fish Pumps* are reciprocating type. The plants use one fish pump for each 500 ton-days of fish. Smaller plants have one pump.

*Dock Facilities* are 2,400 square feet for each fish pump.

## C. Equipment Subroutine

The material base cost of almost all pieces of equipment are estimated by the equation

$$\text{Base Cost} = a (\text{SIZE})^b \quad (1)$$

The installation cost, labor cost, and incidental costs are determined by

$$\text{Subsidiary Costs} = (\text{Base Cost}) \cdot d^i \quad (2)$$

where  $d$  = cost factors in LIBRE,  $i = 1, 2, 3, 4$ .

The subprogram associated with the fisheries costing programs uses the following variables:

COST (1)	Base Cost
COST (2)	Field Materials Cost
COST (3)	Labor Cost
COST (4)	Indirect Cost
COST (5)	Total Cost
COST (6)	Uncertainty in Cost

The base cost is updated by multiplying the value determined in equation (2) by the Marshall and Stevens index BB (1).

The factors accounting for materials cost, labor cost, indirect cost, and uncertainty cost as well as the constants  $a$  and  $b$  are stored in program LIBRE.

The factors are:

AA (IX,7)	= Unit Cost ( $a$ )
AA (IX,8)	= Exponential in Cost Equation ( $b$ )
AA (IX,11)	= Materials Cost Factor
AA (IX,12)	= Direct Cost Factor
AA (IX,13)	= Indirect Cost Factor
AA (IX,14)	= Uncertainty Cost Factor

In a limited number of the subprograms, the factor  $a$  depends on a second size variable. In this case the cost is entered directly into the subprogram:

i.e. SCREW R

Furthermore, in some cases, it is desired to have a materials option. Several approaches have been used in the program:

i.e. PMPCNT  
STORAG

In subsequent changes it is recommended that the following procedure be used. The material is selected in the program and designated by IA (IX,5)=INTEGER. For example if the equipment is to be constructed of monel then IA (IX,5) = 8: it is not necessary that the integer be associated with the same material for each item of equipment. In the subprogram one has the statements

```
IF (IA (IX,5). EQ. 8) BB (2) = 6.1
COST (1) = COST (1) * BB (2)
```

The second card comes after the computation of the indirect, labor, and materials cost based on the initial base cost.

The factor BB(2) can be entered from the main program (XXIPA, BIOLOG, etc.) as well. In addition a print statement is added to be consistent with the new option.

Usually the sizing equation is adequately represented by one sizing variable. This term is designated AA (IX,17). Occasionally it is necessary to have two variables, in which case the variable is usually AA (IX, 18), although on occasion AA (IX,20) has been used.

To illustrate the costing program we consider a typical subprogram BUCKET, the program for the bucket conveyor.

#### SUBROUTINE BUCKET\*

1. IX + 71
2. Q = AA (IX,7)
3. IF (AA (IX,18). GR. 30. and. AA (IX, 18). LE. 75),  
AA (IX,7) = AA (IX,7) + 180
4. IF (AA (IX,18). GR. 75.) AA (IX,7) =  
AA (IX,7) + 280.
5. COST (1) = AA (IX,7 \* AA (IX,17)  
\*\* AA (IX,8) \* BB (1)
6. COST (1) = COST (1) \* .001

\* FORMAT, DIMENSION, PRINT, common statements have been omitted.

7. COST (2) = COST (1) \* AA (IX,11)
8. COST (3) = COST (1) \* AA (IX,12)
9. COST (4) = COST (1) \* AA (IX,13)
10. COST (5) = COST (1) + COST (2) +  
COST (3) + COST (4)
11. COST (6) = COST (5) \* AA (IX,15)
12. DO 1 I = 1,6
13. 1 COST A (I) = COST A (I) +  
COST (I)
14. AA (IX,7) = Q

Statements 2 and 14 are necessary in order that the values in LIBRE remain constant when the subroutine is used repeatedly.

Statements 3 and 4 adjust the value of the constant *a* [AA (IX,7)] for different values of AA (IX,18) which is the capacity of the conveyor in tons. The size unit AA (IX,17) is the height in feet.

Statements 5 and 6 determine the base cost in thousand dollar groupings. In 7-11 the costs of materials, labor, incidentals, and cost variation as well as total cost are determined.

In statements 12 and 13 the running cost of the plant option (IPA, Biological, etc.) is computed.

If different materials of construction were used then one would add the statement

$$\text{COST (1) = COST (1) * BB (2)}$$

between statements 9 and 10.

#### D. Program Input

The input to the FPC program can be divided into two parts: a) the "standard" input which is common to all of the different processes; b) the "optional" input presented in Section III, which discusses the individual processer; here we shall explain the standard input.

The standard input consists of four cards. The first of these enters integer input data, the remaining three enter input data in the floating point format.

<i>Program Variable</i>	<i>Columns</i>	<i>Description</i>
I. Card 1:	Format: (8I10)	
A. Iz	1-10	Fixes process to be analyzed. 1 = fish meal 2 = IPA 3 — biological 4 = press cake — biological 7 = press cake — IPA extrac- tion
B. Options	11-20	
1. fish meal		
IPTION (1)		1 = solubles are product
IPTION (2)		2 = solubles recycled
2. IPA		1 = wet deboning
IPTION (1)		blank = no deboning
II. Card 2:	Format (3E 12.5)	
tons	1-12	The tons of fish to be processed per day.
BB(1)	13-24	The Marshall-Stevens index tak- ing the 1970 index of 297.5 as one.
BB(50)	25-36	The operating days per year.
III. Card 3:	Format (5E 12.5)	
BB(5)	1-12	Cost of the fish in ¢/lb.
BB(6)	13-24	Cost of electricity in ¢/KWHr.
BB(7)	25-36	Labor and supervisory costs in dollars/hr.
BB(8)	37-48	Depreciation and interest in per- cent per year.
BB(10)	49-60	Fuel cost in dollars per therm.
IV. Card 4:	Format (3E 12.5)	
BB(30)	1-12	Oil composition of the fish in weight percent.
BB(31)	13-24	Protein composition percent.
BB(32)	25-36	Ash composition in percent.
V. (For Biological and Presscake programs only)		
Card 5:	Format (5E 12.5)	
BB(40)	1-12	The effectiveness of the enzyme being used in lbs. of enzyme re- quired per 100 lb. of fish being processed. (For press cake Biological, it is per 100 lb. of press cake being processed.)
BB(41)	13-24	Price of enzyme is \$/lb.

BB(42) 25-36

The percentage of the total dissolved solids stream coming out of the wiped film evaporator (see Figure 2) which is packaged in paste form.

BB(43) 37-48

The effectiveness of the antioxidant being used, in lbs. of antioxidant required per 100 lb. of fish or 100 lb. of press cake.

BB(44) 49-60

Price of antioxidant in \$/lb.

#### VI. (For Press cake — IPA extraction only)

Card 1: Format (8I10)  
40

The number of IPA extraction stages (if different than four) should appear.

### E. Program Output

The output of the cost analysis program is presented in seven separate sections:

- 1) Printout of input data.
- 2) Detailed equipment costs.
- 3) Material and energy balance.
- 4) Cost of facilities.
- 5) Capital costs.
- 6) Operating costs.
- 7) Production Cost of FPC.

Each of these sections is printed out in the form of a table. The contents of these tables will now be taken up in turn.

1) *Input Data.*—Identifies the process being analyzed, prints out all of the external input data and operating options.

2) *Detailed Equipment Costs.*—This is the most extensive table of the output. It presents the total cost and the cost breakdown of each major item of equipment required in a given process. Each equipment item is identified, its capacity, capacity units, and major construction material is printed. Following this information the total cost and the cost breakdown for this equipment are given. The cost breakdown uses the scheme of Reference (6) which is identified in the table headings. That is,

the first column labelled "Base Cost" gives the FOB. to manufacturer cost for this type and capacity equipment. This cost is multiplied by the Marshall and Stevens index given in the input data. The methods used computing this cost, the sources of the required internal data and the means for modifying these data are presented in Appendix A.

The subsequent three columns present additional costs which are incurred before the purchased equipment becomes operable.

Column 2, the "Material Costs" includes such diverse items as piping, electrical wiring, equipment base, and heat insulation. Column 3, the "Labor Costs" are the labor costs incurred during installation, and Column 4, the "Indirect Costs", summarizes remaining expenses such as shipping, insurance, construction overhead, and construction engineering costs.

All of these cost items are calculated as factors of the first column. These factors vary with equipment type but not with capacity. For each equipment item they are tabulated in the subprogram LIBRE and are easily accessible for modification.

The fifth column, titled "Module Cost", is a summation of the four previous columns and represents the capital investment required to design, order, ship, and install a given equipment item. Finally, the last column, titled "Range", is an estimate of the reliability of

these cost figures. This estimate is based upon the cost data available at the end of 1969 and summarized in the LIBRE subprogram. As time passes and cost figures are modified, the range estimate should be changed as well.

The information described above is printed out individually for each major piece of equipment even if multiple items of identical type and capacity of equipment are required. The sequence of printing out this information starts with equipment required to unload and store the fish (that is, the first item is always the fish pumps), and after that follows the main process streams. For example, in the fish meal plant analysis the equipment required to process the solids stream is presented first, then come the centrifuges required for oil separation, the evaporators required to concentrate the dissolved solids, and finally equipment items which do not really fit into the process stream, as the boiler, fork lift, or the cost of the instrumentation loops.

3) *Material and Energy Balance.*—This table presents first the overall, then the detailed material and energy balance. In the overall section of the table the total steam, electricity, and cooling water used in the process is given. The fish feed is broken down into the oil, protein, and ash components.

The detailed portion of the table prints out the process stream balances in terms of hourly throughput. The sequence of printout generally follows the process stream flow lines as shown in Figures 1 to 6. Where branches in the process stream occur (for example at the separation of oil and stickwater for the fish meal plant) the balance calculation follows one of the streams to completeness and returns to the branch point to pick up the remaining stream.

4) *Cost of Facilities and Site Development.*—This table summarizes the cost of land, docks, warehouses, and process buildings. The cost breakdown is similar to that described for Table 2. The data used in the calculations are stored in subroutine LIBRE and are printed out for easy reference in the table.

5) *Summary of Fixed Costs.*—This is a summation of total capital costs. It includes

the already detailed costs for equipment and facilities plus provisions for spare parts, engineering of the plant, and contingencies. The latter three are calculated as fractions of the summarized equipment cost.

6) *Operating Costs.*—This table presents the total and detailed plant operating costs on a daily and yearly basis. The quantities of all the materials used in the process and their daily costs are printed out first. This portion of the table contains also such items as electricity, packaging, and labor and supervision man-hours. Under the title "City Water" only the water used in the process which must be of drinking quality is included. The cost of process water (i.e. for scrubbers and condensers) is calculated in terms of the electricity needed to pump it.

The second portion of the table includes items which are calculated as fractions of the total capital or equipment costs. These are depreciation (at a percentage figure given in the input), maintenance, and insurance. The factors used to calculate these costs appear in subroutine OPERAT. Where not supplied in the input, the prices of the process material are stored under the designation BB(I) in subroutine LIBRE.

The third portion of the table summarizes the production rate of various products on a daily and yearly basis.

7) *Production Cost of FPC.*—The last table is entitled "Production Cost of FPC." In this table the following are listed:

- a) by-products of the process
- b) the assumed selling price in cents/pound
- c) the by-products total worth.

Two prices of FPC appear at the end of the printout. The first price is calculated by dividing total operating cost by the FPC produced per year. The second price takes into account the process by-products by subtracting their total worth from the total operating cost before dividing by the FPC produced per year. The calculations and printout take place in the subprogram OPERAT. The assumed selling prices of the by-products are found in LIBRE [BB(66) to BB(68)] and can easily be changed.

## APPENDIX

### A. Internal Program Changes

#### A-1. INTERNAL DATA CHANGES

There are several occasions when it may be necessary to update the program. These include the following:

- 1) The estimated cost of an item of equipment is in error
- 2) a new piece of equipment is to be added
- 3) the equipment sizing routine is to be altered
- 4) a new option is to be added to the plant options
- 5) a change in the cost of chemicals.

Most changes, especially of the types 1 and 5, may be made directly in the program LIBRE. Changes in bare cost, incidentals, labor, and materials for the process equipment may be made by substitution of the appropriate cards in LIBRE.

#### Example 1

The cards in LIBRE for a Rotary Dryer are:

AA (21,7) = 1000.  
AA (21,8) = .5  
AA (21,11) = .30  
AA (21,12) = .30  
AA (21,14) = .30

For these values the base cost of a dryer with 400 square feet is estimated to be \$20,000.

The manufacturer's estimates for this equipment were \$30,000, with the installed cost, labor cost, and incidentals estimated correctly.

Solution:

The base cost of the equipment too low. The simplest adjustment is to alter the base cost AA (21,7) to give the correct value. However, an increase of the base cost results in a incidental increase as well. The recommended solution is to substitute for the above cards in LIBRE the new cards.

AA (21,7) = 1500.  
AA (21,8) = .50  
AA (21,11) = .20  
AA (21,12) = .20  
AA (21,14) = .20

#### Example 2

The price of sulfuric acid is 30% more expensive at Plant A than it is at the other plants.

Solution:

The card [AA (100,14) = 1.00] in LIBRE is replaced with AA (100,14) = 1.30.

Occasionally in some items of equipment, such as a screw conveyor, one cannot alter the program by a single change of cards in LIBRE. The reason for this is that the base cost is a function of the diameter of the conveyor, which is an additional input variable to the costing subroutine. In this case it is necessary to alter the costing subroutine itself.

#### Example 3

The cost of the screw conveyor with a diameter greater than 2" has been found to overestimate the cost by a factor of 12. The labor cost, the incidentals, and the installation costs are correctly estimated. All other estimates are correct.

Here one cannot simply change LIBRE since the modification would appear for other sizes as well. There are many ways of modifying the program; one way would be to add the card to the subroutine SCREWWR.

If (AA (IX,18).GT.12.) AA (IX,7) = .5\* AA (IX,7) which states that if the diameter is greater than 12 then the base cost is reduced by 50%.

The addition of a new equipment item requires three changes to the program.

1) First the new subroutine is named and given a previously unassigned index number. The Fortran statement of the program would be closely modeled after existing subroutines. It is strongly recommended that AA (IX,17) be used to designate the principal variable in the costing equation.

2) The variables for the costing equations are added to LIBRE. These should include

AA (IX,7)	Base Cost
AA (IX,8)	EXPONENT
AA (IX,11)	Materials
AA (IX,12)	Labor
AA (IX,13)	Incidentals
AA (IX,15)	Range of COSTS

3) The calling subroutine must be added to the primary subroutines. This calling sequence will include at least a sizing equation and the call statement.

```
AA (IX,17) = SIZE * .01/24  
CALL EQUIPM
```

#### A-2. EQUIPMENT SIZING AND PROCESS CHANGES

The equipment sizing routine is altered by changing statements in the primary subroutines.

#### Example 4

The area of heat exchangers in square feet was found to be 12% of the water evaporated rather than 10%, for the preheater to the distillation column.

Solution:

The subprogram XXIPA has the statement

```
FF = STEAMS * .1  
AA (67,17) = FF
```

These two cards are removed and replaced with

```
AA (67,17) = STEAMS * .12
```

Which not only makes the desired change but increases the efficiency of the program as well.

Major changes in program options must be made in the subprograms. In addition changes must be made in the main program as well. In general, there is no simple way of making these modifications.

#### Example 5

It is wished to add a costing subprogram for the VIOBIN program.

The procedure is to write a subprogram in Fortran for the VIOBIN program analogous to the program for the IPA process.

In addition changes are required in the program MAIN and the program OPERAT.

The user by referring to the above programs and using the example of the IPA process, can by analogy make the appropriate changes necessary for VIOBIN.

The printout can be modified by substitution of Format cards in the appropriate program.

## B. References

1. Gaden, E. L., Jr., "World Protein Resources," Chem. Engr. Progress, 65, (9), September, 1969.
2. Roels, O. A., "Marine Protein," Chem. Engr. Progress, 65, (9), 27, September, 1969.
3. Klumpar, I. V., "Process Predesign by Computer," Chem. Engr., 76, 114, September 22, 1969.
4. Drayer, D. E., "How to Computerize Plant Cost Estimations," Petro/Chem. Engineer, 42, 39, May, 1970.
5. "Economic Indicators," Chem. Engr., 77, 250, May 4, 1970.
6. Guthrie, K. M., "Capital Cost Estimating," Chem. Engr., 76, 115, March 24, 1969.
7. Drew, J. W., and Ginder, A. F., "How to Estimate the Cost of Pilot-Plant Equipment," Chem. Engr., 77, 100, February 9, 1970.
8. Dryden, C. E., and Furlow, R. H., "Chemical Engineering Costs," Ohio State University, Columbus, 1966.
9. Mills, H. E., "Costs of Process Equipment," Chem. Engr., 71, 133, March 16, 1964.
10. Clerk, Jackson, "Multiplying Factors Give Installed Costs of Process Equipment," Chem. Engr., 70, 182, February 18, 1962.
11. Miller, C. A., "New Cost Factors," Chem. Engr., 72, 226, September 13, 1965.
12. "Centrifuges Exemplify Chem. Show Trends," Chem. & Engr. News, 56, December 15, 1969.
13. Ambler, C. M., "How to Select the Optimum Centrifuge," Chem. Engr., 76, 96, October 20, 1969.
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15. Drayer, D. E., "How to Estimate Plant Cost-Capacity Relationship," Petro/Chem. Engineer, 42, 10, May, 1970.
16. Kapfer, W. H., "Appraising Rate of Return Methods," Chem. Engr., Progress, 65, 55, November, 1969.
17. Ernst, R. C., "FPC: The NMFS Experiment and Demonstration Plant Process," Commercial Fisheries Review, 33(2), 22-28, February, 1971.

## C. FORTRAN Listing of Program

The FORTRAN listing of the program appears as Table I.

## D. Sample Problems

To illustrate the capabilities of the program a cost study spanning the feasible range of plant sizes was conducted. The plant capacities chosen were 50, 200, and 1,000 tons of fish per day. Fish availability time in each case was 200 days per year. For all processes except the Press cake-IPA this corresponds also to the plant operation time. For the Press cake-IPA process the IPA extraction portion of the plant

can operate for an additional 50 days to process the stored press cake. Fish food composition corresponded to a "lean" species (oil fraction = 0.04) and a "fat" species (oil fraction = 0.12). The price of fish was taken as 1¢/lb. for these examples.

#### 1. SAMPLE OUTPUT

The entire output printout for an IPA process plant having a capacity of 200 tons/day and sized for a "lean" fish feed is presented in the subsequent pages. The number headings identifying the tables are explained in Section IV-E. The detailed equipment printout table, IPA Plant Cost Analysis, (Table II,) can be interpreted by following the process description given in Section III-C.

### E. Study Summarization

The output of the study is summarized in Tables III to VI. The first three present data for each of the three plant capacities producing FPC. Table VI summarizes the results of the bench mark fish meal process.

349. Use of abstracts and summaries as communication devices in technical articles. By F. Bruce Sanford. February 1971, iii + 11 pp., 1 fig.

350. Research in fiscal year 1969 at the Bureau of Commercial Fisheries Biological Laboratory, Beaufort, N.C. By the Laboratory staff. November 1970, ii + 49 pp., 21 figs., 17 tables.
351. Bureau of Commercial Fisheries Exploratory Fishing and Gear Research Base, Pascagoula, Mississippi, July 1, 1967 to June 30, 1969. By Harvey R. Bullis, Jr., and John R. Thompson. November 1970. iv + 29 pp., 29 figs., 1 table.
352. Upstream passage of anadromous fish through navigation locks and use of the stream for spawning and nursery habitat, Cape Fear River, N.C., 1962-66. By Paul R. Nichols and Darrell E. Louder. October 1970, iv + 12 pp., 9 figs., 4 tables.
354. Sanitation guidelines for the control of *Salmonella* in the production of fish meal. By E. Spencer Garrett and Richard Hamilton. October 1971, iv + 7 pp., 9 figs. For sale by the Superintendent of Documents, U.S. Government Printing Office, Washington, D.C., 20402. Price 25 cents. Stock number 0320-0023.
356. Floating laboratory for study of aquatic organisms and their environment. By George R. Snyder, Theodore H. Blahm, and Robert J. McConnell. May 1971, iii + 16 pp., 11 figs.
361. Regional and other related aspects of shellfish consumption — some preliminary findings from the 1969 Consumer Panel Survey. By Morton M. Miller and Darrel A. Nash. June 1971, iv + 18 pp., 19 figs., 3 tables, 10 apps.

# Table I.—FORTRAN listing of program.

FOR.S MAIN.MAIN  
FOR S9A-07/12-11:03 (0.)

## MAIN PROGRAM

STORAGE USED: CODE(1) 000407; DATA(0) 000330; BLANK COMMON(2) 000000

### COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016  
0005 BLOCK4 000012

### EXTERNAL REFERENCES (BLOCK, NAME)

0006 I IBRE  
0007 FPCXX1  
0010 XXIPA  
0011 BIOLOG  
0012 PRESCK  
0013 PRSIPA  
0014 FASCIL  
0015 CAPTOL  
0016 OPERAT  
0017 NINTR\$  
0020 NRDU\$  
0021 NIO\$  
0022 NRDC\$  
0023 NPRT\$  
0024 NSTOP\$

### STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000010	100F	0000	000052	1000F	0000	000062	1001F	0000	000072	1002F	0000	000102	1003F					
0000	000041	1007F	0000	000011	101F	0000	000114	1010F	0000	000120	1011F	0000	000132	1012F					
0000	000142	1013F	0000	000154	1014F	0000	000166	1015F	0000	000201	1016F	0000	000213	1017F					
0000	000013	102F	0000	000226	1020F	0000	000233	1021F	0000	000244	1022F	0000	000255	1023F					
0000	000015	103F	0000	000264	1030F	0000	000271	1031F	0000	000277	1032F	0000	000305	1033F					
0000	000313	1034F	0000	000017	1040F	0000	000030	1041F	0001	000004	106G	0001	000002	2L					
0001	000304	200L	0001	000403	999L	0003	000000	AA	0003	R	004704	BB	0004	R	000000	COST			
0004	R	000007	COSTA	0003	003700	IA	0005	I	000000	IPTION	0000	I	000006	IU	0000	I	000005	IV	
0000	I	000004	IW	0000	T	000003	IX	0000	I	000002	IY	0000	I	000001	IZ	0000	I	000000	J
0000	R	000007	TONS																

00100 1\* C FPC PROCESS COST ANALYSIS PROGRAM  
00101 2\* COMMON/BLOCK1/AA(100,20),IA(100,5),BB(100)  
00103 3\* COMMON/BLOCK2/ COST(7),COSTA(7)  
00104 4\* COMMON/BLOCK4/ IPTION(10)  
00105 5\* 2 DO 1 J = 1,7  
00110 6\* COST(J) = 0.0  
00111 7\* 1 COSTA(J) = 0.0

Table I.-- Continued.

```

00113      8*      CALL LIBRE
00114      9*      READ(5,100,END=999) IZ,IY,IX,IW,IV,IU
00124     10*      100  FORMAT(8I10)
00125     11*      READ 101,TONS,BB(1),BB(50)
00132     12*      101  FORMAT(3E12.5)
00133     13*      BB(1) = BB(1)*297./>RU.
00134     14*      READ 102,BB(5),BB(6),BB(7),BB(8),BB(10)
00143     15*      102  FORMAT(5E12.5)
00144     16*      READ 103,BB(30),BB(31),BB(32)
00151     17*      103  FORMAT(3E12.5)
00152     18*      BB(91) = IZ
00153     19*      IPTION(1)=IY
00154     20*      IF(IZ.EQ.7) TPTION(5) =IW
00156     21*      1040 FORMAT(//44H          THE WET DEBONING OPTION IS APPROPRIATE)
00157     22*      1041 FORMAT(//44H          THE DRY DEBONING OPTION IS APPROPRIATE)
00160     23*      IF(IZ .EQ. 1) PRINT 1000
00163     24*      IF(IZ .EQ. 2) PRINT 1001
00166     25*      IF(IZ .EQ. 3) PRINT 1002
00171     26*      IF(IZ .EQ. 4) PRINT 1003
00174     27*      IF(IZ.EQ.7) PRINT 1007
00177     28*      1007 FORMAT(1H1//20X,40H PRESS CAKE IPA PROCESS COST ANALYSIS )
00200     29*      1000 FORMAT(1H1//20X30H FISH MEAL PLANT COST ANALYSIS )
00201     30*      1001 FORMAT(1H1//20X30H TPA PLANT COST ANALYSIS )
00202     31*      1002 FORMAT(1H1//20X35H BIOLOGICAL PROCESS COST ANALYSIS )
00203     32*      1003 FORMAT(1H1//20X44H PRESS CAKE BIOLOGICAL PROCESS COST ANALYSIS )
00204     33*      PRINT 1010
00206     34*      1010 FORMAT(//16H          INPUT DATA )
00207     35*      PRINT 1011,TONS
00212     36*      PRINT 1012,BB(1)
00215     37*      PRINT 1013,BB(5)
00220     38*      PRINT 1014,BB(6)
00223     39*      PRINT 1017,BB(10)
00226     40*      PRINT 1015,BB(7)
00231     41*      PRINT 1016,BB(8)
00234     42*      PRINT 1030
00236     43*      BB(33)=100.0-BB(30)-BB(31)-BB(32)
00237     44*      PRINT 1031,BB(30)
00242     45*      PRINT 1032,BB(31)
00245     46*      PRINT 1033,BB(32)
00250     47*      PRINT 1034,BB(33)
00253     48*      1011 FORMAT(//8X31H PLANT SIZE           =,F10.2,9H TONS/DAY )
00254     49*      1012 FORMAT(/8X31H MARSHAL/STEVENS INDEX       =,F10.3 )
00255     50*      1013 FORMAT(/8X31H COST OF FISH           =,F10.2,9H CENTS/LR )
00256     51*      1014 FORMAT(/8X31H ELECTRICITY COSTS        =,F10.2,10H CENTS/KWH)
00257     52*      1015 FORMAT(/8X31H LABOR AND SUPV. COSTS     =,F10.2,12H DOLLARS/HR
00257     53*      C )
00260     54*      1016 FORMAT(/8X31H DEPRECIATION AND INT. CHARGE =,F10.2,10H PERCENT )
00261     55*      1017 FORMAT(/8X31H FUEL COST                 =,F10.2,15H DOLLARS/TH
00261     56*      CERM )
00262     57*      PRINT 1020
00264     58*      PRINT 1023,BB(50)
00267     59*      IF(IZ.NE.1) GO TO 200
00271     60*      IF(IY .EQ. 1) PRINT 1022
00274     61*      IF(IY .EQ. 2) PRINT 1021
00277     62*      200  CONTINUE
00300     63*      1020 FORMAT(//23H          OPERATING OPTIONS )
00301     64*      1021 FORMAT(//23H          OPERATING OPTIONS )

```

Table I.--Continued.

```

00302 65* 1022 FORMAT(/8X45H SOLUBLE FISH SOLIDS REMOVED AS PRODUCT TY=1 )
00303 66* 1023 FORMAT(/8X26H OPERATING DAYS PER YEAR =,F8.0)
00304 67* 1030 FORMAT(/8X18H FISH COMPOSITION )
00305 68* 1031 FORMAT(/13X11H OIL =,F6.2,8H PERCENT)
00306 69* 1032 FORMAT( 13X11H PROTEIN =,F6.2,8H '-'' )
00307 70* 1033 FORMAT( 13X11H ASH =,F6.2,8H '-'' )
00310 71* 1034 FORMAT( 13X11H WATER =,F6.2,8H '-'' )
00311 72* IPTION(5)=IV
00312 73* IF(IX.EQ.1) PRINT 1040
00315 74* IF(IX.EQ.2) PRINT 1041
00320 75* IF(IZ.EQ. 1) CALL FPCXX1(TONS)
00322 76* IF(IZ.EQ.2) CALL VXTPA(TONS)
00324 77* IF(IZ.EQ. 3) CALL BIOLOG(TONS)
00326 78* IF(IZ.EQ. 4) CALL PRESCK(TONS)
00330 79* IF(IZ.EQ.7) CALL PRSIPA(TONS)
00332 80* CALL FASCIL(TONS)
00333 81* CALL CAPTOL(TONS)
00334 82* CALL OPERAT(TONS)
00335 83* GO TO 2
00336 84* 999 STOP
00337 85* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

QFOR.S FPCXX1.FPCXX1  
FOR S9A-07/12-11:03 (0,)

SUBROUTINE FPCXX1 ENTRY POINT 002231

STORAGE USED: CODE(1) 002315; DATA(0) 000600; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK4 000012  
0004 BLOCK1 005050  
0005 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0006 PMPREC  
0007 RELT  
0010 STORAG  
0011 PMPCNT  
0012 BUCKET  
0013 DRYERR  
0014 SCREWR  
0015 SCREEN  
0016 BLENDR  
0017 HAMMER  
0020 SCALE  
0021 BAGGMA  
0022 CNTFGE  
0023 SHARP  
0024 EVPHOR  
0025 ROILER  
0026 CONDEN  
0027 MATER  
0030 NPRT\$  
0031 NI02\$  
0032 NI01\$  
0033 NEXP6\$  
0034 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000214	1010F	0000	000065	1021F	0000	000047	1022F	0000	000203	1034F	0000	000174	1041F
0000	000215	1060F	0000	000226	1061F	0000	000237	1062F	0000	000250	1063F	0000	000261	1064F
0000	000272	1065F	0000	000303	1066F	0000	000314	1067F	0000	000325	1068F	0000	000336	1069F
0000	000347	1070F	0000	000360	1071F	0000	000371	1072F	0000	000413	1073F	0000	000402	1074F
0001	000027	111G	0001	000111	136G	0001	000146	155G	0001	000220	176G	0000	000103	2000F
0001	000377	250G	0001	000514	3L	0000	000116	3000F	0001	000602	327G	0001	000530	4L
0001	001032	422G	0000	000156	4242F	0001	001073	437G	0001	001457	51L	0001	000563	52L
0001	001663	664G	0004	R 000000	AA	0004	R 004704	BB	0000	R 000024	BULK	0005	R 000000	COST
0005	R 000007	COSTA	0000	R 000046	FISH	0000	R 000013	G	0000	R 000032	GAL	0000	R 000031	GALL
0000	R 000007	GALLON	0000	R 000010	GALS	0000	R 000014	HP	0000	R 000016	HPOWER	0000	I 000000	I
0004	I 003720	IA	0000	000557	INJP\$	0003	I 000000	IPTION	0000	I 000041	IXX	0000	I 000040	J
0000	I 000021	NA	0000	I 000023	NB	0000	I 000012	NUM	0000	I 000026	N1	0000	R 000042	PXX

Table I.-- Continued.

```

0000 R 000044 SCRUB      0000 R 000043 SOL      0000 R 000045 STM      0000 R 000011 SUMHP    0000 R 000015 TANK
0000 R 000033 TONA      0000 R 000034 TONB    0000 R 000035 TONC    0000 R 000037 TOND    0000 R 000006 TONSA
0000 R 000020 TONSB    0000 R 000022 TONSC    0000 R 000030 TONSSW  0000 R 000025 TONST   0000 R 000036 XLOOPS
0000 R 000017 XNUM      0000 R 000021 Z1      0000 R 000003 Z2      0000 R 000004 Z3      0000 R 000005 Z4
0000 R 000001 Z6      0000 R 000027 Z7

```

```

00101 1*          SUBROUTINE FPCXX1(TONS)
00101 2*          C
00101 3*          C   FISH MEAL PRODUCTION
00101 4*          C
00103 5*          COMMON/BLOCK4/ IPTION(10)
00104 6*          COMMON/BLOCK1/AA(100,20),IA(100,5),BB(100)
00105 7*          COMMON/BLOCK2/ COST(7),CONSTA(7)
00106 8*          BB(3)=1.
00107 9*          BB(2)=1.
00110 10*         DO 10 I=30,33
00113 11*         10   BB(I) = BB(I)*0.01
00115 12*         BB(33)= 1.-BB(30)-BB(31)-BB(32)
00116 13*         AA(91,2)= ((BB(31)*.85) + BB(32))* TONS*.2.
00117 14*         AA(91,3) = (1.2*TONS)-AA(91,2)
00120 15*         Z6= TONS*(BB(31)*.15)/AA(91,3)
00121 16*         Z1=AA(91,3)/TONS
00122 17*         Z2=AA(91,2)*.5/AA(91,3)
00123 18*         Z3=TONS * BB(30)/(AA(91,3)+(0.5*AA(91,2)))
00124 19*         Z4=AA(91,2)/TONS
00125 20*         1022 FORMAT(/ 25H PAYLOADER AND FORK LIFT , 10X ,15H           ,10H
00125 21*         1           ,F10.3,30X,F10.3)
00126 22*         1021 FORMAT(/ 25H CONTROL INSTRUMENTATION , 10X ,15H           ,10H
00126 23*         1           ,F10.3,30X,F10.3)
00127 24*         PRINT 2000
00131 25*         2000 FORMAT(1H1//55H DETAILED EQUIPMENT COSTS (ALL COSTS IN 1000.0 DOL
00131 26*         CLARS) )
00132 27*         PRINT 3000
00134 28*         3000 FORMAT (/18H           EQUIPMENT TYPE,10X10H CAPACITY,12X9H MATERIAL,
00134 29*         C60H BASE MATERIALS LABOR INDIRECT MODULE RANGE ,/6
00134 30*         C0X60H COST COSTS COSTS COSTS COST + OR - )
00135 31*         DO 1 I=1,7
00140 32*         COSTA(I)=0.
00141 33*         COST(I)=0.
00142 34*         1 CONTINUE
00142 35*          C
00142 36*          C   UNLOADING AND STORAGE OF FISH
00142 37*          C
00144 38*         TONSA=TONS*2000./8.33
00145 39*         GALLON= TONSA/(24.*60.)
00146 40*         GALS =GALLON*1.3
00147 41*         SUMHP= 0.
00150 42*         IA(65,1) = 0
00151 43*         IA(65,2) = 1.0
00152 44*         AA(65,17) = GALS*15
00153 45*         NUM = TONS/600. +1
00154 46*         DO 143 I=1,NUM
00157 47*         SUMHP=SUMHP+(AA(65,17)*.001*1.5)
00160 48*         143 CALL PMPREC

```

29

Table I.-- Continued.

```

00162 49* IA(65,2) = 0.0
00163 50* IF(TONSA.LT.30000.) G=(30000./(24.*60.))*15.
00165 51* IF(TONSA.GE.30000.) G=(450000./(24.*60.))*15.
00167 52* IF(TONS.LE.150.) AA(70,18)= 36.
00171 53* IF(TONS.GT.150.) AA(70,18)= 48.
00173 54* AA(70,17)=100.
00174 55* CALL BELT
00175 56* DO 81 I=1,2
00200 57* AA(40,17)=TONS*32.05*3.
00201 58* IA(40,1)=0
00202 59* IA(40,2)=2
00203 60* CALL STORAG
00204 61* IA(40,2)=0
00205 62* 81 CONTINUE
00207 63* AA(66,17)=30.*30.*TONS/(24.*60.)
00210 64* CALL PMPCNT
00211 65* HP=.001*AA(66,17)
00212 66* SUMHP=HP+SUMHP
00213 67* TANK=240.*TONS*1.
00214 68* IA(40,1)=2
00215 69* AA(40,17)=TANK
00216 70* AA(40,18)=1.0
00217 71* CALL STORAG
00220 72* TONSA=TONS*.8*2000./(8.33*16.)
00221 73* TONSA=TONSA*71/.8
00222 74* HPOWER= .01*TONSA
00223 75* NUM=(HPOWER/20.)+ 1.
00224 76* XNUM=NUM
00225 77* TONSB=TONS/24.
00226 78* AA(71,18)= TONSB
00227 79* AA(71,17)= 20.
00230 80* CALL BUCKET
00230 81* C
00230 82* C FISH COOKERS AND SCREW PRESS
00230 83* C
00231 84* BB(2) = 0.67
00232 85* IA(21,5)= 2
00233 86* AA(21,17) = 0.25*TONS
00234 87* CALL DRYERR
00235 88* IA(21,5) = 0
00236 89* IF (TONS.GT.300.) NA=(TONS/250.) +1.
00240 90* IF (TONS.LE.300.) NA=(TONS/100.) +1.
00240 91* C PUMP TO PRESS
00242 92* AA(66,17)=(AA(01,3)+AA(91,2))*2000.*30./(16.*60.*8.33)
00243 93* IA(66,1)=0
00244 94* CALL PMPCNT
00245 95* HP=.001*AA(66,17)
00246 96* SUMHP=SUMHP+HP
00247 97* DO 2 I= 1,NA
00252 98* IA(17,5)=3
00253 99* BB(2)=1.1
00254 100* IF(TONS.GT.300.) AA(17,17) = 21.
00256 101* IF(TONS.GT.300.) AA(17,18) = 16.
00260 102* IF(TONS.LE.300.) AA(17,18) = 12.
00262 103* IF(TONS.LE.300.) AA(17,17) = 15.
00264 104* CALL SCREWR
00264 105* C PUMP FROM PRESS TO SCREEN

```

## Table I.-- Continued.

```

00265 106* AA(66,17)=AA(91,3)*2000.*30./(16.*60.*8.33)
00266 107* IA(66,1)=0
00267 108* CALL PMPCNT
00270 109* HP=.001*AA(66,17)
00271 110* SUMHP=SUMHP+HP
00272 111* IF(TONS.GT.300.) AA(51,17)=5.0
00274 112* IF(TONS.LE.300.) AA(51,17)=2.0
00276 113* CALL SCREEN
00277 114* 2 CONTINUE
00301 115* TONSS=TONS*74
00302 116* IF(IPTION(1).EQ.2) TONSS=TONSS+(TONS*Z1*2.*Z6)
00304 117* IF(TONSS.GT.300.) GO TO 3
00306 118* NB=(TONSS/100.)*1
00307 119* AA(21,17)=100.*3.8
00310 120* GO TO 4
00311 121* 3 NB=(TONSS/250.)*1.
00312 122* AA(21,17)=250.*3.8
00313 123* 4 CONTINUE
00313 124* C
00313 125* C FISH MEAL STREAM
00313 126* C
00314 127* IF(IPTION(1).EQ.1) GO TO 52
00314 128* C PUMP FROM PRESS TO MIXFR
00316 129* AA(66,17)=AA(91,2)*2000.*30./(16.*60.*8.33)
00317 130* IA(66,1)=0
00320 131* CALL PMPCNT
00321 132* HP=.001*AA(66,17)
00322 133* SUMHP=SUMHP+HP
00323 134* AA(57,17)=(AA(91,2)+TONS*71*76*2.)*2000./62.4
00324 135* CALL BLENDR
00325 136* 52 CONTINUE
00326 137* DO 5 I=1,NB
00331 138* IA(21,5)=3
00332 139* CALL DRYERR
00333 140* 5 CONTINUE
00333 141* C PUMP TO DRYER
00335 142* AA(66,17)=TONSS*2000.*30./(16.*60.*8.33)
00336 143* IA(66,1)=0
00337 144* CALL PMPCNT
00340 145* HP=.001*AA(66,17)
00341 146* SUMHP=SUMHP+HP
00342 147* AA(81,18)=10.
00343 148* AA(81,17)=TONSS*0.33
00344 149* BULK=15.*TONSS
00345 150* TONST=(TONS*Z4*.5)+(TONS*Z4*.5*Z3)
00346 151* AA(90,18)=TONSS-TONST
00347 152* IF(IPTION(1).EQ.2) AA(90,18)=AA(90,18)+(TONS*71*Z6)
00351 153* AA(90,18)=AA(90,18)*2000./16.
00352 154* IF(IPTION(1).EQ.2) TONST=TONST+(TONS*Z1*76)
00354 155* AA(90,13)=TONS*74*.5*Z3*2000.*.01
00355 156* AA(57,17)=(AA(90,3)+AA(90,13)/2000.)*2000./62.4
00356 157* CALL BLENDR
00357 158* AA(90,3)=TONST
00357 159* C PUMP FROM DRYER TO MIXFR
00360 160* AA(66,17)=AA(90,3)*2000.*30./(24.*60.*8.33)
00361 161* CALL PMPCNT
00362 162* HP=.001*AA(66,17)

```

Table I.-- Continued.

00363	163*	SUMHP=SUMHP+HP
00364	164*	AA(40,17)=(AA(90,3)+AA(90,13)/2000.)*2000./8.33*15.
00365	165*	IA(40,1)=0
00366	166*	CALL STORAG
00366	167*	C PUMP TO CURING
00367	168*	IA(66,1)=0
00370	169*	AA(66,17)=AA(40,17)*30./(15.*16.*60.)
00371	170*	CALL PMPCNT
00372	171*	HP=.001*AA(66,17)
00373	172*	SUMHP=SUMHP+HP
00374	173*	AA(18,17)= 1.30 * TONST/16.
00375	174*	CALL HAMMER
00376	175*	AA(72,17) = 18.
00377	176*	CALL SCALE
00400	177*	IA(75,1)=0.0
00401	178*	IA(75,2)=0.0
00402	179*	AA(75,17)=AA(90,3)*20./(60.*16.)
00403	180*	CALL BAGGMA
00404	181*	AA(75,17) = AA(75,17)*60*16
00405	182*	HP=XNUM*20.
00406	183*	SUMHP=SUMHP + (.001*HP)
00407	184*	AA(54,17)=HP
00407	185*	C
00407	186*	C FISH OIL STREAM
00407	187*	C
00410	188*	AA(40,17)=AA(91,3)*2000./(16.*8.33)*1.
00411	189*	IA(40,1)=0
00412	190*	CALL STORAG
00413	191*	AA(66,17)=AA(40,17)*30./60.
00414	192*	CALL PMPCNT
00415	193*	CALL PMPCNT
00416	194*	HP=.001*AA(66,17)
00417	195*	SUMHP=SUMHP+HP
00420	196*	SUMHP=SUMHP+HP
00421	197*	DO 11 I=1,N11
00424	198*	AA(54,17)=20.
00425	199*	11 CALL CNTFGE
00427	200*	TONSA= TONSA* Z3*1.1
00430	201*	HP= .025*TONSA
00431	202*	AA(52,17)= HP
00432	203*	N1=(HP/20.) +1.
00433	204*	HP=20*N1
00434	205*	SUMHP= SUMHP+ HP
00435	206*	AA(52,17)=20.
00436	207*	DO 12 I=1,N1
00441	208*	12 CALL SHARP
00443	209*	TONSA=TONS*.0*.8*.13*2000./8.33
00444	210*	TONSA=TONSA*Z1*Z3/ (.8*.13)
00445	211*	Z7= 1.-Z3
00446	212*	IA(40,1)=2
00447	213*	AA(40,17)=TONSA*7./3.
00450	214*	AA(40,18)=1.0
00451	215*	CALL STORAG
00452	216*	IA(66,1)=0
00453	217*	AA(66,17)=TONSA*30./(3.*16.*60.)
00454	218*	SUMHP= SUMHP + (AA(66,17)*.001)
00455	219*	SUMHP= SUMHP + (AA(66,17)*.001)

## Table I.-- Continued.

00456 220\* AA(66,17)= AA(66,17)\*30.  
 00457 221\* CALL PMPCNT  
 00460 222\* CALL PMPCNT  
 00460 223\* C  
 00460 224\* C FISH OIL STORAGE (15DAYS)  
 00460 225\* C  
 00461 226\* AA(90,5)=TONS\*Z1\*Z3  
 00462 227\* AA(40,17)=AA(90,5)\*2000./R.33\*15.  
 00463 228\* IA(40,1)=0  
 00464 229\* CALL STORAG  
 00465 230\* AA(66,17)=AA(40,17)\*30./(60.\*15.\*16.)  
 00466 231\* CALL PMPCNT  
 00467 232\* HP=.001\*AA(66,17)  
 00470 233\* SUMHP=SUMHP+HP  
 00470 234\* C FISH SOLUABLES STREAM  
 00470 235\* C  
 00470 236\* C PUMP TO ACID MIX TANK  
 00471 237\* TONSSW=TONS\*71\*Z7  
 00472 238\* IA(66,1)=0  
 00473 239\* AA(66,17)=30.\*TONSSW\*2000./(8.33\*16.\*60.)  
 00474 240\* CALL PMPCNT  
 00475 241\* HP=.001\*AA(66,17)  
 00476 242\* SUMHP=SUMHP+HP  
 00477 243\* GALL=TONSSW\*.2  
 00500 244\* GAL= TONSSW\*.01  
 00501 245\* IA(40,1)=2  
 00502 246\* AA(40,17)= GAL\*2000./(8.33)  
 00503 247\* AA(40,18)=1.0  
 00504 248\* CALL STORAG  
 00505 249\* IA(40,1)=2  
 00506 250\* AA(40,18)=1.0  
 00507 251\* AA(40,17)= GALL\*2000./(8.33)  
 00510 252\* CALL STORAG  
 00511 253\* GAL=TONSSW\*2000./(8.33\*16.)  
 00512 254\* AA(66,17)=GAL\*30./60.  
 00513 255\* SUMHP= SUMHP +(AA(66,17)\*.001)  
 00514 256\* SUMHP= SUMHP +(AA(66,17)\*.001)  
 00515 257\* IA(66,1) =0  
 00516 258\* CALL PMPCNT  
 00517 259\* CALL PMPCNT  
 00520 260\* TONA=TONS\*.87\*.8\*2000.\*.001/(8.33\* 1.82)  
 00521 261\* TONA=TONS\*Z7\*Z1/(.87\*.8)  
 00522 262\* AA(90,14)= TONS\*Z7\*71\*.001  
 00523 263\* AA(40,17)= TONA\* 70.0  
 00524 264\* IA(40,1) = 1.0  
 00525 265\* IA(40,2) = 1.0  
 00526 266\* CALL STORAG  
 00527 267\* IA(40,1) = 0.0  
 00530 268\* IA(40,2) = 0.0  
 00531 269\* TONB= TONA/(16.\*60.)  
 00532 270\* AA(66,17)= 30.\*TONB  
 00533 271\* IA(66,1) = 2  
 00534 272\* CALL PMPCNT  
 00535 273\* SUMHP=SUMHP+(AA(66,17)\*.001)  
 00536 274\* IA(66,1) =0.0  
 00537 275\* TONA= TONS\*.80\*0.87\* 2000./16.  
 00540 276\* TONA=TONA\*Z1\*77/(.8\*.87)

Table I.-- Continued.

```

00541 277* AA(33,17) = TONA / 20.
00542 278* CALL EVPHOR
00543 279* CALL EVPHOR
00544 280* CALL EVPHOR
00545 281* TONC = TONA*.06/(.87*.3)
00546 282* TONC=TONC*Z6*.87/(Z7*.06)
00546 283* C PUMP TO CONCENTRATOR
00547 284* AA(66,17)=TONC*2000.*30./(8.33*60.)
00550 285* IA(66,1)=0
00551 286* CALL PMPCNT
00552 287* HP=.001*AA(66,17)
00553 288* SUMHP=SUMHP+HP
00554 289* AA(33,17)=TONC/25.
00555 290* CALL EVPHOR
00556 291* AA(90,4)=TONS*Z1*Z6*2.*1.
00557 292* AA(40,17)=AA(90,4)*2000./(8.33*16.)*1.
00560 293* IA(40,1)=0
00561 294* CALL STORAG
00562 295* AA(66,17)=30.*AA(40,17)/60.
00563 296* CALL PMPCNT
00564 297* CALL PMPCNT
00565 298* HP=.001*AA(66,17)
00566 299* SUMHP=SUMHP+HP
00567 300* SUMHP=SUMHP+HP
00570 301* IF(IPTION(1),EQ.2) GO TO 51
00570 302* C
00570 303* C CONDENSED FISH SOLUBLES STORAGE (15 DAYS)
00570 304* C
00572 305* AA(40,17)=AA(90,4)*2000./8.33*15.
00573 306* IA(40,1)=0
00574 307* CALL STORAG
00575 308* 51 CONTINUE
00575 309* C
00575 310* C SUMMATION OF STEAM, WATER, AND ELECTRICITY
00575 311* C
00576 312* AA(27,18)= 150.
00577 313* AA(27,17)= TONS*2.*2000./(3.*16.)
00577 314* C
00577 315* C BOILER WATER TREATMENT
00577 316* C
00600 317* COST(5)=1.000
00601 318* COST(1)=COST(5)
00602 319* PRINT 4242,COST(1),COST(5)
00606 320* 4242 FORMAT(/25H BOILER WATER TREATMENT , 10X ,15H ,10H
00606 321* 1 ,F10.3,30X,F10.3)
00607 322* COSTA(1)=COSTA(1)+COST(1)
00610 323* COSTA(5)=COSTA(5)+COST(5)
00610 324* C
00610 325* C FUEL OIL STORAGE
00610 326* C
00611 327* IA(40,1)=2
00612 328* AA(40,17)=TONS*6000./387.*15.
00613 329* CALL STORAG
00614 330* AA(66,17)=30.*AA(40,17)/(15.*60.)
00615 331* CALL PMPCNT
00616 332* HP=.001*AA(66,17)
00617 333* SUMHP=SUMHP+HP

```

Table I.-- Continued.

```

nn620 334*      CALL BOILER
nn621 335*      XLOOPS= 9 + NA +NB
nn622 336*      TOND=TONA/2.4 -TONC/2.4 +(TONC*.4)
nn623 337*      AA(91,5) = (TONA-TOND)/(0.6*8.33)
nn624 338*      AA(90,17)= (TONC*.4)
nn625 339*      AA(90,16)= (TONA-TONC)/2.4
nn626 340*      AA(66,17)=4*(AA(90,16) +AA(90,17)) +1.5*TONS
nn626 341*      C
nn626 342*      C SEA WATER PUMPS
nn626 343*      C
nn627 344*      IA(66,1)=1
nn630 345*      IA(66,4)=2
nn631 346*      CALL PMPCNT
nn632 347*      IA(66,1)=0
nn633 348*      IA(66,4)=0
nn634 349*      SUMHP= SUMHP + (AA(66,17))*0.001*1.5)
nn635 350*      COST(1)=XLOOPS *AA(100,1)
nn636 351*      COST(5)=COST(1)
nn637 352*      COSTA(1) = COSTA(1) + COST(1)
nn640 353*      COSTA(5)=COSTA(5) + COST(5)
nn641 354*      PRINT 1021 COST(1),COST(5)
nn645 355*      AA(8,17) = TONS
nn646 356*      CALL CONDEN
nn647 357*      COST(1)=AA(100,2)
nn650 358*      COST(5)=COST(1)
nn651 359*      COSTA(1)=COST(1) + COSTA(1)
nn652 360*      COSTA(5)=COSTA(5) + COST(5)
nn653 361*      PRINT 1022, COST(1),COST(5)
nn657 362*      AA(72,17)=18.
nn660 363*      CALL SCALE
nn661 364*      CALL SCALE
nn662 365*      PRINT 1041,(COSTA(J),J=1,6)
nn670 366*      1041 FORMAT(/25H TOTAL COSTS ,35X6F10.3)
nn671 367*      COSTA(7)=0.02*COSTA(1)
nn672 368*      IF(IPTION(1),EQ.2) AA(90,4)=0.
nn674 369*      1034 FORMAT(/ 40H TOTAL COST OF FEPC PLANT ,F16.3)
nn675 370*      PRINT 1010
nn677 371*      1010 FORMAT(1H1)
nn700 372*      HP = TONS*0.00124 +13.6
nn701 373*      SUMHP = HP + SUMHP
nn702 374*      HP = 40*TONS/3.
nn703 375*      SUMHP = HP + SUMHP
nn704 376*      AA(90,2)= SUMHP* .7457 * 16.
nn705 377*      AA(90,1)= TONS* 6000./387.
nn706 378*      AA(100,10)=COSTA(5)
nn707 379*      IXX =(16.0*(TONS/50.0)**.31) +0.5
nn710 380*      PXX =IXX
nn711 381*      AA(90,9) =PXX*10.
nn712 382*      AA(90,8) =IXX*8.0
nn712 383*      C
nn712 384*      C MATERIAL BALANCE INFORMATION PRINTOUT
nn712 385*      C
nn713 386*      CALL MATER(TONS)
nn714 387*      TONS = TONS/16
nn715 388*      AA(90,15)= TONS*2000.*.2
nn716 389*      PRINT 1060,AA(90,15)
nn721 390*      1060 FORMAT(/8X26H COOKERS STFAM ,F8.0,7H LB/HR )

```

Table I.--Continued.

nn722	391*	AA(91,3)= AA(91,3)* 2000./16.	
nn723	392*	AA(91,2)= AA(91,2)* 2000./16.	
nn724	393*	PRINT 1061,AA(91,3)	
nn727	394*	PRINT 1062,AA(91,2)	
nn732	395*	1061 FORMAT(/8X26H PRESS LIQUOR	,F8.0,7H LB/HR )
nn733	396*	1062 FORMAT(/8X26H PRESS CAKE	,F8.0,7H LB/HR )
nn734	397*	AA(91,1)= AA(91,3)*77	
nn735	398*	PRINT 1063,AA(91,1)	
nn740	399*	1063 FORMAT(/8X26H STICK WATER	,F8.0,7H LB/HR )
nn741	400*	AA(90,5) = AA(90,5)*2000.0/16	
nn742	401*	PRINT 1064, AA(90,5)	
nn745	402*	1064 FORMAT(/8X26H FISH OIL	,F8.0,7H LB/HR )
nn746	403*	PRINT 1065,AA(90,16)	,
nn751	404*	1065 FORMAT(/8X26H TRIPLE EVAP. STEAM	,F8.0,7H LB/HR )
nn752	405*	AA(91,4)= 0.15*BB(31)*.01*TONS*2000.0/0.30	
nn753	406*	PRINT 1066 ,AA(91,4)	
nn756	407*	1066 FORMAT(/8X26H TRIPLE EVAP. CONCENTRATE	,F8.0,7H LB/HR )
nn757	408*	AA(91,5)=AA(90,16)*4.0	
nn760	409*	PRINT 1067 ,AA(91,5)	
nn763	410*	1067 FORMAT(/8X26H TRIPLE EVAP. COOLING	,F8.0,7H GAL/HR )
nn764	411*	PRINT 1068,AA(90,17)	
nn767	412*	1068 FORMAT(/8X26H CONCENTRATOR EVAP. STEAM	,F8.0,7H LB/HR )
nn770	413*	AA(91,6) =AA(90,17)*4.0	
nn771	414*	PRINT 1069,AA(91,6)	
nn774	415*	1069 FORMAT(/8X26H CONC. COOLING WATER	,F8.0,7H GAL/HR )
nn775	416*	SOL =AA(90,4)*2000.0/16	
nn776	417*	PRINT 1070,SOL	
01001	418*	1070 FORMAT(/8X26H FISH SOLUBLES	,F8.0,7H LB/HR )
01002	419*	AA(90,18)=AA(90,18)/16	
01003	420*	PRINT 1071,AA(90,18)	
01006	421*	1071 FORMAT(/8X26H DRYFR STEAM	,F8.0,7H LB/HR )
01007	422*	SCRUB=180*TONS	
01010	423*	PRINT 1072,SCRUB	
01013	424*	1072 FORMAT(/8X26H SCRUBBER WATER	,F8.0,7H GAL/HR )
01014	425*	STM=AA(27,17)-AA(90,18)-AA(90,17)-AA(90,16)	
01015	426*	PRINT 1074,STM	
01020	427*	1074 FORMAT(/8X26H MISCELLANEOUS STEAM	,F8.0,7H LB/HR )
01021	428*	FISH =AA(90,3)*2000.0/16	
01022	429*	PRINT 1073,FISH	
01025	430*	1073 FORMAT(/8X26H FISH MFAL	,F8.0,7H LB/HR )
01026	431*	TONS = TONS*16	
01027	432*	AA(90,5) = AA(90,5)*16.0/2000.0	
01030	433*	AA(91,2)= AA(91,2)*16./2000.	
01031	434*	AA(91,3)= AA(91,3)*16./2000.	
01032	435*	AA(90,13) = AA(90,13) + (AA(90,3)+AA(90,7)+AA(90,20)+AA(90,4))	
01033	436*	AA(90,14)=AA(90,14)*2000.	
01034	437*	RETURN	
01035	438*	END	

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S PRSIPA,PRSIPA  
 FOR S9A-07/12-11:03 (1,)

SUBROUTINE PRSIPA ENTRY POINT 003537

STORAGE USED: CODE(1) 003617; DATA(0) 001410; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK2 000016  
 0004 DATA1 000050  
 0005 BLOCK1 005050  
 0006 BLOCK4 000012

EXTERNAL REFERENCES (BLOCK, NAME)

0007 PMPREC  
 0010 BELT  
 0011 SCALE  
 0012 STORAG  
 0013 REFRIG  
 0014 SILO  
 0015 BUCKET  
 0016 DRYERR  
 0017 SCREWR  
 0020 SCREEN  
 0021 PMPCNT  
 0022 GRINDR  
 0023 REACTR  
 0024 AGITOR  
 0025 HEATEX  
 0026 COLUMN  
 0027 VESSEL  
 0030 CNTFGE  
 0031 SHARP  
 0032 EVPHOR  
 0033 HAMMER  
 0034 BAGGMA  
 0035 ROILER  
 0036 CONDEN  
 0037 MATER  
 0040 SQRT  
 0041 NPRT\$  
 0042 NI02\$  
 0043 NI01\$  
 0044 NEXP6\$  
 0045 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000453	1003F	0000	000364	1021F	0000	000375	1022F	0000	000443	1041F	0001	000020	1136
0000	000464	1201F	0000	000476	1202F	0000	000510	1203F	0000	000522	1204F	0001	003005	1204G
0000	000534	1205F	0000	000546	1206F	0000	000560	1207F	0000	000572	1208F	0000	000617	1209F

Table I.--Continued.

0001	000025	121G	0000	0006n4	1210F	0000	000632	1211F	0000	000644	1212F	0000	000656	1213F
0000	000674	1214F	0000	0007n5	1215F	0000	000716	1216F	0000	000727	1217F	0000	000740	1218F
0000	000751	1219F	0000	0007n2	1220F	0000	000773	1221F	0000	001004	1222F	0000	001015	1223F
0000	001026	1224F	0000	001040	1225F	0000	001052	1226F	0000	001064	1227F	0000	001076	1228F
0000	001110	1230F	0000	001122	1231F	0000	001134	1232F	0000	001146	1233F	0001	000032	127G
0001	003210	1330G	0001	003221	1336G	0001	003232	1344G	0001	003243	1352G	0001	003254	1360G
0001	003265	1366G	0001	003276	1374G	0001	003307	1402G	0001	003320	1410G	0001	003331	1416G
0001	000144	163G	0001	0003u1	237G	0000	000340	3000F	0000	000352	3006F	0001	0006n5	323G
0001	000671	345G	0001	0007n2	350G	0001	000734	361G	0001	000735	364G	0001	000755	372G
0001	000760	377G	0000	0004n7	4242F	0000	000425	4243F	0001	001145	433G	0001	002574	44L
0001	001226	450G	0001	002574	49L	0001	001336	507G	0001	002273	51L	0001	001400	516G
0001	002417	52L	0001	002137	716G	0001	002206	734G	0005 R	000000	AA	0000 R	000240	ABC
0000 R	000245	ACID	0005 R	0047n4	BB	0003 R	000000	COST	0003 R	000007	COSTA	0004 R	000000	DATB
0000 R	000172	DAYS	0000 R	000173	DAYSr	0000 R	000273	DAZOIL	0000 R	000201	DENS	0000 R	000216	DRYSLD
0000 R	000241	DX	0000 R	0002n3	FACT10	0000 R	000310	FISH	0000 R	000211	G	0000 R	000246	GAL
0000 R	000206	GALLON	0000 R	0002n7	GALS	0000 R	000272	HOTH20	0000 R	000171	HOUR	0000 R	000212	HP
0000 R	000276	HWAT	0000 I	000167	I	0005 I	003720	IA	0000	001346	INJPS	0000 I	000234	IP
0006 I	000000	IPTION	0000 I	000230	IR	0000 I	000231	rRR	0000 I	000235	IU	0000 I	000337	IXX
0000 I	000224	J	0000 I	000325	K	0000 I	000176	LOOPS	0000 R	000166	MATRL	0000 I	000214	NA
0000 I	000204	NOREAC	0000 I	000225	NQUIP	0000 I	000210	NUM	0000 I	000223	NUMZ	0000 I	000242	NUTH
0000 I	000302	NZ	0000 I	000271	N2	0000 I	000266	N3	0000 R	000265	OIL	0000 R	000262	PRDCTA
0000 R	000263	PRDCTB	0000 R	000247	SAA	0000 R	000267	SAB	0000 R	000244	SACID	0000 R	000233	SAG
0000 R	000300	SAQT	0000 R	000161	SBOT	0000 R	000255	SBOTT	0000 R	000275	SBQGT	0000 R	000274	SBQT
0000 R	000270	SCB	0000 R	000175	SOLLTO	0000 R	000177	STFAM	0000 R	000256	STEAMR	0000 R	000200	STEAMW
0000 R	000250	STEAM1	0000 R	000261	STFAM2	0000 R	000252	STFAM3	0000 R	000253	STEAM4	0000 R	000306	STEAM6
0000 R	000254	STEAM9	0000 R	000000	STM	0000 R	000143	STMM	0000 R	000154	STOP	0000 R	000055	STRM
0000 R	000132	STRMM	0000 R	000170	SUMHP	0000 R	000232	TANK	0000 R	000257	TANKA	0000 R	0003n1	TASA
0000 R	000303	TASB	0000 R	0003n4	TASC	0000 R	000305	TASD	0000 R	000277	TONA	0000 R	0002n5	TONSA
0000 R	000213	TONSG	0000 R	000222	TONSX	0000 R	000226	VES	0000 R	000227	VESS	0000 R	000261	WASTE
0000 R	000174	WATAD	0000 R	000264	WATER	0000 R	000202	WATOIL	0000 R	000260	WIDTH	0000 R	000236	XIP
0000 R	000237	XIR	0000 R	000243	XIRR	0000 R	000217	XLIQD	0000 R	000307	XLOOPS	0000 R	000215	XNA
0000 R	000220	XOIL	0000 R	000221	XSQL	0000 R	000326	XXA	0000 R	000327	XXB	0000 R	000330	XXC
0000 R	000331	XXD	0000 R	000332	XXE	0000 R	000333	XXG	0000 R	000334	XXH	0000 R	000335	XXI
0000 R	000336	XXJ	0000 R	000311	YYA	0000 R	000312	YYB	0000 R	000313	YYC	0000 R	000314	YYD
0000 R	000315	YYE	0000 R	000316	YYG	0000 R	000317	YYH	0000 R	000320	YYI	0000 R	000321	YYJ
0000 R	000322	YYK	0000 R	000323	YYL	0000 R	000324	YYM						

```

00101 1* SUBROUTINE PRSIPA(TONS)
00103 2* COMMON/BLOCK2/ COST(7),COSTA(7)
00104 3* COMMON/ DATA1 / DATR(8,5)
00105 4* COMMON/BLOCK1/ AA(100,20),IA(100,5),BR(100)
00106 5* COMMON/BLOCK4/ IPTION(10)
00107 6* DIMENSION STM(5,0),STRM(5,9),STRMM(9),STMM(9)
00110 7* DIMENSION STOP(5),SBOT(5)
00111 8* REAL MATR1
00111 9* C
00111 10* C NORMALIZATION
00111 11* C
00112 12* DO 1 I=1,7
00115 13* COST(I)=0.
00116 14* 1 COSTA(I)=0.
00120 15* DO 2 I=1,20
00123 16* AA(90,I)=0.
00124 17* 2 AA(91,I)=0.

```

Table I.-- Continued.

```

00126 18* DO 10 I =30,33
00131 19* 10 BB(I)= BB(I)* 0.01
00133 20* SUMHP= 0.
00134 21* HOUR= 24.
00135 22* DAYS= 30.
00136 23* AA(72,17)=18.
00137 24* DAYSR = 3.
00140 25* WATAU = 0.2
00141 26* SOLLIQ= 2.5
00141 27* C STEAMW IS THE STEAM REQUIRED FOR THE WET DEBONING OPTION
00142 28* LOOPS=0
00143 29* STEAM=0.
00144 30* STEAMW = 0.
00145 31* DENS = 0.9
00146 32* WATOIL=2.
00147 33* FACT10=1.
00150 34* NOREAC= IPTION(5)
00151 35* IF(NOREAC.EQ.0) NOREAC = 4
00151 36* C
00151 37* C UNLOADING AND STORAGE OF FISH
00151 38* C
00153 39* TONSA = TONS* 2000./8.33
00154 40* GALLON= TONSA / (HOUR* 60.)
00155 41* GALS = GALLON * 1.3
00156 42* IA(65,1) = 0.
00157 43* IA(65,2) = 1.0
00160 44* AA(65,17)= GALS * 30.
00161 45* NUM =(TONS/500.) + 1
00162 46* DO 143 I=1,NUM
00165 47* SUMHP= SUMHP +(2.*AA(65,17)*.0015)
00166 48* 143 CALL PMPREC
00170 49* IA(65,2) = 0.
00171 50* IF (TONSA.LT.30000.) G = 30000./(24.*60.) * 15.
00173 51* IF (TONSA.GE.30000.) G = 450000./(24.*60.) * 15.
00175 52* IF (TONS.LE.150.) AA(70,18) = 36.
00177 53* IF (TONS.GT.150.) AA(70,18) = 48.
00201 54* AA(70,17)= 100.
00202 55* CALL BELT
00203 56* CALL SCALE
00204 57* HP=(TONS * 0.00124 ) + 13.6
00205 58* SUMHP = HP + SUMHP
00206 59* AA(40,17) = DAYS * TONS
00207 60* IA(40,1) = 0.
00210 61* IA(40,2) = 2
00211 62* CALL STORAG
00212 63* IA(40,2) = 0
00213 64* AA(85,17) = 0.5* TONS * DAYSR
00214 65* IA(85,1) = 30
00215 66* CALL REFRIG
00216 67* SUMHP= SUMHP +(4.72*AA(85,17))
00217 68* IA(7,1) = 1
00220 69* AA(7,17) = 27.4* TONS
00221 70* CALL SILO
00222 71* TONSG = TONS/24.
00223 72* AA(71,18) = TONSG
00224 73* AA(71,17) = 20.
00225 74* CALL BUCKET

```

Table I.--Continued.

00226 75\* HP= TONS \* 0.00106  
 00227 76\* SUMHP = HP + SUMHP  
 00227 77\* C  
 00227 78\* C FISH COOKERS AND SCREW PRESS  
 00227 79\* C  
 00230 80\* AA(91,16) = WATAD\* TONS  
 00231 81\* AA(91,10) = TONS + AA(91,16)  
 00232 82\* IF(TONS.GT.450) NA= (TONS/250.)+ 1.  
 00234 83\* IF(TONS.LE.450) NA= (TONS/100.)+ 1.  
 00236 84\* DO 3 I=1,NA  
 00241 85\* BB(2)=2.1  
 00242 86\* XNA=NA  
 00243 87\* IA(21,5) = 4  
 00244 88\* AA(21,17)= TONS/XNA  
 00245 89\* CALL DRYERR 6  
 00246 90\* IA(17,5) = 3  
 00247 91\* BB(2)=2.6  
 00250 92\* IF(TONS.GT.450.) AA(17,17)= 21.  
 00252 93\* IF(TONS.GT.450.) AA(17,18)= 16.  
 00254 94\* IF(TONS.LE.450.) AA(17,18)= 12.  
 00256 95\* IF(TONS.LE.450.) AA(17,17)= 15.  
 00260 96\* CALL SCREW R 7  
 00261 97\* IF(TONS.GT.450) AA(51,17)= 10.  
 00263 98\* IF(TONS.LE.450) AA(51,17)= 4.  
 00265 99\* CALL SCREEN 9  
 00266 100\* 3 CONTINUE  
 00270 101\* DRYSLD=(BB(32)+0.85\*BB(31))\*TONS  
 00271 102\* XLIQD= (BB(31)\*0.15+ BB(30)+ RB(33))\* TONS +AA(91,16)  
 00272 103\* XOIL= BB(30) \* TONS/XLIQD  
 00273 104\* XSOL= BB(31) \* 0.15\* TONS/XLIQD  
 00274 105\* AA(90,16)= DRYSLD \* SOLLIQ  
 00275 106\* AA(90,18)=AA(91,10)-AA(90,16)  
 00275 107\* C  
 00275 108\* C SOLIDS STREAM = AA(90,16)  
 00275 109\* C  
 00276 110\* TONSX=TONS  
 00277 111\* TONS=AA(90,16)\*FACT10  
 00300 112\* TONSG = AA(90,16) / HOUR  
 00301 113\* AA(7,17) = 50.0\* AA(90,16) / (62.4\*DENS) \* 2000.  
 00302 114\* IA(7,1) = 1  
 00303 115\* CALL SILO 11  
 00304 116\* AA(66,17) = AA(90,16)\*2000./ (HOUR\*8.33\*60.) \* 25.  
 00305 117\* CALL PMPCNT 10  
 00306 118\* HP= AA(66,17)/25.  
 00307 119\* SUMHP = HP+ SUMHP  
 00310 120\* CALL PMPCNT 11  
 00311 121\* SUMHP= HP + SUMHP  
 00312 122\* IF (TONSG .GT.6) AA(50,17)= 6.  
 00314 123\* IF (TONSG .GT.6) NUMZ = (TONSG/6.) + 1.  
 00316 124\* IF (TONSG .LE.6) AA(50,17)= 3.  
 00320 125\* IF (TONSG .LE.6) NUMZ = (TONSG/3.) + 1.  
 00322 126\* DO 720 J= 1,NUMZ  
 00325 127\* 720 CALL GRINDR  
 00327 128\* HP= 40.\* TONSG/3.  
 00330 129\* SUMHP= HP + SUMHP  
 00330 130\* C  
 00330 131\* C EXTRACTION VESSELS MATERIAL BALANCE

## Table I.-- Continued.

```

00330 132* C 1-OIL 2-PROTEIN 3-ACA 4-WATER 5-IPA NOREAC=NUMBER OF REACTORS
00330 133* C
00331 134*          NQUIP= NOREAC + 1
00332 135*          STM(1,1) = (SOLLIO-1.)*DRYSLD*XOIL
00333 136*          STM(3,1)=DRYSLD*BR(32)/(RR(32) + (0.85*BB(31)))
00334 137*          STM(2,1)=(DRYSLD-STM(3,1)) + ((SOLLIO-1.)*DRYSLD*XSOI)
00335 138*          STM(4,1) = (SOLLIO-1.)*DRYSLD*(1.- XSOI-XOIL)
00336 139*          STM(5,1) = 0.0
00337 140*          STRM(1,NQUIP)=0.
00340 141*          STRM(2,NQUIP)=0.
00341 142*          STRM(3,NQUIP)=0.
00342 143*          STRM(4,NQUIP) = WATNOL*2.804*AA(90,16)/22.264
00343 144*          STRM(5,NQUIP) = STRM(4,NQUIP)*19.46/2.804
00344 145*          DO 121 I=1,NOREAC
00347 146*          DO 121 J=1,5
00352 147*          STM(J,I+1)= STM(J,I)*DATB(I,J)
00353 148*          IF(I.EQ.1.AND.J.FQ.5) STM(5,2)= STM(4,1)*DATB(1,5)
00355 149*          121 CONTINUE
00360 150*          DO 122 I=NOREAC,1,-1
00363 151*          DO 122 J=1,5
00366 152*          122 STRM(J,I) = STRM(J,I+1)+STM(J,I)
00371 153*          DO 123 I=1,NQUIP
00374 154*          STMM(I)=0.
00375 155*          STRMM(I)=0.
00376 156*          DO 123 J=1,5
00401 157*          STMM(I)=STMM(I) + STM(J,I)
00402 158*          STRMM(I)= STRMM(I) + STRM(J,I)
00403 159*          123 CONTINUE
00403 160* C
00403 161* C REACTOR VESSELS
00403 162* C
00406 163*          VES= TONS* 30.
00407 164*          AA(49,17) = VES
00410 165*          VESS = TONS* 16.
00411 166*          IR= 1
00412 167*          IF(VES.GT.10000.) IR= (VES/10000.) + 1.
00414 168*          IF(VESS.GT.10000.) VES = 10000.
00416 169*          IRR=1
00417 170*          IF(VESS.GT.10000.) IRR=(VESS/10000.) + 1.
00421 171*          TANK = 800.* TONS / 50.
00422 172*          AA(40,18)=3.2
00423 173*          AA(41,18)=3.2
00424 174*          AA(40,17)= TANK
00425 175*          CALL STORAG
00426 176*          SAG= STRMM(2) * 2000./(24.*8.33*60.) *(24./HOUR)
00427 177*          IP=1
00430 178*          IF(SAG.GT.1250.) IP=(SAG/1250.) + 1.
00432 179*          DO 93 IU=1,IP
00435 180*          XIP=IP
00436 181*          AA(66,17) =(SAG/XIP) * 24.
00437 182*          CALL PMPCNT
00440 183*          93 CONTINUE
00442 184*          IF (VESS.GT.10000.) VESS = 10000.
00442 185* C MISCELLA TANK
00444 186*          XIP=IR
00445 187*          IP=(TONS*60./(50.*144.*XIP)) + 2.
00446 188*          AA(51,17) = IP

```

Table I.--Continued.

```

00447 189*      DO 41 I = 1,TR
00452 190*      LOOPS= LOOPS + 3
00453 191*      AA(49,17) = VFS
00454 192*      CALL REACTR
00455 193*      CALL SCREEN
00456 194*      AA(73,17) = 0.005* VFS
00457 195*      IF(AA(73,17).LT.2.) AA(73,17)=2.
00461 196*      IA(73,5) = 2.
00462 197*      CALL AGITOR
00463 198*      SUMHP = SUMHP + 2.5
00464 199*      XIR=IR
00465 200*      SUMHP= SUMHP+ AA(73,17)
00466 201*      AA(66,17)= TONS* 2000./(HOUR*8.33*XIR) * (22./60.)
00467 202*      CALL PMPCNT
00470 203*      ABC= AA(66,17)/22.
00471 204*      IF(ABC.LE.2.) HP= 2.
00473 205*      IF(ABC.GT.2.) HP= ABC
00475 206*      SUMHP= HP + SUMHP
00476 207*      IA(17,5) = 5
00477 208*      DX= SQRT(TONS/50.) * 8. /SQRT(XIP)
00500 209*      AA(17,17) = 6
00501 210*      AA(17,18) = DX
00502 211*      CALL      SCREWR
00503 212*      41 CONTINUE
00505 213*      NUTH=NOREAC - 1
00505 214*      C
00505 215*      C OTHER REACTION VFSSELS
00505 216*      C
00506 217*      DO 42 J = 1,IRR
00511 218*      XIP=IRR
00512 219*      IP=(TONS*60./(50.*XIP*144.)) + 2.
00513 220*      AA(51,17)=IP
00514 221*      LOOPS= LOOPS + (3*NUTH)
00515 222*      DO 42 I = 1,3
00520 223*      XIRR=IRR
00521 224*      SUMHP=SUMHP + 2.5
00522 225*      AA(66,17)= TONS*2000./(24.*8.33*XIRR)*(22./60.)
00523 226*      CALL PMPCNT
00524 227*      ABC= AA(66,17)/ 22.
00525 228*      IF(ABC.GT.2.) HP=ABC
00527 229*      IF(ABC.LE.2.) HP=2.
00531 230*      SUMHP= SUMHP + HP
00532 231*      AA(49,17)= VESS
00533 232*      CALL REACTR
00534 233*      CALL SCREEN
00535 234*      AA(73,17)= 0.005*VESS
00536 235*      IF(AA(73,17).LT.2.) AA(73,17)= 2.
00540 236*      IA(73,5) = 2
00541 237*      SUMHP = SUMHP + AA(73,17)
00542 238*      CALL AGITOR
00543 239*      DX= SQRT(TONS/50) * 8. / SQRT(XIP)
00544 240*      AA(17,18)= DX
00545 241*      AA(17,17)= 6.
00546 242*      IA(17,5)= 5
00547 243*      CALL SCREWR
00550 244*      42 CONTINUE
00553 245*      TONS=TONSX

```

Table I.--Continued.

```

nn553 246* C
nn553 247* C MIXING TANK SECTION
nn553 248* C
nn554 249* SACID= STRMM(1)*.n01*70.
nn555 250* IA(40,1)= 1
nn556 251* IA(40,2)= 1
nn557 252* AA(40,17) = SACID
nn560 253* CALL STORAG
nn560 254* C ACID STORAGE TANK
nn561 255* IA(40,2) = n
nn562 256* LOOPS=LOOPS+ 2
nn563 257* ACID = STRMM(1) *.0n1
nn564 258* IA(66,1) = 2
nn565 259* AA(66,17)= 30.*ACTD* 200n./ (8.33*60.*HOUR*1.8)
nn566 260* CALL PMPCNT
nn566 261* C PUMP FROM ACID STORAGE TO MIX TANK
nn567 262* GAL=STRMM(1)* 200n./ (8.33 )
nn570 263* SUMHP= SUMHP + (.n015*AA(66,17))
nn571 264* AA(40,17) = GAL * .n1
nn572 265* AA(66,17) = GAL *30./ (HOUR*60.)
nn573 266* IA(66,1) = n
nn574 267* IA(40,1) = 2
nn575 268* SUMHP= SUMHP + (AA(66,17)*.0015)
nn576 269* CALL PMPCNT
nn576 270* C PUMP FROM PRESS TO ACID MIX TANK
nn577 271* CALL STORAG
nn577 272* C ACID MIX TANK
nn600 273* CALL PMPCNT
nn600 274* C PUMP FROM ACID MIX TANK TO MISCELLA TANK
nn600 275* C
nn600 276* C MISCELLA TANK BEFORE PREHEATER ( 1 HOUR HOLDUP)
nn600 277* C
nn601 278* SAA= 1.001* STRMM(1)
nn602 279* AA(40,17)= SAA*200n./ (HOUR*8.33)
nn603 280* IA(40,1) = 1
nn604 281* CALL STORAG
nn605 282* AA(66,17) = 30. * AA(40,17)
nn606 283* IA(66,1) = n
nn607 284* CALL PMPCNT
nn610 285* SUMHP = SUMHP + (.n015*AA(66,17))
nn611 286* PRINT 3000
nn613 287* 3000 FORMAT(/50H STORAGE TANK BEFORE PREHEATER
nn613 288* C
nn613 289* C STEAM REQUIREMENTS
nn613 290* C
nn614 291* STEAM1 = AA(90,16)*FACT1n*35./50.
nn615 292* STEAM2 = AA(90,16)*FACT1n*20./50.
nn616 293* STEAM3 = AA(90,16)*FACT1n*20./50.
nn617 294* STEAM4 = AA(90,16)*FACT1n*20./50.
nn620 295* STEAM = STEAM1+STEAM2+STEAM3+STEAM4
nn620 296* C PREHEATER FOR DISTILLATION COLUMN
nn621 297* STEAM9= STRMM(1)*1.n01 * 200n./HOUR * .1
nn622 298* STEAM= STEAM + STEAM9
nn623 299* AA(67,17) = STEAM9 * .1
nn624 300* CALL HEATEX
nn624 301* C
nn624 302* C DISTILLATION COLUMN - MATERIAL BALANCE

```

Table I.--Continued.

```

00624 303* C
00625 304* STOP(1) = STRM(5,1) * .99887
00626 305* STOP(2) = STOP(1) * .1445
00627 306* SBOT(1) = STRM(5,1) * .00113
00630 307* SBOT(2) = STRM(4,1) - STOP(2)
00631 308* SBOT(3) = STRM(1,1) + STRM(1,2) + STRM(1,3) + (.001*STRMM(1))
00632 309* SBOTT = SBOT(1) + SBOT(2) + SBOT(3)
00632 310* C
00632 311* C DISTILLATION COLUMN
00632 312* C REBOILER
00632 313* C
00633 314* STEAMR=AA(90,16) * FACT10*10709./50.
00634 315* AA(67,17) = .1* STEAMR
00635 316* CALL HEATEX
00636 317* STEAM= STEAM + STEAMR
00637 318* TANKA= FACT10* AA(90,16)* 100./50.
00637 319* C TANK ASSOCIATED WITH DISTILLATION COLUMN
00640 320* IA(40,1) = 1
00641 321* AA(40,17) = TANKA
00642 322* CALL STORAG
00643 323* WIDTH= 4.* SQRT(AA(90,16)*FACT10/75.)
00644 324* I= WIDTH/2.
00645 325* WIDTH= 2*I
00646 326* IF(WIDTH.LT.4.001) WIDTH = 4.
00650 327* AA(43,18) = 24.
00650 328* C AA(43,18) = THE TRAY SPACING IN INCHES
00651 329* AA(43,20) = WIDTH
00652 330* AA(43,17) = 54.
00652 331* C AA(43,17) = THE COLUMN HEIGHT IN FEET
00653 332* AA(43,1) = .4
00654 333* CALL COLUMN
00655 334* IA(42,4)=2
00656 335* IA(42,2)=1
00657 336* IA(42,3)=1
00660 337* AA(42,18)=WIDTH
00661 338* AA(42,19)=54.
00662 339* CALL VESSEL
00663 340* LOOPS = LOOPS+5
00664 341* WASTE = (.00113*STRM(5,1)) + (.0001*(PRDCTA+PRDCTB))
00665 342* AA(40,17) = WASTE* 2000./ 8.33 * DAYSR
00666 343* IA(40,1) = 0
00667 344* CALL STORAG
00670 345* LOOPS = LOOPS + 1
00670 346* C IPA STORAGE TANK(MAKEUP IPA)
00670 347* C CONDENSER FOR DISTILLATION COLUMN
00671 348* WATER = 669.* FACT10* AA(90,16)/ 50.
00672 349* AA(67,17) = WATER* 8.33 * 60. * .01
00673 350* CALL HEATEX
00674 351* AA(66,17) = 105. * (AA(90,16)*FACT10/75.) * 20.
00675 352* CALL PMPCNT
00676 353* HP= 2.* (AA(90,16)* FACT10/75.)
00677 354* SUMHP = HP + SUMHP
00677 355* C CENTRIFUGE SECTION
00700 356* MATRL = SBOTT + AA(90,18)
00701 357* OIL = STRM(1,1) + (AA(90,18)*XOIL)
00702 358* AA(40,17) = MATRL* 2000. / (HOUR*8.33)
00703 359* IA(40,1) = 1

```

Table I.-- Continued.

```

00704 360*      CALL STORAG
00705 361*      AA(66,17) = 30.* AA(40,17)
00706 362*      IA(66,1) = 0
00707 363*      CALL PMPCNT
00710 364*      SUMHP= SUMHP + 0.0015*AA(66,17)
00710 365*      C  NUMBER OF CENTRIFUGES
00711 366*      HP = MATRL*0.01* 2000./(HOUR*8.33)
00712 367*      N3 = (HP/20.) + 1.
00713 368*      HP = 20* N3
00714 369*      SUMHP = SUMHP + HP
00715 370*      DO 47  I =1,N3
00720 371*      AA(54,17) = 20.
00721 372*      CALL CNTFGE
00722 373*      47  CONTINUE
00724 374*      LOOPS = LOOPS + N3
00725 375*      SAB= OIL * 1.1
00726 376*      SCB= MATRL - OIL
00726 377*      C  SECOND CENTRIFUGE
00727 378*      HP= SAB *0.025* 2000./(HOUR*24.)
00730 379*      N2= (HP/20.) + 1.
00731 380*      HP= N2* 20
00732 381*      SUMHP= SUMHP + HP
00733 382*      DO 46 I=1,N2
00736 383*      AA(52,17) =20.
00737 384*      CALL SHARP
00740 385*      46  CONTINUE
00742 386*      HOTH20 = 0.1 * OI1
00742 387*      C  OIL STORAGE
00743 388*      DAZOIL=15.
00744 389*      AA(40,17) =DAZOIL*OIL*2000./8.33
00745 390*      IA(40,1) = 0
00746 391*      CALL STORAG
00747 392*      AA(66,17)=AA(40,17)*30./(60.*HOUR*DAZOIL)
00750 393*      IA(66,1)=0.
00751 394*      CALL PMPCNT
00752 395*      CALL PMPCNT
00753 396*      SUMHP=SUMHP + (2.*AA(66,17)*.001)
00753 397*      C
00753 398*      C  DISSOLVED SOLIDS STREAM
00753 399*      C
00754 400*      SBQT = SCB
00755 401*      SBQQT= (STRM(2,1)+(XLIQD*X SOL)) * 2.
00756 402*      HWAT= SBQT - SBQQT
00757 403*      IF(HWAT.GE.0.) GO TO 51
00761 404*      PRINT 3006
00763 405*      3006  FORMAT(/50H FISH SOLIDABLES ARE MORE THAN 50 PERCENT PROTEIN  )
00764 406*      AA(90,4) = SBQT
00765 407*      GO TO 52
00766 408*      51  CONTINUE
00767 409*      AA(90,4) = SBQQT
00770 410*      TONA=SBQQT/HOUR*2000.
00771 411*      AA(33,17) = TONA/ 20.
00772 412*      CALL EVPHOR
00773 413*      CALL EVPHOR
00774 414*      CALL EVPHOR
00775 415*      SAQT = STRM(2,1)/0.3
00776 416*      IF(SAQT.GE.SBQT) SAQT = SBQT

```

Table I.-- Continued.

```

01000 417* AA(33,17) = SAQT * 2000. / (HOUR* 25.)
01001 418* STEAM = STEAM + (HWAT * 2000./HOUR)
01002 419* CALL EVPHOR
01003 420* IA(66,1)=0.
01004 421* AA(66,17)=3n.*SRQQT *2000./(10.*6n.*HOUR)
01005 422* CALL PMPCNT
01006 423* HP=.001*AA(66,17)
01007 424* SUMHP=SUMHP + HP
01007 425* C
01007 426* C ACID MIX TANK
01007 427* C
01010 428* AA(40,17)=SRQQT *2000./(10.*1.)*.01
01011 429* IA(40,1)=2
01012 430* CALL STORAG
01013 431* IA(40,1)=0
01013 432* C
01013 433* C STORAGE OF FISH SOLUBLES(15 DAYS)
01013 434* C
01014 435* IA(66,1)=0
01015 436* AA(66,17)=3n.*AA(40,17)/(60.*HOUR)
01016 437* CALL PMPCNT
01017 438* HP=.001*AA(66,17)
01020 439* SUMHP=SUMHP + HP
01021 440* IA(40,1)=2
01022 441* AA(40,17)=SRQQT *2000./10. *15.
01023 442* CALL STORAG
01024 443* IA(40,1)=0.
01025 444* 52 CONTINUE
01025 445* C
01025 446* C ACID TANK AND FISH SOLUBLES STORAGE
01025 447* C
01025 448* C
01025 449* C DRYING AND CONDITIONING OPERATION(SOLIDS FROM EXTRACTION VESSELS)
01025 450* C
01026 451* TASA= STMM(NOREAC+1)/2.
01027 452* NZ= NOREAC + 1
01030 453* TASB= STM(1,NZ) + STM(2,NZ) + STM(3,NZ) +(0.05*STM(4,NZ))
01030 454* 1 + (STM(5,NZ)*1.E-04 * 1.0 )
01031 455* TASC= STM(4,NZ) * .05
01032 456* TASD= STM(5,NZ) * .0999
01033 457* STEAM6 = (TASC + (1.0 * TASD)) * 2000. / HOUR
01034 458* STEAM= STEAM + STEAM6
01034 459* C DRYER - CONDITIONER
01035 460* AA(21,17) = 3.8* 16.* TASA/ 24.
01036 461* IA(21,5) = 6.
01037 462* BB(2) = 0.9
01040 463* CALL DRYERR
01041 464* BB(2) = 1.0 D
01042 465* IA(21,5) = 7
01043 466* CALL DRYERR
01044 467* BB(2) = 1.0 SD
01045 468* IA(21,5) = 7
01046 469* CALL DRYERR
01047 470* IA(21,5) = 8 SD
01050 471* BB(2) = 1.0 C
01051 472* CALL DRYERR
01052 473* LOOPS = L00PS + 4

```

## Table I.-- Continued.

```

01053 474*      AA(17,18) = 6.
01054 475*      AA(17,17) = 20.
01055 476*      IA(17,5) = 1
01056 477*      CALL SCREWR
01056 478* C   CONVEYER FOR MILL
01057 479*      IF(IPTION(2),F0.3) GO TO 44
01061 480*      AA(18,17) = (TASB/8.)
01062 481*      CALL HAMMER
01063 482*      HP = TASB * 2000.* 75./(HOUR*700.)
01064 483*      SUMHP = SUMHP + HP
01065 484*      PRDCTA= STM(2,NOREAC+1)          + STM(3,NOREAC+1)
01066 485*      PRDCTA=PRDCTA/0.95
01067 486*      PRDCTB= 0.
01070 487*      AA(75,17) = PRDCTA * 2000./(25. * HOUR * 60.)
01071 488*      CALL BAGGMA
01072 489*      CALL SCALE
01073 490*      AA(75,17) = AA(75,17) * HOUR * 60.
01074 491*      GO TO 49
01075 492*      44 CONTINUE
01075 493*      C
01075 494*      C AT THE TIME THIS CODE WAS COMPILED THERE IS NO SATISFACTORY METHOD
01075 495*      C OF SEPARATING ASH AND DRY PROTEIN- SPACE IS PROVIDED WHEN THIS
01075 496*      C TECHNOLOGY BECOMES AVAILABLE
01075 497*      C
01076 498*      49 CONTINUE
01076 499*      C
01077 500*      AA(27,18) =150.
01100 501*      AA(27,17)=STEAM
01101 502*      CALL BOILER
01102 503*      IA(40,1)=2
01103 504*      AA(40,17)=STEAM*1000.*HOUR/(8.33*140000.)*15.
01104 505*      CALL STORAG
01105 506*      IA(66,1)=0
01106 507*      AA(66,17)=30.*AA(40,17)/(60.*15.*HOUR)
01107 508*      CALL PMPCNT
01110 509*      HP=.001*AA(66,17)
01111 510*      SUMHP=SUMHP
01111 511* C   CONTROL LOOPS
01112 512*      XL00PS = L00PS
01113 513*      COST(1) = X100PS*AA(100,1)
01114 514*      COST(5) = COST(5)
01115 515*      COSTA(1) = COSTA(1) + COST(1)
01116 516*      COSTA(5) = COSTA(5) + COST(5)
01117 517*      PRINT 1021, COST(1),COST(5)
01117 518* C   FORK LIFT
01123 519*      1021 FORMAT(/25H CONTR0L INSTRUMENTATION ,35X,F10.3,30X,F10.3)
01124 520*      COST(1) = AA(100,20)
01125 521*      COST(5) = COST(1)
01126 522*      COSTA(1) = COSTA(1)+ COST(1)
01127 523*      COSTA(5) = COSTA(5)+ COST(5)
01130 524*      PRINT 1022, COST(1),COST(5)
01134 525*      AA(8,17) = TONS
01135 526*      CALL CONDEN
01136 527*      1022 FORMAT(/ 25H PAYLOADNER          ,10X,25X,F10.3,30X,F10.3)
01136 528*      C
01136 529*      C   BOILER WATER TREATMENT
01136 530*      C

```

Table I.-- Continued.

```

01137 531* COST(5)=1.
01140 532* COST(1)=COST(5)
01141 533* PRINT 4242, COST(1),COST(5)
01145 534* 4242 FORMAT(/25H BOILER WATER TREATMENT , 10X ,15H ,10H
01145 535* 1 ,F10.3,30X,F10.3)
01146 536* COSTA(1)=COSTA(1) + COST(1)
01147 537* COSTA(5)=COSTA(5) + COST(5)
01147 538* C
01147 539* C SEA WATER PUMPS
01147 540* C
01150 541* AA(90,10)=WATER*60. + 4.*STEAM
01151 542* AA(66,17) = AA(90,10)*1.2/60.
01152 543* IA(66,1)=1.
01153 544* IA(66,4)=2.
01154 545* CALL PMPCNT
01155 546* IA(66,1)=0
01156 547* IA(66,4)=0
01157 548* HP= .001*AA(66,17)
01160 549* SUMHP=SUMHP + HP
01160 550* C
01160 551* C CARBON ADSORBER
01160 552* C
01161 553* COST(1)=2.
01162 554* COST(5)=COST(1)
01163 555* PRINT 4243, COST(1),COST(5)
01167 556* COSTA(1)=COSTA(1) + COST(1)
01170 557* COSTA(5)=COSTA(5) + COST(5)
01171 558* 4243 FORMAT(/25H CARBON ADSORBER , 10X ,15H ,10H
01171 559* 1 ,F10.3,30X,F10.3)
01171 560* C
01171 561* C VENT CONDENSER
01171 562* C
01172 563* AA(66,17)=20.
01173 564* IA(67,1)=1
01174 565* IA(67,4)= 4
01175 566* CALL HEATEX
01176 567* IA(67,1)=0
01177 568* IA(67,4)=0
01200 569* CALL SCALE
01201 570* CALL SCALE
01202 571* PRINT 1041,(COSTA(J),J=1,6)
01210 572* 1041 FORMAT(/25H TOTAL COSTS ,35X*6F10.3)
01211 573* AA(90,2) = SUMHP*.7457 * 24.
01212 574* AA(100,10)= COSTA(5)
01213 575* AA(90,1) = STEAM*1000.*24./140000.
01213 576* C MATERIAL BALANCE
01214 577* AA(90,3) = PRDCTB
01215 578* AA(90,7) = PRDCTA
01216 579* AA(90,5)=0I1
01217 580* AA(90,18)=WASTE
01220 581* AA(90,19)=ACID
01221 582* CALL MATER(TONS)
01222 583* FISH = TONS*2000./24.
01223 584* PRINT 1003 , FISH
01226 585* 1003 FORMAT(/7X27H FISH TO EXTRACTION VESSELS,F8.0,7H LB/HR )
01227 586* YYA=STEAM1
01230 587* PRINT 1201,YYA

```

Table I.--Continued.

01233	588*	1201	FORMAT(/8X,35H STEAM(STIRRED VESSEL 1 )	,F8.0,7H LB/HR )
01234	589*		YYB=STEAM2	
01235	590*		PRINT 1202,YYB	
01240	591*	1202	FORMAT(/8X,35H STEAM(STIRRED VESSEL 2 )	,F8.0,7H LB/HR )
01241	592*		YYC= STEAM3	
01242	593*		PRINT 1203,YYC	
01245	594*	1203	FORMAT(/8X,35H STEAM(STIRRED VESSEL 3 )	,F8.0,7H LB/HR )
01246	595*		YYD= STEAM4	
01247	596*		PRINT 1204,YYD	
01252	597*	1204	FORMAT(/8X,35H STEAM(STIRRED VESSEL 4 )	,F8.0,7H LB/HR )
01253	598*		YYE = STEAM0	
01254	599*		PRINT 1205,YYE	
01257	600*	1205	FORMAT(/8X,35H STEAM(PREHEATER-DISTILLATION)	,F8.0,7H LB/HR )
01260	601*		YYG= STEAMR	
01261	602*		PRINT 1206,YYG	
01264	603*	1206	FORMAT(/8X,35H STEAM(REBOTLER)	,F8.0,7H LB/HR )
01265	604*		YYH = STEAM6	
01266	605*		PRINT 1207,YYH	
01271	606*	1207	FORMAT(/8X,35H STEAM(ROTARY DRYER FPC )	,F8.0,7H LB/HR )
01272	607*		YYI= STEAMW	
01273	608*		PRINT 1208,YYI	
01276	609*	1208	FORMAT(/8X,35H STEAM(ROTARY DRYER BONE MEAL	,F8.0,7H LB/HR )
01277	610*		YYJ=(STEAM*4.)	
01300	611*		PRINT 1209,YYJ	
01303	612*		YYK= WATER	
01304	613*		PRINT 1210,YYK	
01307	614*	1210	FORMAT(/8X,35H COOLING WATER DISTILLATION COND.	,F8.0,9H GAL/MIN )
01307	615*		C )	
01310	616*	1209	FORMAT(/8X,35H COOLING WATER CONDENSER	,F8.0,9H GAL/MIN
01310	617*		C )	
01311	618*		YYL= STEAM	
01312	619*		PRINT 1211,YYL	
01315	620*	1211	FORMAT(/8X,35H TOTAL STEAM	,F8.0,7H LB/HR )
01316	621*		YYM = (STEAM*4.) + WATER	
01317	622*		PRINT 1212,YYM	
01322	623*	1212	FORMAT(/8X,35H TOTAL WATER	,F8.0,7H LB/HR )
01323	624*		PRINT 1213	
01325	625*	1213	FORMAT(/40X, 9H STEAM 1,7X,9H STREAM 2,7X,9H STREAM 3,7X,9H STR	
01325	626*		CEAM 4,7X,9H STREAM 5,)	
01326	627*		PRINT 1214,(STRM(1,K),K=1,5)	
01334	628*		PRINT 1215,(STRM(3,K),K=1,5)	
01342	629*		PRINT 1216,(STRM(2,K),K=1,5)	
01350	630*		PRINT 1217,(STRM(4,K),K=1,5)	
01356	631*		PRINT 1218,(STRM(5,K),K=1,5)	
01364	632*		PRINT 1219,(STM (1,K),K=1,5)	
01372	633*		PRINT 1220,(STM (3,K),K=1,5)	
01400	634*		PRINT 1221,(STM (2,K),K=1,5)	
01406	635*		PRINT 1222,(STM (4,K),K=1,5)	
01414	636*		PRINT 1223,(STM (5,K),K=1,5)	
01422	637*	1214	FORMAT(/10X20H RAFFINATE OIL	,10X,4(F10.3, 8X),F10.3)
01423	638*	1215	FORMAT(/10X20H RAFFINATE ASH	,10X,4(F10.3, 8X),F10.3)
01424	639*	1216	FORMAT(/10X20H RAFFINATE PROTEIN	,10X,4(F10.3, 8X),F10.3)
01425	640*	1217	FORMAT(/10X20H RAFFINATE WATER	,10X,4(F10.3, 8X),F10.3)
01426	641*	1218	FORMAT(/10X20H RAFFINATE ALCOHOL	,10X,4(F10.3, 8X),F10.3)
01427	642*	1219	FORMAT(/10X20H EXTRACT OIL	,10X,4(F10.3, 8X),F10.3)
01430	643*	1220	FORMAT(/10X20H EXTRACT ASH	,10X,4(F10.3, 8X),F10.3)
01431	644*	1221	FORMAT(/10X20H EXTRACT PROTEIN	,10X,4(F10.3, 8X),F10.3)

Table I.-- Continued.

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01432 645* 1222 FORMAT(/10X20H EXTRACT WATER ,10X,4(F10.3, 8X),F10.3)
01433 646* 1223 FORMAT(/10X20H EXTRACT ALCOHOL ,10X,4(F10.3, 8X),F10.3)
01434 647*
01435 648* XXA= STMM(5)* 2000./24.
01440 649* 1224 FORMAT(/8X,35H FLOW FROM EXTRACTION VESSEL 4 ,F8.0,7H LB/HR )
01441 650* XXB= STRMM(1)* 2000./24.
01442 651* 1225 FORMAT(/8X,35H FLOW FROM EXTRACTION VESSEL 1 ,F8.0,7H LB/HR )
01443 652* PRINT 1225, XXB
01446 653* XXC=MATRL*2000./HOUR
01447 654* PRINT 1226,XXC
01452 655* 1226 FORMAT(/8X,35H AQUEDIUS STREAM(CENTRIFUGE) ,F8.0,7H LB/HR )
01453 656* XXD=(STOP(1)+STOP(2))*2000./24.
01454 657* PRINT 1227,XXD
01457 658* 1227 FORMAT(/8X,35H TOPS FROM DISTILLATION COLUMN ,F8.0,7H LB/HR )
01460 659* XXE= SBOT*2000./24.
01461 660* PRINT 1228,XXE
01464 661* 1228 FORMAT(/8X,35H BOTTOMS FROM DISTILLATION COLUMN ,F8.0,7H LB/HR )
01465 662* XXG= AA(90,5)*2000./24.
01466 663* PRINT 1230,XXG
01471 664* 1230 FORMAT(/8X,35H FISH OIL PRODUCT ,F8.0,7H LB/HR )
01472 665* XXH=AA(90,3)*2000./24.
01473 666* 1231 FORMAT(/8X,35H FISH PROTEIN CONCENTRATE ,F8.0,7H LB/HR )
01474 667* XXI=AA(90,7)*2000./24.
01475 668* PRINT 1232, XXH
01500 669* PRINT 1231, XXI
01503 670* 1232 FORMAT(/8X,35H BONE MEAL CONCENTRATE ,F8.0,7H LB/HR )
01504 671* AA(95,1)=SBOT
01505 672* XXJ = AA(95,1)* 2000./24.
01506 673* PRINT 1233, XXJ
01511 674* 1233 FORMAT(/8X,35H FISH SOLUBLES ,F8.0,7H LB/HR )
01512 675* IXX=(14.0*(TONS/50.)**.31) + 0.5
01513 676* AA(90,8)=IXX*8
01514 677* AA(90,9)=(YYJ+YYK)*24.
01515 678* AA(90,13) = AA(90,13) + (AA(90,3)+AA(90,7)+AA(90,20)+AA(90,4))
01516 679* RETURN
01517 680* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S BIOL0G,BIOL0G  
FOR S9A-07/12-11:04 (0,)

SUBROUTINE BIOL0G ENTRY POINT 002306

STORAGE USED: CODE(1) 002350; DATA(0) 000733; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 RLOCK1 005050  
0004 RLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 PMPREC  
0006 RELT  
0007 STORAG  
0010 REFRIG  
0011 PMPCNT  
0012 SILO  
0013 BUCKET  
0014 GRINDR  
0015 REACTR  
0016 AGIT0R  
0017 SCREEN  
0020 SCREW R  
0021 DRYERR  
0022 HAMMER  
0023 BAGGMA  
0024 SCALE  
0025 SHARP  
0026 FVPFLM  
0027 EVPSPR  
0030 ROILER  
0031 CONDEN  
0032 MATER  
0033 MRDC\$  
0034 NIO2\$  
0035 NPRT\$  
0036 NIO1\$  
0037 NEXP6\$  
0040 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001	000367	100L	0000	000041	1000F	0000	000050	1001F	0000	000065	1002F	0000	000252	1003F
0000	000263	1004F	0000	000274	1005F	0000	000342	1006F	0000	000353	1007F	0000	000364	1008F
0000	000375	1009F	0001	000564	101L	0000	000406	1010F	0000	000417	1011F	0000	000430	1012F
0000	000441	1013F	0000	000452	1014F	0000	000305	1015F	0000	000463	1016F	0000	000474	1017F
0000	000505	1018F	0000	000516	1019F	0001	000627	102L	0000	000527	1020F	0000	000207	1021F
0000	000225	1022F	0000	000540	1023F	0000	000551	1024F	0001	000712	103L	0000	000316	1033F
0000	000243	1041F	0001	000006	106G	0000	000027	111F	0000	000327	1111F	0001	000013	114G
0001	000020	122G	0000	000100	2000F	0001	000134	201G	0000	000113	3000F	0000	000171	4242F

Table I.-- Continued.

0000	000153	4249F	0001	001160	4706	0000	000031	5000F	0001	001234	5106	0001	001730	7076
0001	001757	722G	0003	R 000000	AA	0000	R 000012	ADDT	0003	R 004704	BB	0000	R 000024	COOL
0004	R 000000	COST	0004	R 000007	COSTA	0000	R 000023	FISH	0000	R 000006	G	0000	R 000002	GALLON
0000	R 000003	GALS	0000	R 000007	HP	0000	I 000000	I	0003	I 003720	IA	0000	I 000720	INJPS
0000	I 000014	INST	0000	T 000005	IXX	0000	I 000022	J	0000	I 000010	LOOPS	0000	I 000005	NUM
0000	R 000026	PXX	0000	R 000016	SLDS	0000	R 000004	SUMHP	0000	R 000001	TONSA	0000	R 000011	TONSG
0000	R 000015	VOLD	0000	R 000013	VOLT	0000	R 000017	WATER	0000	R 000020	WATEVP	0000	R 000021	XLOOPS

```

00101 1* SUBROUTINE RI0LOG(TONS)
00103 2* COMMON/BLOCK1/AA(100,20),IA(100,5),BB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* DO 1 I=1,7
00110 5* COST(I) =0.0
00111 6* 1 COSTA(I)=0.0
00113 7* DO 2 I=1,20
00116 8* AA(90,I) =0.0
00117 9* 2 AA(91,I) =0.0
00121 10* DO 10 I=30,33
00124 11* 10 BB(I) = BB(I)*0.01
00126 12* READ 11 ,BB(40),BR(41),BR(42),BB(43),RB(44)
00135 13* 111 FORMAT(5E12,5)
00136 14* PRINT 5000
00140 15* 5000 FORMAT(/8X36H ANTI0XIDANT PRICE AND EFFECTIVENESS )
00141 16* PRINT 1001,BR(44),RB(43)
00145 17* PRINT 1000
00147 18* 1000 FORMAT(/8X31H ENZYME PRICE AND EFFECTIVENESS )
00150 19* PRINT 1001,RB(41),BR(40)
00154 20* 1001 FORMAT(/8X8H PRICE =,F5.2,12H DOLLARS/LR,,F8.3,32H LR REQUIRFD PF
00154 21* CR 100 LB OF FISH )
00155 22* IF(BB(42) .GT. 0.0) PRINT 1002,BB(42)
00161 23* 1002 FORMAT(/8XFA.2,51H PERCENT OF DISOLVED PROTEIN PACKAGED AS BCF PA
00161 24* CSTE )
00162 25* PRINT 2000
00164 26* 2000 FORMAT(1H1//55H DETAILED EQUIPMENT COSTS (ALL COSTS IN 1000.0 DOL
00164 27* CLARS) )
00165 28* PRINT 3000
00167 29* 3000 FORMAT (//18H EQUIPMENT TYPE,10X10H CAPACITY,12X9H MATERIAL,
00167 30* C60H BASE MATFRIALS LABOR INDIRECT MODULE RANGF ,/6
00167 31* C0X60H COST COSTS COSTS COSTS COST + OR - )
00167 32* C
00167 33* C UNLOADING AND STORAGE OF FISH
00167 34* C
00170 35* TONSA=TONS*2000./R.*33
00171 36* GALLON= TONSA/(24.*60.)
00172 37* GALS =GALLON*1.3
00173 38* SUMHP= 0.
00174 39* IA(65,1) = 0
00175 40* IA(65,2) = 1.0
00176 41* AA(65,17)= GALS*30.
00177 42* NUM = TONS/500 + 1
00200 43* DO 143 I=1,NUM
00203 44* 143 CALL PMPREC
00205 45* IA(65,2) = 0.0
00206 46* SUMHP= SUMHP +(AA(65,17)*.001*1.5)

```

## Table I.-- Continued.

00207 47\* SUMHP= SUMHP +(AA(65,17)\*.001\*1.5)  
 00210 48\* IF(TONSA.LT.30000.) G=(30000./(24.\*60.))\*15.  
 00212 49\* IF(TONSA.GE.30000.) G=(450000./(24.\*60.))\*15.  
 00214 50\* IF(TONS.LE.150.) AA(70,18)= 36.  
 00216 51\* IF(TONS.GT.150.) AA(70,18)= 48.  
 00220 52\* AA(70,17)=100.  
 00221 53\* CALL BELT  
 00222 54\* HP = TONS\*0.00124 +13.6  
 00223 55\* SUMHP = HP + SUMHP  
 00224 56\* AA(40,17)=30.0\*TONS  
 00225 57\* IA(40,1)=0.0  
 00226 58\* IA(40,2)=2  
 00227 59\* CALL STORAG  
 00230 60\* IA(40,2)=0  
 00231 61\* AA(85,17)=0.5\*TONS\*3.0  
 00232 62\* IA(85,1) =30  
 00233 63\* CALL REFRIG  
 00234 64\* SUMHP = SUMHP + 4.72\*AA(85,17)  
 00235 65\* COST(1)=1.19  
 00236 66\* IF(TONS.GE.300) COST(1)=1.88  
 00240 67\* COST(5)=COST(1)  
 00241 68\* PRINT 4249, COST(1), COST(5)  
 00245 69\* COSTA(1)=COSTA(1)+COST(1)  
 00246 70\* COSTA(5)=COSTA(5)+COST(5)  
 00247 71\* 4249 FORMAT(/25H BRINE MAKE-UP+SALT STOR., 10X ,15H ,10H  
 00247 72\* 1 ,F10.3,30X,F10.3)  
 00247 73\* C PUMP FOR BRINE MAKE-UP (BRONZF)  
 00250 74\* IA(66,1)=1  
 00251 75\* AA(66,17)=TONS\*3.\*2000./(24.\*60.\*62.4)\*.69\*7.75  
 00252 76\* CALL PMPCNT  
 00253 77\* IA(66,1)=0  
 00254 78\* HP=.001\*AA(66,17)  
 00255 79\* SUMHP=SUMHP+HP  
 00255 80\* C PUMP FOR WATER INTO BRINE MAKE-UP  
 00256 81\* AA(66,17)=AA(66,17)\*.917  
 00257 82\* IA(66,1)=0  
 00260 83\* CALL PMPCNT  
 00261 84\* HP=.001\*AA(66,17)  
 00262 85\* SUMHP=SUMHP+HP  
 00262 86\* C  
 00262 87\* C FISH STORAGE FOR 3 DAYS  
 00262 88\* C  
 00263 89\* IA(7,1)=1  
 00264 90\* AA(7,17)=3.\*TONS\*2000.\*1.69/62.4  
 00265 91\* CALL SILO  
 00266 92\* LOOPS=0.0  
 00267 93\* LOOPS=LOOPS+3.  
 00270 94\* CALL SILO  
 00271 95\* TONSG=TONS/24.  
 00272 96\* AA(71,18)= TONSG  
 00273 97\* AA(71,17)= 20.  
 00274 98\* CALL BUCKET  
 00275 99\* HP = TONS\*0.00106  
 00276 100\* SUMHP = HP + SUMHP  
 00276 101\* C  
 00276 102\* C FISH GRINDING AND DIGESTION  
 00276 103\* C

Table I.--Continued.

```

00277 104* 100 IF(TONSG .LT. 3) AA(50,17)=3
00301 105* IF(TONSG .GT. 6) AA(50,17)=6
00303 106* IF(AA(50,17) .GT. 0.0) CALL GRINDR
00305 107* TONSG = TONSG-AA(50,17)
00306 108* IF(TONSG .GT. 0.2) GO TO 100
00310 109* HP = 40*TONSG/3
00311 110* SUMHP=HP+SUMHP
00311 111* C PUMP AFTER GRINDFR
00312 112* AA(66,17)=30.*TONS*2000./(24.*60.*8.33)
00313 113* IA(66,1)=0
00314 114* CALL PMPCNT
00315 115* SUMHP=SUMHP+.001*AA(66,17)
00315 116* C PUMP BEFORE DIGESTER
00316 117* CALL PMPCNT
00317 118* SUMHP=.001*AA(66,17)+SUMHP
00320 119* AA(40,17) = 2*TONS*2000./(8.33*24)
00321 120* IA(40,1) = 1
00322 121* CALL STORAG
00323 122* IA(40,1) = 0
00324 123* AA(90,15)=TONS*.0084
00325 124* AA(90,13)=(BR(30)+BR(31)+BR(32))*TONS*.0001
00326 125* AA(90,17)=TONS*.0432
00327 126* AA(90,14)=TONS*.0192
00330 127* AA(90,12)=TONS*(BR(40)/100.0)
00331 128* ADDT=0.0
00332 129* ADDT=AA(90,12)+AA(90,13)+AA(90,15)+AA(90,17)+AA(90,14)
00333 130* AA(91,1)=ADDT+2.*TONS
00334 131* VOLT=AA(91,1)*2000/(8.33*4.8)
00335 132* AA(51,2) = 2.0
00336 133* AA(51,17) = 2.0
00337 134* AA(49,17)=VOLT/3
00340 135* IF(AA(49,17) .LT. 10000) AA(73,17) = AA(49,17)*0.005
00342 136* IF(AA(49,17) .LT. 10000) GO TO 101
00344 137* IF( AA(49,17) .GT. 10000) AA(73,17) = 50.
00346 138* IF(AA(49,17) .GT. 10000) AA(49,17)=10000
00350 139* 101 AA(66,17)=30.*AA(49,17)*4.8/(60.*24.)
00351 140* IA(66,1)=0
00352 141* CALL REACTR
00353 142* CALL AGITOR
00354 143* CALL SCREEN
00355 144* CALL REACTR
00356 145* CALL AGITOR
00357 146* CALL SCREEN
00360 147* CALL REACTR
00361 148* CALL AGITOR
00362 149* CALL SCREEN
00363 150* INST = 3
00364 151* HP = 3*AA(73,17)
00365 152* SUMHP = HP + SUMHP
00366 153* VOLD =VOLT -AA(49,17)*3
00367 154* 102 IF(VOLD .LT. 500) GO TO 103
00371 155* IF(VOLD .LT. 10000) AA(49,17)=VOLD
00373 156* IF(AA(49,17) .LT. 10000) AA(73,17) = AA(49,17)*0.005
00375 157* IF(VOLD .GT. 10000) AA(49,17)=10000
00377 158* IF( AA(49,17) .GT. 10000) AA(73,17) = 50.
00401 159* CALL REACTR
00402 160* CALL AGITOR

```

## Table I.-- Continued.

```

00403 161*      CALL SCREEN
00404 162*      INST = INST + 1
00405 163*      VOLD = VOLD -AA(40,17)
00406 164*      HP = AA(73,17)
00407 165*      SUMHP = HP + SUMHP
00410 166*      GO TO 102
00411 167*      103  CONTINUE
00411 168*      C
00411 169*      C BONE FEED STREAM
00411 170*      C
00412 171*      BB(2)=1.
00413 172*      SLDS=((40./667.)*RB(31))+((110./250.)*BR(32))+((10./500.)*BR(30))
00413 173*      C)*TONS+((125./299.3)*ADDT*(110./250.))
00414 174*      WATER=TONS*(1.+BB(33)+(174.3/299.3)*ADDT
00415 175*      AA(91,10)=(((180./667.)*BR(31))+((112./500.)*BB(30))+((50./250.)*B
00415 176*      CB(32)))*TONS+((125./299.3)*ADDT*(50./250.))+((1058./7216.5)*WATER)
00416 177*      AA(91,2)=(320./160.)*SLDS
00416 178*      C PUMP FOR SLUDGE FROM CENTRIFUGE
00417 179*      IA(66,1)=0
00420 180*      AA(66,17)=AA(91,10)*30.*2000./(24.*8.33*60.)
00421 181*      CALL PMPCNT
00422 182*      HP=.001*AA(66,17)
00423 183*      SUMHP=HP+SUMHP
00423 184*      C
00423 185*      C SCREW CONVEYOR
00423 186*      C
00424 187*      AA(17,18)=6
00424 188*      C FISH OIL STREAM
00424 189*      C
00425 190*      AA(91,3)=AA(91,1)-AA(91,2)
00425 191*      C PUMPS BEFORE AND AFTER HOLD TANK OF FIRST CENTRIFUGE
00426 192*      IA(66,1)=0
00427 193*      AA(17,17)=20
00430 194*      IA(17,5)=1
00431 195*      CALL SCREWR
00432 196*      IA(21,5)=3
00433 197*      AA(21,17)=AA(91,2)*2.5
00434 198*      CALL DRYERR
00435 199*      AA(90,3)=(SLDS+AA(91,10)-((1058./7216.5)*WATER))/.9
00436 200*      AA(91,12)=AA(91,2)+AA(91,10)-AA(90,3)
00436 201*      C
00436 202*      C BAGGING MACHINE FOR BONE MEAL
00436 203*      C
00437 204*      AA(75,17)=AA(90,3)*2000./(24.*60.*25.)
00440 205*      IA(75,2)=0
00441 206*      IA(75,1)=0
00442 207*      AA(18,17)=AA(90,3)/24.
00443 208*      CALL HAMMER
00444 209*      CALL BAGGMA
00445 210*      AA(75,5)=AA(75,17)
00446 211*      AA(72,17) = 18.
00447 212*      CALL SCALE
00447 213*      C
00450 214*      AA(66,17)=AA(91,3)*30.*2000./(8.33*24.*60.)
00451 215*      CALL PMPCNT
00452 216*      CALL PMPCNT
00453 217*      SUMHP=2.*.001*AA(66,17)+SUMHP

```

Table I.--Continued.

```

00454 218* AA(72,17)=18.
00455 219* CALL SCALE
00456 220* AA(40,17) = AA(91,3)*2000./(8.33*24.)
00457 221* IA(40,1) = 1
00460 222* CALL STORAG
00461 223* IA(40,1) = 0
00462 224* AA(91,6)=((447./667.)*BB(31))+((3./500.)*BB(30))+((90./250.)*BB(3
00462 225* 2)))*TONS+((125./299.3)*ANNT*(90./250.))+((5998./7216.5)*WATER)
00463 226* AA(91,4)=AA(91,3)-AA(91,6)-AA(91,10)
00464 227* HP= 0.01*AA(91,3)*2000.0/(8.33*24.0)
00465 228* SUMHP =HP+SUMHP
00466 229* NUM = HP/20. +1
00467 230* DO 20 I=1,NUM
00472 231* AA(52,17)=20.
00473 232* 20 CALL SHARP
00475 233* HP = 0.025*AA(91,4)*2000.0/(8.33*24.0)
00476 234* SUMHP=SUMHP+HP
00476 235* C PUMPS BEFORE AND AFTER HOLD TANK FOR SECOND CENTRIFUGE
00477 236* IA(66,1)=0
00500 237* AA(66,17)=AA(91,4)*2000.*30./(8.33*24.*60.)
00501 238* CALL PMPCNT
00502 239* CALL PMPCNT
00503 240* SUMHP=2.*.001*AA(66,17)+SUMHP
00504 241* AA(40,17) = AA(91,4)*2000./(8.33*24.)
00505 242* CALL STORAG
00506 243* NUM= HP/20. +1
00507 244* DO 30 I=1,NUM
00512 245* AA(52,17) =20.0
00513 246* 30 CALL SHARP
00513 247* C
00513 248* C HOLD TANK FOR FISH OIL
00513 249* C
00515 250* AA(90,5)=TONS*RB(30)*.75
00516 251* AA(40,17)=AA(90,5)*2000./(8.33*24.)
00517 252* CALL STORAG
00517 253* C
00517 254* C FISH OIL STORAGE (15 DAYS)
00517 255* C
00520 256* AA(40,17)=15.*AA(90,5)*2000./8.33
00521 257* IA(40,1) =0.0
00522 258* CALL STORAG
00523 259* AA(66,17)=AA(90,5)*30.*2000.0/(8.33*24.*60)
00524 260* SUMHP= SUMHP+(AA(66,17)*0.001)
00525 261* SUMHP= SUMHP+(AA(66,17)*0.001)
00526 262* IA(66,1)=0
00527 263* CALL PMPCNT
00530 264* CALL PMPCNT
00530 265* C
00530 266* C DISSOLVED SOLIDS STREAM
00530 267* C
00530 268* C PUMPS BEFORE AND AFTER HOLD TANK
00531 269* IA(66,1)=0
00532 270* AA(66,17)=AA(91,6)*2000./(8.33*24.*60.)*30.
00533 271* CALL PMPCNT
00534 272* CALL PMPCNT
00535 273* SUMHP=SUMHP+.2.*.001*AA(66,17)
00536 274* AA(40,17) = AA(91,6)*2000./(8.33*24.)

```

## Table I.--Continued.

```

00537 275*      IA(40,1) = 1
00540 276*      CALL STORAG
00541 277*      IA(40,1) = 0
00542 278*      WATEVP=(5998./7216.5)*WATER-(AA(91,6)-(5998./7216.5)*WATER)
00543 279*      AA(91,13)=WATEVP
00544 280*      AA(31,17)=AA(91,13)*2000.0/(24*25)
00545 281*      CALL EVPFLM
00546 282*      AA(91,7)=2.*(AA(91,6)-(5998./7216.5)*WATER)
00547 283*      AA(90,6)=AA(91,7)*BR(42)*0.01
00550 284*      AA(72,17) = 18.
00551 285*      CALL SCALE
00551 286*      C
00551 287*      C HOLD TANK
00551 288*      C
00552 289*      AA(40,17)=AA(91,7)*2000.0/(8.33*24.)*1.
00553 290*      IA(40,1)=1
00554 291*      CALL STORAG
00555 292*      IA(40,1)=0
00555 293*      C PUMP AFTER WIPE FILM FVAPORATOR
00556 294*      IA(66,1)=0
00557 295*      AA(66,17)=AA(91,7)*2000.*30.0/(8.33*24.*60.)
00560 296*      CALL PMPCNT
00561 297*      HP=.001*AA(66,17)
00562 298*      SUMHP=HP+SUMHP
00562 299*      C PUMP BEFORE CANNING MACHINE
00563 300*      AA(66,17)=AA(90,6)*2000.*30.0/(8.33*24.*60.)
00564 301*      IF(BB(42).GT.0.0) CALL PMPCNT
00566 302*      HP=.001*AA(66,17)
00567 303*      SUMHP=HP+SUMHP
00570 304*      AA(75,17)=AA(90,6)*2000.0/(8.33*24.0*60.0*5.0)
00571 305*      IA(75,1)=1.0
00572 306*      IA(75,2)=2.0
00573 307*      IF(BB(42).GT.0.0) CALL BAGGMA
00575 308*      IA(75,1) = 0.0
00576 309*      AA(75,4)=AA(75,17)
00577 310*      AA(75,4)=AA(75,4)*60.*24.
00600 311*      IA(75,2)=0.0
00601 312*      AA(91,9)=AA(91,7)-AA(90,6)
00601 313*      C PUMP BEFORE SPRAY DRYER
00602 314*      AA(66,17)=AA(91,9)*2000.*30.0/(8.33*60.*24.)*
00603 315*      CALL PMPCNT
00604 316*      HP=.001*AA(66,17)
00605 317*      SUMHP=HP+SUMHP
00606 318*      AA(90,7)=AA(91,9)/(2.*.95)
00607 319*      AA(91,14)=AA(91,9)-AA(90,7)
00610 320*      AA(30,17)=AA(91,14)*2000.0/24.0
00611 321*      CALL EVPSPR
00612 322*      AA(72,17) = 18.
00613 323*      CALL SCALE
00614 324*      IA(75,1)=0.
00615 325*      IA(75,2)=0.
00616 326*      AA(75,17)=AA(90,7)*2000.0/(24*60*25)
00617 327*      IF(BB(42).GT.100) CALL BAGGMA
00621 328*      AA(75,17)=AA(75,17)+AA(75,5)
00622 329*      AA(75,17)=AA(75,17)*60.*24.
00622 330*      C
00622 331*      C SUMMATION OF STEAM,WATER AND ELECTRICITY

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Table I.--Continued.

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nn622 332* C
nn623 333* AA(91,15)=(AA(91,11)+AA(91,12)+AA(91,13)+AA(91,14))*1.05
nn624 334* AA(27,17)=AA(91,15)*2000.0/24
nn624 335* C
nn624 336* C BOILER WATER TREATMENT
nn624 337* C
nn625 338* COST(5)=1.00n
nn626 339* COST(1)=COST(5)
nn627 340* PRINT 4242,COST(1),COST(5)
nn633 341* COSTA(1)=COSTA(1)+COST(1)
nn634 342* COSTA(5)=COSTA(5)+COST(5)
nn635 343* 4242 FORMAT(/25H BOILER WATER TREATMENT , 10X ,15H ,10H
nn635 344* 1 ,F10.3,3nX,F10.3)
nn635 345* C
nn635 346* C SEA WATER PUMPS
nn635 347* C
nn636 348* AA(90,10)=33.1*(AA(91,13)+AA(91,14))*1.2
nn637 349* AA(66,17)=AA(90,10)*2000.0/(8.33*24*60*n,066)
nn640 350* IA(66,1)=1
nn641 351* IA(66,4)=2
nn642 352* CALL PMPCNT
nn643 353* IA(66,1)=0
nn644 354* IA(66,4)=0
nn645 355* CALL BOILER
nn645 356* C
nn645 357* C FUEL OIL STORAGE (15 DAYS)
nn645 358* C
nn646 359* IA(40,1)=2
nn647 360* AA(40,17)=AA(27,17)/A.33*24*.0112*15.
nn650 361* CALL STORAG
nn651 362* IA(66,1)=0
nn652 363* AA(66,17)=30.*AA(40,17)/(15.*60.*24.)
nn653 364* CALL PMPCNT
nn654 365* HP=.001*AA(66,17)
nn655 366* SUMHP=SUMHP+HP
nn656 367* SUMHP = SUMHP+(AA(66,17)*.001*1.5)
nn657 368* AA(90,9)=4.*TONS+(174.3/299.3)*ADDT+.1*AA(91,4)+.1*AA(91,15)
nn660 369* XLOOPS=L00PS+10.+3.*TNST
nn661 370* COST(1)=XLOOPS *AA(100,1)
nn662 371* COST(5)=COST(1)
nn663 372* COSTA(1) = COSTA(1) + COST(1)
nn664 373* COSTA(5)=COSTA(5) + COST(5)
nn665 374* PRINT 1021 COST(1),COST(5)
nn671 375* 1021 FORMAT(/ 25H CONTROL INSTRUMENTATION , 10X ,15H ,10H
nn671 376* 1 ,F10.3,3nX,F10.3)
nn672 377* AA(8,17) = TONS
nn673 378* CALL CONDEN
nn674 379* COST(1)=AA(100,2)
nn675 380* COST(5)=COST(1)
nn676 381* COSTA(1)=COST(1) + COSTA(1)
nn677 382* COSTA(5)=COSTA(5) + COST(5)
nn700 383* PRINT 1022,COST(1),COST(5)
nn704 384* 1022 FORMAT(/ 25H PAYLOADER AND FORK LIFT , 10X ,15H ,10H
nn704 385* 1 ,F10.3,3nX,F10.3)
nn705 386* PRINT 1041,(COSTA(J),J=1.6)
nn713 387* 1041 FORMAT(/25H TOTAL COSTS ,35X6F10.3)
nn714 388* COSTA(7)=0.n2*COSTA(1)

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## Table I.--Continued.

00715	389*	AA(100,10)=COSTA(5)	
00715	390*	C	
00715	391*	C MATERIAL BALANCE INFORMATION PRINTOUT. ALL STREAMS HERE CONVERTED TO	
00715	392*	C LB/HR	
00716	393*	AA(90,2)=SUMHP* .7457 * 24.	
00717	394*	AA(90,10)=AA(90,10)/R.33*2000./24.	
00720	395*	CALL MATER(TONS)	
00721	396*	DO 40 I=1,20	
00724	397*	AA(90,I)=AA(90,I)*2000/24	
00725	398*	40 AA(91,I)=AA(91,I)*2000/24	
00727	399*	FISH=TONS*2000/24	
00730	400*	PRINT 1003,FISH	
00733	401*	1003 FORMAT(/8X26H FISH FEED TO GRINDERS ,F8.0,7H LB/HR )	
00734	402*	PRINT 1004,AA(90,12)	
00737	403*	1004 FORMAT(/8X26H ENZYME TO DIGESTERS ,F8.2,7H LB/HR )	
00740	404*	PRINT 1005,AA(90,15)	
00743	405*	1005 FORMAT(/8X26H,CAOH TO DIGESTERS ,F8.0,7H LB/HR )	
00744	406*	PRINT 1015,AA(90,13)	
00747	407*	1015 FORMAT(/8X26H ANTI-OXIDANT TO DIGESTERS ,F8.2,7H LB/HR )	
00750	408*	PRINT 1033,AA(90,17)	
00753	409*	1033 FORMAT(/8X26H 5N NaOH TO DIGESTERS ,F8.2,7H LB/HR )	
00754	410*	PRINT 1111,AA(90,14)	
00757	411*	1111 FORMAT(/8X41H CONCENTRATED SULFURIC ACID TO DIGESTERS ,F8.2,7H LB/	
00757	412*	CHR )	
00760	413*	PRINT 1006,AA(91,2)	
00763	414*	1006 FORMAT(/8X26H FEED TO ROTARY DRYER ,F8.0,7H LB/HR )	
00764	415*	PRINT 1007,AA(91,12)	
00767	416*	1007 FORMAT(/8X26H ROTARY DRYER STEAM ,F8.0,7H LB/HR )	
00770	417*	PRINT 1008,AA(90,3)	
00773	418*	1008 FORMAT(/8X26H BONF FEED ,F8.0,7H LB/HR )	
00774	419*	PRINT 1009,AA(91,3)	
00777	420*	1009 FORMAT(/8X26H DIGESTER LIQUOR ,F8.0,7H LB/HR )	
01000	421*	PRINT 1010,AA(90,5)	
01003	422*	1010 FORMAT(/8X26H FISH OIL ,F8.0,7H LB/HR )	
01004	423*	PRINT 1011,AA(91,6)	
01007	424*	1011 FORMAT(/8X26H FEED TO FILM EVAPORATOR ,F8.0,7H LB/HR )	
01010	425*	PRINT 1012,AA(91,13)	
01013	426*	1012 FORMAT(/8X26H FILM EVAPORATOR STEAM ,F8.0,7H LB/HR )	
01014	427*	COOL =AA(91,13)*4	
01015	428*	PRINT 1013,COOL	
01020	429*	1013 FORMAT(/8X26H FILM EVAPORATOR COOLING ,F8.0,7H GAL/HR )	
01021	430*	PRINT 1014,AA(91,7)	
01024	431*	1014 FORMAT(/8X26H BFC PASTE ,F8.0,7H LB/HR )	
01025	432*	AA(90,13) = 0.0005*(AA(91,7) +AA(90,3))	
01026	433*	PRINT 1016,AA(90,6)	
01031	434*	1016 FORMAT(/8X26H PACAGFD AS BFC PASTE ,F8.0,7H LB/HR )	
01032	435*	PRINT 1017,AA(91,9)	
01035	436*	1017 FORMAT(/8X26H FEED TO SPRAY EVAPORATOR ,F8.0,7H LB/HR )	
01036	437*	PRINT 1018,AA(91,14)	
01041	438*	1018 FORMAT(/8X26H SPRAY EVAPORATOR STEAM ,F8.0,7H LB/HR )	
01042	439*	COOL=4*AA(91,14)	
01043	440*	PRINT 1019,COOL	
01046	441*	1019 FORMAT(/8X26H SPRAY EVAP. COOLING ,F8.0,7H GAL/HR )	
01047	442*	PRINT 1020,AA(90,7)	
01052	443*	1020 FORMAT(/8X26H BFC POWDER ,F8.0,7H LB/HR, )	
01053	444*	AA(91,16)=AA(91,15)-AA(91,14)-AA(91,12)	
01054	445*	PRINT 1023,AA(91,16)	

Table I.--Continued.

```

01057 446* 1023 FORMAT(/8X26H MISC EL ALEOUS STEAM ,F8.0,7H LB/HR )
01060 447* AA(90,9)=AA(90,9)/8.33
01061 448* PRINT 1024 ,AA(90,9)
01064 449* 1024 FORMAT(/8X26H CITY WATER ,F8.0,7H GAL/HR )
01065 450* AA(90,1) = AA(27,17)*24*n.0112
01066 451* AA(90,2) = SIMHP* .7457 * 24.
01067 452* AA(90,3) = AA(90,3)*24/2000
01070 453* AA(90,5) = AA(90,5)*24/2000
01071 454* AA(90,6) = AA(90,6)*24/2000
01072 455* AA(90,7) = AA(90,7)*24/2000
01073 456* IXX =(14.0*(TONS/50.0)**.31) +0.5
01074 457* PXX =IXX
01075 458* AA(90,8) =IXX*8.0
01076 459* AA(90,9) =AA(90,9)*24
01077 460* AA(90,12)=AA(90,12)*24
01100 461* AA(90,13)=AA(90,13)*24
01101 462* AA(90,15)=AA(90,15)*24
01102 463* AA(90,14)=AA(90,14)*24
01103 464* AA(90,17)=AA(90,17)*24
01104 465* RETURN
01105 466* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

QFOR,S XXIPA,XXIPA  
 FOR S9A-07/12-11:04 (0,)

SUBROUTINE XXIPA ENTRY POINT 004256

STORAGE USED: CODE(1) 004346; DATA(0) 001463; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
 0004 BLOCK2 000016  
 0005 BLOCK4 000012

EXTERNAL REFERENCES (BLOCK, NAME)

0006 PMPREC  
 0007 RELT  
 0010 STORAG  
 0011 REFRIG  
 0012 SILO  
 0013 PMPCNT  
 0014 BUCKET  
 0015 PULVER  
 0016 AGITOR  
 0017 REACTR  
 0020 SCREEN  
 0021 SCREW R  
 0022 HEATEX  
 0023 DRYERR  
 0024 HAMMER  
 0025 BAGGMA  
 0026 CNTFGE  
 0027 SHARP  
 0030 VESSEL  
 0031 COLUMN  
 0032 FVPHOR  
 0033 BOILER  
 0034 CONDEN  
 0035 SCALE  
 0036 WATER  
 0037 NPRT\$  
 0040 NI02\$  
 0041 NI01\$  
 0042 SQRT  
 0043 NEXP6\$  
 0044 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001	000342	100L	0000	000477	1003F	0001	000527	101L	0000	000410	1021F	0000	000421	1022F
0000	000467	1041F	0001	002322	1044c	0001	002374	1063G	0000	000365	1110F	0000	000246	1113F
0000	000354	1120F	0001	002566	1142c	0001	000014	116G	0000	000510	1201F	0000	000522	1202F
0000	000534	1203F	0000	000546	1204F	0000	000560	1205F	0000	000572	1206F	0000	000604	1207F

Table I.-- Continued.

0000	000616	1208F	0000	000642	1209F	0000	000630	1210F	0000	000654	1211F	0000	000666	1212F
0000	000700	1213F	0000	000716	1214F	0000	000727	1215F	0000	000740	1216F	0000	000751	1217F
0000	000762	1218F	0000	000773	1219F	0000	001004	1220F	0000	001015	1221F	0000	001026	1222F
0000	001037	1223F	0000	001050	1224F	0000	001062	1225F	0000	001074	1226F	0000	001106	1227F
0000	001120	1228F	0000	001132	1229F	0000	001144	1230F	0000	001156	1231F	0000	001170	1232F
0000	001202	1233F	0001	000041	132G	0001	000046	140G	0001	003504	1442G	0001	003713	1566G
0001	003724	1574G	0001	003735	1602G	0001	003746	1610G	0001	003757	1616G	0001	003770	1624G
0001	000114	163G	0001	004001	1632G	0001	004012	1640G	0001	004023	1646G	0001	004034	1654G
0000	000263	2000F	0001	000426	300G	0001	002105	300L	0000	000276	3001F	0000	000376	3006F
0001	000475	320G	0001	000517	332G	0001	000652	402G	0001	000653	405G	0001	000670	413G
0001	000673	420G	0000	000433	4242F	0000	000451	4243F	0000	000336	4249F	0001	002141	44L
0001	001015	453G	0001	003264	48L	0001	002161	49L	0001	003016	51L	0001	001231	517G
0001	003164	52L	0001	001263	535G	0001	001366	573G	0001	001372	577G	0003	R 000000	AA
0000	R 000165	AABAG	0000	R 000143	ABC	0000	R 000167	ACID	0003	R 004704	BB	0004	R 000000	COST
0004	R 000007	COSTA	0000	R 000144	DX	0000	R 000146	FF	0000	R 000216	FISH	0000	R 000177	FT
0000	R 000112	G	0000	R 000127	GAA	0000	R 000170	GAL	0000	R 000106	GALLON	0000	R 000107	GALS
0000	R 000172	HOP	0000	R 000113	HP	0000	R 000211	HWAT	0000	I 000104	I	0003	I 000370	IA
0000	001426	INJPS	0000	I 000130	IP	0005	I 000000	IPTION	0000	I 000131	IQ	0000	I 000134	IR
0000	I 000135	IRR	0000	I 000140	IU	0000	I 000245	IXX	0000	I 000121	J	0000	I 000122	K
0000	I 000103	LOOPS	0000	I 000120	NA	0000	I 000117	NB	0000	I 000111	NUM	0000	I 000174	N2
0000	I 000201	N3	0000	R 000163	PRDCTA	0000	R 000102	PRDCTB	0000	R 000166	SA	0000	R 000171	SA
0000	R 000173	SAB	0000	R 000137	SAG	0000	R 000213	SAQT	0000	R 000175	SBC	0000	R 000077	SBOT
0000	R 000200	SBOTT	0000	R 000210	SBQQT	0000	R 000207	SBQT	0000	R 000126	SLMXTK	0000	R 000153	STEAM
0000	R 000202	STEAMR	0000	R 000214	STEAMW	0000	R 000152	STEAM1	0000	R 000147	STEAM2	0000	R 000150	STEAM3
0000	R 000151	STEAM4	0000	R 000160	STEAM6	0000	R 000176	STEAM9	0000	R 000000	STM	0000	R 000062	STMM
0000	R 000123	STON	0000	R 000074	STOP	0000	R 000031	STRM	0000	R 000067	STRMM	0000	R 000110	SUMHP
0000	R 000136	TANK	0000	R 000203	TANKA	0000	R 000154	TASA	0000	R 000155	TASB	0000	R 000156	TASC
0000	R 000157	TASD	0000	R 000212	TONA	0000	R 000105	TONSA	0000	R 000125	TONSB	0000	R 000114	TONSG
0000	R 000132	VES	0000	R 000133	VES5	0000	R 000205	WASTE	0000	R 000206	WATER	0000	R 000204	WIDTH
0000	R 000164	XAA	0000	R 000141	XIP	0000	R 000142	XIR	0000	R 000145	XIRR	0000	R 000215	XLOOPS
0000	R 000233	XXA	0000	R 000234	XXB	0000	R 000235	XXC	0000	R 000236	XXD	0000	R 000237	XXE
0000	R 000240	XXF	0000	R 000241	XXG	0000	R 000242	XXH	0000	R 000243	XXI	0000	R 000244	XXJ
0000	R 000217	YYA	0000	R 000220	YYB	0000	R 000221	YYC	0000	R 000222	YYD	0000	R 000223	YYE
0000	R 000224	YYG	0000	R 000225	YYH	0000	R 000226	YYI	0000	R 000227	YYJ	0000	R 000230	YYK
0000	R 000231	YYL	0000	R 000232	YYM	0000	R 000115	ZA1	0000	R 000124	ZA2	0000	R 000116	ZA3
0000	R 000161	ZA7	0000	R 000162	ZAB									

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00101 1*          SUBROUTINE XXIPA(TONS)
00101 2*  C
00101 3*  C  ISOPROPYL ALCOHOL EXTRACTION PROCFS5
00101 4*  C
00101 5*  C
00103 6*  COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 7*  COMMON/BLOCK2/ COST(7),COSTA(7)
00105 8*  COMMON/BLOCK4/ IPTION(10)
00106 9*  DIMENSION STM(5,5),STRM(5,5) , STMM(5), STRMM(5)
00107 10* DIMENSION STOP(3),SBOT(3)
00110 11* AA(72,17)=18.
00111 12* PRDCTB=0.
00112 13* 1113 FORMAT(/ 25H WET DERONER          ,F10.3,25H TONS          SST
00112 14*  C          ,6F10.3)
00113 15* IPTION(2)=IPTION(1)
00114 16* LOOPS=0
00115 17* DO 1 I=1,7

```

Table I.-- Continued.

```

00120 18*      COST(I)=0.0
00121 19*      1  COSTA(I)=0.0
00123 20*      IF(IPTION(1).EQ.2) PRINT 1120
00126 21*      IF(IPTION(1).EQ.1) PRINT 1110
00131 22*      DO 2 I= 1,20
00134 23*      AA (90,I)=0.0
00135 24*      2  AA (91,I)=0.0
00137 25*      DO 10 I =30,33
00142 26*      10  BB(I)=BB(I)*.01
00144 27*      PRINT 2000
00146 28*      2000 FORMAT(1H) //55H DETAILED EQUIPMENT COSTS (ALL COSTS IN 1000.0 DOL
00146 29*      CLARS) )
00147 30*      PRINT 3001
00151 31*      3001 FORMAT (//1AH  EQUIPMENT TYPE,10X10H CAPACITY,12X9H MATERIAL,
00151 32*      C60H  BASE  MATFRALS  LABOR  INDIRECT  MODULE  RANGE ,/6
00151 33*      C0X60H COST  COSTS  COSTS  COSTS  COST  + OR - )
00151 34*      C UNLOADING AND STORAGE OF FISH
00152 35*      TONSA = TONS*2000./8.33
00153 36*      GALLON= TONSA/(24.*60.)
00154 37*      GALS = 1.3* GALLON
00155 38*      SUMHP=0.
00156 39*      IA(65,1) =0.
00157 40*      IA(65,2) =1.0
00160 41*      AA(65,17)= GALS*30.
00161 42*      NUM = TONS/500 + 1
00162 43*      DO 143 I=1,NUM
00165 44*      SUMHP=SUMHP+(1.*AA(65,17)*.001*1.5)
00166 45*      143  CALL PMPREC
00170 46*      IA(65,2)=0.
00171 47*      IF(TONSA.LT.30000.) G=(30000./(24.*60.))*15.
00173 48*      IF(TONSA.GE.30000.) G=(45000./(24.*60.))*15.
00175 49*      IF(TONS.LE.150.) AA(70,18)=36.
00177 50*      IF(TONS.GE.150.) AA(70,18)=48.
00201 51*      AA(70,17)=100.
00202 52*      CALL BELT
00203 53*      HP= TONS*0.00124 + 13.6
00204 54*      SUMHP= SUMHP + Hp
00205 55*      AA(40,17)= 30.0* TONS
00206 56*      IA(40,1) = 0
00207 57*      IA(40,2) = 2
00210 58*      CALL STORAG
00211 59*      IA(40,2)= 0
00212 60*      AA(85,17)= 0.5* TONS* 3.0
00213 61*      IA(85,1) = 30
00214 62*      CALL REFRIG
00215 63*      IA(7,1) = 1
00215 64*      C
00215 65*      C FISH STORAGE FOR 3 DAYS
00215 66*      C
00216 67*      AA(7,17)=3.*TONS*2000.*1.69/62.4
00217 68*      CALL SILO
00220 69*      COST(1)=1.19
00221 70*      IF(TONS.GE.300) COST(1)=1.88
00223 71*      COST(5)=COST(1)
00224 72*      PRINT 4249, COST(1), COST(5)
00230 73*      COSTA(1)=COSTA(1)+COST(1)
00231 74*      COSTA(5)=COSTA(5)+COST(5)

```

Table I.-- Continued.

```

00232 75* 4249 FORMAT(/25H BRINE MAKE-UP+SALT STOR., 10X ,15H ,10H
00232 76* 1 ,F10.3,30X,F10.3)
00232 77* C
00232 78* C PUMP FOR BRINE MAKE-UP (BRONZE)
00232 79* C
00233 80* IA(66,1)=1
00234 81* AA(66,17)=TONS*3.*2000./(24.*60.*62.4)*.69*7.75
00235 82* CALL PMPCNT
00236 83* IA(66,1)=0
00237 84* HP=.001*AA(66,17)
00240 85* SUMHP=SUMHP+HP
00240 86* C
00240 87* C PUMP FOR WATER INTO BRINE MAKE-UP
00240 88* C
00241 89* AA(66,17)=AA(66,17)*.917
00242 90* IA(66,1)=0
00243 91* CALL PMPCNT
00244 92* HP=.001*AA(66,17)
00245 93* SUMHP=SUMHP+HP
00246 94* TONSG= TONS/24.
00247 95* AA(71,18)= TONSG
00250 96* AA(71,17)= 20.
00251 97* CALL BUCKET
00252 98* HP= TONS* 0.00106
00253 99* SUMHP=HP+SUMHP
00253 100* C FISH GRINDING AND EXTRACTION
00254 101* IF(IPTION(J).EQ.1) GO TO 100
00254 102* C
00254 103* C DRY DEBONING
00256 104* AA(11,17)= TONS* 2000./24.
00257 105* BB(2) = 3.0
00260 106* CALL PULVER
00261 107* 1120 FORMAT(/44H THE DRY DEBONING OPTION IS APPROPRIATE)
00262 108* 1110 FORMAT(/44H THE WET DEBONING OPTION IS APPROPRIATE)
00263 109* ZA1=0.
00264 110* ZA3=1.
00265 111* GO TO 101
00266 112* 100 CONTINUE
00266 113* C
00266 114* C WET DEBONING
00266 115* C
00267 116* ZA1=0.04
00270 117* ZA3=0.
00271 118* NB= 1
00272 119* NA= (TONS/75.) + 1.
00273 120* IF(NA.GT.3) NB = 2
00275 121* IF(NA.GT.3) NA = (TONS/150.)+1.
00277 122* DO 113 J = 1,NA
00302 123* LOOPS = LOOPS + 1
00303 124* COST(1) = 22.*BB(1)
00304 125* IF(NB.EQ.2) COST(1)= 40.* BB(1)
00306 126* HP=10.
00307 127* IF(NB.EQ.2) HP= 20.
00311 128* SUMHP = SUMHP + HP
00312 129* COST(2)= COST(1)* .25
00313 130* COST(3)= COST(1)* .25
00314 131* COST(4)= COST(1)* .4

```

Table I.-- Continued.

```

00315 132*      COST(5)= COST(1)+ COST(2) + COST(3) +COST(4)
00316 133*      COST(6)= .1 * COST(1)
00317 134*      DO 114 K=1,7
00322 135*      114 COSTA(K)= COSTA(K) + COST(K)
00324 136*      STON= 75.
00325 137*      IF(NB.EQ.2) STON = 150.
00327 138*      PRINT 1113 ,STON,(COST(K),K=1,6)
00336 139*      LOOPS=LOOPS + 1
00337 140*      113 CONTINUE
00341 141*      101 CONTINUE
00342 142*      ZA2=1. -ZA1
00342 143*      C
00342 144*      C EXTRACTION VESSFLS MATERIAL BALANCE
00342 145*      C 1=OIL 2=PROTEIN 3=ASH 4=WATER 5= IPA
00342 146*      C
00343 147*      STM(1,1)=TONS*RB(30)*7A2
00344 148*      STM(1,2)=.17*STM(1,1)
00345 149*      STM(1,3)=.29*STM(1,2)
00346 150*      STM(1,4)=.5*STM(1,3)
00347 151*      STM(1,5)=.25*STM(1,4)
00350 152*      STM(2,1)=TONS*7A2*RB(31)
00351 153*      STM(2,2)=.8*STM(2,1)
00352 154*      STM(2,3)=.98*STM(2,2)
00353 155*      STM(2,4)=1.0*STM(2,3)
00354 156*      STM(2,5)=.99*STM(2,4)
00355 157*      STM(3,1)=TONS*7A3*RB(32)
00356 158*      STM(3,2)=.81*STM(3,1)
00357 159*      STM(3,3)=.98*STM(3,2)
00360 160*      STM(3,4)=.99*STM(3,3)
00361 161*      STM(3,5)=.99*STM(3,4)
00362 162*      STM(4,1)=TONS*7A2*RB(33)
00363 163*      STM(4,2)=.29*STM(4,1)
00364 164*      STM(4,3)=.56*STM(4,2)
00365 165*      STM(4,4)=.60*STM(4,3)
00366 166*      STM(4,5)=.12*STM(4,4)
00367 167*      STM(5,1)=0.
00370 168*      STM(5,2)=TONS/50.*1.5
00371 169*      STM(5,3)=1.29*STM(5,2)
00372 170*      STM(5,4)=1.87*STM(5,3)
00373 171*      STM(5,5)=1.84*STM(5,4)
00374 172*      STRM(1,5)=0.
00375 173*      STRM(2,5)=0.
00376 174*      STRM(3,5)=0.
00377 175*      STRM(5,5)=TONS*2.
00400 176*      STRM(4,5)=0.
00401 177*      DO 122 I=4,1,-1
00404 178*      DO 122 J=1,5
00407 179*      122 STRM(J,I)= STRM(J,I+1) -STM(J,I+1) +STM(J,I)
00412 180*      DO 123 I=1,5
00415 181*      STMM(I)=0.
00416 182*      STRMM(I)=0.
00417 183*      DO 123 J= 1,5
00422 184*      STMM(I)=STMM(I) + STM(J,I)
00423 185*      STRMM(I)=STRMM(I)+ STRM(J,I)
00424 186*      123 CONTINUE
00424 187*      C
00424 188*      C EXTRACTION VESSFL

```

Table I.--Continued.

```

00424 189* C
00427 190*
00430 191* TONSA=(TONS*ZA1) + (TONS*BB(32)*ZA2*(1.-ZA3))
00431 192* TONSB= TONS-TONSA
00431 193* C SLMXTK= 875.* TONSR / 50.
00432 194* MIX TANK
00433 195* GALS= 875.* TONS/50.
00434 196* AA(73,17)= GALS*.005
00435 197* IA(66,1)= 2
00436 198* IA(73,5)= 2
00436 198* AA(40,17)= GALS
00437 199* AA(40,18)= 3.2
00440 200* AA(41,12)=3.2
00441 201* IA(40,1)= 1
00442 202* CALL STORAG
00443 203* GAA= STMM(1)*2000./(24.*60.)
00444 204* GAA=GAA/8.33
00445 205* AA(66,17)=GAA*30.
00446 206* IF(GAA.GT.125.) IP= (GAA/125.) + 1
00450 207* IF(GAA.LE.125.) IP=1
00452 208* DO 40 I0=1,IP
00455 209* HP=(AA(66,17)*.001)
00456 210* SUMHP=HP+SUMHP
00457 211* CALL PMPCNT
00460 212* AA(66,17)=(STMM(1)+STRMM(2))*2000.*30./(24.*60.*8.33)
00461 213* SUMHP=.001*AA(66,17)+SUMHP
00462 214* 40 CALL PMPCNT
00464 215* IF (GALS. GT. 10000.) AA(73,17)=50.
00466 216* CALL AGITOR
00466 217* C
00466 218* C REACTOR VESSFLS
00466 219* C
00467 220* AA(51,17)=TONS*60./50.
00470 221* IP=(AA(51,17)/144.) +2.
00471 222* AA(51,17) =IP
00472 223* VES= TONS* 30.
00473 224* AA(49,17) = VES
00474 225* VESS= TONS*16.
00475 226* IR=1
00476 227* IF(VES.GT.10000.) IR= (VES/10000.) + 1.
00500 228* IRR=1
00501 229* IF(VESS.GT.10000.) IRR= (VESS/10000.)*1.
00503 230* IF(VES.GT.10000.) VES = 10000.
00505 231* TANK= 800.* TONS/50.
00506 232* AA(40,18) = 3.2
00507 233* AA(41,18) = 3.2
00510 234* AA(40,17) = TANK
00511 235* CALL STORAG
00512 236* SAG= STRMM(2)*2000./(24.*8.33*60.)
00513 237* IP=1
00514 238* IF(SAG.GT.1250.) IP =(SAG/1250.) + 1.
00516 239* DO 93 IU=1,IP
00521 240* XIP = IP
00522 241* AA(66,17) = (SAG/XIP)* 24.
00523 242* CALL PMPCNT
00524 243* CALL PMPCNT
00525 244* HP=.001*AA(66,17)
00526 245* SUMHP=SUMHP+HP

```

## Table I.--Continued.

```

00527 246*      SUMHP=SUMHP+HP
00530 247*      93  CONTINUE
00532 248*      IF (VESS.GT.10000.) VESS=10000.
00534 249*      DO 41 I = 1,IR
00537 250*      LOOPS = LOOPS + 3
00540 251*      AA(49,17)= VES
00541 252*      CALL REACTR
00542 253*      CALL SCREEN
00543 254*      AA(73,17)= .005*VES
00544 255*      IF (AA(73,17).LT.2.) AA(73,17)=2.
00546 256*      IA(73,5)= 2
00547 257*      CALL AGITOR
00550 258*      SUMHP=SUMHP + 2.5
00551 259*      XIR= IR
00552 260*      SUMHP = SUMHP + AA(73,17)
00553 261*      AA(66,17) = TONS*2000./(24.*8.33*XIR) *(22./60.)
00554 262*      CALL PMPCNT
00555 263*      ABC= AA(66,17)/22.
00556 264*      IF (ABC.LE.2.) HP=2.
00560 265*      IF (ABC.GT.2.) HP=ABC
00562 266*      SUMHP= HP + SUMHP
00563 267*      IA(17,5)=5
00564 268*      DX= SQRT(TONS/50.) * 8.
00565 269*      AA(17,17) = 6
00566 270*      AA(17,18) = DX
00567 271*      CALL SCREW
00570 272*      41  CONTINUE
00572 273*      DO 42 J= 1,IR
00575 274*      LOOPS = LOOPS + 9
00576 275*      DO 42 I = 1,3
00601 276*      XIRR=IRR
00602 277*      SUMHP=SUMHP + 2.5
00603 278*      AA(66,17) = TONS*2000./(24.*8.33*XIRR) *(22./60.)
00604 279*      CALL PMPCNT
00605 280*      ABC= AA(66,17)/22.
00606 281*      IF (ABC.GT.2.) HP=ABC
00610 282*      IF (ABC.LE.2.) HP=2.
00612 283*      SUMHP= HP + SUMHP
00613 284*      AA(49,17)=VES
00614 285*      CALL REACTR
00615 286*      CALL SCREEN
00616 287*      AA(73,17)= .005*VES
00617 288*      IF (AA(73,17).LT.2.) AA(73,17)=2.
00621 289*      IA(73,5) = 2
00622 290*      SUMHP = SUMHP + AA(73,17)
00623 291*      CALL AGITOR
00624 292*      DX= SQRT(TONS/50.) * 8.
00625 293*      AA(17,18) = DX
00626 294*      AA(17,17) = 6.
00627 295*      IA(17,5)=5
00630 296*      CALL SCREW
00631 297*      42  CONTINUE
00631 298*      C PUMPS IN THE EXTRACTION PROCESS
00631 299*      C PUMPS FOR S-1
00634 300*      AA(66,17)=STMM(2)*30.*2000./(24.*60.*8.33)
00635 301*      CALL PMPCNT
00636 302*      SUMHP=.001*AA(66,17)+SUMHP

```

## Table I.-- Continued.

```

00636 303* C PUMP FOR S=2
00637 304* AA(66,17)=STMM(3)*2000.*30./(24.*60.*8.33)
00640 305* CALL PMPCNT
00641 306* SUMHP=.001*AA(66,17)+SUMHP
00641 307* C PUMP FOR S=3
00642 308* AA(66,17)=STMM(4)*2000.*30./(24.*60.*8.33)
00643 309* CALL PMPCNT
00644 310* SUMHP=.001*AA(66,17)+SUMHP
00644 311* C PUMP FOR M=3
00645 312* AA(66,17)=STRMM(3)*2000.*30./(24.*60.*8.33)
00646 313* CALL PMPCNT
00647 314* SUMHP=.001*AA(66,17)+SUMHP
00647 315* C PUMP FOR SOLIDS INTO DRYER
00650 316* AA(66,17)=STMM(5)*2000.*30./(24.*60.*8.33)
00651 317* CALL PMPCNT
00652 318* SUMHP=.001*AA(66,17)+SUMHP
00652 319* C PUMP FOR M=4
00653 320* AA(66,17)=STRMM(4)*2000.*30./(24.*60.*8.33)
00654 321* CALL PMPCNT
00655 322* SUMHP=.001*AA(66,17)+SUMHP
00655 323* C PUMP FOR SOLVENT
00656 324* AA(66,17)=TONS*2.*2000.*30./(24.*60.*8.33)
00657 325* CALL PMPCNT
00660 326* SUMHP=.001*AA(66,17)+SUMHP
00660 327* C REFLUX CONDENSER
00660 328* C
00661 329* FF = 25.* TONS/ 50.
00662 330* AA(67,17) = FF
00663 331* CALL HEATEX
00663 332* C
00663 333* C STEAM REQUIREMENTS
00664 334* STEAM2= TONS* 20./50.
00665 335* STEAM3= TONS* 20./50.
00666 336* STEAM4= TONS* 20./50.
00667 337* STEAM1= TONS* 35./50.
00670 338* STEAM= STEAM1+STEAM2+STEAM3+STEAM4
00670 339* C
00670 340* C SOLIDS FROM THE EXTRACTION VESSEL
00670 341* C
00671 342* TASA= STMM(5) /2.
00672 343* TASB=STM(1,5)+STM(2,5)+STM(3,5)+.05*STM(4,5)+STM(5,5)*.126*.05+STM
00672 344* 1(5,5)*.0001*.874
00673 345* TASC=.95*.126*STM(5,5)+.95*STM(4,5)
00674 346* TASD=STM(5,5)*.874*.9999
00675 347* STEAM6= (TASC + (1.0*TASD)) * 2000. /24.
00676 348* STEAM= STEAM6 + STEAM
00676 349* C DRYERS
00677 350* AA(21,17) = 3.8* 16.* TASA/24.
00700 351* IA(21,5) = 6
00701 352* BB(2) = .9
00702 353* CALL DRYERR
00703 354* BB(2)=1.0
00704 355* AA(21,17)=AA(21,17)
00705 356* IA(21,5) = 7
00706 357* CALL DRYERR
00707 358* AA(17,18)=6.
00710 359* AA(17,17)=6.

```

## Table I.--Continued.

```

00711 360* IA(17,5)=1
00712 361* CALL SCREWR
00713 362* BB(2)=1.
00714 363* IA(21,5)=7
00715 364* AA(21,17)=AA(21,17)
00716 365* CALL DRYERR
00717 366* AA(21,17)=AA(21,17)
00720 367* IA(21,5) = 8
00721 368* BB(2)=1.0
00722 369* CALL DRYERR
00723 370* AA(17,18)=6
00724 371* AA(17,17)=6
00725 372* IA(17,5)=1
00726 373* CALL SCREWR
00727 374* L00PS = L00PS + 2
00730 375* L00PS = L00PS + 2
00731 376* AA(17,18) = 6.
00732 377* AA(17,17) = 20.
00733 378* IA(17,5) = 1
00734 379* CALL SCREWR
00735 380* ZA7= .96
00736 381* IF(IPTION(2).NE.1) ZA7=1.
00740 382* ZA8=1.-ZA7
00741 383* IF(IPTION(2).NE.1.AND.IPTION(2).NE.2) GO TO 300
00743 384* AA(18,17) =(TASB/ 8.)
00744 385* CALL HAMMER
00745 386* HP = (TASB *2000.*75./(8. * 700.))
00746 387* HP = HP/3.
00747 388* SUMHP=SUMHP+HP
00750 389* IF(IPTION(2).EQ.1) GO TO 44
00750 390* C DRY DEBONING OPTiON
00752 391* PRDCTA=((STM(2,5)*ZA7) + (STM(3,5)*7A8))/.95
00753 392* PRDCTB=((STM(2,5)*ZA8) + (STM(3,5)*7A7))/.95
00754 393* AA(75,17)=PRDCTA*2000./(25.*24.*60.)
00755 394* CALL BAGGMA
00756 395* XAA=AA(75,17)
00757 396* AA(75,17)=PRDCTB*2000./(25.*24.*60.)
00760 397* CALL BAGGMA
00761 398* AA(75,17)=AA(75,17)+XAA
00762 399* AA(75,17)=AA(75,17)*24.*60.
00763 400* GO TO 49
00764 401* 300 CONTINUE
00765 402* AA(18,17)=TASB/8.
00766 403* CALL HAMMER
00767 404* HP=(TASB*2000.*75./(8.*700.))
00770 405* HP=HP/3.
00771 406* SUMHP=SUMHP+HP
00772 407* PRDCTA=((STM(2,5)+STM(3,5))/.95)
00773 408* AA(75,17)=PRDCTA*2000./(25.*24.*60.)
00774 409* CALL BAGGMA
00775 410* AA(75,17)=AA(75,17)*24.*60.
00776 411* GO TO 49
00777 412* 44 CONTINUE
00777 413* C WET DEBONING OPTiON
01000 414* AA(75,17) =((STM(2,5)*ZA7) + (STM(3,5)*7A8))/.95
01001 415* PRDCTA=AA(75,17)
01002 416* AA(75,17) = AA(75,17)* 2000./(24.*60.*100.) * 4.

```

Table I.-- Continued.

```

01003 417*      CALL BAGGMA
01004 418*      AABAG=AA(75,17)
01005 419*      49 CONTINUE
01005 420*      C
01005 421*      C MIXING TANK SECTION
01005 422*      C
01006 423*      SA = STRMM(1)*.001*70.
01007 424*      IA(40,1) = 1
01010 425*      IA(40,2) = 1
01011 426*      AA(40,17) = SA
01012 427*      CALL STORAG
01013 428*      IA(40,2) = 0
01014 429*      L00PS = L00PS + 2
01015 430*      ACID= STRMM(1)*.001
01016 431*      IA(66,1) = 2
01017 432*      AA(66,17) = 30.*ACTD *2000./(8.33*60.*24.* 1.8)
01020 433*      CALL PMPCNT
01021 434*      GAL= STRMM(1) * 2000. / (8.33
01022 435*      HP=.001*AA(66,17)
01023 436*      SUMHP = HP + SUMHP
01024 437*      AA(40,17)= GAL *.01
01025 438*      AA(66,17)= GAL*30./(24.*60.)
01026 439*      IA(66,1) = 0
01027 440*      IA(40,1) = 2
01030 441*      HP=.001*AA(66,17)
01031 442*      SUMHP = SUMHP + HP
01032 443*      SUMHP=SUMHP+HP
01033 444*      CALL PMPCNT
01034 445*      CALL STORAG
01035 446*      CALL PMPCNT
01035 447*      C
01035 448*      C CENTRIFUGE SECTION
01035 449*      C
01036 450*      SAA=STRMM(1)*1.001
01037 451*      HOP= SAA*2000.*.01/(24.*8.33
01040 452*      NUM=(HOP/20.) + 1.
01041 453*      HP= NUM* 20
01042 454*      SUMHP= HP + SUMHP
01043 455*      DO 45 I =1,NUM
01046 456*      AA(54,17)=20.
01047 457*      CALL CNTFGE
01050 458*      45 CONTINUE
01052 459*      SAB= STRM(1,1)*1.1
01053 460*      HP=SAB*.025*2000./(8.33*24.)
01054 461*      N2= (HP/20.) + 1.
01055 462*      HP=N2*20
01056 463*      SUMHP=SUMHP+HP
01056 464*      C PUMP BETWEEN CENTRIFUGES
01057 465*      AA(66,17)=SAB*2000.*30./(24.*60.*8.33)
01060 466*      CALL PMPCNT
01061 467*      SUMHP=.001*AA(66,17)+SUMHP
01062 468*      DO 46 I =1,N2
01065 469*      AA(52,17)= 20.
01066 470*      CALL SHARP
01066 471*      C
01066 472*      C FISH OIL STORAGE TANK (15 DAYS)
01066 473*      C

```

## Table I.-- Continued.

```

01067 474* AA(90,5)=STRM(1,1)
01070 475* AA(40,17)=AA(90,5)*2000.*15./7.75
01071 476* IA(40,1)=1
01072 477* CALL STORAG
01073 478* AA(66,17)=AA(40,17)*30./(24.*15.*60.)
01074 479* CALL PMPCNT
01075 480* SUMHP=.001*AA(66,17)+SUMHP
01076 481* 46 CONTINUE
01076 482* C
01076 483* C MISCELLA TANK (M-1)
01076 484* C
01100 485* SBC=STRMM(1)-(.5*STRM(1,1))
01101 486* AA(40,18)=3.2
01102 487* AA(41,18)=3.2
01103 488* AA(40,17)=SBC*2000./(24.*8.33)
01104 489* IA(40,1)=1
01105 490* CALL STORAG
01106 491* AA(66,17)=30.*(AA(40,17)/60.)
01107 492* IA(66,1)=0
01110 493* CALL PMPCNT
01111 494* CALL PMPCNT
01112 495* HP=.001*AA(66,17)
01113 496* SUMHP=SUMHP+HP
01114 497* SUMHP=SUMHP+HP
01114 498* C PREHEATER FOR DISTILLATION COLUMN
01114 499* C
01115 500* SBC=STRMM(1) - (.5*STRM(1,1))
01116 501* STEAM9=SBC*2000./24.*.1
01117 502* STEAM = STEAM + STEAM9
01120 503* FT= STEAM9* .1
01121 504* AA(67,17) = FT
01122 505* CALL HEATEX
01122 506* C
01122 507* C DISTILLATION COLUMN (MATERIAL BALANCE)
01122 508* C
01123 509* STOP(1)=STRM(5,1)*.99887*.874
01124 510* STOP(2) =STOP(1) *.1445
01125 511* SBOT(1)=STRM(5,1)*.00113*.874
01126 512* SBOT(2)=STRM(4,1)+.125*STRM(5,1)-STOP(2)
01127 513* SBOT(3) = STRM(1,1)* .5
01130 514* SBOTT= SBOT(1) + SBOT(2) + SBOT(3)
01130 515* C
01130 516* C CENTRIFUGE
01130 517* C
01131 518* AA(66,17)=30.*SBOTT*2000./(60.*24.*8.33)
01132 519* IA(66,1) = 0
01133 520* CALL PMPCNT
01134 521* SUMHP=.001*AA(66,17)+SUMHP
01135 522* HP= SBOTT*2000./(24.*8.33 ) *.01
01136 523* N3=(HP/20.) + 1
01137 524* HP= 20* N3
01140 525* SUMHP= HP + SUMHP
01141 526* DO 47 I=1,N3
01144 527* AA(54,17) = 20.
01145 528* CALL CNTRFGE
01146 529* 47 CONTINUE
01150 530* LOOPS = LOOPS + (N1M+ N2 + N3)

```

Table I.-- Continued.

```

01150 531* C
01150 532* C DISTILLATION COLUMN
01150 533* C
01151 534* STEAMR=TONS*10709./50.*(STRM(5,5)/(TONS*2.))
01152 535* AA(67,17)=.1*STEAMP
01153 536* CALL HEATEX
01154 537* STEAM = STEAMR + STEAMP
01155 538* TANKA = TONS* 100. /50.
01156 539* IA(40,1)= 1
01157 540* AA(40,17)=TANKA*2000./ (24.*8.33)
01160 541* CALL STORAG
01161 542* AA(66,17)=(TANKA-(.01*STRM(5,5)))*(2000.*30.)/(24.*60.*8.33)
01162 543* CALL PMPCNT
01163 544* SUMHP=.001*AA(66,17)+SUMHP
01164 545* WIDTH = 4. * SQRT(TONS/75.)
01165 546* I = WIDTH/2.
01166 547* WIDTH = 2 * I
01167 548* IF (WIDTH.LT.4.001) WIDTH = 4.
01171 549* AA(43,18) = 24.
01172 550* AA(43,20)=WIDTH
01173 551* AA(43,17)= 54.
01174 552* AA(43,1) = .4
01175 553* IA(42,4)=2
01176 554* IA(42,2)=1
01177 555* IA(42,3)=1
01200 556* AA(42,18)=WIDTH
01201 557* AA(42,19)=54
01202 558* CALL VESSEL
01203 559* CALL COLUMN
01204 560* LOOPS = LOOPS + 5
01205 561* WASTE=.01*STRM(5,5)
01206 562* AA(40,17)=(WASTE*2000./8.33*15.)
01207 563* IA(40,1) = 0
01210 564* CALL STORAG
01211 565* AA(66,17)=AA(40,17)*30./ (24.*60.*15.)
01212 566* CALL PMPCNT
01213 567* SUMHP=.001*AA(66,17)+SUMHP
01214 568* LOOPS = LOOPS + 1
01214 569* C CONDENSER(DISTILLATION COLUMN)
01215 570* WATER=669.*TONS/50.*(STRM(5,5)/(TONS*2.))
01216 571* AA(67,17)=WATER*8.33*60.*.01
01217 572* CALL HEATFX
01220 573* AA(66,17)=(TANKA/60.)*30.
01221 574* CALL PMPCNT
01222 575* HP = 2. *(TONS /75.)
01223 576* SUMHP=SUMHP+HP
01223 577* C
01223 578* C FISH SOLUABLES
01223 579* C
01224 580* SBQT=SBQT(2) + STRM(2,1)
01225 581* SBQQT=STRM(2,1)*2.
01226 582* HWAT=SBQT-SBQQT
01227 583* 3006 FORMAT(/50H FISH SOLUABLES ARE MORE THAN 50 PERCENT PROTEIN
01230 584* IF(HWAT.GE.0.) GO TO 51
01232 585* PRINT 3006
01234 586* AA(90,4)=SBQT
01235 587* GO TO 52

```

## Table I.-- Continued.

```

01236 588*      51 CONTINUE
01236 589*      C
01236 590*      C      WATER SOLUBLES HOLD TANK (1 HR)
01236 591*      C
01237 592*      AA(40,17)=SBQT*2000./(24.*8.4)*1.
01240 593*      IA(40,1)=1
01241 594*      CALL STORAG
01242 595*      IA(40,1)=0
01243 596*      IA(66,1)=0
01244 597*      AA(66,17)=30.*AA(40,17)/60.
01245 598*      CALL PMPCNT
01246 599*      HP=.001*AA(66,17)
01247 600*      SUMHP=SUMHP+HP
01250 601*      AA(90,4)=SBQQT
01251 602*      TONA=SBQT*2000./24.
01252 603*      AA(33,17)=TONA/20.
01253 604*      CALL EVPHOR
01254 605*      CALL EVPHOR
01255 606*      CALL EVPHOR
01256 607*      SAQT=STRM(2,1)/.3
01257 608*      IF(SAQT.GE.SBQT) SAQT=SBQT
01261 609*      AA(33,17)=SAQT*2000./(24.*25.)
01262 610*      CALL EVPHOR
01263 611*      STEAM=STEAM+(HWAT*2000./24.)
01264 612*      IA(66,1)=0
01265 613*      AA(66,17)=30.*STRM(2,1)*2.*2000./(10.*60.*24.)
01266 614*      CALL PMPCNT
01267 615*      HP=.001*AA(66,17)
01270 616*      SUMHP=SUMHP+HP
01270 617*      C
01270 618*      C      ACID MIX TANK
01270 619*      C
01271 620*      AA(40,17)=STRM(2,1)*2.*2000./(10.*1.)*.01
01272 621*      IA(40,1)=2
01273 622*      CALL STORAG
01274 623*      IA(40,1)=0
01274 624*      C
01274 625*      C      STORAGE OF FISH SOLUBLES (15 DAYS)
01274 626*      C
01275 627*      IA(66,1)=0
01276 628*      AA(66,17)=30.*AA(40,17)/(60.*24.)
01277 629*      CALL PMPCNT
01300 630*      HP=.001*AA(66,17)
01301 631*      SUMHP=SUMHP+HP
01302 632*      IA(40,1)=2
01303 633*      AA(40,17)=STRM(2,1)*2.*2000./(10.)*15.
01304 634*      CALL STORAG
01305 635*      IA(40,1)=0
01306 636*      52 CONTINUE
01307 637*      IF(IPTION(2),NF.1) GO TO 48
01311 638*      IF (IPTION(2),EQ.1) LOOPS = LOOPS + 1
01311 639*      C WET DEBONING OPTION
01313 640*      AA(91,2) = TONS - STMM(1)
01313 641*      C PUMP FOR BONE FEED TO DRYER
01314 642*      AA(66,17)=AA(91,2)*2000.*30./(24.*60.*8.33)
01315 643*      CALL PMPCNT
01316 644*      SUMHP=.001*AA(66,17)+SUMHP

```

Table I.-- Continued.

```

01317 645* IA(21,5)=3
01320 646* AA(21,7)=AA(91,2)*3.8*2./3.
01321 647* STEAMW=AA(91,2)*2000./24.
01322 648* STEAM=STEAM + STEAMW
01323 649* CALL DRYERR
01324 650* AA(90,3)=((TONS*(RB(31)+RB(32)+BB(30))) - STM(1,1) -STM(2,1)
01324 651* - STM(3,1) ) * 1.1
01324 652* C HAMMER MILL FOR WET DEBONING OPTION
01325 653* AA(18,17) = AA(90,3) / 24.
01326 654* CALL HAMMER
01327 655* AA(75,17)=AA(90,3)*2000.*.04/(24.*60.)
01330 656* CALL BAGGMA
01331 657* AA(75,17)=(AA(75,17) +AABAG) *24.*60.
01332 658* 48 CONTINUE
01332 659* C BOILER
01333 660* AA(27,18) =150.
01334 661* AA(27,17)=STEAM
01335 662* CALL BOILER
01336 663* IA(40,1)=2
01337 664* AA(40,17)=STEAM*1000.*24./(8.33*140000.)*15.
01340 665* CALL STORAG
01341 666* IA(66,1)=0
01342 667* AA(66,17)=30.*AA(40,17)/(60.*15.*24.)
01343 668* CALL PMPCNT
01344 669* HP=.001*AA(66,17)
01345 670* SUMHP=SUMHP+HP
01345 671* C CONTROL LOOP
01346 672* XLOOPS = LOOPS
01347 673* COST(1) = XLOOPS*AA(100,1)
01350 674* COST(5) = COST(5)
01351 675* COSTA(1) = COSTA(1) + COST(1)
01352 676* COSTA(5) = COSTA(5) + COST(5)
01353 677* PRINT 1021, COST(1),COST(5)
01353 678* C FORK LIFT
01357 679* 1021 FORMAT(/25H CONTROL INSTRUMENTATION ,35X,F10.3,30X,F10.3)
01360 680* COST(1) = AA(100,20)
01361 681* COST(5) = COST(1)
01362 682* COSTA(1) = COSTA(1) + COST(1)
01363 683* COSTA(5) = COSTA(5) + COST(5)
01364 684* PRINT 1022, COST(1),COST(5)
01370 685* AA(8,17) = TONS
01371 686* CALL CONDEN
01372 687* 1022 FORMAT(/ 25H PAYLOADER ,10X,25X,F10.3,30X,F10.3)
01372 688* C
01372 689* C BOILER WATER TREATMENT
01372 690* C
01373 691* COST(5)=1.000
01374 692* COST(1)=COST(5)
01375 693* PRINT 4242,COST(1),COST(5)
01401 694* 4242 FORMAT(/25H BOILER WATER TREATMENT , 10X ,15H ,10H
01401 695* 1 ,F10.3,30X,F10.3)
01402 696* COSTA(1)=COSTA(1)+COST(1)
01403 697* COSTA(5)=COSTA(5)+COST(5)
01403 698* C
01403 699* C SEA WATER PUMPS
01403 700* C
01404 701* AA(90,10)=WATER*60.+0.*STEAM

```

Table I.--Continued.

```

01405 702* AA(66,17)=AA(90,10)*1.2/60.
01406 703* IA(66,1)=1
01407 704* IA(66,4)=2
01410 705* CALL PMPCNT
01411 706* IA(66,1)=0
01412 707* IA(66,4)=0
01413 708* HP=.001*AA(66,17)
01414 709* SUMHP=SUMHP+HP
01414 710* C
01414 711* C CARBON ADSORBER
01414 712* C
01415 713* COST(1)=2.000
01416 714* COST(5)=COST(1)
01417 715* PRINT 4243,COST(1),COST(5)
01423 716* COSTA(1)=COSTA(1)+COST(1)
01424 717* COSTA(5)=COSTA(5)+COST(5)
01425 718* 4243 FORMAT(/25H CARBON ADSORBER 10X ,15H ,10H
01425 719* 1 ,F10.3,3X,F10.3)
01425 720* C
01425 721* C VENT CONDENSER
01425 722* C
01426 723* AA(67,17)=20
01427 724* IA(67,1)=1
01430 725* IA(67,4)=4
01431 726* CALL HEATEX
01432 727* IA(67,1)=0
01433 728* IA(67,4)=0
01434 729* CALL SCALE
01435 730* CALL SCALE
01436 731* CALL SCALE
01437 732* CALL SCALE
01440 733* PRINT 1041,(COSTA(J),J=1,6)
01446 734* 1041 FORMAT(/25H TOTAL COSTS ,35X,6F10.3)
01447 735* AA(90,2) = SUMHP*.7457 * 24.
01450 736* AA(100,10) = COSTA(5)
01451 737* AA(90,1) = STEAM*1000.*24./140000.
01451 738* C MATERIAL BALANCE
01452 739* IF(IPTION(2).EQ.2) AA(90,3)=PRDCTR
01454 740* AA(90,7) = PRDCTR
01455 741* AA(90,18)=WASTE
01456 742* AA(90,19)=ACID
01457 743* CALL MATER(TONS)
01460 744* FISH = TONS*2000./24.
01461 745* PRINT 1003 , FISH
01464 746* 1003 FORMAT(/7X27H FISH TO EXTRACTION VESSELS,F8.0,7H LB/HR )
01465 747* YYA=STEAM1
01466 748* PRINT 1201,YYA
01471 749* 1201 FORMAT(/8X,35H STEAM(STIRRED VESSEL 1 ) ,F8.0,7H LB/HR )
01472 750* YYB=STEAM2
01473 751* PRINT 1202,YYB
01476 752* 1202 FORMAT(/8X,35H STEAM(STIRRED VESSEL 2 ) ,F8.0,7H LB/HR )
01477 753* YYC= STEAM3
01500 754* PRINT 1203,YYC
01503 755* 1203 FORMAT(/8X,35H STEAM(STIRRED VESSEL 3 ) ,F8.0,7H LB/HR )
01504 756* YYD= STEAM4
01505 757* PRINT 1204,YYD
01510 758* 1204 FORMAT(/8X,35H STEAM(STIRRED VESSEL 4 ) ,F8.0,7H LB/HR )

```

Table I.-- Continued.

01511	759*	YYE = STEAM0	
01512	760*	PRINT 1205,YYF	
01515	761*	1205 FORMAT(/8X,35H STEAM(PREHEATER-DISTILLATION)	,F8.0,7H LB/HR )
01516	762*	YYG= STEAMR	
01517	763*	PRINT 1206,YYG	
01522	764*	1206 FORMAT(/8X,35H STEAM(BOILER)	,F8.0,7H LB/HR )
01523	765*	YYH = STEAM6	
01524	766*	PRINT 1207,YYH	
01527	767*	1207 FORMAT(/8X,35H STEAM(ROTARY DRYER FPC )	,F8.0,7H LB/HR )
01530	768*	YYI= STEAMW	
01531	769*	PRINT 1208,YYI	
01534	770*	1208 FORMAT(/8X,35H STEAM(ROTARY DRYER BONE MEAL)	,F8.0,7H LB/HR )
01535	771*	YYJ=(STEAM*4.)	
01536	772*	PRINT 1209,YYJ	
01541	773*	YYK= WATER	
01542	774*	PRINT 1210,YYK	
01545	775*	1210 FORMAT(/8X,35H COOLING WATER DISTILLATION COND.	,F8.0,8H GAL/MIN)
01546	776*	1209 FORMAT(/8X,35H COOLING WATER CONDENSER	,F8.0,8H GAL/HR )
01547	777*	YYL= STEAM	
01550	778*	PRINT 1211,YYL	
01553	779*	1211 FORMAT(/8X,35H TOTAL STEAM	,F8.0,7H LB/HR )
01554	780*	YYM=((STEAM*4.)+WATER*60.)*8.33	
01555	781*	PRINT 1212,YYM	
01560	782*	1212 FORMAT(/8X,35H TOTAL WATER	,F8.0,7H LB/HR )
01561	783*	PRINT 1213	
01563	784*	1213 FORMAT(/40X, 9H STREAM 1,7X,9H STREAM 2,7X,9H STREAM 3,7X,9H STR	
01563	785*	CEAM 4,7X,9H STREAM 5,/) )	
01564	786*	PRINT 1214,(STRM(1,K),K=1,5)	
01572	787*	PRINT 1215,(STRM(2,K),K=1,5)	
01600	788*	PRINT 1216,(STRM(3,K),K=1,5)	
01606	789*	PRINT 1217,(STRM(4,K),K=1,5)	
01614	790*	PRINT 1218,(STRM(5,K),K=1,5)	
01622	791*	PRINT 1219,(STM(1,K),K=1,5)	
01630	792*	PRINT 1220,(STM(2,K),K=1,5)	
01636	793*	PRINT 1221,(STM(3,K),K=1,5)	
01644	794*	PRINT 1222,(STM(4,K),K=1,5)	
01652	795*	PRINT 1223,(STM(5,K),K=1,5)	
01660	796*	1214 FORMAT(/10X20H RAFFINATE OIL	,10X,4(F10.3, AX),F10.3)
01661	797*	1215 FORMAT(/10X20H RAFFINATE ASH	,10X,4(F10.3, AX),F10.3)
01662	798*	1216 FORMAT(/10X20H RAFFINATE PROTEIN	,10X,4(F10.3, AX),F10.3)
01663	799*	1217 FORMAT(/10X20H RAFFINATE WATER	,10X,4(F10.3, AX),F10.3)
01664	800*	1218 FORMAT(/10X20H RAFFINATE ALCOHOL	,10X,4(F10.3, AX),F10.3)
01665	801*	1219 FORMAT(/10X20H EXTRACT OIL	,10X,4(F10.3, AX),F10.3)
01666	802*	1220 FORMAT(/10X20H EXTRACT ASH	,10X,4(F10.3, AX),F10.3)
01667	803*	1221 FORMAT(/10X20H EXTRACT PROTEIN	,10X,4(F10.3, AX),F10.3)
01670	804*	1222 FORMAT(/10X20H EXTRACT WATER	,10X,4(F10.3, AX),F10.3)
01671	805*	1223 FORMAT(/10X20H EXTRACT ALCOHOL	,10X,4(F10.3, AX),F10.3)
01672	806*	XXA= STMM(5)* 2000./24.	
01673	807*	PRINT 1224, XXA	
01676	808*	1224 FORMAT(/8X,35H FLOW FROM EXTRACTION VESSEL 4	,F8.0,7H LB/HR )
01677	809*	XXB= STRMM(1)* 2000./24.	
01700	810*	1225 FORMAT(/8X,35H FLOW FROM EXTRACTION VESSEL 1	,F8.0,7H LB/HR )
01701	811*	PRINT 1225, XXB	
01704	812*	XXC = (SAA-(.5*CTRM(1,1)))*2000./24.	
01705	813*	PRINT 1226,XXC	
01710	814*	1226 FORMAT(/8X,35H AQUENOUS STREAM(CENTRIFUGE)	,F8.0,7H LB/HR )
01711	815*	XXD=(STOP(1)+CTOP(2))*2000./24.	

Table I.-- Continued.

```

01712 816*          PRINT 1227,XXD
01715 817*    1227  FORMAT(/8X,35H TOPS FROM DISTILLATION COLUMN      ,F8.0,7H LB/HR )
01716 818*          XXE= SBOTT*2000./24.
01717 819*          PRINT 1228,XXE
01722 820*    1228  FORMAT(/8X,35H BOTTOMS FROM DISTILLATION COLUMN  ,F8.0,7H LB/HR )
01723 821*          XXF=(.5*STRM(1,1)*2000./24.)
01724 822*          PRINT 1229,XXF
01727 823*    1229  FORMAT(/8X,35H OIL FROM SECOND CENTRIFUGE      ,F8.0,7H LB/HR )
01730 824*          XXG= AA(90,5)*2000./24.
01731 825*          PRINT 1230,XXG
01734 826*    1230  FORMAT(/8X,35H FISH OIL PRODUCT                    ,F8.0,7H LB/HR )
01735 827*          XXH=AA(90,3)*2000./24.
01736 828*    1231  FORMAT(/8X,35H FISH PROTEIN CONCENTRATE        ,F8.0,7H LB/HR )
01737 829*          XXI=AA(90,7)*2000./24.
01740 830*          PRINT 1232,XXH
01743 831*          PRINT 1231,XXI
01746 832*    1232  FORMAT(/8X,35H BONE MEAL CONCENTRATE            ,F8.0,7H LB/HR )
01747 833*          AA(95,1) = STRM(1,2) * 2.
01750 834*          XXJ = AA(95,1)* 2000./24.
01751 835*          PRINT 1233,XXJ
01754 836*    1233  FORMAT(/8X,35H FISH SOLUBLES                    ,F8.0,7H LB/HR )
01755 837*          IXX=(14.0*(TONS/50.)*.31) + 0.5
01756 838*          AA(90,8)=IXX*8
01757 839*          AA(90,9)=(YYJ+YYK*60.)*24.
01760 840*          AA(90,13) = AA(90,13) + (AA(90,3)+AA(90,7)+AA(90,20)+AA(90,4))
01761 841*          RETURN
01762 842*          END

```

END OF COMPILATION:            NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S PRESCK,PRESCK  
FOR S9A-07/12-11:04 (1,)

SUBROUTINE PRESCK ENTRY POINT 002401

STORAGE USED: CODE(1) 002445; DATA(0) 001006; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 PMPREC  
0006 BELT  
0007 STORAG  
0010 REFRIG  
0011 SILO  
0012 PMPCNT  
0013 BUCKET  
0014 DRYERR  
0015 SCREWR  
0016 SCREEN  
0017 REACTR  
0020 AGITOR  
0021 HAMMER  
0022 BAGGMA  
0023 FVPFLM  
0024 EVPSPR  
0025 CHARP  
0026 ROILER  
0027 CONDEN  
0030 SCALE  
0031 MATER  
0032 NRDC\$  
0033 NIO2\$  
0034 NPRT\$  
0035 NIO1\$  
0036 NEXP6\$  
0037 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000046	1000F	0000	000055	1001F	0000	000073	1002F	0000	000260	1003F	0000	000271	1004F
0000	000302	1005F	0000	000313	1006F	0000	000324	1007F	0000	000335	1008F	0000	000370	1009F
0001	000722	101L	0000	000401	1010F	0000	000412	1011F	0000	000423	1012F	0000	000434	1013F
0000	000445	1014F	0000	000456	1015F	0000	000467	1016F	0000	000346	1017F	0000	000500	1018F
0000	000511	1019F	0001	000757	102L	0000	000522	1020F	0000	000533	1021F	0000	000544	1022F
0000	000555	1023F	0001	001042	103L	0000	000566	1030F	0000	000577	1031F	0000	000610	1032F
0000	000357	1033F	0000	000251	1041F	0000	000215	1050F	0000	000233	1051F	0001	000024	106G
0000	000034	111F	0001	000031	114G	0001	000036	122G	0000	000106	2000F	0001	000152	201G
0000	000121	3000F	0001	000446	305G	0000	000177	4242F	0000	000161	4249F	0000	000036	5000F

Table I.-- Continued.

0001	001450	600G	0001	001525	622G	0001	002001	727G	0001	002027	742G	0003	R	000000	AA
0003	R	004704	BB	0000	R	000030	COOL	0004	R	000000	COST	0004	R	000007	COSTA
0000	R	000027	FISH	0000	R	000006	G	0000	R	000002	GALLON	0000	R	000003	GALS
0000	I	000000	I	0003	I	003720	IA	0000	I	000771	TNJP	0000	I	000017	INST
0000	I	000026	J	0000	I	000010	LOOPS	0000	I	000012	NA	0000	I	000005	NUM
0000	R	000033	PXX	0000	R	000021	SLDS	0000	R	000031	STEAM	0000	R	000004	SUMHP
0000	R	000011	TONSG	0000	R	000020	VOLD	0000	R	000016	VOLT	0000	R	000023	WATER
0000	R	000015	XLIQD	0000	R	000025	XLOOPS	0000	R	000013	XNA	0000	R	000024	WATEVP

```

00101 1* SUBROUTINE PRESCK(TONS)
00103 2* COMMON/BLOCK1/AA(100,20),TA(100,5),BB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* DO 1 I=1,7
00110 5* COST(I)=0.0
00111 6* 1 COSTA(I)=0.0
00113 7* DO 2 I=1,20
00116 8* AA(90,I)=0.0
00117 9* 2 AA(91,I)=0.0
00121 10* DO 10 I=30,33
00124 11* 10 BB(I)=BB(I)*0.01
00126 12* READ 111, BB(40),BR(41),BR(42),BR(43),BR(44)
00135 13* 111 FORMAT(5E12.5)
00136 14* PRINT 5000
00140 15* 5000 FORMAT(/8X36H ANTI-OXIDANT PRICE AND EFFECTIVENESS )
00141 16* PRINT 1001,BR(44),BB(43)
00145 17* PRINT 1000
00147 18* 1000 FORMAT(/8X31H ENZYME PRICE AND EFFECTIVENESS )
00150 19* PRINT 1001,BR(41),BR(40)
00154 20* 1001 FORMAT(/8X8H PRICE =,F5.2,12H DOLLARS/LB,,F8.3,38H LB REQUIRED PE
00154 21* CR 100 LB OF PRESS CAKE )
00155 22* IF(BB(42) .GT. 0.0) PRINT 1002,BR(42)
00161 23* 1002 FORMAT(/8XF8.2,51H PERCENT OF DISSOLVED PROTEIN PACKAGED AS BCF PA
00161 24* CSTE )
00162 25* PRINT 2000
00164 26* 2000 FORMAT(1H1//55H DETAILED EQUIPMENT COSTS (ALL COSTS IN 1000.0 DOL
00164 27* CLARS) )
00165 28* PRINT 3000
00167 29* 3000 FORMAT (/18H EQUIPMENT TYPE,10X10H CAPACITY,12X9H MATERIAL,
00167 30* C60H BASE MATERIALS LABOR INDIRECT MODULE RANGE ,/6
00167 31* C0X60H COST COSTS COSTS COSTS COST + OR - )
00167 32* C
00167 33* C UNLOADING AND STORAGE OF FISH
00167 34* C
00170 35* TONSA=TONS*2000./8.*33
00171 36* GALLON= TONSA/(24.*60.)
00172 37* GALS =GALLON*1.3
00173 38* SUMHP= 0.
00174 39* IA(65,1) = 0
00175 40* IA(65,2) = 1.0
00176 41* AA(65,17)= GALS*30.
00177 42* NUM = TONS/500 + 1
00200 43* DO 143 I=1,NUM
00203 44* 143 CALL PMPREC
00205 45* IA(65,2) = 0.0

```

Table I.--Continued.

```

00206 46* SUMHP= SUMHP +(AA(65,17)*.001*1.5)
00207 47* SUMHP= SUMHP +(AA(65,17)*.001*1.5)
00210 48* IF(TONSA.LT.30000.) G=(30000./(24.*60.))*15.
00212 49* IF(TONSA.GE.30000.) G=(450000./(24.*60.))*15.
00214 50* IF(TONS.LE.150.) AA(70,1A)= 36.
00216 51* IF(TONS.GT.150.) AA(70,1A)= 48.
00220 52* AA(70,17)=100.
00221 53* CALL BELT
00222 54* HP = TONS*0.00124 +13.6
00223 55* SUMHP = HP + SUMHP
00224 56* AA(40,17)=30.0*TONS
00225 57* IA(40,1)=0.0
00226 58* IA(40,2)=2
00227 59* CALL STORAG
00230 60* IA(40,2)=0
00231 61* AA(85,17)=0.5*TONS*3.0
00232 62* IA(85,1) =30
00233 63* CALL REFRIG
00234 64* SUMHP = SUMHP + 4.72*AA(85,17)
00235 65* IA(7,1)=1
00235 66* C
00235 67* C FISH STORAGE FOR 3 DAYS
00235 68* C
00236 69* AA(7,17)=3.*TONS*2000.*1.69/62.4
00237 70* CALL SILO
00240 71* COST(1)=1.19
00241 72* IF(TONS.GE.300) COST(1)=1.88
00243 73* COST(5)=COST(1)
00244 74* PRINT 4249, COST(1), COST(5)
00250 75* COSTA(1)=COSTA(1)+COST(1)
00251 76* COSTA(5)=COSTA(5)+COST(5)
00252 77* 4249 FORMAT(/25H BRINE MAKE-UP+SALT STOR., 10X ,15H
00252 78* 1 ,F10.3,30X,F10.3)
00252 79* C
00252 80* C PUMP FOR BRINE MAKE-UP (BRONZF)
00252 81* C
00253 82* IA(66,1)=1
00254 83* AA(66,17)=TONS*3.*2000./(24.*60.*62.4)*.69*7.75
00255 84* CALL PMPCNT
00256 85* IA(66,1)=0
00257 86* HP=.0010*AA(66,17)
00260 87* SUMHP=SUMHP+HP
00260 88* C
00260 89* C PUMP FOR WATER INTO BRINE MAKE-UP
00260 90* C
00261 91* AA(66,17)=AA(66,17)*.917
00262 92* IA(66,1)=0
00263 93* CALL PMPCNT
00264 94* HP=.0010*AA(66,17)
00265 95* SUMHP=SUMHP+HP
00266 96* LOOPS=0.0
00267 97* LOOPS=LOOPS+3.
00270 98* TONSG=TONS/24.
00271 99* AA(71,18)= TONSG
00272 100* AA(71,17)= 20.
00273 101* CALL BUCKET
00274 102* HP = TONS*0.00106

```

## Table I.-- Continued.

```

00275 103*          SUMHP = HP + SUMHP
00275 104*          C
00275 105*          C FISH COOKERS AND SCREW PRESS
00275 106*          C
00276 107*          AA(91,16) = 0.2*TONS
00277 108*          AA(91,10)=TONS+AA(91,16)
00300 109*          IF (TONS .GT. 450) NA=(TONS/250) +1.
00302 110*          IF (TONS .LE. 450) NA=(TONS/100) +1.
00304 111*          DO 3 I=1,NA
00307 112*          BB(2)=2.1
00310 113*          XNA = NA
00311 114*          IA(21,5)=4
00312 115*          AA(21,17)=TONS/XNA
00313 116*          CALL DRYERR
00313 117*          C PUMP TO PRESS
00314 118*          AA(66,17)=AA(91,10)*30.*2000./(24.*8.33*60.)
00315 119*          IA(66,1)=0
00316 120*          CALL PMPCNT
00317 121*          HP=.001*AA(66,17)
00320 122*          SUMHP=HP+SUMHP
00321 123*          IA(17,5)=3
00322 124*          BB(2)=2.6
00323 125*          IF (TONS .GT. 450) AA(17,17)= 21.
00325 126*          IF (TONS .GT. 450) AA(17,18)= 16.
00327 127*          IF (TONS .LE. 450) AA(17,18)= 12.
00331 128*          IF (TONS .LE. 450) AA(17,17)= 15.
00333 129*          CALL SCREWR
00334 130*          IF (TONS .GT. 450) AA(51,17)= 10.0
00336 131*          IF (TONS .LE. 450) AA(51,17)= 4.0
00340 132*          CALL SCREEN
00341 133*          3 CONTINUE
00343 134*          DRYSLD=(.8*BR(32)+.94*BB(31))*TONS
00344 135*          XLIQD=(BB(30)+BB(31)+.06*BR(31)+.2*BB(32))*TONS+AA(91,16)
00345 136*          AA(90,16)=2.86*DRYSLD
00345 137*          C
00345 138*          C FISH DIGESTION AND SCREENING
00345 139*          C
00345 140*          C
00345 141*          C SCREW CONVEYOR
00345 142*          C
00346 143*          AA(17,18)=6
00347 144*          AA(17,17)=20
00350 145*          IA(17,5)=1
00351 146*          CALL SCREWR
00352 147*          AA(90,18)=AA(91,10)-AA(90,16)
00353 148*          AA(90,5)=TONS*BB(30)*(397./500.)
00354 149*          AA(7,17)=27.4*AA(90,16)*50.
00355 150*          CALL SILO
00356 151*          AA(91,17)=AA(91,10)-AA(90,16)-AA(90,5)
00356 152*          C PUMP FOR WATER AND SLUDGE
00357 153*          AA(66,17)=AA(91,17)*2000.*30./(24.*60.*8.33)
00360 154*          IA(66,1)=0
00361 155*          CALL PMPCNT
00362 156*          HP=.001*AA(66,17)
00363 157*          SUMHP=HP+SUMHP
00364 158*          AA(90,15)=AA(90,16)*.0084
00365 159*          AA(90,13)=(BR(30)+BR(31)+BR(32))*TONS*.0001

```

Table I.-- Continued.

```

nn366 160* AA(90,17)=TONS*0.022
nn367 161* AA(90,12)=AA(90,16)*RB(40)/100.0
nn370 162* AA(91,1)=AA(90,16)+AA(90,17)+AA(90,15)+AA(90,12)+AA(91,17)+AA(90,1
nn370 163* C3)
nn371 164* VOLT=AA(91,1)*2000/(8.33*4.8)
nn372 165* AA(51,2)=2.0
nn373 166* AA(51,17)=2.0
nn374 167* AA(49,17)=VOLT/3
nn375 168* IF(AA(49,17) .LT. 10000) AA(73,17) = AA(49,17)*0.005
nn377 169* IF(AA(49,17) .LT. 10000) GO TO 101
nn401 170* IF( AA(49,17) .GT. 10000) AA(73,17) = 50.
nn403 171* IF(AA(49,17) .GT. 10000) AA(49,17)=10000
nn405 172* 101 CALL REACTR
nn406 173* CALL AGITOR
nn407 174* CALL SCREEN
nn410 175* CALL REACTR
nn411 176* CALL AGITOR
nn412 177* CALL SCREEN
nn413 178* CALL REACTR
nn414 179* CALL AGITOR
nn415 180* CALL SCREEN
nn416 181* INST = 3
nn417 182* HP = 3*AA(73,17)
nn420 183* SUMHP = HP + SUMHP
nn421 184* VOLD =VOLT -AA(49,17)*3
nn422 185* 102 IF(VOLD .LT. 500) GO TO 103
nn424 186* IF(VOLD .LT. 10000) AA(49,17)=VOLD
nn426 187* IF(AA(49,17) .LT. 10000) AA(73,17) = AA(49,17)*0.005
nn430 188* IF(VOLD .GT. 10000) AA(49,17)=10000
nn432 189* IF( AA(49,17) .GT. 10000) AA(73,17) = 50.
nn434 190* CALL REACTR
nn435 191* CALL AGITOR
nn436 192* CALL SCREEN
nn437 193* INST = INST + 1
nn440 194* VOLD = VOLD -AA(49,17)
nn441 195* HP = AA(73,17)
nn442 196* SUMHP = HP + SUMHP
nn443 197* GO TO 102
nn444 198* 103 CONTINUE
nn444 199* C
nn444 200* C BONE FEED STREAM
nn444 201* C
nn445 202* BB(2)=1.
nn446 203* SLDS=((55./667.)*RB(31))+((68./145.)*RB(32))+((103./500.)*(14./10
nn446 204* C3.)*BB(30))*TONS+((20./112.)*(AA(90,12)+AA(90,13)+AA(90,15)+AA(90
nn446 205* 1,17))*(68./145.))
nn447 206* AA(91,2)=(340./137.)*SLDS
nn447 207* C
nn447 208* C SCREW CONVEYOR
nn447 209* C
nn450 210* AA(17,18)=6
nn451 211* AA(17,17)=20
nn452 212* IA(17,5)=1
nn453 213* CALL SCREWR
nn454 214* IA(21,5)=3
nn455 215* AA(21,17)=AA(91,2)*2.5
nn456 216* CALL DRYERR

```

Table I.-- Continued.

00457 217\* AA(90,3)=1.05\*SLDS  
 00460 218\* AA(91,12)=AA(91,2)-AA(90,3)  
 00460 219\* C  
 00460 220\* C BAGGING MACHINE AND HAMMER MILL FOR BONE FEED  
 00460 221\* C  
 00461 222\* AA(75,17)=AA(90,3)\*2000./(24.\*60.\*25.)  
 00462 223\* IA(75,2)=0  
 00463 224\* IA(75,1)=0  
 00464 225\* AA(18,17)=AA(90,3)/24.  
 00465 226\* CALL HAMMER  
 00466 227\* CALL BAGGMA  
 00467 228\* AA(75,5)=AA(75,17)  
 00467 229\* C  
 00467 230\* C  
 00467 231\* C DIGESTED SOLIDS STREAM  
 00467 232\* C  
 00470 233\* AA(91,3) =AA(91,1)-AA(91,2)  
 00471 234\* AA(40,17) = AA(91,3)\*2000/(8.33\*24)  
 00472 235\* IA(40,1)=1  
 00473 236\* CALL STORAG  
 00474 237\* IA(40,1) = 0  
 00474 238\* C PUMPS BEFORE AND AFTER HOLD TANK  
 00475 239\* IA(66,1)=0  
 00476 240\* AA(66,17)=AA(40,17)\*30./60.  
 00477 241\* CALL PMPCNT  
 00500 242\* CALL PMPCNT  
 00501 243\* SUMHP=SUMHP+2.\*.001\*AA(66,17)  
 00502 244\* AA(91,6)=AA(91,3)  
 00503 245\* PR0D=((612./667.)\*BB(31))+((89./103.)\*(103./500.)\*BB(30))+((77./1  
 00503 246\* C45.)\*BB(32))\*TONS+((20./112.)\*(AA(90,12)+AA(90,13)+AA(90,15)+AA(9  
 00503 247\* 10,17))\*(77./145.))  
 00504 248\* WATER=AA(91,3)-PR0D  
 00505 249\* WATEVP =WATER-PR0D  
 00506 250\* HP=.01\*AA(91,3)\*2000./(8.33\*24.)  
 00507 251\* SUMHP=HP+SUMHP  
 00510 252\* AA(91,13)=WATEVP  
 00511 253\* AA(31,17)=AA(91,13)\*2000./(24.\*25)  
 00512 254\* CALL EVPFLM  
 00512 255\* C  
 00512 256\* C HOLD TANK FOR DIGESTED SOLIDS  
 00512 257\* C  
 00513 258\* AA(91,7)=2.\*PR0D  
 00514 259\* AA(40,17)=AA(91,7)\*2000./(8.33\*24.)  
 00515 260\* IA(40,1)=0  
 00516 261\* CALL STORAG  
 00516 262\* C PUMP AFTER WIPEO FILM EVAPORATOR  
 00517 263\* AA(66,17)=AA(40,17)\*30./60  
 00520 264\* IA(66,1)=0  
 00521 265\* CALL PMPCNT  
 00522 266\* HP=.001\*AA(66,17)  
 00523 267\* SUMHP=HP+SUMHP  
 00524 268\* AA(90,6)=AA(91,7)\*RB(42)\*.01  
 00524 269\* C PUMP BEFORE CANNING MACHINE  
 00525 270\* AA(66,17)=AA(90,6)\*2000.\*30./(8.33\*24.\*60.)  
 00526 271\* IF(BB(42).GT.0.0) CALL PMPCNT  
 00530 272\* HP=.001\*AA(66,17)  
 00531 273\* SUMHP=HP+SUMHP

## Table I.-- Continued.

```

00532 274*      AA(75,17)=AA(90,6)*2000.0/(8.33*24.0*60.0*5.0)
00533 275*      IA(75,1)=1.0
00534 276*      IA(75,2)=2.0
00535 277*      IF(BB(42).GT.0.0) CALL RAGGMA
00537 278*      AA(75,4)=AA(75,17)
00540 279*      IA(75,1)=0.0
00541 280*      IA(75,2)=0.0
00542 281*      AA(75,4)=AA(75,4)*60.*24.
00543 282*      AA(91,9)=AA(91,7)-AA(90,6)
00544 283*      AA(90,7)=AA(91,9)/(2.*.95)
00544 284*      C PUMP BEFORE SPRAY DRYER
00545 285*      AA(66,17)=AA(90,7)*2000.*30./(8.33*60.*24.)
00546 286*      IA(66,1)=0
00547 287*      CALL PMPCNT
00550 288*      HP=.001*AA(66,17)
00551 289*      SUMHP=HP+SUMHP
00552 290*      AA(91,14)=AA(91,9)-AA(90,7)
00553 291*      AA(30,17)=AA(91,14)*2000.0/24.0
00554 292*      CALL EVPSPR
00555 293*      AA(75,17)=(AA(75,17)+AA(75,5))*60.*24.
00556 294*      IF(BB(42).GT.100) CALL RAGGMA
00560 295*      AA(75,17)=AA(75,17)*60.*24.
00560 296*      C
00560 297*      C FISH OIL STREAM
00560 298*      C
00561 299*      AA(40,17)=AA(90,18)*2000/(8.33*24)
00562 300*      IA(40,1) = 0
00563 301*      CALL STORAG
00563 302*      C PUMPS AFTER SCREFN AND BEFORE CENTRIFUGE
00564 303*      AA(66,17)=AA(40,17)*30./60.
00565 304*      IA(66,1)=0
00566 305*      CALL PMPCNT
00567 306*      CALL PMPCNT
00570 307*      HP=.001*AA(66,17)
00571 308*      SUMHP=HP+SUMHP
00572 309*      SUMHP=HP+SUMHP
00573 310*      AA(91,4) = 1.1*AA(90,5)
00574 311*      HP = 0.01*AA(90,18)*2000.0/(8.33*24.0)
00575 312*      SUMHP =HP+SUMHP
00576 313*      NUM = HP/20. +1
00577 314*      DO 40 I=1,NUM
00602 315*      AA(52,17)=20.
00603 316*      40 CALL SHARP
00605 317*      AA(40,17) = AA(91,4)*2000/(8.33*24)
00606 318*      CALL STORAG
00606 319*      C PUMP BEFORE AND AFTER HOLD TANK
00607 320*      AA(66,17)=AA(40,17)*30./60.
00610 321*      IA(66,1)=0
00611 322*      CALL PMPCNT
00612 323*      CALL PMPCNT
00613 324*      HP=.001*AA(66,17)
00614 325*      SUMHP=HP+SUMHP
00615 326*      SUMHP=HP+SUMHP
00616 327*      HP = 0.025*AA(91,4)*2000.0/(8.33*24.0)
00617 328*      SUMHP =HP+SUMHP
00620 329*      NUM= HP/20. +1
00621 330*      DO 30 I=1,NUM

```

Table I.-- Continued.

00624 331\* AA(52,17) = 20.0  
 00625 332\* 30 CALL SHARP  
 00625 333\* C  
 00625 334\* C FISH OIL STORAGE (15 DAYS)  
 00625 335\* C  
 00627 336\* AA(40,17) = AA(90,5) \* 2000. / R. 33 \* 15.  
 00630 337\* IA(40,1) = 0.0  
 00631 338\* CALL STORAG  
 00632 339\* AA(66,17) = AA(90,5) \* 30.0 \* 2000.0 / (8.33 \* 24 \* 60)  
 00633 340\* SUMHP = SUMHP + (AA(66,17) \* 0.001)  
 00634 341\* IA(66,1) = 1  
 00635 342\* CALL PMPCNT  
 00635 343\* C  
 00635 344\* C SUMMATION OF STEAM, WATER AND ELECTRICITY  
 00635 345\* C  
 00636 346\* AA(91,15) = (AA(91,11) + AA(91,12) + AA(91,13) + AA(91,14)) \* 1.05 +  
 00636 347\* C 1.05 \* (AA(91,16) + AA(91,18) + AA(91,19))  
 00637 348\* AA(27,17) = AA(91,15) \* 2000.0 / 24  
 00640 349\* CALL BOILER  
 00640 350\* C  
 00640 351\* C BOILER WATER TREATMENT  
 00640 352\* C  
 00641 353\* COST(1) = 1.000  
 00642 354\* COST(5) = COST(1)  
 00643 355\* PRINT 4242, COST(1), COST(5)  
 00647 356\* 4242 FORMAT(/25H BOILER WATER TREATMENT , 10X , 15H , 10H  
 00647 357\* 1 , F10.3, 3X, F10.3)  
 00650 358\* COSTA(5) = COSTA(5) + COST(5)  
 00651 359\* COSTA(1) = COSTA(1) + COST(1)  
 00651 360\* C  
 00651 361\* C FUEL OIL STORAGE (15 DAYS)  
 00651 362\* C  
 00652 363\* IA(40,1) = 2  
 00653 364\* AA(40,17) = AA(27,17) / R. 33 \* 24 \* .0012 \* 15.  
 00654 365\* CALL STORAG  
 00655 366\* AA(66,1) = 0  
 00656 367\* AA(66,17) = 30. \* AA(40,17) / (15. \* 60.)  
 00657 368\* CALL PMPCNT  
 00660 369\* HP = .0010 \* AA(66,17)  
 00661 370\* SUMHP = SUMHP + HP  
 00661 371\* C  
 00661 372\* C SEA WATER PUMPS  
 00661 373\* C  
 00662 374\* AA(90,10) = 4. \* 8.33 \* (AA(91,13) + AA(91,14) + AA(91,18) + AA(91,19)) \* 1.2  
 00663 375\* AA(66,17) = AA(90,10) \* 2000.0 / (8.33 \* 24 \* 60 \* 0.066)  
 00664 376\* IA(66,1) = 1  
 00665 377\* IA(66,4) = 2  
 00666 378\* CALL PMPCNT  
 00667 379\* IA(66,4) = 0  
 00670 380\* IA(66,1) = 0  
 00671 381\* SUMHP = SUMHP + (AA(66,17) \* .001 \* 1.5)  
 00672 382\* AA(90,9) = 1.1 \* (3 \* TONS + AA(90,15) / .15 + 0.1 \* AA(91,4) + AA(91,16))  
 00673 383\* XLOOPS = LOOPS + 18. + 3. \* INST \* NA  
 00674 384\* COST(1) = XLOOPS \* AA(100,1)  
 00675 385\* COST(5) = COST(1)  
 00676 386\* COSTA(1) = COSTA(1) + COST(1)  
 00677 387\* COSTA(5) = COSTA(5) + COST(5)

## Table I.-- Continued.

```

00700 388*          PRINT 1050 COST(1),COST(5)
00704 389* 1050 FORMAT(/ 25H CONTROL INSTRUMENTATION , 10X ,15H          ,10H
00704 390*          1          ,F10.3,30X,F10.3)
00705 391*          AA(8,17) = TONS
00706 392*          CALL CONDEN
00707 393*          AA(72,17) = 1R.
00710 394*          CALL SCALE
00711 395*          CALL SCALE
00712 396*          CALL SCALE
00713 397*          CALL SCALE
00714 398*          COST(1)=AA(100,2)
00715 399*          COST(5)=COST(1)
00716 400*          COSTA(1)=COST(1)          + COSTA(1)
00717 401*          COSTA(5)=COSTA(5) + COST(5)
00720 402*          PRINT 1051, COST(1),COST(5)
00724 403* 1051 FORMAT(/ 25H PAYLOADFR AND FORK LIFT , 10X ,15H          ,10H
00724 404*          1          ,F10.3,30X,F10.3)
00725 405*          PRINT 1041,(COSTA(J),J=1.6)
00733 406* 1041 FORMAT(/25H TOTAL COSTS          ,35X6F10.3)
00734 407*          COSTA(7)=0.02*COSTA(1)
00735 408*          AA(100,10)=COSTA(5)
00735 409* C
00735 410* C MATERIAL BALLANCE INFORMATION PRINTOUT. ALL STREAMS HERE TN LB/HR
00735 411* C
00736 412*          AA(90,2)= SUMHP* .7457 * 24.
00737 413*          AA(90,10)=AA(90,10)*2000./(24.*8.33)
00740 414*          CALL MATER(TONS)
00741 415*          DO 50 I=1,20
00744 416*          AA(90,I)=AA(90,I)*2000/24
00745 417* 50          AA(91,I)=AA(91,I)*2000/24
00747 418*          FISH=TONS*2000/24
00750 419*          PRINT 1003,FISH
00753 420* 1003 FORMAT(/8X26H FISH FED TO COOKERS          ,F8.0,7H LB/HR )
00754 421*          PRINT 1004,AA(91,16)
00757 422* 1004 FORMAT(/8X26H COOKERS STEAM          ,F8.0,7H LB/HR )
00760 423*          PRINT 1005,AA(90,16)
00763 424* 1005 FORMAT(/8X26H PRECS CAKE TO DIGESTERS          ,F8.0,7H LB/HR )
00764 425*          PRINT 1006,AA(91,17)
00767 426* 1006 FORMAT(/8X26H FISH SOL. TO DIGESTERS          ,F8.0,7H LB/HR )
00770 427*          PRINT 1007,AA(90,12)
00773 428* 1007 FORMAT(/8X26H ENZYME TO DIGESTERS          ,F8.2,7H LB/HR )
00774 429*          PRINT 1008,AA(90,15)
00777 430* 1008 FORMAT(/8X26H CAOH TO DIGESTERS          ,F8.2,7H LB/HR )
01000 431*          PRINT 1017,AA(90,13)
01003 432* 1017 FORMAT(/8X26H ANTIoxidANT TO DIGESTERS          ,F8.2,7H LB/HR )
01004 433*          PRINT 1033,AA(90,17)
01007 434* 1033 FORMAT(/8X26H 5N NaOH TO DIGESTERS          ,F8.2,7H LB/HR )
01010 435*          PRINT 1009,AA(91,2)
01013 436* 1009 FORMAT(/8X26H FEED TO ROTARY DRYER          ,F8.0,7H LB/HR )
01014 437*          PRINT 1010,AA(91,12)
01017 438* 1010 FORMAT(/8X26H ROTARY DRYFR STEAM          ,F8.0,7H LB/HR )
01020 439*          PRINT 1011,AA(90,3)
01023 440* 1011 FORMAT(/8X26H BONF FFED PRODUCT          ,F8.0,7H LB/HR )
01024 441*          PRINT 1012,AA(91,3)
01027 442* 1012 FORMAT(/8X26H DIGESTFR LIQUOR          ,F8.0,7H LB/HR )
01030 443*          PRINT 1013,AA(91,6)
01033 444* 1013 FORMAT(/8X26H FEED TO FIM EVAPORATOR          ,F8.0,7H LB/HR )

```

## Table I.--Continued.

```

01034 445*          PRINT 1014,AA(91,13)
01037 446*    1014  FORMAT(/8X26H FILM EVAPORATOR STEAM ,F8.0,7H LB/HR )
01040 447*          COOL =AA(91,13)*4
01041 448*          PRINT 1015,COOL
01044 449*    1015  FORMAT(/8X26H FILM EVAPORATOR COOLING ,F8.0,7H,GAL/HR )
01045 450*          PRINT 1016,AA(91,7)
01050 451*    1016  FORMAT(/8X26H FISH PASTE ,F8.0,7H LB/HR )
01051 452*          AA(90,13)=0.05*AA(91,7)*n.01
01052 453*          PRINT 1018,AA(90,6)
01055 454*    1018  FORMAT(/8X26H PACKAGED AC FISH PASTE ,F8.0,7H LB/HR )
01056 455*          PRINT 1019,AA(91,9)
01061 456*    1019  FORMAT(/8X26H FEED TO SPRAY EVAPORATOR ,F8.0,7H LB/HR )
01062 457*          PRINT 1020,AA(91,14)
01065 458*    1020  FORMAT(/8X26H SPRAY EVAPORATOR STEAM ,F8.0,7H LB/HR )
01066 459*          COOL=4*AA(91,14)
01067 460*          PRINT 1021,COOL
01072 461*    1021  FORMAT(/8X26H SPRAY EVAP. COOLING ,F8.0,7H GAL/HR )
01073 462*          PRINT 1022,AA(90,7)
01076 463*    1022  FORMAT(/8X26H DRY CONCENTRATE ,F8.0,7H LB/HR )
01077 464*          PRINT 1023,AA(90,5)
01102 465*    1023  FORMAT(/8X26H FISH OIL ,F8.0,7H LB/HR )
01103 466*          STEAM=AA(27,17)-AA(91,12)-AA(91,13)-AA(91,14)-AA(91,18)-AA(91,19)
01103 467*          C-AA(91,16)
01104 468*          PRINT 1030,STEAM
01107 469*    1030  FORMAT(/8X26H MISCELLANEOUS STEAM ,F8.0,7H LB/HR )
01110 470*          AA(90,9)=AA(90,9)/8.33
01111 471*          PRINT 1031,AA(90,9)
01114 472*    1031  FORMAT(/8X26H CITY WATER ,F8.0,7H GAL/HR )
01115 473*          AA(90,10)=AA(90,10)*24./2n00.
01116 474*          PRINT 1032,AA(90,10)
01121 475*    1032  FORMAT(/8X26H PROCESS WATER ,F8.0,7H GAL/HR )
01122 476*          AA(90,1) = AA(27,17)*24*n.0112
01123 477*          AA(90,2) = SIMHP* .7457 * 24.
01124 478*          AA(90,3) = AA(90,3)*24/2n00
01125 479*          AA(90,5) = AA(90,5)*24/2n00
01126 480*          AA(90,6) = AA(90,6)*24/2n00
01127 481*          AA(90,7) = AA(90,7)*24/2n00
01130 482*          IXX =(14.0*(TONS/50.0)**.31) +0.5
01131 483*          PXX =IXX
01132 484*          AA(90,8) =IXX*8.0
01133 485*          AA(90,9) =AA(90,9)*24
01134 486*          AA(90,12)=AA(90,12)*24
01135 487*          AA(90,13)=AA(90,13)*24
01136 488*          AA(90,15)=AA(90,15)*24
01137 489*          AA(90,17)=AA(90,17)*24
01140 490*          RETURN
01141 491*          END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S HOPPER,HOPPER  
FOR S9A-07/12-11:04 (0,)

SUBROUTINE HOPPER ENTRY POINT 00007\*

STORAGE USED: CODE(1) 000100; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NIO1\$  
0010 NIO2\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000043	116G	0001	000055	125G	0003 R	000000	AA	0003 R	004704	BB
0004 R	000000	COST	0004 R	000007	COSTA	0000 I	000001	I	0003	003720	IA	0000	000021	INJP\$
0000 I	000000	IX	0000 I	000002	J									

```

00101      1*      SUBROUTINE HOPPER
00103      2*          IX = 6
00104      3*      COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00105      4*      COMMON /BLOCK2/ COST(7),COSTA(7)
00106      5*      COST(1) = COST(1)*AA(IX,18)
00107      6*      COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00110      7*      COST(2) = COST(1)*AA(IX,11)
00111      8*      COST(3) = COST(1)*AA(IX,12)
00112      9*      COST(4) = COST(1)*AA(IX,13)
00113     10*      COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114     11*      COST(6) = COST(5)*AA(IX,15)
00115     12*      DO 1 I=1,6
00120     13*          1 COSTA(I)=COST(I)+COSTA(I)
00122     14*          PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00131     15*      1000 FORMAT(/25H CONICAL HOPPER          ,F10.3,15H CUBIC FT.          ,10H
00131     16*          C SST          ,6F10.3)
00132     17*      RETURN
00133     18*      END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

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# Table I.-- Continued.

FOR,S SILO,SILO  
FOR S9A-07/12-11:04 (0,)

SUBROUTINE SILO ENTRY POINT 000116

STORAGE USED: CODE(1) 000122; DATA(0) 000050; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0000	000020	1001F	0001	000047	1206	0001	000063	1306	0001	000101	1406	
0003	R	000000	AA	0003	R	004704	BB	0004	R	000000	COST	0004	R	000007	COSTA
0003	I	003720	IA	0000	000040	INJPS	0000	I	000000	IX	0000	I	000002	J	

```

00101    1*      SUBROUTINE SILO
00103    2*      IX=7
00104    3*      COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00105    4*      COMMON/BLOCK2/ COST(7),COSTA(7)
00106    5*      IF(IA(7,1).EQ.1) AA(7,11)=0.20
00110    6*      COST(1)= BB(1)* AA(7,7)*AA(7,17)**AA(7,8)
00111    7*      COST(1)= .001* COST(1)
00112    8*      COST(2) = COST(1)* AA(7,11)
00113    9*      COST(3)= COST(1)* AA(7,12)
00114   10*      COST(4)= COST(1)* AA(7,13)
00115   11*      COST(5)= COST(1)+ COST(2)+COST(3) +COST(4)
00116   12*      COST(6)= COST(1)*AA(7,15)
00117   13*      DO 1 I =1,7
00122   14*          1 COSTA(I)=COST(I) + COSTA(I)
00124   15*          IF(IA(7,1).EQ.0) PRINT 1000 ,AA(7,17),(COST(I),I=1,6)
00134   16*          IF(IA(7,1).EQ.1) PRINT 1001,AA(7,17),(COST(J),J=1,6)
00144   17*      1000 FORMAT(/ 25H STORAGEE BIN           ,F10.3,15H GALLONS X E+03,10H
00144   18*          1 STEEL           ,6F10.3)
00145   19*      1001 FORMAT(/25H REDWOOD STORAGEE BIN     ,F10.0,15H CUBIC FEET   ,10H
00145   20*          CREDWOOD        ,6F10.3 )
00146   21*      RETURN
00147   22*      END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

@FOR,S CONDENS CONDENS  
FOR S9A-07/12-11:04 (0,)

SUBROUTINE CONDENS ENTRY POINT 000065

STORAGE USED: CODE(1) 000071; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000036	116G	0001	000050	125G	0003 R	000000	AA	0003 R	004704	BB
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I	0003	003720	IA
0000	I	000000	IX	0000	I	000002	J					0000	000022	INJP\$

```

00101      1*      SUBROUTINE CONDENS
00103      2*      IX=8
00104      3*      COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00105      4*      COMMON/BLOCK2/ COST(7),COSTA(7)
00106      5*      COST(1)=BB(1)*AA(8,7)*AA(8,17)**AA(8,8)
00107      6*      COST(1) = COST(1)*0.001
00110      7*      COST(2) = COST(1) * AA(8,11)
00111      8*      COST(3) = COST(1) * AA(8,12)
00112      9*      COST(4) = COST(1) * AA(8,13)
00113     10*      COST(5)= COST(1)+ COST(2) + COST(3) + COST(4)
00114     11*      COST(6)= COST(1)*AA(8,15)
00115     12*      DO 1 I= 1,7
00120     13*          1 COSTA(I) = COSTA(I) + COST(I)
00122     14*      PRINT 1000, AA(8,17), (COST(J),J=1,6)
00131     15*      1000 FORMAT(/ 25H SCRUBBERS ,F10.3,15H TONS PROCESSED,10H
00131     16*          1 STEEL ,6F10.3)
00132     17*      RETURN
00133     18*      END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

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Table I.-- Continued.

FOR,S PULVER,PULVER  
FOR S9A-07/12-11:04 (0,)

SUBROUTINE PULVER ENTRY POINT 000073

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000043	117G	0001	000055	126G	0003 R	000000	AA	0003 R	004704	BB
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I	0003	003720	IA
0000	I	000000	IX	0000	I	000002	J					0000	000022	INJP\$

```

00101 1* SUBROUTINE PULVER
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=11
00106 5* 1000 FORMAT(/ 25H PULVERIZER ,F10.3,15H POUNDS/HOUR ,10H
00106 6* 1 SS ,6F10.3)
00107 7* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00110 8* COST(1)=COST(1)*.001
00111 9* COST(2)= COST(1)*AA(IX,11)
00112 10* COST(3)= COST(1)*AA(IX,12)
00113 11* COST(4)= COST(1)*AA(IX,13)
00114 12* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00115 13* COST(6)= COST(5)*AA(IX,15)
00116 14* DO 1 I=1,6
00121 15* 1 COSTA(I)=COST(I)+COSTA(I)
00123 16* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00132 17* RETURN
00133 18* END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S SCREWR,SCREWR  
FOR S9A-07/12-11:04 (0,)

SUBROUTINE SCREWR ENTRY POINT 000246

STORAGE USED: CODE(1) 000257; DATA(0) 000126; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000052	1000F	0000	000020	1001F	0000	000003	1002F	0000	000035	1006F	0001	000212	13L
0001	000224	14L	0001	00017	140G	0001	000135	150G	0001	000161	162G	0001	000201	174G
0001	000220	206G	0001	000036	31L	0003 R	000000	AA	0003 R	004704	BB	0004 R	000000	COST
0004 R	000007	COSTA	0000 I	000001	I	0003 I	003720	IA	0000	000105	INJP\$	0000 I	000000	IX
0000 I	000002	J												

```

00101    1*    SUBROUTINE SCREWR
00103    2*    COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104    3*    COMMON/BLOCK2/ COST(7), COSTA(7)
00105    4*    IX=17
00106    5*    IF(AA(IX,18).LT.6.1) GO TO 31
00110    6*    AA(17,7) = 270.
00111    7*    AA(17,8) = 0.80
00112    8*    IF(AA(IX,18).LT.12.1) GO TO 31
00114    9*    AA(17,7) = 290.
00115   10*    AA(17,8) = 0.75
00116   11*    IF(AA(IX,18).LT.14.1) GO TO 31
00120   12*    AA(17,7) = 300.
00121   13*    AA(17,8) = 0.60
00122   14*    31 CONTINUE
00123   15*    IF(IA(17,5).EQ.2) BB(2) = 5.0
00125   16*    IF(IA(17,5).EQ.5) BB(2) = 5.3
00127   17*    COST(1) = BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00130   18*    COST(1) = COST(1)*.001
00131   19*    COST(1) = BB(2)*COST(1)
00132   20*    COST(2) = COST(1)*AA(IX,11)
00133   21*    COST(3) = COST(1)*AA(IX,12)
00134   22*    COST(4) = COST(1)*AA(IX,13)

```

Table I.-- Continued.

```

00135 23*      COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00136 24*      COST(6)= COST(1)*AA(IX,15)
00137 25*      DO 1 I=1,6
00142 26*      1 COSTA(I)=COST(I)+COSTA(I)
00144 27*      IF(IA(17,5).EQ.5) PRINT 1006, AA(17,17),(COST(J),J=1,6)
00154 28*      IF(IA(17,5).EQ.5) GO TO 14
00156 29*      IF(IA(17,5).EQ.3) PRINT 1002,AA(IX,17),(COST(J),J=1,6)
00166 30*      IF(IA(17,5).EQ.3) GO TO 14
00170 31*      1002 FORMAT(/25H SCREW PRESS           ,F10.0,15H FEET           ,10H
00170 32*      C SST           ,6F10.3)
00171 33*      PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00200 34*      IF(IA(17,5).EQ.2) GO TO 13
00202 35*      GO TO 14
00203 36*      13 PRINT 1001,AA(17,17),(COST(J),J=1,6)
00212 37*      1001 FORMAT(/ 25H SCREW PRESS           ,F10.3,15H FEET           ,10H
00212 38*      1 STEEL           ,6F10.3)
00213 39*      14 CONTINUE
00214 40*      IA(17,5) = 1
00215 41*      1006 FORMAT(/25H PULP PRESS           ,F10.3,15H FEET           ,10H
00215 42*      1 STEEL           ,6F10.3)
00216 43*      1000 FORMAT(/ 25H SCREW CONVEYER           ,F10.3,15H FEET           ,10H
00216 44*      1 SS           ,6F10.3)
00217 45*      BB(2)=1.
00220 46*      RETURN
00221 47*      END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR S HAMMER, HAMMER  
FOR S9A-07/12-11:04 (0,)

SUBROUTINE HAMMER ENTRY POINT 000107

STORAGE USED: CODE(1) 000114; DATA(0) 000034; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000057	121G	0003	000071	130G	0001	000034	2L	0003	R	000000	AA
0003	R	004704	BB	0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I
0000	000023	INJP\$	0000	I	000000	IX	0000	I	000002	J					

```

00101    1*      SUBROUTINE HAMMER
00103    2*      COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104    3*      COMMON /BLOCK2/ COST(7),COSTA(7)
00105    4*      IX = 18
00106    5*      IF(AA(18,17).LT.1.) COST(1)=.5
00110    6*      IF(AA(18,17).LT.1.) GO TO 2
00112    7*      COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00113    8*      2  COST(2)=COST(1)*AA(IX,11)
00114    9*      COST(3) = COST(1)*AA(IX,12)
00115   10*      COST(4) = COST(1)*AA(IX,13)
00116   11*      COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00117   12*      COST(6) = COST(5)*AA(IX,15)
00120   13*      DO 1 I=1,6
00123   14*      1  COSTA(I)=COST(I)+COSTA(I)
00125   15*      PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00134   16*      1000 FORMAT(/25H HAMMER MILL ,F10.3,15H TONS PER HR. ,10H
00134   17*      C SST ,6F10.3)
00135   18*      RETURN
00136   19*      END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S DRYER,DRYER  
FOR S9A-07/12-11:04 (0,)

SUBROUTINE DRYER ENTRY POINT 000073

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000043	117G	0001	000055	126G	0003	R	000000	AA	0003	R	004704	BB		
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I	0003		003720	IA	0000	000022	INJP\$
0000	I	000000	IX	0000	I	000002	J											

```

00101 1* SUBROUTINE DRYER
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=19
00106 5* 1000 FORMAT(/ 25H DRUM DRYER ,F10.3,15H SQUARE FEET ,10H
00106 6* 1 SS ,6F10.3)
00107 7* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00110 8* COST(1)=COST(1)*.001
00111 9* COST(2)= COST(1)*AA(IX,11)
00112 10* COST(3)= COST(1)*AA(IX,12)
00113 11* COST(4)= COST(1)*AA(IX,13)
00114 12* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00115 13* COST(6)= COST(5)*AA(IX,15)
00116 14* DO 1 I=1,6
00121 15* 1 COSTA(I)=COST(I)+COSTA(I)
00123 16* PRINT 1000, AA(IX,17), (COST(J),J=1,6)
00132 17* RETURN
00133 18* END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S DRYERP, DRYERP  
 FOR S9A-07/12-11:04 (0,)

SUBROUTINE DRYERP ENTRY POINT 000073

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
 0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
 0006 NPRT\$  
 0007 NIO1\$  
 0010 NIO2\$  
 0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000003	117G	0001	000055	126G	0003 R	000000	AA	0003 R	004704	BB
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I	0003	003720	IA
0000	I	000000	IX	0000	I	000002	J					0000	000022	INJPS

```

00101 1* SUBROUTINE DRYERP
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=20
00106 5* 1000 FORMAT(/ 25H PAN DRYER ,F10.3,15H SQUARE FEET ,10H
00106 6* 1 SS ,6F10.3)
00107 7* COST(1)= BB(1)*AA(TX,7)*AA(IX,17)**AA(IX,8)
00110 8* COST(1)=COST(1)*.001
00111 9* COST(2)= COST(1)*AA(TX,11)
00112 10* COST(3)= COST(1)*AA(TX,12)
00113 11* COST(4)= COST(1)*AA(TX,13)
00114 12* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00115 13* COST(6)= COST(5)*AA(TX,15)
00116 14* DO 1 I=1,6
00121 15* 1 COSTA(I)=COST(I)+COSTA(I)
00123 16* PRINT 1000, AA(IX,17), (COST(J),J=1,6)
00132 17* RETURN
00133 18* END
  
```

END OF COMPILATION: NO DIAGNOSTICS.

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Table I.-- Continued.

FOR,S DRYERR,DRYERR  
FOR S9A-07/12-11:04 (0,)

SUBROUTINE DRYERR ENTRY POINT 000300

STORAGE USED: CODE(1) 000305; DATA(0) 000153; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK2 000016  
0004 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NIO1\$  
0010 NIO2\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000052	1000F	0000	000121	1001F	0000	000067	1003F	0000	000104	1004F	0001	000073	122G
0001	000247	13L	0001	000111	132G	0001	000261	14L	0001	000127	142G	0001	000145	152G
0001	000176	171G	0001	000222	203G	0001	000242	217G	0001	000255	227G	0000	000003	3006F
0000	000020	3007F	0000	000035	3008F	0004 R	000000	AA	0004 R	004704	BB	0003 R	000000	COST
0003 R	000007	COSTA	0000 I	000001	I	0004 I	003720	IA	0000	000142	INJP\$	0000 I	000000	IX
0000 I	000002	J												

```

00101      1*      SUBROUTINE DRYERR
00103      2*      COMMON/BLOCK2/ COST(7),COSTA(7)
00104      3*      COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00105      4*      IX=21
00106      5*      COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107      6*      COST(1)=COST(1)*.001
00110      7*      COST(1)=BB(2)*COST(1)
00111      8*      COST(2)= COST(1)*AA(IX,11)
00112      9*      COST(3)= COST(1)*AA(IX,12)
00113     10*      COST(4)= COST(1)*AA(IX,13)
00114     11*      COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00115     12*      IF(IA(21,5).GE.6.AND.IA(21,5).LE.8) BB(2)=3.2*BB(2)
00117     13*      COST(1)=BB(2)*COST(1)
00120     14*      COST(6)= COST(5)*AA(IX,15)
00121     15*      DO 1 I=1,6
00124     16*      1 COSTA(I)=COST(I)+COSTA(I)
00126     17*      IF(IA(21,5).EQ.6) PRINT 3006,AA(21,17),(COST(I),I=1,6)
00136     18*      IF(IA(21,5).EQ.7) PRINT 3007,AA(21,17),(COST(I),I=1,6)
00146     19*      IF(IA(21,5).EQ.8) PRINT 3008,AA(21,17),(COST(I),I=1,6)
00156     20*      IF(IA(21,5).GE.6) GO TO 14
00160     21*      3006 FORMAT(/25H DRYER

```

,F10.3,25H AREA(SQ.FEET SST

Table I.--Continued.

```

nn160 22*      C      ,6(F10.3))
nn161 23*    3007  FORMAT(/25H STRIPPER DRYFR      ,F10.3,25H AREA(SQ.FEET SST
nn161 24*      C      ,6(F10.3))
nn162 25*    3008  FORMAT(/25H CONDITIoNER      ,F10.3,25H AREA(SQ.FEET SSTT
nn162 26*      C      ,6(F10.3))
nn163 27*      IF(IA(21,5).EQ.2) GO TO 13
nn165 28*      IF(IA(21,5).EQ.3) PRINT 1003,AA(IX,17),(COST(J),J=1,6)
nn175 29*      IF(IA(21,5).EQ.3) GO TO 14
nn177 30*      IF(IA(21,5).EQ.4) PRINT 1004,AA(IX,17),(COST(J),J=1,6)
nn207 31*      IF(IA(21,5).EQ.4) GO TO 14
nn211 32*    1000  FORMAT(/ 25H ROTARY VACUUM DRYER  ,F10.3,15H SQUARE FEET ,10H
nn211 33*      1 SS      ,6F10.3)
nn212 34*    1003  FORMAT(/ 25H STEAM TUBE DRYER    F10.3,15H SQUARE FEET ,10H
nn212 35*      1 STEEL  ,6F10.3)
nn213 36*    1004  FORMAT(/25H STEAM COOKER        ,F10.0,15H SQUARE FEET ,10H
nn213 37*      C SST      ,6F10.3)
nn214 38*      PRINT 1000, AA(IX,17),(COST(J),J=1,6)
nn223 39*      GO TO 14
nn224 40*      13 PRINT 1001,AA(21,17),(COST(J),J=1,6)
nn233 41*    1001  FORMAT(/ 25H STEAM COOKER      ,F10.3,15H SQUARE FEET ,10H
nn233 42*      1 STEEL  ,6F10.3)
nn234 43*      14 CONTINUE
nn235 44*      IA(21,5)= 1
nn236 45*      BB(2)=1.
nn237 46*      BB(3)=1.
nn240 47*      RETURN
nn241 48*      END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S BOILER,BOILER  
FOR S9A-07/12-11:04 (0,)

SUBROUTINE BOILER ENTRY POINT 000114

STORAGE USED: CODE(1) 000120; DATA(0) 000040; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NIO1\$  
0010 NIO2\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000004	1000F	0001	000060	122G	0001	000077	132G	0003 R	000000	AA	0003 R	004704	BB
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000002	I	0003	003720	IA
0000	I	000000	IX	0000	I	000003	J	0000	R	000001	S	0000	000030	INJPS

```

00101    1*      SUBROUTINE BOILER
00103    2*      COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104    3*      COMMON/BLOCK2/ COST(7),COSTA(7)
00105    4*      IX=27
00106    5*      S=AA(27,7) +(0.3*AA(27,18))
00107    6*      IF(AA(27,18).GT.150.) S= 500.
00111    7*      IF(AA(27,18).GT.300.) S= 560.
00113    8*      S=0.001*S
00114    9*      COST(1)= S*RB(1)*AA(27,17)**AA(27,8)
00115   10*      COST(2)= COST(1)*AA(27,11)
00116   11*      COST(3)= COST(1)*AA(27,12)
00117   12*      COST(4)= COST(1)*AA(27,13)
00120   13*      COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00121   14*      DO 1 I=1,6
00124   15*      COST(6)= COST(5)*AA(27,15)
00125   16*      1 COSTA(I) =COSTA(I) + COST(I)
00127   17*      PRINT 1000, AA(IX,17), (COST(J),J=1,6)
00136   18*      1000 FORMAT(/25H BOILER ,F10.3,15H POUNDS/HOUR ,10H
00136   19*      1 SS ,6F10.3)
00137   20*      RETURN
00140   21*      END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR, S EVPSPR, EVPSPR  
 FOR S9A-07/12-11:04 (0,)

SUBROUTINE EVPSPR ENTRY POINT 000070

STORAGE USED: CODE(1) 000075; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK2 000016  
 0004 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
 0006 NPRT\$  
 0007 NI01\$  
 0010 NI02\$  
 0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000040	115G	0001	000052	124G	0004 R	000000	AA	0004 R	004704	BB
0003	R	000000	COST	0003	R	000007	COSTA	0000	I	000001	T	0004	003720	IA
0000	I	000000	IX	0000	I	000002	J					0000	000021	INJP\$

```

00101      1*      SUBROUTINE FVPSPR
00103      2*      COMMON /BLOCK2/ COST(7),COSTA(7)
00104      3*      COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00105      4*      IX=30
00106      5*      COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107      6*      COST(2) = COST(1)*AA(IX,11)
00110      7*      COST(3) = COST(1)*AA(IX,12)
00111      8*      COST(4) = COST(1)*AA(IX,13)
00112      9*      COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00113     10*      COST(6) = COST(5)*AA(IX,15)
00114     11*      DO 1 I=1,6
00117     12*          1 COSTA(I)=COST(I)+COSTA(I)
00121     13*          PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00130     14*      1000 FORMAT(/25H SPRAY EVAPORATOR ,F10.2,15H LB/HR EVAP. ,10H
00130     15*          CSST ,6F10.3)
00131     16*      RETURN
00132     17*      END
  
```

END OF COMPILATION: NO DIAGNOSTICS.

100

Table I.--Continued.

FOR,S EVPFLM,EVPFLM  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE EVPFLM ENTRY POINT 000n67

STORAGE USED: CODE(1) 000073; DATA(0) 000030; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK2 000016  
0004 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000044	117G	0001	000052	124G	0004 R	000n00	AA	0004 R	0047n4	BB
0003	R	000000	COST	0003	R	0000n7	COSTA	0000	I	000002	I	0004	003720	IA
0000	I	000000	IX	0000	I	0000n1	J					0000	000021	INJPS

```

00101      1*      SUBROUTINE EVPFLM
00103      2*      COMMON /BLOCK2/ COST(7),COSTA(7)
00104      3*      COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00105      4*      IX=31
00106      5*      COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107      6*      COST(2) = COST(1)*AA(IX,11)
00110      7*      COST(3) = COST(1)*AA(IX,12)
00111      8*      COST(4) = COST(1)*AA(IX,13)
00112      9*      COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00113     10*      COST(6) = COST(5)*AA(IX,15)
00114     11*      PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00123     12*      DO 1 I=1,6
00126     13*          1 COSTA(I)=COST(I)+COSTA(I)
00130     14*      1000 FORMAT(/25H WIPED FILM EVAPORATOR ,F10.2,15H SQUARE FT. ,10H
00130     15*      CSST ,6F10.3)
00131     16*      RETURN
00132     17*      END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

101

Table I.--Continued.

@FOR,S EVPSPR,EVPSPR  
FOR S9A-07/12-11:04 (0,)

SUBROUTINE EVPSPR ENTRY POINT 000n7n

STORAGE USED: CODE(1) 000075; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK2 000016  
0004 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000040	1156	0001	000052	1246	0004 R	000000	AA	0004 R	0047n4	BB
0003	R	000000	COST	0003	R	0000n7	COSTA	0000	I	000001	I	0004	003720	IA
0000	I	000000	IX	0000	I	0000n2	J					0000	000021	INJPS

```

00101 1*      SUBROUTINE EVPSPR
00103 2*      COMMON /BLOCK2/ COST(7),COSTA(7)
00104 3*      COMMON /BLOCK1/ AA(100,20),IA(100,5),RB(100)
00105 4*      IX=30
00106 5*      COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6*      COST(2) = COST(1)*AA(IX,11)
00110 7*      COST(3) = COST(1)*AA(IX,12)
00111 8*      COST(4) = COST(1)*AA(IX,13)
00112 9*      COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00113 10*     COST(6) = COST(5)*AA(IX,15)
00114 11*     DO 1 I=1,6
00117 12*     1 COSTA(I)=COST(I)+COSTA(I)
00121 13*     PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00130 14*     1000 FORMAT(/25H SPRAY EVAPORATOR ,F10.2,15H LB/HR EVAP. ,10H
00130 15*     CSST ,6F10.3)
00131 16*     RETURN
00132 17*     END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S EVPFLM,EVPFLM  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE EVPFLM ENTRY POINT 000n67

STORAGE USED: CODE(1) 000073; DATA(0) 00003n; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK2 000016  
0004 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000044	117G	0001	000052	124G	0004 R	000000	AA	0004 R	0047n4	BB
0003	R	000000	COST	0003	R	0000n7	COSTA	0000	I	000002	I	0004	003720	IA
0000	I	000000	IX	0000	I	0000n1	J					0000	000021	INJPS

```

00101 1* SUBROUTINE EVPFLM
00103 2* COMMON /BLOCK2/ COST(7),COSTA(7)
00104 3* COMMON /BLOCK1/ AA(100,2n),IA(100,5),BB(100)
00105 4* IX=31
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(2) = COST(1)*AA(IX,11)
00110 7* COST(3) = COST(1)*AA(IX,12)
00111 8* COST(4) = COST(1)*AA(IX,13)
00112 9* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00113 10* COST(6) = COST(5)*AA(IX,15)
00114 11* PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00123 12* DO 1 I=1,6
00126 13* 1 COSTA(I)=COST(I)+COSTA(I)
00130 14* 1000 FORMAT(/25H WIPED FILM EVAPORATOR ,F10.2,15H SQUARE FT. ,10H
00130 15* CSST ,6F10.3)
00131 16* RETURN
00132 17* END
    
```

END OF COMPILATION: No DIAGNOSTICS.

Table I.-- Continued.

FOR,S STORAG,STORAG  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE STORAG ENTRY POINT 000177

STORAGE USED: CODE(1) 000204; DATA(0) 000104; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001	000012	10L	0001	000121	1001L	0000	000004	1010F	0000	000021	1011F	0000	000036	1028F	
0000	000053	1029F	0001	000064	130G	0001	000114	147G	0001	000130	157G	0001	000144	167G	
0001	000160	177G	0001	000016	20L	0001	000041	21L	0001	000151	28L	0001	000135	29L	
0001	000165	30L	0003	R	000000	AA	0003	R	004704	BB	0000	R	000001	CAST	
0004	R	000007	COSTA	0000	I	000002	I	0003	I	003720	IA	0000	000074	INJPS	
0000	I	000003	J									0000	I	000000	IX

```

00101    1*      SUBROUTINE STORAG
00103    2*      COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104    3*      COMMON /BLOCK2/ COST(7),COSTA(7)
00105    4*      AA(40,17) = AA(40,17)*C.01
00106    5*      IF (AA(40,17) .GT. 10.0) GO TO 10
00110    6*      IX = .40
00111    7*      GO TO 20
00112    8*      10  IX = 41
00113    9*      AA(41,17) = AA(40,17)
00114   10*      20  COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00115   11*      CAST = COST(1)
00115   12*      C SST MATERIAL FACTOR = AA(40,1A), INDEX = IA(40,U) = 1
00116   13*      IF (IA(40,1) - 1) 21,22,21
00121   14*      22  COST(1) = COST(1)*AA(IX,18)
00122   15*      21  COST(2) = COST(1)*AA(IX,11)
00123   16*      COST(3) = CAST*AA(IX,12)
00124   17*      COST(4) = COST(1)*AA(IX,13)
00125   18*      COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00126   19*      COST(6) = COST(5)*AA(IX,15)
00127   20*      DO 1 I=1,6
00132   21*      1  COSTA(I)=COST(I)+COSTA(I)
    
```

Table I.-- Continued.

```

00134 22*      AA(IX,17) = AA(IX,17)*100.0
00135 23*      IF(IA(40,2) .EQ. 1) GO TO 29
00137 24*      IF(IA(40,2) .EQ. 2) GO TO 28
00141 25*      IF (IA(40,1) - 1)1000,1001,1000
00144 26*      1000 PRINT 1010,AA(IX,17),(COST(J),J=1,6)
00153 27*      GO TO 30
00154 28*      1001 PRINT 1011,AA(IX,17),(COST(J),J=1,6)
00163 29*      GO TO 30
00164 30*      29  PRINT 1029,AA(IX,17),(COST(J),J=1,6)
00173 31*      GO TO 30
00174 32*      28  PRINT 1028,AA(IX,17),(COST(J),J=1,6)
00203 33*      GO TO 30
00204 34*      1010 FORMAT(/25H SHOP FAB. STORAGE TANK ,F10.0,15H GALLONS ,10H
00204 35*      C STEEL ,6F10.3)
00205 36*      1011 FORMAT(/25H SHOP FAB. STORAGE TANK ,F10.0,15H GALLONS ,10H
00205 37*      C SST ,6F10.3)
00206 38*      1028 FORMAT(/25H WATER DUMP TANK ,F10.0,15H GALLONS ,10H
00206 39*      CSTEEL ,6F10.3)
00207 40*      1029 FORMAT(/25H ACID STORAGE TANK ,F10.0,15H GALLONS ,10H
00207 41*      C SST ,6F10.3)
00210 42*      30  CONTINUE
00211 43*      RETURN
00212 44*      END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S VESSEL,VESSEL  
 FOR S9A-07/12-11:05 (0,)

SUBROUTINE VESSEL ENTRY POINT 000210

STORAGE USED: CODE(1) 000215; DATA(0) 000065; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
 0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
 0006 NPRT\$  
 0007 NIO1\$  
 0010 NIO2\$  
 0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000004	1000F	0001	000141	144G	0001	000157	156G	0001	000172	165G	0000	000021	2000F					
0001	000077	3L	0001	000105	4L	0001	000163	5L	0003	R	000000	AA	0003	R	004704	BB			
0004	R	000000	COST	0004	R	000007	COSTA	0000	R	000001	F	0000	I	000003	I	0003	I	003720	IA
0000	000054	INJP\$	0000	I	000000	IX	0000	R	000002	U									

```

00101      1*      SUBROUTINE VESSEL
00103      2*      COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104      3*      COMMON/BLOCK2/ COST(7),COSTA(7)
00105      4*      IX=42
00106      5*      IF(IA(42,3),EQ.1) F=AA(42,1)
00110      6*      IF(IA(42,3),EQ.2) F=AA(42,2)
00112      7*      IF(IA(42,3),EQ.3) F=AA(42,3)
00114      8*      U=AA(42,18)**1.6*AA(42,19)*0.132
00115      9*      IF(IA(42,2),EQ.1) COST(1)=.313*U**0.81*BB(1)
00117     10*      IF(IA(42,2),EQ.2) COST(2)=.260*U**0.759*BB(1)
00121     11*      IF(IA(42,2),NF.1) GO TO 3
00123     12*      AA(42,11)= 1.038
00124     13*      AA(42,12)= .992
00125     14*      AA(42,13)= 1.20
00126     15*      GO TO 4
00127     16*      3 AA(42,11) = 0.645
00130     17*      AA(42,12) = 0.615
00131     18*      AA(42,13) = 0.916
00132     19*      4 CONTINUE
00133     20*      COST(4)= COST(1)* AA(IX,13)
00134     21*      COST(3)= COST(1)* AA(IX,12)
00135     22*      COST(2)= COST(1)* AA(IX,11)
00136     23*      COST(1) =COST(1)*F
  
```

Table I.--Continued.

```

00137 24* COST(5)=COST(1)+COST(2)+COST(N)+COST(4)
00140 25* AA(42,17)=3.14159*.75*AA(42,18)*AA(42,18)*AA(42,19)
00141 26* COST(7)=0.
00142 27* COST(6)= COST(1)*AA(1X,1X)
00143 28* DO 1 I=1,7
00144 29* 1 COSTA(I) = COSTA(1) +COST(I)
00150 30* 1000 FORMAT(/ 25H PRESSURE VESSEL ,F10.3,14H CUBIC FEET ,10H
00151 31* 1 SS ,6F10.3)
00152 32* IF(IA(42,4).EQ.2) GO TO 5
00153 33* PRINT 1000, AA(1Y,17), (COST(I),I=1,6)
00162 34* 5 PRINT 2000, AA(1X,17),(COST(I),I=1,6)
00171 35* 2000 FORMAT(/25H DIST. COLUMN SHELL ,F10.3,15H CUBIC FEET ,10H
00171 36* 1 SS ,6F10.3)
00172 37* RETURN
00173 38* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S COLUMN,COLUMN  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE COLUMN ENTRY POINT 000157

STORAGE USED: CODE(1) 000163; DATA(0) 000044; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000005	1000F	0001	000130	136G	0001	000142	145G	0003 R	000000	AA	0003 R	004704	BB	
0004	R	000000	COST	0004	R	000007	COSTA	0000	R	000002	FM	0000	R	000001	FS
0000	I	000004	I	0003	I	003720	IA	0000		000034	INJP\$	0000	I	000000	IX

```

00101    1*      SUBROUTINE COLUMN
00103    2*      COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104    3*      COMMON/BLOCK2/ COST(7),COSTA(7)
00105    4*      IX=43
00106    5*      1000 FORMAT(/ 25H DISTI LATION COLUMN      ,F10.3,15H FEET(HIGHT)      ,10H
00106    6*      1 SS      ,6F10.3)
00107    7*      FS=1.0+ (0.4)**((24.-AA(43,18))/6.)
00110    8*      FM=AA(43,1)
00111    9*      FT=0.
00112   10*      IF(AA(43,2).GT.2.) FT=AA(43,4)
00114   11*      IF(AA(43,2).GT.4.) FT=AA(43,5)
00116   12*      IF(IA(43,3).EQ.2) FM=n.
00120   13*      IF(AA(43,17).LE.4.) AA(43,7)=8.3*(AA(43,20) )
00122   14*      IF(AA(43,17).GE.4.) AA(43,7)=AA(43,20)*(AA(43,20)+4.3)
00124   15*      COST(1)= (AA(43,17)**AA(43,8))*AA(43,7)*BB(1)*(FS+FT)
00125   16*      COST(1)=COST(1)*.001
00126   17*      COST(2)= COST(1)* AA(IX,11)
00127   18*      COST(3)= COST(1)* AA(IX,12)
00130   19*      COST(4)= COST(1)* AA(IX,13)
00131   20*      COST(7)=0.
00132   21*      COST(1)= COST(1)*(1.+FM)
00133   22*      COST(5)=COST(1)+COST(2)+COST(3)+COST(4)
00134   23*      COST(6)= COST(1)*AA(IX,15)
00135   24*      DO 1 I=1,7
    
```

Table I.--Continued.

```

nn140 25*      1 COSTA(I) = COSTA(I) +COST(I)
nn142 26*      PRINT 1000, AA(43.17),(COST(I),I=1,6)
nn151 27*      RETURN
nn152 28*      END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S REACTR,REACTR  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE REACTR ENTRY POINT 000072

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000042	116G	0001	000054	125G	0003 R	000000	AA	0003 R	004704	BB
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I	0003	003720	IA
0000	I	000000	IX	0000	T	000002	J					0000	000021	INJP\$

```

00101      1*      SUBROUTINE REACTR
00103      2*      COMMON/BLOCK1/AA(100,20),IA(100,5),BB(100)
00104      3*      COMMON/BLOCK2/ COST(7),COSTA(7)
00105      4*      IX=49
00106      5*      COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107      6*      COST(1) = COST(1)*AA(49,18)
00110      7*      COST(2) = COST(1)*AA(IX,11)
00111      8*      COST(3) = COST(1)*AA(IX,12)
00112      9*      COST(4) = COST(1)*AA(IX,13)
00113     10*      COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114     11*      COST(6) = COST(5)*AA(IX,15)
00115     12*      DO 1 I=1,6
00120     13*          1 COSTA(I)=COST(I)+COSTA(I)
00122     14*      PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00131     15*      1000 FORMAT(/25H JACKETED REACTOR VESSEL ,F10.0,15H GALLONS ,10H
00131     16*      CSST ,6F10.3)
00132     17*      RETURN
00133     18*      END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

@FOR,S GRINDR,GRINDR  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE GRINDR ENTRY POINT 000n72

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000042	116G	0001	000054	125G	0003 R	000000	AA	0003 R	004704	BB
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I	0003	003720	IA
0000	I	000000	IX	0000	I	000002	J					0000	000021	INJPS

```

00101 1* SUBROUTINE GRINDR
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX=50
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1) = COST(1)*AA(50,18)
00110 7* COST(2) = COST(1)*AA(IX,11)
00111 8* COST(3) = COST(1)*AA(IX,12)
00112 9* COST(4) = COST(1)*AA(IX,13)
00113 10* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11* COST(6) = COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(/25H FISH GRINDER ,F10.3,15H TONS/HR ,10H
00131 16* CSST ,6F10.3)
00132 17* RETURN
00133 18* END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

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Table I.-- Continued.

FOR,S SCREEN,SCREEN  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE SCREEN ENTRY POINT 000n72

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000042	116G	0001	000054	125G	0003 R	000000	AA	0003 R	004704	BB
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I	0003	003720	IA
0000	I	000000	IX	0000	I	000002	J					0000	000021	INJP5

```

00101 1* SUBROUTINE SCREEN
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX = 51
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1) = COST(1)*AA(IX,18)
00110 7* COST(2) = COST(1)*AA(IX,11)
00111 8* COST(3) = COST(1)*AA(IX,12)
00112 9* COST(4) = COST(1)*AA(IX,13)
00113 10* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11* COST(6) = COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(/25H VIBRATING SCREEN ,F10.3,15H SURFACE SQ FT.,10H
00131 16* C SST ,6F10.3)
00132 17* RETURN
00133 18* END
    
```

END OF COMPILATION:

NO DIAGNOSTICS.

Table I.-- Continued.

FOR, S SHARP, SHARP  
 FOR S9A-07/12-11:05 (0,)

SUBROUTINE SHARP ENTRY POINT 000073

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
 0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
 0006 NPRT\$  
 0007 NIO1\$  
 0010 NIO2\$  
 0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000043	116G	0001	000055	125G	0003 R	000000	AA	0003 R	004704	BB
0004 R	000000	COST	0004 R	000007	COSTA	0000 I	000001	I	0003	003720	IA	0000	000022	INJP\$
0000 I	000000	IX	0000 I	000002	J									

```

00101 1*      SUBROUTINE SHARP
00103 2*      COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3*      COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4*      IX=52
00106 5*      COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6*      COST(1)=COST(1)*.001
00110 7*      COST(2)= COST(1)*AA(IX,11)
00111 8*      COST(3)= COST(1)*AA(IX,12)
00112 9*      COST(4)= COST(1)*AA(IX,13)
00113 10*     COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00114 11*     COST(6)= COST(5)*AA(IX,15)
00115 12*     DO 1 I=1,6
00120 13*     1 COSTA(I)=COST(I)+COSTA(I)
00122 14*     PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00131 15*     1000 FORMAT(/25H SHARPIES CENTRIFUGE ,F10.3,15H HORSEPOWER ,10H
00131 16*     1 SS ,6F10.3)
00132 17*     RETURN
00133 18*     END
  
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S BOWL,BOWL  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE BOWL ENTRY POINT 000n73

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NIO1\$  
0010 NIO2\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000043	116G	0001	000055	125G	0003 R	000000	AA	0003 R	004704	BB
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I	0003	003720	IA
0000	I	000000	IX	0000	I	000002	J					0000	000022	INJPS

```

00101    1*      SUBROUTINE    BOWL
00103    2*      COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104    3*      COMMON/BLOCK2/ COST(7),COSTA(7)
00105    4*      IX=53
00106    5*      COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107    6*      COST(1)=COST(1)*.001
00110    7*      COST(2)= COST(1)*AA(IX,11)
00111    8*      COST(3)= COST(1)*AA(IX,12)
00112    9*      COST(4)= COST(1)*AA(IX,13)
00113   10*      COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00114   11*      COST(6)= COST(5)*AA(IX,15)
00115   12*      DO 1 I=1,6
00120   13*          1 COSTA(I)=COST(I)+COSTA(I)
00122   14*      PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00131   15*      1000 FORMAT(/25H SOLID BOWL CFNTRIFUGE ,F10.3,15H HORSEPOWER ,10H
00131   16*          1 SS ,6F10.3)
00132   17*      RETURN
00133   18*      END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S CNTFGE,CNTFGE  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE CNTFGE ENTRY POINT 000067

STORAGE USED: CODE(1) 000074; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRTS\$  
0007 NIO1\$  
0010 NIO2\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000037	116G	0001	000051	125G	0003	R	000000	AA	0003	R	004704	BB	
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I	0003	003720	IA	0000	000022	INJPS
0000	I	000000	IX	0000	I	000002	J										

```

00101 1* SUBROUTINE CNTFGE
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=54
00106 5* COST(1)= BB(1)*AA(54,7)*AA(54,17)**AA(54,8)
00107 6* COST(1)=COST(1)*.001
00110 7* COST(2)= COST(1)* AA(54,11)
00111 8* COST(3)= COST(1)* AA(54,12)
00112 9* COST(4)= COST(1)* AA(54,13)
00113 10* COST(5)= COST(1) + COST(2) + COST(3)+COST(4)
00114 11* COST(6)= COST(5)* AA(54,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I) =COST(I) + COSTA(I)
00122 14* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(/25H DISK TYPE CENTRIFUGE ,F10.3,15H HORSEPOWER ,10H
00131 16* 1 SS ,6F10.3)
00132 17* RETURN
00133 18* END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S BLENDR,BLENDR  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE BLENDR ENTRY POINT 000n7n

STORAGE USED: CODE(1) 000075; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NIO1\$  
0010 NIO2\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000040	115G	0001	000052	124G	0003 R	000000	AA	0003 R	004704	BB
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I	0003	003720	IA
0000	I	000000	IX	0000	I	000002	J					0000	000021	INJPS

```

00101 1*      SUBROUTINE BLENDR
00103 2*      COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3*      COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4*      IX = 57
00106 5*      COST(1) = BB(1)*AA(IX,7)*AA(IX,17)*AA(IX,8)
00107 6*      COST(2) = COST(1)*AA(IX,11)
00110 7*      COST(3) = COST(1)*AA(IX,12)
00111 8*      COST(4) = COST(1)*AA(IX,13)
00112 9*      COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00113 10*     COST(6) = COST(5)*AA(IX,15)
00114 11*     DO 1 I=1,6
00117 12*       1 COSTA(I)=COST(I)+COSTA(I)
00121 13*     PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00130 14*     1000 FORMAT(/25H SOLIDS BLENDR          ,F10.3,15H CUBIC FT / HR.,10H
00130 15*     C SST          ,6F10.3)
00131 16*     RETURN
00132 17*     END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S PMPREC,PMPREC  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE PMPREC ENTRY POINT 000210

STORAGE USED: CODE(1) 000217; DATA(0) 000107; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 AL0G  
0006 NEXP6\$  
0007 NPRT\$  
0010 NI01\$  
0011 NI02\$  
0012 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000005	1000F	0000	000022	1001F	0000	000037	1002F	0000	000054	1003F	0001	000054	11L	
0001	000060	12L	0001	000103	130G	0001	000135	14L	0001	000130	145G	0001	000151	15L	
0001	000144	155G	0001	000200	16L	0001	000160	165G	0001	000165	17L	0001	000174	175G	
0003	R	000000	AA	0003	R	004704	BB	0000	R	000002	CAST	0004	R	000000	COST
0000	R	000000	EXP	0000	I	000003	I	0003	I	000720	IA	0000	000076	INJP\$	
0000	I	000004	J									0004	R	000007	COSTA
												0000	I	000001	IX

```

00101      1*      SUBROUTINE PMPREC
00103      2*      COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104      3*      COMMON /BLOCK2/ COST(7),COSTA(7)
00105      4*      IX = 65
00106      5*      AA(IX,17) = AA(IX,17)*0.001
00107      6*      EXP = AA(IX,8) + AA(IX,9)*LOG(AA(IX,17))
00110      7*      COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**EXP
00111      8*      IF(AA(IX,17) .LT. 0.1) COST(1) = 0.9
00113      9*      CAST = COST(1)
00114     10*      IF (IA(IX,1) - 1) 10,11,10
00117     11*      10 COST(1) = COST(1)*AA(IX,19)
00120     12*      GO TO 12
00121     13*      11 COST(1) = COST(1)*AA(IX,18)
00122     14*      12 COST(2) = COST(1)*AA(IX,11)
00123     15*      COST(3) = CAST*AA(IX,12)
00124     16*      COST(4) = COST(1)*AA(IX,13)
00125     17*      COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00126     18*      COST(6) = COST(5)*AA(IX,15)
00127     19*      DO 1 I=1,6
00132     20*      1 COSTA(I)=COST(I)+COSTA(I)
    
```

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Table I.-- Continued.

```

00134 21*      AA(IX,17) = 1000.*AA(IX,17)
00135 22*      IF(IA(IX,2) .EQ. 1) GO TO 17
00137 23*      IF(IA(IX,1) - 1) 13,14,15
00142 24*      13  PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00151 25*      GO TO 16
00152 26*      14  PRINT 1001,AA(IX,17),(COST(J),J=1,6)
00161 27*      GO TO 16
00162 28*      15  PRINT 1002,AA(IX,17),(COST(J),J=1,6)
00171 29*      GO TO 16
00172 30*      17  PRINT 1003,AA(IX,17),(COST(J),J=1,6)
00201 31*      16  CONTINUE
00202 32*      1000 FORMAT(/25H RECIPROCATING PUMP      ,F10.0,15H GPM TIMES PSI ,10H
00202 33*      C STEEL      ,6F10.3)
00203 34*      1001 FORMAT(/25H RECIPROCATING PUMP      ,F10.0,15H GPM TIMES PSI ,10H
00203 35*      C BRONZE     ,6F10.3)
00204 36*      1002 FORMAT(/25H RECIPROCATING PUMP      ,F10.0,15H GPM TIMES PSI ,10H
00204 37*      C SST        ,6F10.3)
00205 38*      1003 FORMAT(/25H FISH PUMPS              ,F10.0,15H GPM TIMES PSI ,10H
00205 39*      C STEEL     ,6F10.3)
00206 40*      RETURN
00207 41*      END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

@FOR,S PMPCNT,PMPCNT  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE PMPCNT ENTRY POINT 000212

STORAGE USED: CODE(1) 000217; DATA(0) 000107; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 AL06  
0006 NEXP6\$  
0007 NPR1\$  
0010 NI01\$  
0011 NI02\$  
0012 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000022	1000F	0000	000037	1001F	0000	000054	1002F	0000	000005	1003F	0001	000054	11L	
0001	000060	12L	0001	000103	130G	0001	000151	14L	0001	000130	145G	0001	000165	15L	
0001	000144	155G	0001	000200	16L	0001	000160	166G	0001	000135	17L	0001	000174	176G	
0003	R	000000	AA	0003	R	000470	BB	0000	R	000002	CAST	0004	R	000000	COST
0000	R	000000	EXP	0000	I	000003	I	0003	I	003720	IA	0000	000076	INJP\$	
0000	I	000004	J									0004	R	000007	COSTA
												0000	I	000001	IX

```

00101      1*      SUBROUTINE PMPCNT
00103      2*      COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104      3*      COMMON /BLOCK2/ COST(7),COSTA(7)
00105      4*      IX = 66
00106      5*      AA(IX,17) = AA(IX,17)*0.001
00107      6*      EXP = AA(IX,8) + AA(IX,9)*LOG(AA(IX,17))
00110      7*      COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**EXP
00111      8*      IF(AA(IX,17) .LT. 0.1) COST(1) = 0.4
00113      9*      COST = COST(1)
00114     10*      IF (IA(IX,1) - 1) 12,11,10
00117     11*      10 COST(1) = COST(1)*AA(IX,19)
00120     12*      GO TO 12
00121     13*      11 COST(1) = COST(1)*AA(IX,18)
00122     14*      12 COST(2) = COST(1)*AA(IX,11)
00123     15*      COST(3) = COST*AA(IX,12)
00124     16*      COST(4) = COST(1)*AA(IX,13)
00125     17*      COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00126     18*      COST(6) = COST(5)*AA(IX,15)
00127     19*      DO 1 I=1,6
00132     20*      1 COSTA(I)=COST(I)+COSTA(I)
    
```

Table I.--Continued.

```

00134 21*      AA(IX,17) = 1000.0*AA(IX,17)
00135 22*      IF(IA(66,4).EQ.2) GO TO 17
00137 23*      IF(IA(IX,1) - 1) 13,14,15
00142 24*      13  PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00151 25*      GO TO 16
00152 26*      17  PRINT 1003,AA(IX,17),(COST(J),J=1,6)
00161 27*      GO TO 16
00162 28*      1003  FORMAT(/25H SEA WATER PUMPS           ,F10.3,15H GPM TIMES PSI ,10H
00162 29*      1  BRONZE      ,6F10.3)
00163 30*      14  PRINT 1001,AA(IX,17),(COST(J),J=1,6)
00172 31*      GO TO 16
00173 32*      15  PRINT 1002,AA(IX,17),(COST(J),J=1,6)
00202 33*      16  CONTINUE
00203 34*      1000  FORMAT(/25H CENTRIFUGAL PUMP           ,F10.3,15H GPM TIMES PSI ,10H
00203 35*      C  STEEL      ,6F10.3)
00204 36*      1001  FORMAT(/25H CENTRIFUGAL PUMP           ,F10.0,15H GPM TIMES PSI ,10H
00204 37*      C  BRONZE    ,6F10.3)
00205 38*      1002  FORMAT(/25H CENTRIFUGAL PUMP           ,F10.3,15H GPM TIMES PSI ,10H
00205 39*      C  SST       ,6F10.3)
00206 40*      RETURN
00207 41*      END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S HEATEX, HEATEX  
FOR S9A-07/12-11:05 (0.)

SUBROUTINE HEATEX ENTRY POINT 000164

STORAGE USED: CODE(1) 000171; DATA(0) 000101; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK2 000016  
0004 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001	000107	1001L	0001	000123	1002.	0000	000004	1010F	0000	000021	1011F	0000	000036	1013F	
0000	000053	1014F	0001	000025	11L	0001	000031	12L	0001	000060	126G	0001	000035	13L	
0001	000102	142G	0001	000116	152G	0001	000132	162G	0001	000145	174G	0001	000152	30L	
0001	000136	4L	0004	R	000000	AA	0004	R	004704	BB	0000	R	000001	CAST	
0003	R	000007	COSTA	0000	I	000002	I	0004	I	003720	IA	0000	000071	INJP\$	
0000	I	000003	J									0000	I	000000	IX

00101 1\* SUBROUTINE HEATEX  
00103 2\* COMMON /BLOCK2/ COST(7),COSTA(7)  
00104 3\* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)  
00105 4\* IX=67  
00106 5\* COST(1) = BR(1)\*AA(IX,7)\*AA(IX,17)\*\*AA(IX,8)  
00107 6\* CAST = COST(1)  
00110 7\* IF (IA(67,1) - 1) 10,11,12  
00113 8\* 10 GO TO 13  
00114 9\* 11 COST(1) = COST(1)\*AA(67,18)  
00115 10\* GO TO 13  
00116 11\* 12 COST(1) = COST(1)\*AA(67,19)  
00117 12\* GO TO 13  
00120 13\* 13 COST(2) = COST(1)\*AA(IX,11)  
00121 14\* COST(3) = CAST\*AA(IX,12)  
00122 15\* COST(4) = COST(1)\*AA(IX,13)  
00123 16\* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)  
00124 17\* COST(6) = COST(5)\*AA(IX,15)  
00125 18\* DO 1 I=1,6  
00130 19\* 1 COSTA(I)=COST(I)+COSTA(I)  
00130 20\* C MATERIAL FACTORS IA(67,1) = 0.1\*2 IMPLIES SHELL/TUBE =ST/ST,ST/SST  
00130 21\* C AND SST/SST

Table I.-- Continued.

```

nn132 22*      IF(IA(67,4),FQ,4) GO TO 4
nn134 23*      IF (IA(67,1) - 1) 1n00,1n01,1n02
nn137 24*      1000 PRINT 1010,AA(IX,17),(COST(J),J=1,6)
nn146 25*      GO TO 30
nn147 26*      1001 PRINT 1011,AA(IX,17),(COST(J),J=1,6)
nn156 27*      GO TO 30
nn157 28*      1002 PRINT 1013,AA(IX,17),(COST(J),J=1,6)
nn166 29*      1010 FORMAT(/25H HEAT FXCHANGFR      ,F10.3,15H SURFACE SQ FT.,10H
nn166 30*      C ST/ST      ,6F10.3)
nn167 31*      1011 FORMAT(/25H HEAT FXCHANGFR      ,F10.3,15H SURFACE SQ FT.,10H
nn167 32*      C ST/SST      ,6F10.3)
nn170 33*      1013 FORMAT(/25H HEAT FXCHANGFR      ,F10.3,15H SURFACE SQ FT.,10H
nn170 34*      C SST/SST      ,6F10.3)
nn171 35*      4 PRINT 1014,AA(IX,17),(COST(J),J=1,6)
nn200 36*      GO TO 30
nn201 37*      1014 FORMAT(/25H VENT CONDENSFR      ,F10.3,15H SURFACE SQ FT.,10H
nn201 38*      1 ST/SST      ,6F10.3)
nn202 39*      30 CONTINUE
nn203 40*      RETURN
nn204 41*      END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S BELT,BELT  
FOR S9A-07/12-11:05 (1,)

SUBROUTINE BELT ENTRY POINT 000123

STORAGE USED: CODE(1) 000130; DATA(0) 000041; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NIO1\$  
0010 NIO2\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000004	1000F	0001	000071	124G	0001	000103	133G	0003 R	000000	AA	0003 R	004704	BB
0004 R	000000	COST	0004 R	000007	COSTA	0000 I	000002	I	0003	003720	IA	0000	000027	INJPS
0000 I	000000	IX	0000 I	000003	J	0000 R	000001	Q						

```

00101 1* SUBROUTINE BELT
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=70
00106 5* Q= AA(IX,7)
00107 6* IF(AA(IX,18).GT.35.) AA(IX,7)=AA(IX,7)+ 80.
00111 7* IF(AA(IX,18).GT.47.) AA(IX,7)=AA(IX,7)+ 210.
00113 8* 1000 FORMAT(/25H BELT CONVEYER ,F10.3,15H FFET(LENGTH) ,10H
00113 9* 1 ,6F10.3)
00114 10* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00115 11* COST(1)=COST(1)*.001
00116 12* COST(2)= COST(1)*AA(IX,11)
00117 13* COST(3)= COST(1)*AA(IX,12)
00120 14* COST(4)= COST(1)*AA(IX,13)
00121 15* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00122 16* COST(6)= COST(5) * AA(IX,15)
00123 17* DO 1 I = 1,6
00126 18* 1 COSTA(I) = COST(I) + COSTA(I)
00130 19* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00137 20* AA(IX,7)=Q
00140 21* RETURN
00141 22* END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

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Table I.--Continued.

FOR S BUCKET, BUCKET  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE BUCKET ENTRY POINT 000134

STORAGE USED: CODE(1) 000141; DATA(0) 000041; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000004	1000F	0001	000102	1246	0001	000114	1336	0003 R	000000	AA	0003 R	004704	BB
0004 R	000000	COST	0004 R	000007	COSTA	0000 I	000002	I	0003	003720	IA	0000	000027	INJPS
0000 I	000000	IX	0000 I	000003	J	0000 R	000001	a						

```

00101 1* SUBROUTINE BUCKET
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=71
00106 5* Q= AA(IX,7)
00107 6* 1000 FORMAT(/25H BUCKET CONVEYER ,F10.3,15H FEET(HEIGHT) ,10H
00107 7* 1 SS ,6F10.3)
00110 8* IF(AA(IX,18).GT.30..AND.AA(IX,18).LE.75.) AA(IX,7)=AA(IX,7)+180.
00112 9* IF(AA(IX,18).GT.75.) AA(IX,7)=AA(IX,7)+ 280.
00114 10* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00115 11* COST(1)=COST(1)*.001
00116 12* COST(2)= COST(1)*AA(IX,11)
00117 13* COST(3)= COST(1)*AA(IX,12)
00120 14* COST(4)= COST(1)*AA(IX,13)
00121 15* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00122 16* COST(6)= COST(5)*AA(IX,15)
00123 17* DO 1 I=1,6
00126 18* 1 COSTA(I)=COST(I)+COSTA(I)
00130 19* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00137 20* AA(IX,7)=Q
00140 21* RETURN
00141 22* END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S SCALE,SCALE  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE SCALE ENTRY POINT 000116

STORAGE USED: CODE(1) 000123; DATA(0) 000036; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NPRT\$  
0006 NIO1\$  
0007 NIO2\$  
0010 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000005	1000F	0001	000066	126G	0001	000100	135G	0003 R	000000	AA	0003 R	004704	BB	
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000003	I	0003	003720	IA	
0000	I	000002	IS	0000	I	000000	IX	0000	I	000004	J	0000 R	000001	SIZE	
													0000	000025	INJP\$

```

00101      1*          SUBROUTINE SCALE
00103      2*          COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104      3*          COMMON/BLOCK2/ COST(7),COSTA(7)
00105      4*          IX=72
00106      5*          1000 FORMAT(/ 25H SCALE                      ,F10.3,15H TONS          ,10H
00106      6*          1  SS          ,6F10.3)
00107      7*          SIZE=AA(IX,17)
00110      8*          IS = SIZE/17.9
00111      9*          IF(IS.EQ.1) COST(1)=AA(72,20)*BB(1)
00113     10*          IF(IS.EQ.2) COST(1)=AA(72,18)*BB(1)
00115     11*          IF(IS.EQ.3) COST(1)=AA(72,19)*BB(1)
00117     12*          COST(2)=      AA(72,11) * COST(1)
00120     13*          COST(3)= 0.00
00121     14*          COST(4)= AA(IX,13)*COST(1)
00122     15*          COST(5)= COST(1)+COST(2)+COST(3) +COST(4)
00123     16*          COST(6)=COST(1)*AA(IX,15)
00124     17*          COST(7)=0.
00125     18*          DO 1  I=1,7
00130     19*          1  COSTA(I)=COST(I)+COSTA(I)
00132     20*          PRINT 1000 , AA(IX,17),(COST(J),J=1,6)
00141     21*          RETURN
00142     22*          END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

@FOR,S AGITOR,AGITOR  
FOR S9A-07/12-11:05 (0,)

SUBROUTINE AGITOR ENTRY POINT 000n73

STORAGE USED: CODE(1) 000100; DATA(0) 000033; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000043	116G	0001	000055	125G	0003 R	000000	AA	0003 R	004704	BB
0004 R	000000	COST	0004 R	000007	COSTA	0000 I	000001	I	0003	003720	IA	0000	000022	INJPS
0000 I	000000	IX	0000 I	000002	J									

```

00101 1* SUBROUTINE AGITOR
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* IX=73
00106 5* COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1)=COST(1)*.001
00110 7* COST(2)= COST(1)*AA(IX,11)
00111 8* COST(3)= COST(1)*AA(IX,12)
00112 9* COST(4)= COST(1)*AA(IX,13)
00113 10* COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00114 11* COST(6)= COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000, AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(/ 25H AGITATOR-PROPELLAR ,F10.3,15H HORSEPOWER ,10H
00131 16* 1 SS ,6F10.3)
00132 17* RETURN
00133 18* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR S BALMTL BALMIL  
 FOR S9A-07/12-11:06 (0,)

SUBROUTINE BALMIL ENTRY POINT 000n72

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
 0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
 0006 NPRT\$  
 0007 NIO1\$  
 0010 NIO2\$  
 0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000042	1166	0001	000054	1256	0003 R	000000	AA	0003 R	004704	BB
0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I	0003	003720	IA
0000	I	000000	IX	0000	I	000002	J					0000	000021	INJPS

```

00101 1*      SUBROUTINE BALMIL
00103 2*      COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3*      COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4*      IX = 74
00106 5*      COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6*      COST(1) = COST(1)*AA(IX,18)
00110 7*      COST(2) = COST(1)*AA(IX,11)
00111 8*      COST(3) = COST(1)*AA(IX,12)
00112 9*      COST(4) = COST(1)*AA(IX,13)
00113 10*     COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11*     COST(6) = COST(5)*AA(IX,15)
00115 12*     DO 1 I=1,6
00120 13*       1 COSTA(I)=COST(I)+COSTA(I)
00122 14*     PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00131 15*     1000 FORMAT(/25H BALL MILL          ,F10.3,15H TONS PER HR. ,10H
00131 16*       C SST          ,6F10.3)
00132 17*     RETURN
00133 18*     END
  
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S BAGGMA,BAGGMA  
FOR S9A-07/12-11:06 (0,)

SUBROUTINE BAGGMA ENTRY POINT 000125

STORAGE USED: CODE(1) 000132; DATA(0) 000051; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0000	000020	1001F	0001	000053	120G	0001	000070	130G	0001	000107	140G					
0003	R	000000	AA	0003	R	004704	BB	0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000001	I
0003	I	003720	IA	0000		000037	INJ\$	0000	I	000000	IX	0000	I	000002	J				

```

00101      1*      SUBROUTINE BAGGMA
00103      2*      COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104      3*      COMMON/BLOCK2/ COST(7),COSTA(7)
00105      4*      IX=75
00106      5*      IF(IA(75,2).EQ.2) AA(75,7)=AA(75,1)
00110      6*      COST(1)= BB(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00111      7*      COST(1)=COST(1)*.001
00112      8*      COST(2)= COST(1)*AA(IX,11)
00113      9*      COST(3)= COST(1)*AA(IX,12)
00114     10*      COST(4)= COST(1)*AA(IX,13)
00115     11*      COST(5)= COST(1)+COST(2)+COST(3)+COST(4)
00116     12*      COST(6)= COST(5)*AA(IX,15)
00117     13*      DO 1 I=1,6
00122     14*      1 COSTA(I)=COST(I)+COSTA(I)
00124     15*      IF(IA(IX,1).EQ.0) PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00134     16*      IF(IA(IX,1).EQ.1)PRINT 1001,AA(IX,17),(COST(J),J=1,6)
00144     17*      1000 FORMAT(/ 25H BAGGING MACHINE           ,F10.3,15H BAGS/MIN           ,10H
00144     18*      1 SS           ,6F10.3)
00145     19*      1001 FORMAT(/ 25H CANNING MACHINE           ,F10.3,15H CANS/MIN           ,10H
00145     20*      CSST           ,6F10.3)
00146     21*      RETURN
00147     22*      END
    
```

Table I.--Continued.

FOR,S FILTER,FILTER  
FOR S9A-07/12-11:06 (0,)

SUBROUTINE FILTER ENTRY POINT 000n7>

STORAGE USED: CODE(1) 000077; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NIO1\$  
0010 NIO2\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000042	116G	0001	000054	125G	0003 R	000000	AA	0003 R	004704	BB
0004 R	000000	COST	0004 R	000007	COSTA	0000 I	000001	I	0003	003720	IA	0000	000021	INJPS
0000 I	000000	IX	0000 I	000002	J									

```

00101 1* SUBROUTINE FILTER
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX= 78
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* COST(1) = COST(1)*AA(IX,18)
00110 7* COST(2) = COST(1)*AA(IX,11)
00111 8* COST(3) = COST(1)*AA(IX,12)
00112 9* COST(4) = COST(1)*AA(IX,13)
00113 10* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00114 11* COST(6) = COST(5)*AA(IX,15)
00115 12* DO 1 I=1,6
00120 13* 1 COSTA(I)=COST(I)+COSTA(I)
00122 14* PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00131 15* 1000 FORMAT(/25H ROT. DRUM FILTER ,F10.3,15H SURFACE SQ.FT.,10H
00131 16* C SST ,6F10.3)
00132 17* RETURN
00133 18* END
    
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S CRANES,CRANES  
FOR S9A-07/12-11:06 (0,)

SUBROUTINE CRANES ENTRY POINT 000141

STORAGE USED: CODE(1) 000146; DATA(0) 000063; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NI01\$  
0010 NI02\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0000	000020	1001F	0000	000035	1002F	0001	000026	11L	0001	000032	12L				
0001	000055	123G	0001	000073	135G	0001	000100	14L	0001	000107	145G	0001	000114	15L				
0001	000123	155G	0001	000127	16L	0003	R	000000	AA	0003	R	004704	BB	0004	R	000000	COST	
0004	R	000007	COSTA	0000	I	000001	I	0003	I	003720	IA	0000	000053	INJP\$	0000	I	000000	IX
0000	I	000002	J															

```

00101 1* SUBROUTINE CRANES
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON /BLOCK2/ COST(7),COSTA(7)
00105 4* IX= 80
00106 5* COST(1) = BR(1)*AA(IX,7)*AA(IX,17)**AA(IX,8)
00107 6* IF (IA(80,1) - 1) 12,11,10
00112 7* 10 COST(1) = COST(1)*AA(IX,19)
00113 8* GO TO 12
00114 9* 11 COST(1) = COST(1)*AA(IX,18)
00115 10* 12 COST(2) = COST(1)*AA(IX,11)
00116 11* COST(3) = COST(1)*AA(IX,12)
00117 12* COST(4) = COST(1)*AA(IX,13)
00120 13* COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00121 14* COST(6) = COST(5)*AA(IX,15)
00122 15* DO 1 I=1,6
00125 16* 1 COSTA(I)=COST(I)+COSTA(I)
00127 17* IF (IA(80,1) - 1) 13,14,15
00132 18* 13 PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00141 19* GO TO 16
00142 20* 14 PRINT 1001,AA(IX,17),(COST(J),J=1,6)
00151 21* GO TO 16
00152 22* 15 PRINT 1002,AA(IX,17),(COST(J),J=1,6)
    
```

Table I.--Continued.

00161	23*	16	CONTINUE	
00162	24*	1000	FORMAT(/25H OVERHEAD CRANE 20FT SPAN,F10.3,15H TONS LIFT	,10H
00162	25*	C	STEEL ,6F10.3)	
00163	26*	1001	FORMAT(/25H OVERHEAD CRANE 30FT SPAN,F10.3,15H TONS LIFT	,10H
00163	27*	C	STEEL ,6F10.3)	
00164	28*	1002	FORMAT(/25H OVERHEAD CRANE 40FT SPAN,F10.3,15H TONS LIFT	,10H
00164	29*	C	STEEL ,6F10.3)	
00165	30*		RETURN	
00166	31*		END	

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR S DRAGMA, DRAGMA  
 FOR S9A-07/12-11:06 (0,)

SUBROUTINE DRAGMA ENTRY POINT 000143

STORAGE USED: CODE(1) 000151; DATA(0) 000051; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
 0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
 0006 NPRT\$  
 0007 NI01\$  
 0010 NI02\$  
 0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000110	1416	0001	000122	1506	0001	000026	2L	0001	000050	3L					
0003	R	000000	AA	0003	R	004704	BB	0004	R	000000	COST	0004	R	000007	COSTA	0000	I	000002	I
0003		003720	IA	0000		000036	INJP\$	0000	I	000000	IX	0000	R	000001	Q				

```

00101      1*      SUBROUTINE DRAGMA
00103      2*      COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104      3*      COMMON/BLOCK2/ COST(7),COSTA(7)
00105      4*      IX=81
00106      5*      Q= AA(IX,7)
00107      6*      IF(AA(81,18).GT.15.) GO TO 2
00111      7*      AA(81,11)= 0.27
00112      8*      AA(81,12)= 0.42
00113      9*      IF(AA(81,18).LE.13.) AA(81,7)=7.
00115     10*      GO TO 3
00116     11*      2 CONTINUE
00117     12*      IF(AA(81,18).LE.20.) AA(81,7)=10.
00121     13*      IF(AA(81,18).LE.18.) AA(81,7)=9.
00123     14*      AA(81,11)=0.278
00124     15*      AA(81,12)=0.382
00125     16*      3 CONTINUE
00126     17*      1000 FORMAT(/ 25H DRAG CONVEYER          ,F10.3,15H FEET          ,10H
00126     18*      1 SS          ,6F10.3)
00127     19*      COST(1)=BB(1)*AA(81,7)*AA(81,17)**AA(81,8)
00130     20*      COST(1)=COST(1)*.001
00131     21*      COST(2)= COST(1)* AA(IX,11)
00132     22*      COST(3)= COST(1)* AA(IX,12)
00133     23*      COST(4)= COST(1)* AA(IX,13)
00134     24*      COST(5)=COST(1)+COST(2)+COST(3)+COST(4)
  
```

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Table I.-- Continued.

```
00135 25*      AA(IX,15)=.1
00136 26*      COST(7)=0.
00137 27*      COST(6)= COST(1)*AA(IX,15)
00140 28*      DO 1 I=1,7
00143 29*      1  COSTA(I) = COSTA(I) +COST(I)
00145 30*      PRINT 1000, AA(IX,17), (COST(I),I=1,6)
00154 31*      AA(IX,7)=0
00155 32*      RETURN
00156 33*      END
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

@FOR,S REFRIG,REFRIG  
FOR S9A-07/12-11:06 (0,)

SUBROUTINE REFRIG ENTRY POINT 000120

STORAGE USED: CODE(1) 000125; DATA(0) 000031; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NEXP6\$  
0006 NPRT\$  
0007 NIO1\$  
0010 NIO2\$  
0011 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1000F	0001	000036	11L	0001	000042	12L	0001	000070	126G	0001	000045	13L
0001	000102	135G	0003	R	000000	AA	0003	R	004704	8B	0004	R	000000	COST
0000	I	000001	I	0003	T	003720	IA	0000	000021	INJPS	0000	I	000000	IX
											0004	R	000007	COSTA
											0000	I	000002	J

```

00101      1*      SUBROUTINE REFRIG
00103      2*      COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104      3*      COMMON /BLOCK2/ COST(7),COSTA(7)
00105      4*      IX =85
00106      5*      COST(1) = BR(1)*AA(IX,7)*AA(IX,17)*AA(IX,8)
00107      6*      IF (IA(85,1) .GT. 40) GO TO 13
00111      7*      IF (IA(85,1) .GT. 20) GO TO 11
00113      8*      IF (IA(85,1) .GT. 1) GO TO 12
00115      9*      11 COST(1) = COST(1)*AA(85,18)
00116     10*      GO TO 13
00117     11*      12 COST(1) = COST(1)*AA(85,13)
00120     12*      13 COST(2) = COST(1)*AA(IX,11)
00121     13*      COST(3) = COST(1)*AA(IX,12)
00122     14*      COST(4) = COST(1)*AA(IX,13)
00123     15*      COST(5) = COST(1) + COST(2) + COST(3) + COST(4)
00124     16*      COST(6) = COST(5)*AA(IX,15)
00125     17*      DO 1 I=1,6
00130     18*      1 COSTA(I)=COST(I)+COSTA(I)
00132     19*      PRINT 1000,AA(IX,17),(COST(J),J=1,6)
00141     20*      1000 FORMAT(/25H MECHANICAL REFRIGERAT. ,F10.3,15H TONS ,10H
00141     21*      C ,6F10.3)
00142     22*      RETURN
00143     23*      END
    
```

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Table I.--Continued.

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S WATER,MATER  
FOR S9A-07/12-11:06 (0,)

SUBROUTINE MATER ENTRY POINT 000113

STORAGE USED: CODE(1) 000121; DATA(0) 000151; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0004 NPRT\$  
0005 NI02\$  
0006 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0001	000002	105G	0000	000005	1050F	0000	000020	1051F	0000	000031	1052F	0000	000045	1053F	
0000	000061	1054F	0000	000075	1055F	0000	000106	1056F	0000	000117	1057F	0000	000130	1058F	
0003	R	000000	AA	0000	R	000003	ASH	0003	R	004704	BB	0000	I	000000	I
0000	000141	INJPs	0000	R	000001	OIL	0000	R	000002	PROT	0000	R	000004	WATER	

```

00101 1* SUBROUTINE MATER(TONS)
00103 2* COMMON/BLOCK1/AA(100,20),IA(100,5),BB(100)
00104 3* DO 10 I=30,32
00107 4* 10 BB(I)=BB(I)*100.0
00111 5* PRINT 1050
00113 6* 1050 FORMAT(1H1//20X33H MATERIAL AND ENERGY INFORMATION ,//5X8H GFNERA
00113 7* CL)
00114 8* PRINT 1051,TONS
00117 9* 1051 FORMAT(/8X26H FISH =,F9.3,9H TONS/DAY)
00120 10* OIL =TONS*BB(30)*0.01
00121 11* PROT =TONS*BB(31)*0.01
00122 12* ASH =TONS*BB(32)*0.01
00123 13* PRINT 1052,BB(30),OIL
00127 14* PRINT 1053,BB(31),PROT
00133 15* PRINT 1054,BB(32),ASH
00137 16* 1052 FORMAT(/8X10H OF WHICH ,F6.2,12H PERCENT OR,FR.3,20H - '' - IS
00137 17* C OIL )
00140 18* 1053 FORMAT( 8X10H ,F6.2,12H - ''- OR,FR.3,20H - ''-
00140 19* C PROTEIN)
00141 20* 1054 FORMAT( 8X10H ,F6.2,12H - ''- OR,FR.3,20H - ''-
00141 21* C ASH )
00142 22* PRINT 1055,AA(27,17)
00145 23* 1055 FORMAT(/8X26H PROCESS STEAM =,F8.0,7H LB/HR )
00146 24* WATER=AA(90,10)
00147 25* PRINT 1056,WATER
00152 26* 1056 FORMAT(/8X26H PROCESS COOLING WATER =,F8.0,7H GAL/HR )

```

Table I.-- Continued.

```
00153 27*      PRINT 1057,AA(90,2)
00156 28*      1057  FORMAT(/8X26H ELECTRICITY           ,F8.0,7H KWHR )
00157 29*      PRINT 1058
00161 30*      1058  FORMAT(///5X23H EQUIPMENT FLOW RATES )
00162 31*      RETURN
00163 32*      END
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.--Continued.

FOR,S CAPTOL,CAPTOL  
FOR S9A-07/12-11:06 (0,)

SUBROUTINE CAPTOL ENTRY POINT 000111

STORAGE USED: CODE(1) 000113; DATA(0) 000073; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050  
0004 BLOCK2 000016

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NPRT\$  
0006 NIO2\$  
0007 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000003	1001F	0000	000012	1002F	0000	000021	1003F	0000	000030	1004F	0000	000037	1005F				
0000	000046	1020F	0000	000055	2000F	0000	000056	2001F	0003	R	000000	AA	0003	004704	BB			
0004	000000	COST	0004	R	000007	COSTA	0000	R	000001	COSTT	0000	R	000000	COSTTT	0000	R	000002	DOSTT
0003	003720	IA	0000	000066	INJP\$													

```

00101 1* SUBROUTINE CAPTOL (TONS)
00103 2* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* COMMON/BLOCK2/ COST(7),COSTA(7)
00105 4* 1001 FORMAT(//,25X,20H EQUIPMENT ,F10.3)
00106 5* 1002 FORMAT(//,25X,20H SPARE PARTS ,F10.3)
00107 6* 1003 FORMAT(//,25X,20H FACILITIES ,F10.3)
00110 7* 1004 FORMAT(//,25X,20H ENGINEERING ,F10.3)
00111 8* 1005 FORMAT(//,25X,20H CONTINGENCIES ,F10.3,/)
00112 9* 1020 FORMAT(//,25X,20H TOTAL CAPITAL COSTS,F10.3,/)
00113 10* 2000 FORMAT(1H1)
00114 11* 2001 FORMAT(20X,30H SUMMARY OF FIXED COSTS ,/)
00115 12* PRINT 2000
00117 13* PRINT 2001
00121 14* COSTTT=0.
00122 15* COSTT=COSTA(5)
00123 16* PRINT 1001,COSTT
00126 17* COSTTT=COSTT+COSTTT
00127 18* COSTT=.02*COSTA(1)
00130 19* PRINT 1002,COSTT
00133 20* COSTTT=COSTT+COSTTT
00134 21* COSTT=AA(100,9)
00135 22* PRINT 1003,COSTT
00140 23* COSTTT=COSTT+COSTTT
00141 24* COSTT=COSTTT*AA(9A,1)
00142 25* PRINT 1004, COSTT
    
```

Table I.--Continued.

```
00145 26* COSTTT=COSTT+COSTTT
00146 27* DOSTT=COSTTT*AA(9A,2)
00147 28* PRINT 1005,DOSTT
00152 29* COSTTT=DOSTT+COSTTT
00153 30* AA(100,10)=COSTTT
00154 31* PRINT 1020,AA(100,10)
00157 32* RETURN
00160 33* END
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

@FOR,S FASCIL,FASCIL  
FOR 59A-07/12-11:06 (0,)

SUBROUTINE FASCIL ENTRY POINT 000530

STORAGE USED: CODE(1) 000536; DATA(0) 000365; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0004 NPRT\$  
0005 NIO2\$  
0006 NIO1\$  
0007 SQRT  
0010 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000025	1000F	0000	000037	1001F	0000	000077	1010F	0000	000112	1020F	0000	000125	1030F
0000	000140	1040F	0000	000153	1050F	0000	000161	1060F	0000	000173	1070F	0000	000205	1080F
0000	000220	1090F	0000	000226	1100F	0000	000240	1110F	0000	000252	1120F	0000	000264	1130F
0000	000276	1140F	0001	000022	115G	0001	000044	132G	0001	000052	140G	0001	000110	154G
0001	000123	164G	0001	000155	200G	0000	000325	2000F	0001	000170	210G	0001	000235	227G
0001	000250	237G	0001	000336	272G	0000	000311	3012F	0001	000351	302G	0001	000442	344G
0001	000455	354G	0001	000472	366G	0001	000511	401G	0001	000504	90L	0003 R	000000	AA
0000 R	000016	ACRE	0003 R	004704	BB	0000 R	000024	BUILD	0000 R	000000	COST	0000 R	000006	COSTT
0000 R	000022	DOCK	0000 R	000017	FENCF	0003	003720	IA	0000	000354	INJP\$	0000 I	000014	IZ
0000 I	000015	J	0000 T	000021	NOCK	0000 R	000020	PAVE	0000 R	000023	WARE			

```

00101 1* SUBROUTINE FASCIL(TONS)
00103 2* COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)
00104 3* DIMENSION COST(6),COSTT(6)
00105 4* IZ = BB(91)
00106 5* PRINT 1000
00110 6* 1000 FORMAT(1H1//14x43H-COST OF FACILITIES AND SITE DEVELOPMENT )
00111 7* PRINT 1001
00113 8* 1001 FORMAT(/25x85H UNIT NUMBER BASE LA
00113 9* CBOR INDIRECT TOTAL RANGE /25x85H COST
00113 10* C OF UNITS COST COSTS COSTS COSTS + OR - )
00114 11* DO 1 J=1,6
00117 12* COST(J)= 0.0
00120 13* 1 COSTT(J) = n.n
00122 14* ACRE=.0050*TONS
00123 15* COST(2) = AA(99,3)*ACRE
00124 16* COST(5) = COST(2)
00125 17* COST(6) = COST(5)*AA(99,2)
00126 18* PRINT 1010,AA(99,3),ACRE,.(COSTT(J),J=2,6)

```

```

00136 19* 1010 FORMAT(/25H LAND ,F10.3,15H PER ACRE ,6F1
00136 20* C0.3)
00137 21* DO 10 J =2,6
00142 22* 10 COST(J) = COST(J)+COSTT(J)
00144 23* FENCE = 4*SQRT(ACRE*0.0434)
00145 24* COST(2) =FENCE*AA(90,4)
00146 25* COST(3) =COST(2)*AA(99,5)
00147 26* COST(4) =COST(2)*AA(99,1)
00150 27* COST(5) =COST(2)+COST(3)+COST(4)
00151 28* COST(6) = COST(5)*AA(99,2)
00152 29* COST(1) = COST(5)/FENCE
00153 30* DO 20 J=2,6
00156 31* 20 COSTT(J)=COST(J)+COSTT(J)
00160 32* PRINT 1020,COST(1),FENCE,(COST(J),J=2,6)
00170 33* PAVE =0.333*ACRE*43.56
00171 34* COST(2) =PAVE*AA(99,6)
00172 35* COST(3) =COST(2)*AA(99,7)
00173 36* COST(4) =COST(2)*AA(99,1)
00174 37* COST(5) =COST(2)+COST(3)+COST(4)
00175 38* COST(6) = COST(5)*AA(99,2)
00176 39* COST(1) = COST(5)/PAVE
00177 40* DO 30 J=2,6
00202 41* 30 COSTT(J) =COST(J) +COSTT(J)
00204 42* PRINT 1030,COST(1),PAVE,(COST(J),J=2,6)
00214 43* 1020 FORMAT(/25H FENCING ,F10.3,15H PER 1000 FT ,6F1
00214 44* C0.3)
00215 45* 1030 FORMAT(/25H PAVING ,F10.3,15H PER 1,00 SQ.FT,6F1
00215 46* C0.3)
00216 47* NOCK = TONS/500. +1
00217 48* DOCK = 2.4*NOCK
00220 49* COST(2)=DOCK*AA(90,8)
00221 50* COST(3)=COST(2)*AA(99,9)
00222 51* COST(4)=COST(2)*AA(99,1)
00223 52* COST(5)=COST(2)+COST(3)+COST(4)
00224 53* COST(6)=COST(5)*AA(99,2)
00225 54* COST(1) = COST(5)/DOCK
00226 55* DO 40 J=2,6
00231 56* 40 COSTT(J) =COST(J)+COSTT(J)
00233 57* PRINT 1040,COST(1),DOCK,(COST(J),J=2,6)
00243 58* 1040 FORMAT(/25H DOCK FACILITIES ,F10.3,15H PER 1000 SQ.FT,6F1
00243 59* C0.3)
00244 60* PRINT 1050
00246 61* 1050 FORMAT(/25H BULK STORAGE WAREHOUSE , )
00247 62* PRINT 1060,AA(99,10)
00252 63* 1060 FORMAT( 25H ELECTRICAL WIRING ,F10.3,15H PER 1000SQ.FT )
00253 64* PRINT 1070,AA(99,11)
00256 65* 1070 FORMAT( 25H FIRE PREVENTION EQP.,F10.3,15H PER 1000SQ.FT )
00257 66* IF(IZ .EQ. 1) WARE = 0.015*TONS
00261 67* IF(IZ .GT. 1) WARE = 0.003*TONS
00263 68* COST(2) =WARE*(AA(99,10)+AA(99,11)+AA(99,12))
00264 69* COST(3)=COST(2)*AA(99,13)
00265 70* COST(4)=COST(2)*AA(99,1)
00266 71* COST(5)=COST(2)+COST(3)+COST(4)
00267 72* COST(6)=COST(5)*AA(99,2)
00270 73* COST(1) = COST(5)/WARE
00271 74* DO 80 J= 2,6
00274 75* 80 COSTT(J) =COST(J)+COSTT(J)

```

Table I.-- Continued.

```

nn276 76* PRINT 1080,COST(1),WARE,(COST(J),J=2,6)
nn306 77* 1080 FORMAT(/25H TOTAL WAREHOUSE ,F10.3,15H PER 1000 SQ.FT,6F1
nn306 78* C0.3)
nn307 79* PRINT 1090
nn311 80* 1090 FORMAT(/25H PROCESS BUILDING )
nn312 81* PRINT 1100,AA(99,14)
nn315 82* PRINT 1110,AA(99,15)
nn320 83* PRINT 1120,AA(99,16)
nn323 84* PRINT 1130,AA(99,17)
nn326 85* 1100 FORMAT(25H ELECTRICAL WIRING ,F10.3,15H PER 1000 SQ.FT )
nn327 86* 1110 FORMAT(25H HEATING AND VENTIL. ,F10.3,15H PER 1000 SQ.FT )
nn330 87* 1120 FORMAT(25H PLUMBING(GENERAL) ,F10.3,15H PER 1000 SQ.FT )
nn331 88* 1130 FORMAT(26H FIRE PREVENTION EQUIP,F 9.3,15H PER 1000 SQ.FT )
nn332 89* BUILD =0.013*TONS
nn333 90* IF(BUILD .LE. 2) RUTLD = 2.0
nn335 91* COST(2) =AA(99,18)*BUILD
nn336 92* COST(3) =COST(2)*AA(99,19)
nn337 93* COST(4) =COST(2)*AA(99,1)
nn340 94* COST(5) =COST(2)+COST(3)+COST(4)
nn341 95* COST(6) =COST(5)*AA(99,2)
nn342 96* COST(1) = COST(5)/BUILD
nn343 97* DO 140 J=2,6
nn346 98* 140 COSTT(J) = COST(J) +COSTT(J)
nn350 99* PRINT 1140,COST(1),BUILD,(COST(J),J=2,6)
nn360 100* 1140 FORMAT(/25H TOTAL BUILDING COSTS ,F10.3,15H PER 1000 SQ.FT,6F1
nn360 101* C0.3)
nn361 102* IF(IZ .EQ. 1) GO TO 90
nn363 103* COST(1) =150.
nn364 104* COST(5)=COST(1)
nn365 105* DO 150 J=2,6
nn370 106* 150 COSTT(J) = COST(J) +COSTT(J)
nn372 107* PRINT 3012, COST(1),COST(5)
nn376 108* 3012 FORMAT(/45H LABORATORY CONTROL INSTRUMENTATION ,15X,F10.
nn376 109* C3,20X,F10.3)
nn377 110* 90 PRINT 2000,(COSTT(J),J=2,6)
nn405 111* 2000 FORMAT(/25H TOTAL FACILITIES ,35X5F10.3)
nn406 112* AA(100,9)=COSTT(5)
nn407 113* RETURN
nn410 114* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

@FOR,S OPERAT:OPERAT  
FOR S9A-07/12-11:06 (3,)

SUBROUTINE OPERAT ENTRY POINT 001242

STORAGE USED: CODE(1) 001253; DATA(0) 000757; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0004 NPRT\$  
0005 NI02\$  
0006 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000127	1001F	0000	000142	1002F	0000	000155	1003F	0000	000170	1004F	0000	000203	1005F
0000	000214	1006F	0000	000242	1007F	0000	000255	1008F	0000	000270	1009F	0001	001226	101L
0000	000300	1010F	0000	000310	1011F	0000	000320	1012F	0000	000330	1013F	0000	000374	1018F
0000	000407	1019F	0000	000341	1020F	0000	000227	106F	0000	000352	1104F	0000	000363	1105F
0001	000022	1146	0000	000065	2000F	0000	000422	2001F	0000	000453	2002F	0000	000460	2003F
0000	000467	2004F	0000	000476	2005F	0000	000505	2006F	0000	000515	2007F	0000	000524	2008F
0000	000533	2009F	0000	000544	2010F	0000	000554	2011F	0000	000563	2012F	0000	000572	2013F
0000	000601	2014F	0000	000610	2015F	0000	000110	2020F	0000	000117	2021F	0001	000230	3L
0000	000066	3000F	0001	000511	330G	0001	000136	4L	0000	000617	4000F	0000	000625	4001F
0000	000643	4002F	0000	000653	4003F	0000	000663	4005F	0000	000673	4006F	0000	000706	4007F
0001	000233	5L	0001	000447	60L	0000	000077	6000F	0001	000565	71L	0001	000572	72L
0001	000572	75L	0001	000572	76L	0003 R	000000	AA	0003 R	004704	BB	0000 R	000064	RYPR0N
0000 R	000052	CANS	0000 R	000053	CAST	0000 R	000000	CST	0000 R	000024	CSTT	0000 R	000063	FPC
0003	003720	IA	0000	000741	TNJP\$	0000 I	000050	TZ	0000 I	000051	J	0000 R	000060	YCONC
0000 R	000054	YCOST	0000 R	000062	YHTM	0000 R	000055	YMEAL	0000 R	000061	YOIL	0000 R	000057	YPAST
0000 R	000056	YSOL												

00101 1\* SUBROUTINE OPERAT(TONS)  
00101 2\* C SUMMARY OF MATERIAL FLOW STREAMS UNDER THE INDEX AA(90,I)  
00101 3\* C 1=FUEL OIL 2=POWER 3=FISH MEAL 4=FISH SOL. 5= FISH OIL  
00101 4\* C 8=MAN HRS 9=CITY WATER  
00101 5\* C 13=ANIOXID. 14=SUH PH.ACTD  
00103 6\* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)  
00104 7\* DIMENSION CST(20),CSTT(20)  
00105 8\* IZ = BB(91)  
00106 9\* PRINT 2000  
00110 10\* 2000 FORMAT(1H1)  
00111 11\* PRINT 2001  
00113 12\* DO 10 J=1,20  
00116 13\* CST(J)=0.0  
00117 14\* 10 CSTT(J)=0.0

Table I.--Continued.

```

nn276 76* PRINT 1080,COST(1),WARE,(COST(J),J=2,6)
nn306 77* 1080 FORMAT(/25H TOTAL WAREHOUSE ,F10.3,15H PER 1000 SQ.FT,6F1
nn306 78* C0.3)
nn307 79* PRINT 1090
nn311 80* 1090 FORMAT(/25H PROCESS BUILDING )
nn312 81* PRINT 1100,AA(99,14)
nn315 82* PRINT 1110,AA(99,15)
nn320 83* PRINT 1120,AA(99,16)
nn323 84* PRINT 1130,AA(99,17)
nn326 85* 1100 FORMAT(25H ELCTRICAL WIRING ,F10.3,15H PER 1000 SQ.FT )
nn327 86* 1110 FORMAT(25H HEATING AND VENTIL. ,F10.3,15H PER 1000 SQ.FT )
nn330 87* 1120 FORMAT(25H PLUMBING(GENERAL) ,F10.3,15H PER 1000 SQ.FT )
nn331 88* 1130 FORMAT(26H FIRE PREVENTION EQUIP,F 9.3,15HPER 1000 SQ.FT )
nn332 89* BUILD =0.013*TONS
nn333 90* IF(BUILD .LE. 2) RUTLD = 2.0
nn335 91* COST(2) =AA(99,18)*RUIILD
nn336 92* COST(3) =COST(2)*AA(99,19)
nn337 93* COST(4) =COST(2)*AA(99,1)
nn340 94* COST(5) =COST(2)+COST(3)+COST(4)
nn341 95* COST(6) =COST(5)*AA(99,2)
nn342 96* COST(1) = COST(5)/BUILD
nn343 97* DO 140 J=2,6
nn346 98* 140 COSTT(J) = COST(J) +COSTT(J)
nn350 99* PRINT 1140,COST(1),RUIILD,(COST(J),J=2,6)
nn360 100* 1140 FORMAT(/25H TOTAL BUILDING COSTS ,F10.3,15H PER 1000 SQ.FT,6F1
nn360 101* C0.3)
nn361 102* IF(IZ .EQ. 1) GO TO 90
nn363 103* COST(1) =150.
nn364 104* COST(5)=COST(1)
nn365 105* DO 150 J=2,6
nn370 106* 150 COSTT(J) = COST(J) +COSTT(J)
nn372 107* PRINT 3012, COST(1),COST(5)
nn376 108* 3012 FORMAT(/45H LABORATORY CONTROL INSTRUMENTATION ,15X,F10.
nn376 109* C3,20X,F10.3)
nn377 110* 90 PRINT 2000,(COSTT(J),J=2,6)
nn405 111* 2000 FORMAT(/25H TOTAL FACILITIES ,35X5F10.3)
nn406 112* AA(100,9)=COSTT(5)
nn407 113* RETURN
nn410 114* END

```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR,S OPERAT,OPERAT  
FOR S9A-07/12-11:06 (3,)

SUBROUTINE OPERAT ENTRY POINT 001242

STORAGE USED: CODE(1) 001253; DATA(0) 000757; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0004 NPRT\$  
0005 NIO2\$  
0006 NERR3\$

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0000	000127	1001F	0000	000142	1002F	0000	000155	1003F	0000	000170	1004F	0000	000203	1005F
0000	000214	1006F	0000	000242	1007F	0000	000255	1008F	0000	000270	1009F	0001	001226	101L
0000	000300	1010F	0000	000310	1011F	0000	000320	1012F	0000	000330	1013F	0000	000374	1018F
0000	000407	1019F	0000	000341	1020F	0000	000227	106F	0000	000352	1104F	0000	000363	1105F
0001	000022	1146	0000	000065	2000F	0000	000422	2001F	0000	000453	2002F	0000	000460	2003F
0000	000467	2004F	0000	000476	2005F	0000	000505	2006F	0000	000515	2007F	0000	000524	2008F
0000	000533	2009F	0000	000544	2010F	0000	000554	2011F	0000	000563	2012F	0000	000572	2013F
0000	000601	2014F	0000	000610	2015F	0000	000110	2020F	0000	000117	2021F	0001	000230	3L
0000	000666	3000F	0001	000511	3306	0001	000136	4L	0000	000617	4000F	0000	000625	4001F
0000	000643	4002F	0000	000653	4003F	0000	000663	4005F	0000	000673	4006F	0000	000706	4007F
0001	000233	5L	0001	000447	60L	0000	000077	6000F	0001	000565	71L	0001	000572	72L
0001	000572	75L	0001	000572	76L	0003 R	000000	AA	0003 R	004704	BB	0000 R	000064	RYPR00
0000 R	000052	CANS	0000 R	000053	CAST	0000 R	000000	CST	0000 R	000024	CSTT	0000 R	000063	FPC
0003	0003720	IA	0000	000741	TNJP\$	0000 I	000050	TZ	0000 I	000051	J	0000 R	000060	YCONC
0000 R	000054	YCOST	0000 R	000062	YHTM	0000 R	000055	YMFAL	0000 R	000061	YOIL	0000 R	000057	YPAST
0000 R	000056	YSOL												

00101 1\* SUBROUTINE OPERAT(TONS)  
00101 2\* C SUMMARY OF MATERIAL FLOW STREAMS, UNDER THE INDEX AA(90,I)  
00101 3\* C 1=FUEL OIL 2=POWER 3=FISH MEAL 4=FISH SOL. 5= FISH OIL  
00101 4\* C 8=MAN HRS 9=CITY WATER  
00101 5\* C 13=ANIOXID. 14=SUPH. ACTD  
00103 6\* COMMON/BLOCK1/ AA(100,20),IA(100,5),BB(100)  
00104 7\* DIMENSION CST(20),CSTT(20)  
00105 8\* IZ = BB(91)  
00106 9\* PRINT 2000  
00110 10\* 2000 FORMAT(1H1)  
00111 11\* PRINT 2001  
00113 12\* DO 10 J=1,20  
00116 13\* CST(J)=0.0  
00117 14\* 10 CSTT(J)=0.0

Table I.-- Continued.

```

nn121 15*      CST(1) = TONS*BB(5)*20.0
nn122 16*      PRINT 1001,TONS,CST(1)
nn126 17*      CST(2) = AA(90,1)*BR(10)
nn127 18*      PRINT 1002,AA(90,1),CST(2)
nn133 19*      CST(3) =AA(90,2)*RB(6)*0.01
nn134 20*      PRINT 1003,AA(90,2),CST(3)
nn140 21*      CST(4)=AA(90,14)*BR(14)
nn141 22*      IF(IZ .EQ. 1) PRINT 1004,AA(90,14),CST(4)
nn146 23*      IF(IZ .EQ. 3) PRINT 1004,AA(90,14),CST(4)
nn153 24*      IF(IZ.NE.3.AND.IZ.NE.4) GO TO 4
nn155 25*      CST(16)=AA(90,17)*RB(10)
nn156 26*      PRINT 3000,AA(90,17),CST(16)
nn162 27*      4      CST(15)=AA(90,12)*RB(41)
nn163 28*      3000  FORMAT(/25H 5N SODIUM HYDROXIDE      ,F8.0,8H LB      ,5XF8.2)
nn164 29*      IF(IZ .EQ. 3) PRINT 1105,AA(90,12),CST(15)
nn171 30*      IF(IZ .EQ. 4) PRINT 1105,AA(90,12),CST(15)
nn176 31*      CST(14) = AA(90,15)*BB(16)
nn177 32*      IF(IZ .EQ. 3) PRINT 1104,AA(90,15),CST(14)
nn204 33*      IF(IZ .EQ. 4) PRINT 1104,AA(90,15),CST(14)
nn211 34*      IF(IZ .EQ. 3) GO TO 3
nn213 35*      IF(IZ .EQ. 4) GO TO 3
nn215 36*      CST(5)=AA(90,13)*BR(13)
nn216 37*      GO TO 5
nn217 38*      3      CST(5)=AA(90,13)*BR(44)
nn220 39*      5      CONTINUE
nn221 40*      PRINT 1005,AA(90,13),CST(5)
nn225 41*      CST(6)=AA(75,17)*BR(15)
nn226 42*      PRINT 1006,AA(75,17),CST(6)
nn232 43*      CANS=0.0
nn233 44*      CANS=AA(75,4)*RB(15)
nn234 45*      IF(AA(75,4).GT.0) PRINT 106,AA(75,4),CANS
nn241 46*      CST(6)=CST(6)+CANS
nn242 47*      CST(7) =AA(90,9)*RB(9)
nn243 48*      PRINT 1007,AA(90,9),CST(7)
nn247 49*      CST(8) =AA(90,8)*RB(7)
nn250 50*      PRINT 1008,AA(90,8),CST(8)
nn254 51*      CST(9) =AA(100,10)*RB(8)*0.1/3
nn255 52*      PRINT 1009,CST(9)
nn260 53*      CST(10) =AA(100,10)/30.
nn261 54*      PRINT 1010,CST(10)
nn264 55*      CST(11)=CST(8)*0.15
nn265 56*      PRINT 1011,CST(11)
nn270 57*      CST(12) =CST(10)
nn271 58*      6000  FORMAT(25H BOILER WATER TREATMENT ,21XF8.2,12XF6.2,/)
nn272 59*      CAST=3.3
nn273 60*      PRINT 6000,CAST
nn276 61*      PRINT 1012,CST(12)
nn301 62*      CST(13) =CST(8)*0.30
nn302 63*      PRINT 1013,CST(13)
nn305 64*      IF(IZ.NE.2.AND.IZ.NE.6.AND.IZ.NE.7) GO TO 60
nn307 65*      CST(18) =AA(90,18)*BB(18)
nn310 66*      AA(90,18)=AA(90,18)*2000.
nn311 67*      PRINT 1018,AA(90,18),CST(18)
nn315 68*      CST(19) =AA(90,19)*BB(19)
nn316 69*      AA(90,19)=AA(90,19)*2000.
nn317 70*      PRINT 1019, AA(90,19),CST(19)
nn323 71*      60      CONTINUE

```

## Table I.--Continued.

```

00324 72*      YCOST =(CST(1)+CST(2)+CST(3)+CST(4)+CST(5)+CST(6)+CST(7))*BR(50)+
00324 73*      C(CST(8)+CST(9)+CST(10)+CST(11)+CST(12)+CST(13))*360.0 +(CST(14) +
00324 74*      C CST(15)+CST(16)+CST(17)+CST(18))*BB(50)
00325 75*      YCOST=(CST(19)*BB(50)) + YCOST
00326 76*      YCOST=YCOST+CAST*BR(50)
00327 77*      DO 20 J=2,20
00332 78*      CST(J) =CST(J-1) + CST(J)
00333 79*      20  CSTT(J) =CSTT(J-1)+CSTT(J)
00335 80*      CST(20)=CST(20)+CAST
00336 81*      PRINT 1020,CST(20)
00341 82*      PRINT 2002
00343 83*      IF(IZ.NE.2.AND.IZ.NF.6) GO TO 76
00345 84*      IF(IZ.NE.6) GO TO 71
00347 85*      2020 FORMAT(/15X14H HTM FISH MEAL,F8.3,10H TONS/DAY )
00350 86*      AA(90,20)=AA(90,20)/2000.
00351 87*      PRINT 2020,AA(90,20)
00354 88*      GO TO 75
00355 89*      71 IF(IZ.NE.2) GO TO 72
00357 90*      GO TO 75
00360 91*      72 CONTINUE
00361 92*      76 CONTINUE
00362 93*      75 CONTINUE
00363 94*      IF(IZ      .EQ. 1) PRINT 2003,AA(90,3)
00367 95*      IF(IZ      .GT. 1) PRINT 2011,AA(90,3)
00373 96*      IF(IZ .EQ. 1) PRINT 2004,AA(90,4)
00377 97*      IF(IZ.GT.2.AND.IZ.LT.6) PRINT 2012,AA(90,6)
00403 98*      IF(IZ.EQ.7) PRINT 2004,AA(90,4)
00407 99*      IF(IZ.EQ.2) PRINT 2004,AA(90,4)
00413 100*     IF(IZ .GT. 1) PRINT 2013,AA(90,7)
00417 101*     PRINT 2005,AA(90,5)
00422 102*     YMEAL = AA(90,3)*RB(50)
00423 103*     YSOL = AA(90,4)*RB(50)
00424 104*     YPAST = AA(90,6)*RB(50)
00425 105*     YCONC = AA(90,7)*RB(50)
00426 106*     YOIL = AA(90,5)*RB(50)
00427 107*     YHTM=AA(90,20)*BB(50)
00430 108*     IF(IZ.EQ.6) PRINT 2021,YHTM
00434 109*     IF(IZ      .EQ. 1) PRINT 2006,YMEAL
00440 110*     IF(IZ      .GT. 1) PRINT 2010,YMEAL
00444 111*     IF(IZ .EQ. 1) PRINT 2007,YSOL
00450 112*     IF(IZ.GT.2.AND.IZ.LT.6) PRINT 2014,YPAST
00454 113*     IF(IZ.EQ.2) PRINT 2007,YSOL
00460 114*     IF(IZ.EQ.7) PRINT 2007,YSOL
00464 115*     IF(IZ .GT. 1) PRINT 2015,YCONC
00470 116*     2021 FORMAT(/15X 14H HTM FISH MEAL,F8.0,11H TONS/YEAR )
00471 117*     PRINT 2008,YOIL
00474 118*     PRINT 2009,YCOST
00477 119*     1001 FORMAT(/25H FISH                                ,F8.0,8H TONS    ,5XF8.2,12XF6
00477 120*     C.2)
00500 121*     1002 FORMAT(/25H FUEL OIL                                ,F8.0,8H GALLONS,5XF8.2,12XF6
00500 122*     C.2)
00501 123*     1003 FORMAT(/25H ELECTRICITY                                ,F8.0,8H KWHR    ,5XF8.2,12XF6
00501 124*     C.2)
00502 125*     1004 FORMAT(/25H SULPHURIC ACID                            ,F8.0,8H LB      ,5XF8.2,12XF6
00502 126*     C.2)
00503 127*     1005 FORMAT(/25H ANTIOXIDANT                            ,F8.0,8H LB      ,5XF8.2)
00504 128*     1006 FORMAT(/25H PACKAGING                                ,F8.0,8H BAGS   ,5XF8.2,12XF6.

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Table I.- Continued.

```

nn5n4 129*      C2)
nn5n5 130*    106  FORMAT(/25H PACKAGING           ,F8.0,8H CANS      ,5XF8.2,12XF6.
nn5n5 131*      C2)
nn5n6 132*    1007 FORMAT(/25H CITY WATER           ,F8.0,8H GALLONS,5XF8.2,12XF6
nn5n6 133*      C.2)
nn5n7 134*    1008 FORMAT(/25H LABOR AND SUPERVISION ,F8.0,8H MAN HR.,5XF8.2,12XF6
nn5n7 135*      C.2,/)
nn510 136*    1009 FORMAT(/25H DEPRECIATION           ,21XF8.2,12XF6.2)
nn511 137*    1010 FORMAT(/25H MAINTENANCE           ,21XF8.2,12XF6.2)
nn512 138*    1011 FORMAT(/25H PAYROLL EXTRAS        ,21XF8.2,12XF6.2)
nn513 139*    1012 FORMAT(/25H INSURANCE AND TAXES     ,21XF8.2,12XF6.2)
nn514 140*    1013 FORMAT(/25H OVERHEAD             ,21XF8.2,12XF6.2,/)
nn515 141*    1020 FORMAT(/25H TOTAL OPERATING COSTS ,21XF8.2,12XF6.2,/)
nn516 142*    1104 FORMAT(/25H CALCIUM HYDROXIDE        ,F8.0,8H LB       ,5XF8.2)
nn517 143*    1105 FORMAT(/25H ENZYME                 ,F8.0,8H LB       ,5XF8.2)
nn520 144*    1018 FORMAT(/25H ISOPROPYL ALCOHOL       ,F8.0,8H POUNDS  ,5XF8.2,12XF6
nn520 145*      C.2)
nn521 146*    1019 FORMAT(/25H PHOSPHORIC ACID        ,F8.0,8H POUNDS  ,5XF8.2,12XF6
nn521 147*      C.2)
nn522 148*    2001 FORMAT( 20X,17H OPERATING COSTS ,//75H      COST ITFM
nn522 149*      QUANTITY USED COST IN DOLLARS           ,/43X30H PER D
nn522 150*      CAY )
nn523 151*    2002 FORMAT(/20X,17H PRODUCTION RATE )
nn524 152*    2003 FORMAT(/15X12H FISH MEAL ,F10.3,10H TONS/DAY )
nn525 153*    2004 FORMAT(/15X12H FISH SOL. ,F10.3,10H TONS/DAY )
nn525 154*      C
nn526 155*    2005 FORMAT(/15X12H FISH OIL ,F10.3,10H TONS/DAY )
nn527 156*    2006 FORMAT(/15X12H FISH MEAL ,F10.0,11H TONS/YEAR )
nn530 157*    2007 FORMAT(/15X 12H FISH SOL. ,F10.0,11H TONS/YEAR )
nn531 158*    2008 FORMAT(/15X 12H FISH OIL ,F10.0,11H TONS/YEAR )
nn532 159*    2009 FORMAT(/20X24H YEARLY OPERATING COST =,F12.6,8H DOLLARS )
nn533 160*    2010 FORMAT(/15X12H BONE MEAL ,F10.0,11H TONS/YEAR )
nn534 161*    2011 FORMAT(/15X12H BONE MEAL ,F10.3,10H TONS/DAY )
nn535 162*    2012 FORMAT(/15X12H FISH PASTE ,F10.3,10H TONS/DAY )
nn536 163*    2013 FORMAT(/15X12H DRY CONC. ,F10.3,10H TONS/DAY )
nn537 164*    2014 FORMAT(/15X 12H FISH PASTE ,F10.0,11H TONS/YEAR )
nn540 165*    2015 FORMAT(/15X 12H DRY CONC. ,F10.0,11H TONS/YEAR )
nn541 166*      IF (IZ .EQ. 1) GO TO 101
nn543 167*      PRINT 4000
nn545 168*    4000 FORMAT(/20X,24H PRODUCTION COST OF FPC )
nn546 169*      PRINT 4001
nn550 170*    4001 FORMAT(74H BY-PRODUCT           PRICE(CENTS/POUND)           TOTAL WO
nn550 171*      CRTH(DOLLARS/YEAR) )
nn551 172*      YMEAL=YMEAL*2000.*RB(66)/100.
nn552 173*      IF(YMEAL.GT.0) PRINT 4002,BB(66),YMEAL
nn557 174*    4002 FORMAT(/25H BONE MEAL           ,F8.1,13XE12.6)
nn560 175*      YOIL=YOIL*2000.*BB(67)/100.
nn561 176*      PRINT 4003,BB(67),YOIL
nn565 177*    4003 FORMAT(/25H FISH OIL           ,F8.1,13XF12.6)
nn566 178*      YSOL=YSOL*2000.*BB(68)/100.
nn567 179*      IF (IZ.EQ.2.OR. IZ.EQ.7) PRINT 4005,BB(68),YSOL
nn574 180*    4005 FORMAT(/25H FISH SOLUBLES         ,F8.1,13XF12.6)
nn575 181*      YCONC=YCONC*2000.+50*YPACT*2000.
nn576 182*      FPC=(YCOST/YCONC)*100.
nn577 183*      PRINT 4006,FPC
nn602 184*    4006 FORMAT(/20X,32H FPC COST WITHOUT BY-PRODUCTS ,F8.1,13H CENTS/POU
nn602 185*      CND )

```

Table I.-- Continued.

```
00603 186*      BYPROD=YOIL+YSOL+YMEAL+YPAST
00604 187*      YCOST=YCOST-BYPROD
00605 188*      FPC=(YCOST/YCONC)*100.
00606 189*      PRINT 4007,FPC
00611 190*      4007  FORMAT(/20X,32H FPC COST WITH BY-PRODUCTS      ,F8.1,13H CENTS/POU
00611 191*      CND )
00612 192*      101  RETURN
00613 193*      END
```

END OF COMPILATION: NO DIAGNOSTICS.

Table I.-- Continued.

FOR 5 LIBRE, LIBRE  
FOR S9A-07/12-11:06 (1,)

SUBROUTINE LIBRE ENTRY POINT 001077

STORAGE USED: CODE(1) 001106; DATA(0) 000247; BLANK COMMON(2) 000000

COMMON BLOCKS:

0003 DATA1 000050  
0004 BLOCK1 005050

EXTERNAL REFERENCES (BLOCK, NAME)

0005 NERR35

STORAGE ASSIGNMENT (BLOCK, TYPE, RELATIVE LOCATION, NAME)

0004 R 000000 AA            0004 R 004704 BB            0003 R 000000 DATB            0004    003720 IA            0000    000230 INJPS

00101	1*	SUBROUTINE LIBRE	
00103	2*	COMMON/ DATA1 / DATR(8,5)	
00104	3*	COMMON /BLOCK1/ AA(100,20),IA(100,5),BB(100)	
00104	4*	C IDENTIFICATION OF DATA STORED IN LIBRARY SUBROUTINE	
00104	5*	C	
00104	6*	C EQUIPMENT INDEX NUMBERS	
00104	7*	C	
00104	8*	C	
00104	9*	C        6= CONICAL HOPPER	CALLED BY SUB. HOPPER
00104	10*	C        11= PULVERISER	CALLED BY SUB. PULVER
00104	11*	C        17= SCREW CONVEYER	CALLED BY SUB. SCREWR
00104	12*	C        18= HAMMER MILL	CALLED BY SUB. HAMMER
00104	13*	C        19= DRUM DRYER	CALLED BY SUB. DRYER
00104	14*	C        20= PAN DRYER	CALLED BY SUB. DRYERP
00104	15*	C        21= ROTARY VACUUM DRYER	CALLED BY SUB. DRYERR
00104	16*	C        27= BOILER	CALLED BY SUB. BOILER
00104	17*	C        30= SPRAY EVAPORATOR	CALLED BY SUB. EVPSPR
00104	18*	C        31= WIPED FILM EVAPORATOR	CALLED BY SUB. EVPFLM
00104	19*	C        32= FORCED CIRCULATION EVAPORAT.	CALLED BY SUB. EVPFRC
00104	20*	C        33= VERTICAL EVAPORATOR	CALLED BY SUB. EVPHOR
00104	21*	C        40= SHOP FAR. STORAGE TANK	CALLED BY SUB. STORAG
00104	22*	C        42= PRESSURE VESSEL	CALLED BY SUB. VESSEL
00104	23*	C        43= DISTILLATION COLUMN	CALLED BY SUB. COLUMN
00104	24*	C        49= JACKETED REACTING VESSEL	CALLED BY SUB. REACTR
00104	25*	C        50= FISH GRINDER	CALLED BY SUB. GRINDR
00104	26*	C        51= VIBRATING SCREEN	CALLED BY SUB. SCREEN
00104	27*	C        52= SHARPLES CENTRIFUGE	CALLED BY SUB. SHARP
00104	28*	C        53= SOLID BOWL CENTRIFUGE	CALLED BY SUB. BOWL
00104	29*	C        54= V-BASKET CENTRIFUGE	CALLED BY SUB. CNTFGF
00104	30*	C        57= FREE FLOWING SOL. BLENDER	CALLED BY SUB. BLENDR
00104	31*	C        65= RECIPROCAL PUMPS	CALLED BY SUB. PMPREC

Table I.--Continued.

00104	31*	C	66= CENTRIFUGAL PUMPS	CALLED BY SUB	PMPCNT
00104	32*	C	67= SHELL-TUBE HEAT EXCHANGERS	CALLED BY SUB.	HEATEX
00104	33*	C	70= BELT CONVEYER	CALLED BY SUB.	BELT
00104	34*	C	71= BUCKET CONVEYFR	CALLED BY SUB.	BUCKET
00104	35*	C	72= SCALE	CALLED BY SUB.	SCALE
00104	36*	C	73= AGITATOR-PROPELLAR	CALLED BY SUB.	AGITOR
00104	37*	C	74= BALL MILL	CALLED BY SUB.	BALMIL
00104	38*	C	75= BAGGING MACHINE	CALLED BY SUB.	BAGGMA
00104	39*	C	78= ROTARY DRUM FILTER	CALLED BY SUB.	FILTER
00104	40*	C	80= OVERHEAD CRANE	CALLED BY SUB.	CRANES
00104	41*	C	81= DRAG CONVEYER	CALLED BY SUB	DRAGMA
00104	42*	C	85= MECHANICAL REFRIGERATION	CALLED BY SUB.	RFRIG
00104	43*	C	99= FASCILITIFS	CALLED BY SUB.	FASCIL
00104	44*	C			
00104	45*	C	GENERAL IDENTIFICATION OF THE STORED DATA.		
00104	46*	C	THE FOLLOWING DATA WILL IN MOST CASES BE STORED UNDER THE IDENTIFYING INDEX NUMBER FOR EACH IDOM OF EQUIPMENT. VARIATIONS OR ADDITIONS TO THIS PATTERN ARE EXPLAINED UNDER THE RESPECTIVE HEADINGS.		
00104	47*	C			
00104	48*	C			
00104	49*	C			
00104	50*	C	AA(IX,7) =	UNIT COST	
00104	51*	C	AA(IX,8) =	EXPONENT OF COST EQUATION	
00104	52*	C	AA(IX,11) =	FIELD MATERIALS COST FACTOR	
00104	53*	C	AA(IX,12) =	DIRECT LABOR COST FACTOR	
00104	54*	C	AA(IX,13) =	INDIRECT COST FACTOR	
00104	55*	C	AA(IX,15) =	UNCERTAINTY FACTOR FOR BARE MODULE COST	
00104	56*	C			
00104	57*	C	CONICAL HOPPERS. SIZE UNIT CUBIC FEET. REF GUTHRIE		
00105	58*		AA(6,7) =	0.010	
00106	59*		AA(6,8) =	0.68	
00107	60*		AA(6,11) =	0.04	
00110	61*		AA(6,12) =	0.01	
00111	62*		AA(6,13) =	0.42	
00112	63*		AA(6,15) =	0.10	
00113	64*		AA(6,18) =	2.40	
00113	65*	C	FISH STORAGE		
00114	66*		AA(7,7) =	0.9	
00115	67*		AA(7,8) =	0.9	
00116	68*		AA(7,11) =	0.0	
00117	69*		AA(7,12) =	0.10	
00120	70*		AA(7,13) =	.4	
00121	71*		AA(7,15) =	0.1	
00121	72*	C	BAROMETRIC CONDENSER AND SCRUBBERS		
00122	73*		AA(8,7) =	20.	
00123	74*		AA(8,8) =	1.0	
00124	75*		AA(8,11) =	0.33	
00125	76*		AA(8,12) =	0.33	
00126	77*		AA(8,13) =	0.33	
00127	78*		AA(8,15) =	0.1	
00127	79*	C	PULVERIZER		
00130	80*		AA(11, 7) =	500.	
00131	81*		AA(11, 8) =	.75	
00132	82*		AA(11,11) =	.272	
00133	83*		AA(11,12) =	.318	
00134	84*		AA(11,13) =	.4	
00135	85*		AA(11,15) =	.1	
00135	86*	C	SCREW CONVEYER		
00136	87*		AA(17, 7) =	1000.0	

Table I.--Continued.

nn137	88*	AA(17, 8)=	.9
nn140	89*	AA(17,11)=	.272
nn141	90*	AA(17,12)=	.318
nn142	91*	AA(17,13)=	.4
nn143	92*	AA(17,15)=	.1
nn143	93*	C HAMMER MILL SIZE + COST DATA. REF GUTHRIE	
nn143	94*	C SIZE UNIT = TON PER HOUR	
nn144	95*	AA(18,7) =	0.5
nn145	96*	AA(18,8) =	0.85
nn146	97*	AA(18,11) =	0.27
nn147	98*	AA(18,12) =	0.431
nn150	99*	AA(18,13) =	0.44
nn151	100*	AA(18,15) =	0.10
nn151	101*	C DRUM DRYER	
nn152	102*	AA(19, 7)=	3000.
nn153	103*	AA(19, 8)=	.38
nn154	104*	AA(19,11)=	.279
nn155	105*	AA(19,12)=	.461
nn156	106*	AA(19,13)=	.4
nn157	107*	AA(19,15)=	.1
nn157	108*	C PAN DRYER	
nn160	109*	AA(20,7 )=	1900.
nn161	110*	AA(20, 8)=	.38
nn162	111*	AA(20,11)=	.279
nn163	112*	AA(20,12)=	.461
nn164	113*	AA(20,13)=	.4
nn165	114*	AA(20,15)=	.1
nn165	115*	C ROTARY VACUUM DRYER	
nn166	116*	AA(21, 7)=	2500.
nn167	117*	AA(21, 8)=	.45
nn170	118*	AA(21,11)=	.279
nn171	119*	AA(21,12)=	.20
nn172	120*	AA(21,13)=	.16
nn173	121*	AA(21,15)=	.1
nn173	122*	C BOILER	
nn174	123*	AA(27, 7)=	395.5
nn175	124*	AA(27, 8)=	.5
nn176	125*	AA(27,11)=	.19
nn177	126*	AA(27,12)=	.15
nn200	127*	AA(27,13)=	.2
nn201	128*	AA(27,15)=	.1
nn201	129*	C SPRAY EVAPORATOR SIZE UNIT = LB OF WATER EVAP. PER HR	
nn201	130*	C PRAY AND FILM EVAP. INCLUDE SCRUBBERS AND BAR. CONDENSRS. BASE	
nn201	131*	C COST FROM CHEM. FNG. FFB, 9, 1970, OTHER FACTORS EQ. TO EVAP. FROM	
nn201	132*	C GUTHRIE	
nn202	133*	AA(30,7) =	0.050
nn203	134*	AA(30,8) =	1.0
nn204	135*	AA(30,11) =	0.66
nn205	136*	AA(30,12) =	0.24
nn206	137*	AA(30,13) =	0.42
nn207	138*	AA(30,15) =	0.10
nn207	139*	C WIPED FILM EVAPORATORS SIZE UNIT = SQ. FT AREA	
nn210	140*	AA(31,7)=	0.0
nn211	141*	AA(31,8) =	0.31
nn212	142*	AA(31,11) =	0.66
nn213	143*	AA(31,12) =	0.24
nn214	144*	AA(31,13) =	0.42

Table I.-- Continued.

nn215	145*	AA(31,15) = 0.10
nn215	146*	C FORCED CIRCULATION EVAPORATORS SIZE UNIT= SQ FT REF GUTHRIE
nn216	147*	AA(32,7)=0.6
nn217	148*	AA(32,8) = 0.70
nn220	149*	AA(32,11) = 0.66
nn221	150*	AA(32,12) = 0.24
nn222	151*	AA(32,13) = 0.42
nn223	152*	AA(32,15) = 0.10
nn224	153*	AA(32,18) = 2.40
nn224	154*	C VERTICAL EVAPORATORS SIZE UNIT = SQ. FT. REF. GUTHRIE
nn225	155*	AA(33,7) = 0.12
nn226	156*	AA(33,8) = 0.53
nn227	157*	AA(33,11) = 0.66
nn230	158*	AA(33,12) = 0.24
nn231	159*	AA(33,13) = 0.42
nn232	160*	AA(33,15) = 0.10
nn233	161*	AA(33,18) = 2.40
nn233	162*	C STORAGE TANK SIZE AND COST DATA. REF GUTHRIE
nn233	163*	C SIZE UNITS 100 GAL CAPACITY . MATERIAL FACTOR INDEX 18 = SGT
nn234	164*	AA(40,7) = 0.88
nn235	165*	AA(40,8) = 0.31
nn236	166*	AA(40,11) = 0.20
nn237	167*	AA(40,12) = 0.27
nn240	168*	AA(40,13) = 0.49
nn241	169*	AA(40,15) = 0.10
nn242	170*	AA(40,18) = 3.2
nn242	171*	C STORAGE TANK FROM 1000 GAL TO 40000 GAL CAPACITY STEEL + SST REF GUT
nn242	172*	C HRIE. SIZE UNITS 100-DC GAL
nn243	173*	AA(41,7) = 0.5
nn244	174*	AA(41,8) = 0.35
nn245	175*	AA(41,11) = 0.38
nn246	176*	AA(41,12) = 0.10
nn247	177*	AA(41,13) = 0.49
nn250	178*	AA(41,15) = 0.10
nn251	179*	AA(41,18) = 3.2
nn251	180*	C PRESSURE VESSEL
nn251	181*	C FOR THE PRESSURE VESSEL (IA(42,3) DETERMINES THE METAL, IA(42,2) = 1
nn251	182*	C IMPLIES VERTICAL CONSTRUCTION(AA(42,18) IS THE DIAMETER, AA(42,19)
nn251	183*	C IS THE HEIGHT
nn252	184*	AA(42, 1)= 3.67
nn253	185*	AA(42, 2)= 2.25
nn254	186*	AA(42, 3)= 1.0
nn255	187*	AA(42,15)= .1
nn255	188*	C DISTILLATION COLUMN
nn255	189*	C THE METAL, AA(43,20) THE WIDTH, AA(43,18) THE TRAY SEPARATION,
nn255	190*	C AA(43,17) THE HEIGHT
nn255	191*	C DETERMINES THE WIDTH
nn256	192*	AA(43, 4)= 0.4
nn257	193*	AA(43, 5)= 1.8
nn260	194*	AA(43,15)= .1
nn261	195*	AA(43,1)= 1.7
nn262	196*	AA(43,8) = 1.0
nn263	197*	AA(43,11)= .3
nn264	198*	AA(43,12)= .4
nn265	199*	AA(43,13)= .4
nn266	200*	AA(43,15)= .1
nn266	201*	C JACKETED REACTOR VESSEL UNIT COST 3*TANK COST DATA GUTHRIE. SIZE=GAL

Table I.-- Continued.

nn267	202*	AA(49,7) = 0.240
nn270	203*	AA(49,8) = 0.35
nn271	204*	AA(49,11) = 0.38
nn272	205*	AA(49,12) = 0.10
nn273	206*	AA(49,13) = 0.49
nn274	207*	AA(49,15) = 0.10
nn275	208*	AA(49,18) = 3.20
nn275	209*	C FISH GRINDER BASED ON 3 TON/HR UNIT COST OF 18300 DOLLARS. OTHER FAC-
nn275	210*	C TORS AS FOR BALL MILL
nn276	211*	AA(50,7) = 2.54
nn277	212*	AA(50,8) = 0.65
nn300	213*	AA(50,11) = 0.54
nn301	214*	AA(50,12) = 0.195
nn302	215*	AA(50,13) = 0.42
nn303	216*	AA(50,15) = 0.10
nn304	217*	AA(50,18) = 2.4
nn304	218*	C VIBRATING SCREEN FILTERS. SINGLE. SIZE UNIT = SURFACE AREA. REF GUTH.
nn305	219*	AA(51,7) = 0.7
nn306	220*	AA(51,8) = 0.58
nn307	221*	AA(51,11) = 0.27
nn310	222*	AA(51,12) = 0.05
nn311	223*	AA(51,13) = 0.42
nn312	224*	AA(51,15) = 0.10
nn313	225*	AA(51,18) = 2.40
nn313	226*	C SHARPLES CENTRIFUGE
nn314	227*	AA(52,7) = 5200.
nn315	228*	AA(52,8) = .68
nn316	229*	AA(52,11) = .26
nn317	230*	AA(52,12) = .34
nn320	231*	AA(52,13) = .4
nn321	232*	AA(52,15) = .1
nn321	233*	C SOLID BOWL CENTRIFUGE
nn322	234*	AA(53,7) = 1900.
nn323	235*	AA(53,8) = .73
nn324	236*	AA(53,11) = .26
nn325	237*	AA(53,12) = .34
nn326	238*	AA(53,13) = .4
nn327	239*	AA(53,15) = .1
nn327	240*	C VERTICAL BASKET CENTRIFUGE
nn330	241*	AA(54,7) = 620.
nn331	242*	AA(54,8) = 1.
nn332	243*	AA(54,11) = .26
nn333	244*	AA(54,12) = .194
nn334	245*	AA(54,13) = .4
nn335	246*	AA(54,15) = .1
nn335	247*	C FLOWING SOLIDS BLENDER SIZE UNIT = FT**3/HR UNIT NORMALIZED TO GIVE
nn335	248*	C A COST OF 15000 FOR 750 FT**3/HR POWERED BY 25 HP MOTOR
nn336	249*	AA(57,7) = 0.47
nn337	250*	AA(57,8) = 0.52
nn340	251*	AA(57,11) = 0.48
nn341	252*	AA(57,12) = 0.13
nn342	253*	AA(57,13) = 0.42
nn343	254*	AA(57,15) = 0.10
nn343	255*	C CENTRIFUGAL AND REC'D. PUMPS ARE COST FITED BY A QUADRATIC EQ. IN TERMS
nn343	256*	C OF LOG(SIZE). (REF. GUTHRIE) SIZE UNIT = GPM*PSI. THE EQ IS:
nn343	257*	C LOG(COST) = LOG(UNIT COST) + EXP*LOG(SIZE) + BEXP*LOG(SIZE)**2
nn343	258*	C UNIT COST = AA(IX,7) FXP = AA(IX,8) BEXP=AA(IX,9)

Table I.-- Continued.

nn343	259*	C	
nn343	260*	C	CENTRIFUGAL PUMPS. MATERIAL FACTOR IA(66,1)=0/1/2 =FE/BRONZE/SST
nn343	261*	C	AA(66,18)=BRONZF FACTOR, AA(66,19)= SST FACTOR
nn344	262*		AA(66,7) = 0.5
nn345	263*		AA(66,8) = 0.174
nn346	264*		AA(66,9) = 0.049
nn347	265*		AA(66,11) = 0.71
nn350	266*		AA(66,12) = 0.35
nn351	267*		AA(66,13) = 0.44
nn352	268*		AA(66,15) = 0.10
nn353	269*		AA(66,18) = 1.28
nn354	270*		AA(66,19) = 1.93
nn354	271*	C	RECIPROCATING PUMPS. SAME AS FO CENTRIFUGAL (REF GUTHRIE)
nn355	272*		AA(65,7) = 3.2
nn356	273*		AA(65,8) = 0.281
nn357	274*		AA(65,9) = 0.0335
nn360	275*		AA(65,11) = 0.71
nn361	276*		AA(65,12) = 0.70
nn362	277*		AA(65,13) = 0.89
nn363	278*		AA(65,15) = 0.10
nn364	279*		AA(65,18) = 1.25
nn365	280*		AA(65,19) = 2.10
nn365	281*	C	COST AND SIZE VALUES FOR SHELL-TUBE HEAT EXCHANGERS. REF GUTHRIE
nn365	282*	C	SIZE UNITS ARE SQ. FT OF SURFACE AREA
nn366	283*		AA(67,7) = 0.113
nn367	284*		AA(67,8) = 0.622
nn370	285*		AA(67,11) = 0.714
nn371	286*		AA(67,12) = 0.63
nn372	287*		AA(67,13) = 0.947
nn373	288*		AA(67,15) = 0.17
nn373	289*	C	MATERIAL FACTORS FOR HEAT EXCHANGERS. SHELL/TUBE. INDEX 1A = ST/SST
nn373	290*	C	INDEX 19 = SST/SST REF GUTHRIE
nn374	291*		AA(67,18) = 2.25
nn375	292*		AA(67,19) = 3.26
nn375	293*	C	BELT CONVEYER
nn376	294*		AA(70, 7)= 540.
nn377	295*		AA(70, 8)= .65
nn400	296*		AA(70,11)= .27
nn401	297*		AA(70,12)= .39
nn402	298*		AA(70,13)= .4
nn403	299*		AA(70,15)= .1
nn403	300*	C	BUCKET CONVEYER
nn404	301*		AA(71, 7)= 220.
nn405	302*		AA(71, 8)= .65
nn406	303*		AA(71,11)= .278
nn407	304*		AA(71,12)= .562
nn410	305*		AA(71,13)= .4
nn411	306*		AA(71,15)= .1
nn411	307*	C	SCALE
nn412	308*		AA(72,20)= 4.0
nn413	309*		AA(72,18)= 7.2
nn414	310*		AA(72,19)= 8.55
nn415	311*		AA(72,11)= 0.08
nn416	312*		AA(72,13)= 0.4
nn417	313*		AA(72,15)= 0.1
nn417	314*	C	AGITATOR
nn420	315*		AA(73, 7)= 350.

Table I.--Continued.

nn421	316*	AA(73, 8)= .5
nn422	317*	AA(73,11)= .276
nn423	318*	AA(73,12)= .344
nn424	319*	AA(73,13)= .4
nn425	320*	AA(73,15)= .1
nn425	321*	C BALL MILL COST DATA. MATERIAL FACTOR INDEX=18. SIF TONS/HR REF GUTHRIE
nn426	322*	AA(74,7) = 0.55
nn427	323*	AA(74,8) = 0.65
nn430	324*	AA(74,11) = 0.54
nn431	325*	AA(74,12) = 0.195
nn432	326*	AA(74,13) = 0.42
nn433	327*	AA(74,15) = 0.10
nn434	328*	AA(74,18) = 2.4
nn434	329*	C BAGGING MACHINE
nn435	330*	AA(75,7)=3300.
nn436	331*	AA(75,8)=0.8
nn437	332*	AA(75,11)=.40
nn440	333*	AA(75,12)=0.11
nn441	334*	AA(75,13)= .4
nn442	335*	AA(75,15)=.1
nn443	336*	AA(75,1)=1000.
nn443	337*	C ROTARY DRUM FILTERS. SIZE UNITS SQ.FT. SURFACE REF GUTHRIE
nn444	338*	AA(78,7) = 1.40
nn445	339*	AA(78,8) = 0.63
nn446	340*	AA(78,11) = 0.47
nn447	341*	AA(78,12) = 0.13
nn450	342*	AA(78,13) = 0.42
nn451	343*	AA(78,15) = 0.10
nn452	344*	AA(78,18) = 2.4
nn452	345*	C OVERHEAD CRANES. IA(80,1)= INDEX FOR SPAN 0=20FT;1=30FT;2=40FT. SPAN
nn452	346*	C UNIT SIZE FACTORS ARE AA(80,18)=30FT ; AA(80,19)=40FT .SIZE UNIT=TONS
nn453	347*	AA(80,7) =1.2
nn454	348*	AA(80,8) =0.60
nn455	349*	AA(80,11) = 0.46
nn456	350*	AA(80,12) = 0.12
nn457	351*	AA(80,13) = 0.42
nn460	352*	AA(80,15) = 0.10
nn461	353*	AA(80,18) = 1.6
nn462	354*	AA(80,19) = 2.0
nn462	355*	C DRAG CONVEYER
nn463	356*	AA(81,7)=9.
nn464	357*	AA(81,8)=.8
nn465	358*	AA(81,13) =.4
nn466	359*	AA(81,15)= .1
nn466	360*	C MECHANICAL REFRIGRATION. SIZE UNITS= TONS.
nn466	361*	C COOLING TEMP. INDEX = IA(85,1) WHICH SHOULD CONTAIN TEMP. IN DEG F
nn466	362*	C AA(85,18) THEN CONTAINS FACTOR FOR 20 AA(85,19) FOR 0 DEG
nn467	363*	AA(85,7) =2.9
nn470	364*	AA(85,8) = 0.70
nn471	365*	AA(85,11) =0.17
nn472	366*	AA(85,12) =0.14
nn473	367*	AA(85,13) =0.11
nn474	368*	AA(85,15) =0.10
nn475	369*	AA(85,18) =1.95
nn476	370*	AA(85,19) =2.25
nn476	371*	C COST OF FACILITIES INDEX= 99 DETAIL INDEX IDENTIFIES SEP. IDOMS
nn476	372*	C 1= FACILITIES,INDIRECTS 2=FACILITIES CERTAINTY RANGE 3=COST OF LAND

Table I.-- Continued.

nn476	373*	C PER ACRE 4=COST OF FENCE/100n Ft 5=LABOR FACTOR FENCE 6 = COST OF PAV
nn476	374*	C MENT/100n FT**2 7=LABOR FACTOR PAVEMENT 8= COST OF DOCK 9=COST OF CO
nn476	375*	C STRUCT LABOR , 1n=WAREHOUSE LIGHTING COST/100nFTsq 11= WAREH. FIRE PRE
nn476	376*	C VENTION COST 12= WAREH. BASE SHELL COST 13= CONST. LABOR FACTOR 14=LI
nn476	377*	C GHTING 15=HEAT AND VENT. 16= PUMBING 17-FIREPREVENTION 18-RASE 19-LABOR
nn477	378*	AA(98,2)=.1n
nn500	379*	AA(98,1)=0.n75
nn501	380*	AA(99,1) = n.34
nn502	381*	AA(99,2) = n.15
nn503	382*	AA(99,3)=10.n
nn504	383*	AA(99,4) = 1.61
nn505	384*	AA(99,5) = n.32
nn506	385*	AA(99,6) = n.364
nn507	386*	AA(99,7) = 1.75
nn510	387*	AA(99,8) = n.65
nn511	388*	AA(99,9) = 2.50
nn512	389*	AA(99,10) =n.90
nn513	390*	AA(99,11) =1.10
nn514	391*	AA(99,12) =3.22
nn515	392*	AA(99,13) =n.34
nn516	393*	AA(99,14) =1.75
nn517	394*	AA(99,15) =1.50
nn520	395*	AA(99,16) =1.70
nn521	396*	AA(99,17) =1.10
nn522	397*	AA(99,18) =8.80
nn523	398*	AA(99,19) =n.34
nn524	399*	AA(99,20)= 15.
nn525	400*	AA(100,1)=3.
nn526	401*	AA(100,2)=32.
nn527	402*	AA(100,3)= 1.125 E-n2
nn530	403*	AA(100,4)= 5.00
nn531	404*	AA(100,7)= 5.0E-n5
nn532	405*	AA(100,8) = 1.3 E-n5
nn533	406*	AA(100,9) = 1.E-n7
nn534	407*	AA(100,11)=.724
nn535	408*	AA(100,12) = .074
nn536	409*	AA(100,13)=n.1
nn537	410*	AA(100,20) = 20.
nn537	411*	C THE BB(I) COMMON BLOCK INCLUDES BUILT IN PRICE SCHEDULES.
nn537	412*	C 9=CITY WATER 10=FUEL nI 13=ANTIOXIDANT 14=SULPHURIC ACID 15=FISH MEA
nn537	413*	C L BAGS 16=CAOH 66=PRICE OF BONE MEAL(CENTS/LB) 67=PRICE OF FISH OIL
nn537	414*	C (CENTS/LB) 68=PRICE OF FISH SOLUBLES(CENTS/LB)
nn540	415*	BB(9)=.25*.n01
nn541	416*	BB(10)=.n6
nn542	417*	BB(13)=4.00
nn543	418*	BB(14)=.017
nn544	419*	BB(15) = 0.25
nn545	420*	BB(16) = 0.n1
nn546	421*	BB(18)=129.22
nn547	422*	BB(66)=3.5
nn550	423*	BB(67)=4.0
nn551	424*	BB(68)=3.5
nn552	425*	BB(19)=45.
nn552	426*	C
nn552	427*	C DATA FOR ISOPRORYL EXTRACTION (FRACTION OF STREAM EXTRACTD IN STAGE)
nn552	428*	C DATB(STAGE,STREAM) STRFAM INDICES 1-OIL 2-PROTEIN 3-ASH 4-WATER
nn552	429*	C 5-ISOPROPYL ALCOHOL

Table I.-- Continued.

00552	430*	C	
00553	431*		DATB(1,1)= 28./168.
00554	432*		DATB(2,1)= 8./28.
00555	433*		DATB(3,1)= 4./8.
00556	434*		DATB(4,1)= 1./4.
00557	435*		DATB(5,1)= 1./4.
00560	436*		DATB(6,1)= 1./4.
00561	437*		DATB(7,1)= 1./4.
00562	438*		DATB(8,1)= 1./4.
00563	439*		DATB(1,2)= 487./605.
00564	440*		DATB(2,2)= 477./487.
00565	441*		DATB(3,2)= 476./477.
00566	442*		DATB(4,2)= 471./476.
00567	443*		DATB(5,2)= 471./476.
00570	444*		DATB(6,2)= 471./476.
00571	445*		DATB(7,2)= 471./476.
00572	446*		DATB(8,2)= 471./476.
00573	447*		DATB(1,3)= 100./104.
00574	448*		DATB(2,3)= 98./100.
00575	449*		DATB(3,3)= 97./98.
00576	450*		DATB(4,3)= 96./97.
00577	451*		DATB(5,3)= 96./97.
00600	452*		DATB(6,3)= 96./97.
00601	453*		DATB(7,3)= 96./97.
00602	454*		DATB(8,3)= 96./97.
00603	455*		DATB(1,4)= (963.+(.123*125.))/ 3276.
00604	456*		DATB(2,4)= (543.+(.123*161.))/(963.+(.123*125.))
00605	457*		DATB(3,4)= (324.+(.123*301.))/(543.+(.123*161.))
00606	458*		DATB(4,4)= (38.+(.123*553.))/(324.+(.123*301.))
00607	459*		DATB(5,4)= DATB(4,4)
00610	460*		DATB(6,4)= DATB(5,4)
00611	461*		DATB(7,4)= DATB(6,4)
00612	462*		DATB(8,4)= DATB(7,4)
00613	463*		DATB(1,5)= 125.*.877 / 3276.
00614	464*		DATB(2,5)= 161./125.
00615	465*		DATB(3,5)= 301./161.
00616	466*		DATB(4,5)= 553./301.
00617	467*		DATB(5,5)= DATB(4,5)
00620	468*		DATB(6,5)= DATB(5,5)
00621	469*		DATB(7,5)= DATB(6,5)
00622	470*		DATB(8,5)= DATB(7,5)
00623	471*		RETURN
00624	472*		END

END OF COMPILATION:

NO DIAGNOSTICS.

Table I.-- Continued.

MAP  
MAP 22B -07/12-11:06

ADDRESS LIMITS 001000 043715 044000 071006  
STARTING ADDRESS 043307  
WORDS DECIMAL 17870 IBANK 10759 DBANK

	SEGMENT	MAIN	001000	043715	044000	071006
NSWTC\$/FOR	1	001000	001021			
NWBLK\$/FOR	1	001022	001164	0	044000	044006
NFTCH\$/FOR	1	001165	001524	2	044007	044061
EXP\$/FOR	1	001525	001614	2	044062	044102
NTOC\$/FOR	1	001615	003174	2	044103	046602
NOS\$/FOR	1	003175	004263	2	046603	046673
NTAB\$/FOR				2	046674	046732
NERR\$/UOM				0	046733	047000
ERU\$						
NTB\$/FOR	1	004264	004556	2	047001	047022
UOMSYS (COMMON BLOCK)					047023	047037
H\$MONITOR/RALPH	1	004557	006006	2	047040	047677
				4	UOMSYS	
NTS\$/FOR	1	006007	007132	2	047700	047751
AIOG\$/FOR	1	007133	007251	2	047752	050012
NFXP\$/FOR	1	007252	007325	2	050013	050022
SORT\$/FOR	1	007326	007366	2	050023	050034
NTOS\$/FOR	1	007367	011022	2	050035	050417
NOSYM\$/FOR	1	011023	011261	2	050420	050431
NFRR\$/UOM	1	011262	011742	2	050432	050604
BLOCK4 (COMMON BLOCK)					050605	050616
BLOCK2 (COMMON BLOCK)					050617	050634
BLOCK1 (COMMON BLOCK)					050635	055704
DATA1 (COMMON BLOCK)					055705	055754
BLANK\$COMMON (COMMON BLOCK)						
LTBRE	1	011743	013050	0	055755	056223
	3	DATA1		2	BLANK\$COMMON	
				4	BLOCK1	
OPERAT	1	013051	014323	0	056224	057202
	3	BLOCK1		2	BLANK\$COMMON	
FASCIL	1	014324	015061	0	057203	057567
	3	BLOCK1		2	BLANK\$COMMON	
CAPTOL	1	015062	015174	0	057570	057662
	3	BLOCK1		2	BLANK\$COMMON	
				4	BLOCK2	
MATER	1	015175	015315	0	057663	060033
	3	BLOCK1		2	BLANK\$COMMON	
RFRRIG	1	015316	015442	0	060034	060064

Table I.--Continued.

	3	BLOCK1	2	BLANK&COMMON
DRAGMA	1	015443 015613	4	BLOCK2
	3	BLOCK1	0	060065 060135
			2	BLANK&COMMON
CRANES	1	015614 015761	4	BLOCK2
	3	BLOCK1	0	060136 060220
			2	BLANK&COMMON
FILTER	1	015762 016060	4	BLOCK2
	3	BLOCK1	0	060221 060251
			2	BLANK&COMMON
BAGGMA	1	016061 016212	4	BLOCK2
	3	BLOCK1	0	060252 060322
			2	BLANK&COMMON
BALMIL	1	016213 016311	4	BLOCK2
	3	BLOCK1	0	060323 060353
			2	BLANK&COMMON
AGITOR	1	016312 016411	4	BLOCK2
	3	BLOCK1	0	060354 060406
			2	BLANK&COMMON
SCALE	1	016412 016534	4	BLOCK2
	3	BLOCK1	0	060407 060444
			2	BLANK&COMMON
BUCKET	1	016535 016675	4	BLOCK2
	3	BLOCK1	0	060445 060505
			2	BLANK&COMMON
BFLT	1	016676 017025	4	BLOCK2
	3	BLOCK1	0	060506 060546
			2	BLANK&COMMON
HFATEX	1	017026 017216	4	BLOCK2
	3	BLOCK2	0	060547 060647
			2	BLANK&COMMON
PMPONT	1	017217 017435	4	BLOCK1
	3	BLOCK1	0	060650 060756
			2	BLANK&COMMON
PMPREC	1	017436 017654	4	BLOCK2
	3	BLOCK1	0	060757 061065
			2	BLANK&COMMON
BI ENDR	1	017655 017751	4	BLOCK2
	3	BLOCK1	0	061066 061116
			2	BLANK&COMMON
CNTFGE	1	017752 020045	4	BLOCK2
	3	BLOCK1	0	061117 061151
			2	BLANK&COMMON
BOWI	1	020046 020145	4	BLOCK2
	3	BLOCK1	0	061152 061204
			2	BLANK&COMMON
SHARP	1	020146 020245	4	BLOCK2
	3	BLOCK1	0	061205 061237
			2	BLANK&COMMON
SCRFEN	1	020246 020344	4	BLOCK2
	3	BLOCK1	0	061240 061270
			2	BLANK&COMMON
GRINDR	1	020345 020443	4	BLOCK2
	3	BLOCK1	0	061271 061321
			2	BLANK&COMMON
RFACTR	1	020444 020542	4	BLOCK2
			0	061322 061352

Table I.-- Continued.

	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
COLUMN	1	020543 020725	0	061353 061416
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
VFSSEL	1	020726 021142	0	061417 061503
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
STORAG	1	021143 021346	0	061504 061607
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
EVPHOR	1	021347 021445	0	061610 061640
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
EVPRFC	1	021446 021544	0	061641 061671
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
EVPLFM	1	021545 021637	0	061672 061721
	3	BLOCK2	2	BLANK&COMMON
			4	BLOCK1
EVPSPR	1	021640 021734	0	061722 061752
	3	BLOCK2	2	BLANK&COMMON
			4	BLOCK1
BOILER	1	021735 022054	0	061753 062012
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
DRYFRF	1	022055 022361	0	062013 062165
	3	BLOCK2	2	BLANK&COMMON
			4	BLOCK1
DRYFRP	1	022362 022461	0	062166 062220
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
DRYFR	1	022462 022561	0	062221 062253
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
HAMMER	1	022562 022675	0	062254 062307
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
SCRFWR	1	022676 023154	0	062310 062435
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
PULVER	1	023155 023254	0	062436 062470
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
CONDEN	1	023255 023345	0	062471 062521
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
STLO	1	023346 023467	0	062522 062571
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
HOPPER	1	023470 023567	0	062572 062622
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
PRESCK	1	023570 026234	0	062623 063630
	3	BLOCK1	2	BLANK&COMMON
			4	BLOCK2
XXIPA	1	026235 032602	0	063631 065313

Table I.-- Continued.

	3	BLOCK1		2	BLANK&COMMON
	5	BLOCK4		4	BLOCK2
BIOLOG	1	032603 035152		0	065314 066246
	3	BLOCK1		2	BLANK&COMMON
				4	BLOCK2
PRSTPA	1	035153 040771		0	066247 067656
	3	BLOCK2		2	BLANK&COMMON
	5	BLOCK1		4	DATA1
				6	BLOCK4
FPCXX1	1	040772 043306		0	067657 070456
	3	BLOCK4		2	BLANK&COMMON
	5	BLOCK2		4	BLOCK1
MAIN	1	043307 043715		0	070457 071006
	3	BLOCK1		2	BLANK&COMMON
	5	BLOCK4		4	BLOCK2

SYS&RLIB\$. LEVEL 53.29  
 END OF COLLECTION - TIME 4.470 SECONDS

QFIN

RUNID: 7053      ACCOUNT: 154-04-105      PROJECT: FISHFISH

LOAD P0111N 3/0 A                      -1 7053

SERVICE      3/0 P0111N : 7053

TIME: 00:01:02.380      IN: 54      OUT: 0      PAGES: 137

MEMORY TIME: 0:02:50.430

INITIATION TIME: 11:01:32-JUN 12,1971

TERMINATION TIME: 11:07:11-JUN 12,1971

Table II.- IPA plant cost analysis.

IPA PLANT COST ANALYSIS

INPUT DATA

PLANT SIZE = 200.00 TONS/DAY  
 MARSHAL/STEVENS INDEX = 1.135  
 COST OF FISH = 1.00 CENTS/LB  
 ELECTRICITY COSTS = 1.30 CENTS/KWH  
 FUEL COST = .06 DOLLARS/THERM  
 LABOR AND SUPV. COSTS = 4.00 DOLLARS/HR  
 DEPRECIATION AND INT. CHARGE = 15.00 PERCENT

FISH COMPOSITION

OIL = 4.00 PERCENT  
 PROTEIN = 16.00 ''-''  
 ASH = 3.00 ''-''  
 WATER = 77.00 ''-''

OPERATING OPTIONS

OPERATING DAYS PER YEAR = 200.

Table II.-- Continued.

## DETAILED EQUIPMENT COSTS (ALL COSTS IN 1000.0 DOLLARS)

EQUIPMENT TYPE	CAPACITY	MATERIAL	BASE COST	MATERIALS COSTS	LABOR COSTS	INDIRECT COSTS	MODULE COST	RANGE + OR -
FISH PUMPS	1301. GPM TIMES PSI	STEEL	3.919	2.783	2.743	3.488	12.934	1.293
BELT CONVEYER	100.000 FEET(LENGTH)		18.796	5.075	7.350	7.518	38.719	3.872
WATER DUMP TANK	6000. GALLONS	STEEL	2.379	.904	.238	1.165	4.686	.469
MECHANICAL REFRIGERAT.	300.000 TONS		347.856	59.136	48.700	38.264	493.956	49.396
REDWOOD STORAGE BIN	32500. CUBIC FEET	REDWOOD	11.747	2.349	1.175	4.699	19.970	1.175
BRINE MAKE-UP+SALT STOR.			1.190				1.190	
CENTRIFUGAL PUMP	71. GPM TIMES PSI	BRONZE	.512	.364	.140	.225	1.241	.124
CENTRIFUGAL PUMP	65.487 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
BUCKET CONVEYER	20.000 FEET(HEIGHT)	SS	1.750	.487	.984	.700	3.920	.392
PULVERIZER	16666.667 POUNDS/HOUR	SS	17.727	4.822	5.637	7.091	35.277	3.528
SHOP FAB. STORAGE TANK	3500. GALLONS	SST	6.303	2.395	6.303	3.088	18.089	1.809
CENTRIFUGAL PUMP	1000.400 GPM TIMES PSI	SST	1.095	.778	.199	.482	2.554	.255
CENTRIFUGAL PUMP	3123.715 GPM TIMES PSI	SST	1.423	1.010	.258	.626	3.317	.332
AGITATOR=PROPELLAR	17.500 HORSEPOWER	SS	1.662	.459	.572	.665	3.357	.336
SHOP FAB. STORAGE TANK	3200. GALLONS	SST	6.108	2.321	6.108	2.093	17.530	1.753
CENTRIFUGAL PUMP	1698.652 GPM TIMES PSI	SST	1.218	.865	.221	.536	2.839	.284
CENTRIFUGAL PUMP	1698.652 GPM TIMES PSI	SST	1.218	.865	.221	.536	2.839	.284
JACKETED REACTOR VESSEL	6000. GALLONS	SST	18.310	6.958	1.831	8.972	36.071	3.607
VIBRATING SCREEN	3.000 SURFACE SQ FT.	SST	3.606	.974	.180	1.515	6.274	.627
AGITATOR=PROPELLAR	30.000 HORSEPOWER	SS	2.176	.601	.748	.870	4.395	.440
CENTRIFUGAL PUMP	733.627 GPM TIMES PSI	SST	1.043	.740	.189	.459	2.431	.243
PULP PRESS	6.000 FEET	STEEL	5.288	1.438	1.682	2.115	10.523	.529
CENTRIFUGAL PUMP	733.627 GPM TIMES PSI	SST	1.043	.740	.189	.459	2.431	.243
JACKETED REACTOR VESSEL	3200. GALLONS	SST	14.694	5.584	1.469	7.200	28.948	2.895
VIBRATING SCREEN	3.000 SURFACE SQ FT.	SST	3.606	.974	.180	1.515	6.274	.627

Table II.-- Continued.

AGITATOR-PROPELLAR	30.000 HORSEPOWER	SS	2.176	.601	.748	.870	4.395	.440
PULP PRESS	6.000 FEET	STEEL	5.288	1.438	1.682	2.115	10.523	.529
CENTRIFUGAL PUMP	733.627 GPM TIMES PSI	SST	1.043	.740	.189	.459	2.431	.243
JACKETED REACTOR VESSEL	3200. GALLONS	SST	14.694	5.584	1.469	7.200	28.948	2.895
VIBRATING SCREEN	3.000 SURFACE SQ FT.	SST	3.606	.974	.180	1.515	6.274	.627
AGITATOR-PROPELLAR	30.000 HORSEPOWER	SS	2.176	.601	.748	.870	4.395	.440
PULP PRESS	6.000 FEET	STEEL	5.288	1.438	1.682	2.115	10.523	.529
CENTRIFUGAL PUMP	733.627 GPM TIMES PSI	SST	1.043	.740	.189	.459	2.431	.243
JACKETED REACTOR VESSEL	3200. GALLONS	SST	14.694	5.584	1.469	7.200	28.948	2.895
VIBRATING SCREEN	3.000 SURFACE SQ FT.	SST	3.606	.974	.180	1.515	6.274	.627
AGITATOR-PROPELLAR	30.000 HORSEPOWER	SS	2.176	.601	.748	.870	4.395	.440
PULP PRESS	6.000 FEET	STEEL	5.288	1.438	1.682	2.115	10.523	.529
CENTRIFUGAL PUMP	412.565 GPM TIMES PSI	SST	.976	.693	.177	.429	2.275	.227
CENTRIFUGAL PUMP	315.100 GPM TIMES PSI	SST	.956	.679	.173	.421	2.230	.223
CENTRIFUGAL PUMP	297.519 GPM TIMES PSI	SST	.953	.677	.173	.419	2.222	.222
CENTRIFUGAL PUMP	2025.850 GPM TIMES PSI	SST	1.269	.901	.230	.558	2.959	.296
CENTRIFUGAL PUMP	290.051 GPM TIMES PSI	SST	.952	.676	.173	.419	2.219	.222
CENTRIFUGAL PUMP	2008.268 GPM TIMES PSI	SST	1.266	.899	.230	.557	2.952	.295
CENTRIFUGAL PUMP	2000.800 GPM TIMES PSI	SST	1.265	.898	.229	.557	2.950	.295
HEAT EXCHANGER	100.000 SURFACE SQ FT.	ST/ST	2.249	1.606	1.417	2.130	7.403	1.258
DRYER	73.450 AREA(SQ.FEET)	SST	50.846	4.926	3.531	2.825	28.936	2.894
STRIPPER DRYER	73.450 AREA(SQ.FEET)	SST	62.772	5.473	3.923	3.139	32.151	3.215
SCREW CONVEYER	6.000 FEET	SS	.998	.271	.317	.399	1.985	.100
STRIPPER DRYER	73.450 AREA(SQ.FEET)	SST	62.772	5.473	3.923	3.139	32.151	3.215
CONDITIONER	73.450 AREA(SQ.FEET)	SST	62.772	5.473	3.923	3.139	32.151	3.215
SCREW CONVEYER	6.000 FEET	SS	.998	.271	.317	.399	1.985	.100
SCREW CONVEYER	20.000 FEET	SS	2.055	.559	.653	.822	4.089	.205
HAMMER MILL	3.727 TONS PER HR.	SST	1.736	.469	.748	.764	3.717	.372
BAGGING MACHINE	1.725 BAGS/MIN	SS	5.795	2.318	.637	2.318	11.068	1.107

Table II.--Continued.

ACID STORAGE TANK	38. GALLONS	SST	2.367	.473	.200	1.160	4.199	.420
CENTRIFUGAL PUMP	1.506 GPM TIMES PSI	SST	.772	.548	.140	.340	1.800	.180
CENTRIFUGAL PUMP	2711.150 GPM TIMES PSI	STEEL	.709	.503	.248	.312	1.772	.177
SHOP FAB. STORAGE TANK	1301. GALLONS	STEEL	1.393	.529	4.458	.683	7.063	.706
CENTRIFUGAL PUMP	2711.150 GPM TIMES PSI	STEEL	.709	.503	.248	.312	1.772	.177
DISK TYPE CENTRIFUGE	20.000 HORSEPOWER	SS	14.074	3.659	2.730	5.629	26.092	2.609
DISK TYPE CENTRIFUGE	20.000 HORSEPOWER	SS	14.074	3.659	2.730	5.629	26.092	2.609
DISK TYPE CENTRIFUGE	20.000 HORSEPOWER	SS	14.074	3.659	2.730	5.629	26.092	2.609
CENTRIFUGAL PUMP	43.746 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
SHARPLES CENTRIFUGE	20.000 HORSEPOWER	SS	45.257	11.767	15.387	18.103	90.514	9.051
SHOP FAB. STORAGE TANK	30777. GALLONS	SST	13.489	5.126	13.489	6.610	38.714	3.871
CENTRIFUGAL PUMP	.427 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
SHOP FAB. STORAGE TANK	5383. GALLONS	SST	7.327	2.784	7.327	3.590	21.030	2.103
CENTRIFUGAL PUMP	26.913 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
CENTRIFUGAL PUMP	26.913 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
HEAT EXCHANGER	448.365 SURFACE SQ FT. ST/ST		5.720	4.084	3.603	5.417	18.824	3.200
CENTRIFUGAL PUMP	780.882 GPM TIMES PSI	STEEL	.545	.387	.191	.240	1.363	.136
DISK TYPE CENTRIFUGE	20.000 HORSEPOWER	SS	14.074	3.659	2.730	5.629	26.092	2.609
HEAT EXCHANGER	4283.600 SURFACE SQ FT. ST/ST		23.283	16.624	14.669	22.049	76.626	13.026
SHOP FAB. STORAGE TANK	4002. GALLONS	SST	6.605	2.510	6.605	3.237	18.957	1.896
CENTRIFUGAL PUMP	1980.792 GPM TIMES PSI	STEEL	.654	.464	.229	.288	1.635	.163
DIST. COLUMN SHELL	1526.813 CUBIC FEET	SS	65.250	18.455	17.637	21.335	122.677	6.525
DISTILLATION COLUMN	54.000 FEET(HIGHT)	SS	10.605	2.273	3.030	3.030	18.938	1.061
SHOP FAB. STORAGE TANK	14406. GALLONS	STEEL	3.232	1.228	10.342	1.584	16.385	1.639
CENTRIFUGAL PUMP	.200 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
HEAT EXCHANGER	13374.648 SURFACE SQ FT. ST/ST		47.272	33.753	29.782	44.767	155.574	26.448
CENTRIFUGAL PUMP	200.000 GPM TIMES PSI	STEEL	.487	.346	.170	.214	1.217	.122
SHOP FAB. STORAGE TANK	1577. GALLONS	SST	4.768	1.812	4.768	2.336	13.684	1.368
CENTRIFUGAL PUMP	7.884 GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100

Table II.--Continued.

VERTICAL EVAPORATOR	662.220	SURFACE SQ FT.	SST	10.221	6.746	2.453	4.293	23.713	2.371
VERTICAL EVAPORATOR	662.220	SURFACE SQ FT.	SST	10.221	6.746	2.453	4.293	23.713	2.371
VERTICAL EVAPORATOR	662.220	SURFACE SQ FT.	SST	10.221	6.746	2.453	4.293	23.713	2.371
VERTICAL EVAPORATOR	79.588	SURFACE SQ FT.	SST	3.325	2.195	.798	1.397	7.715	.771
CENTRIFUGAL PUMP	59.691	GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
SHOP FAB. STORAGE TANK	29.	GALLONS	STEEL	.678	.136	.183	.332	1.329	.133
CENTRIFUGAL PUMP	.597	GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
SHOP FAB. STORAGE TANK	42977.	GALLONS	STEEL	4.738	1.800	15.161	2.322	24.021	2.402
BOILER	62097.921	POUNDS/HOUR	SS	124.585	23.671	18.688	24.917	191.861	19.186
SHOP FAB. STORAGE TANK	19169.	GALLONS	STEEL	3.572	1.357	11.429	1.750	18.108	1.811
CENTRIFUGAL PUMP	.266	GPM TIMES PSI	STEEL	.400	.284	.140	.176	1.000	.100
CONTROL INSTRUMENTATION				87.000				1.000	
PAYLOADER				20.000				20.000	
SCRUBBERS	200.000	TONS PROCESSED	STEEL	4.540	1.498	1.498	1.498	9.034	.454
BOILER WATER TREATMENT				1.000				1.000	
SEA WATER PUMPS	8179.034	GPM TIMES PSI	BRONZE	1.300	.923	.355	.572	3.151	.315
CARBON ADSORBER				2.000				2.000	
VENT CONDENSER	20.000	SURFACE SQ FT.	ST/SST	1.860	1.328	.521	1.761	5.470	.930
SCALE	18.000	TONS	SS	4.540	.363	.000	1.816	6.719	.454
SCALE	18.000	TONS	SS	4.540	.363	.000	1.816	6.719	.454
SCALE	18.000	TONS	SS	4.540	.363	.000	1.816	6.719	.454
SCALE	18.000	TONS	SS	4.540	.363	.000	1.816	6.719	.454
TOTAL COSTS				1400.533	331.836	319.878	359.491	2163.078	221.047

MATERIAL AND ENERGY INFORMATION

GENERAL

FISH = 200,000 TONS/DAY  
 OF WHICH 4.00 PERCENT OR 8.000 - '' - IS OIL  
 16.00 - '' - OR 32.000 - '' - PROTEIN  
 3.00 - '' - OR 6.000 - '' - ASH

PROCESS STEAM = 62098. LB/HR

PROCESS COOLING WATER = 408952. GAL/HR

ELECTRICITY 12214. KWHR

EQUIPMENT FLOW RATES

FISH TO EXTRACTION VESSELS 16667. LB/HR  
 STEAM(STIRRED VESSEL 1 ) 140. LB/HR  
 STEAM(STIRRED VESSEL 2 ) 80. LB/HR  
 STEAM(STIRRED VESSEL 3 ) 80. LB/HR  
 STEAM(STIRRED VESSEL 4 ) 80. LB/HR  
 STEAM(PREHEATER-DISTILLATION) 4484. LB/HR  
 STEAM(REBOILER) 42836. LB/HR  
 STEAM(ROTARY DRYER FPC ) 2348. LB/HR  
 STEAM(ROTARY DRYER BONE MEAL) 0. LB/HR  
 COOLING WATER CONDENSER 248592. GAL/HR  
 COOLING WATER DISTILLATION COND. 2676. GAL/MIN  
 TOTAL STEAM 62098. LB/HR  
 TOTAL WATER 3406568. LB/HR

	STREAM 1	STREAM 2	STREAM 3	STREAM 4	STREAM 5
RAFFINATE OIL	7.951	1.311	.345	.148	.000
RAFFINATE ASH	1.532	.192	.095	.047	.000
RAFFINATE PROTEIN	7.163	.763	.251	.251	.000

Table II.-- Continued.

RAFFINATE	WATER	152.199	42.859	23.209	13.205	.000
RAFFINATE	ALCOHOL	373.368	379.368	381.108	387.842	400.000
EXTRACT	OIL	8.000	1.360	.394	.197	.049
EXTRACT	ASH	6.000	4.860	4.763	4.715	4.668
EXTRACT	PROTEIN	32.000	25.600	25.088	25.088	24.837
EXTRACT	WATER	154.000	44.660	25.010	15.006	1.801
EXTRACT	ALCOHOL	.000	6.000	7.740	14.474	26.632
FLOW FROM EXTRACTION VESSEL 4		4832.	LB/HR			
FLOW FROM EXTRACTION VESSEL 1		45168.	LB/HR			
AQUEOUS STREAM(CENTRIFUGE)		44882.	LB/HR			
TOPS FROM DISTILLATION COLUMN		31088.	LB/HR			
BOTTOMS FROM DISTILLATION COLUMN		13009.	LB/HR			
OIL FROM SECOND CENTRIFUGE		331.	LB/HR			
FISH OIL PRODUCT		663.	LB/HR			
BONE MEAL CONCENTRATE		0.	LB/HR			
FISH PROTEIN CONCENTRATE		2588.	LB/HR			
FISH SOLUABLES		218.	LB/HR			

Table II.--Continued.

## COST OF FACILITIES AND SITE DEVELOPMENT

	UNIT COST	NUMBER OF UNITS	BASE COST	LABOR COSTS	INDIRECT COSTS	TOTAL COSTS	RANGE + OR -
LAND	10.000 PER ACRE	1.000	10.000	.000	.000	10.000	1.500
FENCING	2.673 PER 1000 FT	.833	1.342	.429	.456	2.227	.334
PAVING	1.125 PER 1000 SQ.FT	14.505	5.280	9.240	1.795	16.315	2.447
DOCK FACILITIES	2.496 PER 1000 SQ.FT	2.400	1.560	3.900	.530	5.990	.899
BULK STORAGE WAREHOUSE							
ELECTRICAL WIRING	.900 PER 1000SQ.FT						
FIRE PREVENTION EQP.	1.100 PER 1000SQ.FT						
TOTAL WAREHOUSE	8.770 PER 1000 SQ.FT	.600	3.132	1.065	1.065	5.262	.789
PROCESS BUILDING							
ELECTRICAL WIRING	1.750 PER 1000 SQ.FT						
HEATING AND VENTIL.	1.500 PER 1000 SQ.FT						
PLUMBING (GENERAL)	1.700 PER 1000 SQ.FT						
FIRE PREVENTION EQUIP	1.100 PER 1000 SQ.FT						
TOTAL BUILDING COSTS	14.784 PER 1000 SQ.FT	2.600	22.880	7.779	7.779	38.438	5.766
LABORATORY CONTROL INSTRUMENTATION			150.000			150.000	
TOTAL FACILITIES			67.074	30.193	19.405	228.233	17.501

Table II.--Continued.

SUMMARY OF FIXED COSTS

EQUIPMENT	2163.078
SPARE PARTS	28.011
FACILITIES	228.233
ENGINEERING	181.449
CONTINGENCIES	260.077
TOTAL CAPITAL COSTS	2860.848

Table II.-- Continued.

OPERATING COSTS		
COST ITEM	QUANTITY USED	COST IN DOLLARS PER DAY
FISH	200. TONS	4000.00
FUEL OIL	10645. GALLONS	638.72
ELECTRICITY	12214. KWHR	158.78
ANTIOXIDANT	45.38 LB	181.54
PACKAGING	2485. BAGS	621.16
CITY WATER	9814840. GALLONS	2453.71
LABOR AND SUPERVISION	176. MAN HR.	704.00
DEPRECIATION		1430.42
MAINTENANCE		95.36
PAYROLL EXTRAS		105.60
BOILER WATER TREATMENT		3.30
INSURANCE AND TAXES		95.36
OVERHEAD		211.20
ISOPROPYL ALCOHOL	8000. POUNDS	516.88
PHOSPHORIC ACID	1084. POUNDS	24.39
TOTAL OPERATING COSTS		11240.43

## PRODUCTION RATE

BONE MEAL	.000 TONS/DAY
FISH SOL.	14.326 TONS/DAY
DRY CONC.	31.058 TONS/DAY
FISH OIL	7.951 TONS/DAY
BONE MEAL	0. TONS/YEAR
FISH SOL.	2865. TONS/YEAR
DRY CONC.	6212. TONS/YEAR
FISH OIL	1590. TONS/YEAR

YEARLY OPERATING COST = .267080+07 DOLLARS

Table II.-- Continued.

BY-PRODUCT	PRODUCTION COST OF FPC PRICE (CENTS/POUND)	TOTAL WORTH (DOLLARS/YEAR)
FISH OIL	4.0	.127211+06
FISH SOLUBLES	3.5	.200561+06
	FPC COST WITHOUT BY-PRODUCTS	21.5 CENTS/POUND
	FPC COST WITH BY-PRODUCTS	18.9 CENTS/POUND

Table III

## Cost Data for 50 ton/day Capacity Plants

Plant Type	Fish Type	Capital Costs \$·10 <sup>6</sup>	Yearly Production Rates and Costs					FPC Cost Disregarding by product ¢/lb	FPC with product ¢/lb
			Bone Meal tons/yr	Fish Paste tons/yr	Dry Con. tons/yr	Fish Oil tons/yr	Operating costs \$·10 <sup>6</sup>		
Biolog- ical	Fat	1.35	1340	-	1360	900	0.985	36.1	30.
Press Cake- Biolog- ical	Fat	1.41	340	-	1960	950	0.896	22.8	20.3
IPA	Lean	1.58	-	720	1550	400	0.987	31.8	29.1
Press Cake-	Fat	1.57	-	1110	1400	1410	0.879	31.2	25.1
IPA	Lean	1.57	-	1110	1400	400	0.88	31.3	27.4

Table IV

## Cost Data for 200 ton/day Capacity Plants

Plant Type	Fish Type	Capital Costs \$·10 <sup>6</sup>	Yearly Production Rates and Costs					FPC Cost Disregarding by product ¢/lb	FPC with by product ¢/lb
			Bone Meal tons/yr	Fish Paste tons/yr	Dry Con. tons/yr	Fish Oil tons/yr	Operating costs \$·10 <sup>6</sup>		
Biological	Fat	2.40	5350	-	5450	3600	2.76	25.3	19.2
Press Cake Biological	Fat	2.65	1380	-	7860	3800	2.40	15.3	12.7
IPA	Lean	2.73	-	2860	6210	1590	2.64	21.2	18.6
Press Cake	Fat	2.82	-	4430	5620	4790	2.22	19.8	13.6
IPA	Lean	2.82	-	4430	5620	1600	2.23	19.8	16.0

Table V

## Cost Data for 1000 ton/day Capacity Plants

Plant Type	Fish Type	Capital Costs \$·10 <sup>6</sup>	Yearly Production Rates and Costs					FPC Cost Disregarding by product ¢/lb	FPC with by product ¢/lb
			Bone Meal tons/yr	Fish Paste tons/yr	Dry Con. tons/yr	Fish Oil tons/yr	Operating costs \$·10 <sup>6</sup>		
Biological	Fat	7.71	26700	-	27300	1800	11.65	21.4	15.3
Press Cake Biological	Fat	8.01	6900	-	39300	1900	9.70	12.3	9.8
IPA	Lean	7.13	-	14300	31000	7900	10.6	17.1	14.4
Press Cake	Fat	7.023	-	22100	28100	24000	8.41	15.0	8.8
IPA	Lean	7.024	-	22100	28100	8000	8.46	15.0	11.1

Table VI  
Cost Data for Fish Meal Plants

Plant Capacity tons/day	Fish Type	Capital Costs \$·10 <sup>6</sup>	Yearly Production and Costs		
			Fish Meal tons/yr	Fish Oil tons/yr	Operating costs \$·10 <sup>6</sup>
50	<i>Fat</i>	.728	2090	1010	0.687
	<i>Lean</i>	.725	1960	340	0.675
200	<i>Fat</i>	1.12	8400	4030	1.72
	<i>Lean</i>	1.11	7860	1340	1.68
1000	<i>Fat</i>	2.84	41800	20000	6.64
	<i>Lean</i>	2.62	39000	6700	6.36